

INTERNATIONAL UNION OF PURE AND APPLIED CHEMISTRY

ANALYTICAL CHEMISTRY DIVISION  
COMMISSION ON SOLUBILITY DATA

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**SOLUBILITY DATA SERIES**

Volume 7

**OXYGEN AND OZONE**

## SOLUBILITY DATA SERIES

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Robert Maxwell  
Publisher at Pergamon Press

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# SOLUBILITY DATA SERIES

Volume 7

## OXYGEN AND OZONE

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**PERGAMON PRESS**

OXFORD · NEW YORK · TORONTO · SYDNEY · PARIS · FRANKFURT

U.K.	Pergamon Press Ltd., Headington Hill Hall, Oxford OX3 0BW, England
U.S.A.	Pergamon Press Inc., Maxwell House, Fairview Park, Elmsford, New York 10523, U.S.A.
CANADA	Pergamon Press Canada Ltd., Suite 104, 150 Consumers Rd., Willowdale, Ontario M2J 1P9, Canada
AUSTRALIA	Pergamon Press (Aust.) Pty. Ltd., P.O. Box 544, Potts Point, N.S.W. 2011, Australia
FRANCE	Pergamon Press SARL, 24 rue des Ecoles, 75240 Paris, Cedex 05, France
FEDERAL REPUBLIC OF GERMANY	Pergamon Press GmbH, 6242 Kronberg-Taunus, Hammerweg 6, Federal Republic of Germany

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First edition 1981

**British Library Cataloguing In Publication Data**

Oxygen and ozone.—(Solubility data series,

ISSN 0191-5622; v. 7)

I. Battino, Rubin

1. Oxygen—Solubility—Tables

2. Ozone—Solubility—Tables

I. Title II. Series

546'.721542 QD181.01

ISBN 0-08-023915-3

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## FOREWORD

*If the knowledge is  
undigested or simply wrong,  
more is not better.*

How to communicate and disseminate numerical data effectively in chemical science and technology has been a problem of serious and growing concern to IUPAC, the International Union of Pure and Applied Chemistry, for the last two decades. The steadily expanding volume of numerical information, the formulation of new interdisciplinary areas in which chemistry is a partner, and the links between these and existing traditional subdisciplines in chemistry, along with an increasing number of users, have been considered as urgent aspects of the information problem in general, and of the numerical data problem in particular.

Among the several numerical data projects initiated and operated by various IUPAC commissions, the *Solubility Data Project* is probably one of the most ambitious ones. It is concerned with preparing a comprehensive critical compilation of data on solubilities in all physical systems, of gases, liquids and solids. Both the basic and applied branches of almost all scientific disciplines require a knowledge of solubilities as a function of solvent, temperature and pressure. Solubility data are basic to the fundamental understanding of processes relevant to agronomy, biology, chemistry, geology and oceanography, medicine and pharmacology, and metallurgy and materials science. Knowledge of solubility is very frequently of great importance to such diverse practical applications as drug dosage and drug solubility in biological fluids, anesthesiology, corrosion by dissolution of metals, properties of glasses, ceramics, concretes and coatings, phase relations in the formation of minerals and alloys, the deposits of minerals and radioactive fission products from ocean waters, the composition of ground waters, and the requirements of oxygen and other gases in life support systems.

The widespread relevance of solubility data to many branches and disciplines of science, medicine, technology and engineering, and the difficulty of recovering solubility data from the literature, lead to the proliferation of published data in an ever increasing number of scientific and technical primary sources. The sheer volume of data has overcome the capacity of the classical secondary and tertiary services to respond effectively.

While the proportion of secondary services of the review article type is generally increasing due to the rapid growth of all forms of primary literature, the review articles become more limited in scope, more specialized. The disturbing phenomenon is that in some disciplines, certainly in chemistry, authors are reluctant to treat even those limited-in-scope reviews exhaustively. There is a trend to preselect the literature, sometimes under the pretext of reducing it to manageable size. The crucial problem with such preselection - as far as numerical data are concerned - is that there is no indication as to whether the material was excluded by design or by a less than thorough literature search. We are equally concerned that most current secondary sources, critical in character as they may be, give scant attention to numerical data.

On the other hand, tertiary sources - handbooks, reference books, and other tabulated and graphical compilations - as they exist today, are comprehensive but, as a rule, uncritical. They usually attempt to cover whole disciplines, thus obviously are superficial in treatment. Since they command a wide market, we believe that their service to advancement of science is at least questionable. Additionally, the change which is taking place in the generation of new and diversified numerical data, and the rate at which this is done, is not reflected in an increased third-level service. The emergence of new tertiary literature sources does not parallel the shift that has occurred in the primary literature.

With the status of current secondary and tertiary services being as briefly stated above, the innovative approach of the *Solubility Data Project* is that its compilation and critical evaluation work involve consolidation and reprocessing services when both activities are based on intellectual and scholarly reworking of information from primary sources. It comprises compact compilation, rationalization and simplification, and the fitting of isolated numerical data into a critically evaluated general framework.

The *Solubility Data Project* has developed a mechanism which involves a number of innovations in exploiting the literature fully, and which contains new elements of a more imaginative approach for transfer of reliable information from primary to secondary/tertiary sources. *The fundamental trend of the Solubility Data Project is toward integration of secondary and tertiary services with the objective of producing in-depth critical analysis and evaluation which are characteristic to secondary services, in a scope as broad as conventional tertiary services.*

Fundamental to the philosophy of the project is the recognition that the basic element of strength is the active participation of career scientists in it. Consolidating primary data, producing a truly critically-evaluated set of numerical data, and synthesizing data in a meaningful relationship are demands considered worthy of the efforts of top scientists. Career scientists, who themselves contribute to science by their involvement in active scientific research, are the backbone of the project. The scholarly work is commissioned to recognized authorities, involving a process of careful selection in the best tradition of IUPAC. This selection in turn is the key to the quality of the output. These top experts are expected to view their specific topics dispassionately, paying equal attention to their own contributions and to those of their peers. They digest literature data into a coherent story by weeding out what is wrong from what is believed to be right. To fulfill this task, the evaluator must cover *all* relevant open literature. No reference is excluded by design and every effort is made to detect every bit of relevant primary source. Poor quality or wrong data are mentioned and explicitly disqualified as such. In fact, it is only when the reliable data are presented alongside the unreliable data that proper justice can be done. The user is bound to have incomparably more confidence in a sufficient evaluative commentary and a comprehensive review with a complete bibliography to both good and poor data.

It is the standard practice that any given solute-solvent system consists of two essential parts: I. Critical Evaluation and Recommended Values, and II. Compiled Data Sheets.

The Critical Evaluation part gives the following information:

- (i) a verbal text of evaluation which discusses the numerical solubility information appearing in the primary sources located in the literature. The evaluation text concerns primarily the quality of data after consideration of the purity of the materials and their characterization, the experimental method employed and the uncertainties in control of physical parameters, the reproducibility of the data, the agreement of the worker's results on accepted test systems with standard values, and finally, the fitting of data, with suitable statistical tests, to mathematical functions;
- (ii) a set of recommended numerical data. Whenever possible, the set of recommended data includes weighted average and standard deviations, and a set of smoothing equations derived from the experimental data endorsed by the evaluator;
- (iii) a graphical plot of recommended data.

The compilation part consists of data sheets of the best experimental data in the primary literature. Generally speaking, such independent data sheets are given only to the best and endorsed data covering the known range of experimental parameters. Data sheets based on primary sources where the data are of a lower precision are given only when no better data are available. Experimental data with a precision poorer than considered acceptable are reproduced in the form of data sheets when they are the only known data for a particular system. Such data are considered to be still suitable for some applications, and their presence in the compilation should alert researchers to areas that need more work.

The typical data sheet carries the following information:

- (i) components - definition of the system - their names, formulas and Chemical Abstracts registry numbers;
- (ii) reference to the primary source where the numerical information is reported. In cases when the primary source is a less common periodical or a report document, published though of limited availability, abstract references are also given;
- (iii) experimental variables;
- (iv) identification of the compiler;
- (v) experimental values as they appear in the primary source. Whenever available, the data may be given both in tabular and graphical form. If auxiliary information is available, the experimental data are converted also to SI units by the compiler.

Under the general heading of Auxiliary Information, the essential experimental details are summarized:

- (vi) experimental method used for the generation of data;
- (vii) type of apparatus and procedure employed;
- (viii) source and purity of materials;
- (ix) estimated error;
- (x) references relevant to the generation of experimental data as cited in the primary source.

This new approach to numerical data presentation, developed during our four years of existence, has been strongly influenced by the diversity of background of those whom we are supposed to serve. We thus deemed it right to preface the evaluation/compilation sheets in each volume with a detailed discussion of the principles of the accurate determination of relevant solubility data and related thermodynamic information.

Finally, the role of education is more than corollary to the efforts we are seeking. The scientific standards advocated here are necessary to strengthen science and technology, and should be regarded as a major effort in the training and formation of the next generation of scientists and engineers. Specifically, we believe that there is going to be an impact of our project on scientific-communication practices. The quality of consolidation adopted by this program offers down-to-earth guidelines, concrete examples which are bound to make primary publication services more responsive than ever before to the needs of users. The self-regulatory message to scientists of 15 years ago to refrain from unnecessary publication has not achieved much. The literature is still, in 1980, cluttered with poor-quality articles. The Weinberg report (in "Reader in Science Information", Eds. J. Sherrod and A. Hodina, Microcard Editions Books, Indian Head, Inc., 1973, p.292) states that "admonition to authors to restrain themselves from premature, unnecessary publication can have little effect unless the climate of the entire technical and scholarly community encourages restraint...". We think that projects of this kind translate the climate into operational terms by exerting pressure on authors to avoid submitting low-grade material. The type of our output, we hope, will encourage attention to quality as authors will increasingly realize that their work will not be suited for permanent retrievability unless it meets the standards adopted in this project. It should help to dispel confusion in the minds of many authors of what represents a permanently useful bit of information of an archival value, and what does not.

If we succeed in that aim, even partially, we have then done our share in protecting the scientific community from unwanted and irrelevant, wrong numerical information.

A. S. Kertes

## PREFACE

Oxygen is the "acid former." Oxygen is 49.5% of the crust of the earth, 29.5% of the whole earth, and 0.96% of the universe by weight. Oxygen also forms about 20.94% of the atmosphere by mol per cent, and it is this latter abundance with which we are concerned in this volume. Oxygen from the air dissolves in the oceans, in all natural waters, in any fluids left out in the open or through which air is bubbled, and, of course, oxygen dissolves in biological fluids.

This volume is concerned with the solubility of oxygen (and ozone) in pure liquids, liquid mixtures, aqueous and organic solutions, biological fluids, and some miscellaneous solvents and mixtures. The coverage is on gas/liquid systems at high and low pressures. However, some fluids such as molten salts, alloys, glasses, and slags have been excluded, as well as polymeric materials. The scientific literature starting historically with W. Henry in 1803 has been systematically searched and the coverage should include most articles published through the end of 1980. (The editor would appreciate hearing about articles which were missed.)

This volume contains individual data sheets for each gas/liquid system in the author(s)' own reported units. In those cases where a given system was studied by several authors data sheets were not prepared for papers containing data of poor precision. However, reference is made to omitted papers. Again, for particular systems which have been studied by several authors, a critical evaluation is done of the data and recommended (or tentative) values are presented for that system along with a brief discussion of the contributions. These smoothed values represent our best judgement at this time. Users may use the smoothed values or the raw data in the individual data sheets.

The oxygen/water system has been widely studied by both chemical and physical means. The agreement between the two approaches is quite remarkable and I continue the recommendation made by R. Battino and H. L. Clever (*Chem. Rev.* 1966, 66, 395-463) to use this system as a reference standard for work in the field. The smoothed values appearing in the critical evaluation section on oxygen/water are currently the best attainable and it is my recommendation that they be used as a reference standard.

For anyone working on data compilations (such as this one) involving solubilities, the principal bugaboo has to be solubility units. In the third edition of Hildebrand and Scott's "Solubility of Nonelectrolytes" they present a table showing the solubility of sulfur ( $S_8$ ) at 25°C in benzene and toluene. In weight per cent sulfur is more soluble in benzene; however, in mol per cent or grams per liter sulfur is more soluble in toluene. There are about ten commonly used solubility units for gas solubilities, some of them historical, some in general use, and some specific to a given discipline. In the data sheets we have tabulated the solubilities in the units reported in the original paper. Where feasible the compilers have converted these solubilities to the Ostwald coefficient and/or the mole fraction solubility at 1 atm (101.325 kPa) partial pressure of gas. The conversions were carried out so that users of this volume would find most solubilities reported in a single unit, which could then be used for comparative purposes. Unless otherwise specified the units for the Bunsen coefficients reported herein are  $\text{cm}^3(\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$ .

Although data are reported in the units presented in the original paper, they are also presented in SI in the tables (where feasible), and always in SI in the "VARIABLES" box. With respect to naming components, we have attempted to use IUPAC nomenclature throughout, the Hill system for the formulas, and the unique Chemical Abstracts Registry Numbers for the substances.

Error estimates are always difficult to do. The individual compilers have either made their own estimates or cited those of the authors. In many cases the source and purity of the materials used in the investigations were missing in the original papers. Authors should be aware that such information is useful for other workers and as a means of validating their own work. Sometimes descriptions of procedures and apparatus were sketchy. The compilers have done their best in obtaining this information from articles which were published in other languages

than English.

The smoothing equations used have been of the simple two-constant form for data of average precision or of the three-constant form used by Weiss based on the Clarke and Glew approach.

$$\Delta\bar{G}_1^\circ/\text{J mol}^{-1} = -RT \ln x_1 = A + BT \quad (1)$$

or

$$\ln x_1 = -\Delta\bar{G}_1^\circ/RT = -(A/R)/T - (B/R) \quad (2)$$

or

$$\ln x_1 = A_0 + A_1/(T/100 \text{ K}) + A_2 \ln(T/100 \text{ K}) \quad (3)$$

Using  $T/100 \text{ K}$  as a variable rather than  $T/\text{K}$  leads to coefficients of similar order of magnitude. The smoothing equations and the thermodynamic functions calculated from them are presented in the "critical evaluation" sections.

Real gas corrections are not necessary for oxygen since the molar volume at STP is  $22,393 \text{ cm}^3\text{mol}^{-1}$  which leads to a correction of 0.09 per cent. Only the data of B. B. Benson and his co-workers are sufficiently precise to require real gas corrections and the reported values were so corrected. The second virial coefficient for oxygen varies smoothly from  $-45 \text{ cm}^3 \text{ mol}^{-1}$  at 200 K to  $-1.0 \text{ cm}^3 \text{ mol}^{-1}$  at 400 K. This converts to correction factors of 0.27 per cent at 200 K to 0.063 per cent at 300 K to 0.003 per cent at 400 K. Again, these corrections are negligible considering the general precision of most of the work reported herein of 0.5 to 2.0 per cent.

In most cases the sorting of systems according to the table of contents was easy. However, for data sheets reporting on solubility in a number of solvents and for some of the "miscellaneous" systems the editor had to make some arbitrary decisions. Common names of solvents are used as well as the systematic names to aid the reader.

The literature search turned up no data for the solubility of oxygen in heavy water,  $\text{D}_2\text{O}$ . This system should be measured. The reader will also note the paucity of high pressure solubility measurements for oxygen. This is no doubt due to the probability of converting the dissolution vessel into a bomb calorimeter.

The Editor appreciates the advice and suggestions made by members of the IUPAC Commission on Solubility Data, the encouragement of the Chief Editor of this series, the cooperation and hard work of the Evaluators and Compilers, and the efforts of the secretaries and assistants who worked on the project - Marty Tucker, Pauline Shively, B. Ramalingam, Tracy Park, Carolyn Dowie, and Lesley Flanagan.

Acknowledgment is made to the National Bureau of Standards for a grant which supported part of this work.

Rubin Battino

Dayton, OH

# THE SOLUBILITY OF GASES IN LIQUIDS

R. Battino, H. L. Clever and C. L. Young

## INTRODUCTION

The Solubility Data Project aims to make a comprehensive search of the literature for data on the solubility of gases, liquids and solids in liquids. Data of suitable accuracy are compiled into data sheets set out in a uniform format. The data for each system are evaluated and where data of sufficient accuracy are available values recommended and in some cases a smoothing equation suggested to represent the variation of solubility with pressure and/or temperature. A text giving an evaluation and recommended values and the compiled data sheets are published on consecutive pages.

## DEFINITION OF GAS SOLUBILITY

The distinction between vapor-liquid equilibria and the solubility of gases in liquids is arbitrary. It is generally accepted that the equilibrium set up at 300K between a typical gas such as argon and a liquid such as water is gas liquid solubility whereas the equilibrium set up between hexane and cyclohexane at 350K is an example of vapor-liquid equilibrium. However, the distinction between gas-liquid solubility and vapor-liquid equilibrium is often not so clear. The equilibria set up between methane and propane above the critical temperature of methane and below the critical temperature of propane may be classed as vapor-liquid equilibrium or as gas-liquid solubility depending on the particular range of pressure considered and the particular worker concerned.

The difficulty partly stems from our inability to rigorously distinguish between a gas, a vapor, and a liquid, which has been discussed in numerous textbooks. We have taken a fairly liberal view in these volumes and have included systems which may be regarded, by some workers, as vapor-liquid equilibria.

## UNITS AND QUANTITIES

The solubility of gases in liquids is of interest to a wide range of scientific and technological disciplines and not solely to chemistry. Therefore a variety of ways for reporting gas solubility have been used in the primary literature and inevitably sometimes, because of insufficient available information, it has been necessary to use several quantities in the compiled tables. Where possible, the gas solubility has been quoted as a mole fraction of the gaseous component in the liquid phase. The units of pressure used are bar, pascal, millimeters of mercury and atmosphere. Temperatures are reported in Kelvin.

## EVALUATION AND COMPILATION

The solubility of comparatively few systems is known with sufficient accuracy to enable a set of recommended values to be presented. This is true both of the measurement near atmospheric pressure and at high pressures. Although a considerable number of systems have been studied by at least two workers, the range of pressures and/or temperatures is often sufficiently different to make meaningful comparison impossible.

Occasionally, it is not clear why two groups of workers obtained very different sets of results at the same temperature and pressure, although both sets of results were obtained by reliable methods and are internally consistent. In such cases, sometimes an incorrect assessment has been given. There are several examples where two or more sets of data have been classified as tentative although the sets are mutually inconsistent.

Many high pressure solubility data have been published in a smoothed form. Such data are particularly difficult to evaluate, and unless specifically discussed by the authors, the estimated error on such values can only be regarded as an "informed guess".



Many of the high pressure solubility data have been obtained in a more general study of high pressure vapor-liquid equilibrium. In such cases a note is included to indicate that additional vapor-liquid equilibrium data are given in the source. Since the evaluation is for the compiled data, it is possible that the solubility data are given a classification which is better than that which would be given for the complete vapor-liquid data (or vice versa). For example, it is difficult to determine coexisting liquid and vapor compositions near the critical point of a mixture using some widely used experimental techniques which yield accurate high pressure solubility data. For example, conventional methods of analysis may give results with an expected error which would be regarded as sufficiently small for vapor-liquid equilibrium data but an order of magnitude too large for acceptable high pressure gas-liquid solubility.

It is occasionally possible to evaluate data on mixtures of a given substance with a member of a homologous series by considering all the available data for the given substance with other members of the homologous series. In this study the use of such a technique has been very limited.

The estimated error is often omitted in the original article and sometimes the errors quoted do not cover all the variables. In order to increase the usefulness of the compiled tables estimated errors have been included even when absent from the original article. If the error on *any* variable has been inserted by the compiler this has been noted.

#### PURITY OF MATERIALS

The purity of materials has been quoted in the compiled tables where given in the original publication. The solubility is usually more sensitive to impurities in the gaseous component than to liquid impurities in the liquid component. However, the most important impurities are traces of a gas dissolved in the liquid. Inadequate degassing of the absorbing liquid is probably the most often overlooked serious source of error in gas solubility measurements.

#### APPARATUS AND PROCEDURES

In the compiled tables brief mention is made of the apparatus and procedure. There are several reviews on experimental methods of determining gas solubilities and these are given in References 1-7.

#### METHODS OF EXPRESSING GAS SOLUBILITIES

Because gas solubilities are important for many different scientific and engineering problems, they have been expressed in a great many ways:

##### The Mole Fraction, $x(g)$

The mole fraction solubility for a binary system is given by:

$$\begin{aligned}x(g) &= \frac{n(g)}{n(g) + n(l)} \\ &= \frac{W(g)/M(g)}{[W(g)/M(g)] + [W(l)/M(l)]}\end{aligned}$$

here  $n$  is the number of moles of a substance (an *amount* of substance),  $W$  is the mass of a substance, and  $M$  is the molecular mass. To be unambiguous, the partial pressure of the gas (or the total pressure) and the temperature of measurement must be specified.

##### The Weight Per Cent Solubility, wt%

For a binary system this is given by

$$\text{wt\%} = 100 W(g)/[W(g) + W(l)]$$

where  $W$  is the weight of substance. As in the case of mole fraction, the pressure (partial or total) and the temperature must be specified. The weight per cent solubility is related to the mole fraction solubility by

$$x(g) = \frac{[\text{wt}\%/M(g)]}{[\text{wt}\%/M(g)] + [(100 - \text{wt}\%)/M(l)]}$$

#### The Weight Solubility, $C_w$

The weight solubility is the number of moles of dissolved gas per gram of solvent when the partial pressure of gas is 1 atmosphere. The weight solubility is related to the mole fraction solubility at one atmosphere partial pressure by

$$x(g) \text{ (partial pressure 1 atm)} = \frac{C_w M(l)}{1 + C_w M(l)}$$

where  $M(l)$  is the molecular weight of the solvent.

#### The Moles Per Unit Volume Solubility, $n$

Often for multicomponent systems the density of the liquid mixture is not known and the solubility is quoted as moles of gas per unit volume of liquid mixture. This is related to the mole fraction solubility by

$$x = \frac{n v^{\circ}(l)}{1 + n v^{\circ}(l)}$$

where  $v^{\circ}(l)$  is the molar volume of the liquid component.

#### The Bunsen Coefficient, $\alpha$

The Bunsen coefficient is defined as the volume of gas reduced to 273.15K and 1 atmosphere pressure which is absorbed by unit volume of solvent (at the temperature of measurement) under a partial pressure of 1 atmosphere. If ideal gas behavior and Henry's law is assumed to be obeyed,

$$\alpha = \frac{V(g)}{V(l)} \frac{273.15}{T}$$

where  $V(g)$  is the volume of gas absorbed and  $V(l)$  is the original (starting) volume of absorbing solvent. The mole fraction solubility  $x$  is related to the Bunsen coefficient by

$$x(1 \text{ atm}) = \frac{\alpha}{\alpha + \frac{273.15}{T} \frac{v^{\circ}(g)}{v^{\circ}(l)}}$$

where  $v^{\circ}(g)$  and  $v^{\circ}(l)$  are the molar volumes of gas and solvent at a pressure of one atmosphere. If the gas is ideal,

$$x = \frac{\alpha}{\alpha + \frac{273.15R}{v^{\circ}(l)}}$$

Real gases do not follow the ideal gas law and it is important to establish the real gas law used for calculating  $\alpha$  in the original publication and to make the necessary adjustments when calculating the mole fraction solubility.

#### The Kuenen Coefficient, $S$

This is the volume of gas, reduced to 273.15K and 1 atmosphere pressure, dissolved at a partial pressure of gas of 1 atmosphere by 1 gram of solvent.

### The Ostwald Coefficient, L

The Ostwald coefficient,  $L$ , is defined as the ratio of the volume of gas absorbed to the volume of the absorbing liquid, all measured at the same temperature:

$$L = \frac{V(g)}{V(l)}$$

If the gas is ideal and Henry's Law is applicable, the Ostwald coefficient is independent of the partial pressure of the gas. It is necessary, in practice, to state the temperature and total pressure for which the Ostwald coefficient is measured. The mole fraction solubility,  $x$ , is related to the Ostwald coefficient by

$$x = \left[ \frac{RT}{P(g) L v^{\circ}(l)} + 1 \right]^{-1}$$

where  $P$  is the partial pressure of gas. The mole fraction solubility will be at a partial pressure of  $P(g)$ .

### The Absorption Coefficient, $\beta$

There are several "absorption coefficients", the most commonly used one being defined as the volume of gas, reduced to 273.15K and 1 atmosphere, absorbed per unit volume of liquid when the total pressure is 1 atmosphere.  $\beta$  is related to the Bunsen coefficient by

$$\beta = \alpha(1-P(l))$$

where  $P(l)$  is the partial pressure of the liquid in atmosphere.

### The Henry's Law Constant

A generally used formulation of Henry's Law may be expressed as

$$P(g) = K_H x$$

where  $K_H$  is the Henry's Law constant and  $x$  the mole fraction solubility. Other formulations are

$$P(g) = K_2 C(l)$$

or

$$C(g) = K_C C(l)$$

where  $K_2$  and  $K_C$  are constants,  $C$  the concentration, and (l) and (g) refer to the liquid and gas phases. Unfortunately,  $K_H$ ,  $K_2$  and  $K_C$  are all sometimes referred to as Henry's Law constants. Henry's Law is a limiting law but can sometimes be used for converting solubility data from the experimental pressure to a partial gas pressure of 1 atmosphere, provided the mole fraction of the gas in the liquid is small, and that the difference in pressures is small. Great caution must be exercised in using Henry's Law.

### The Mole Ratio, $N$

The mole ratio,  $N$ , is defined by

$$N = n(g)/n(l)$$

Table 1 contains a presentation of the most commonly used inter-conversions not already discussed.

For gas solubilities greater than about 0.01 mole fraction at a partial pressure of 1 atmosphere there are several additional factors which must be taken into account to unambiguously report gas solubilities. Solution densities or the partial molar volume of gases must be known. Corrections should be made for the possible non-ideality of the gas or the non-applicability of Henry's Law.

TABLE 1 Interconversion of parameters used for reporting solubility

$$L = \alpha(T/273.15)$$

$$C_w = \alpha/v_o \rho$$

$$K_H = \frac{17.033 \times 10^6 \rho(\text{soln})}{\alpha M(1)} + 760$$

$$L = C_w v_{t,\text{gas}}^o$$

where  $v_o$  is the molal volume of the gas in  $\text{cm}^3 \text{mol}^{-1}$  at  $0^\circ\text{C}$ ,  $\rho$  the density of the solvent at the temperature of the measurement,  $\rho(\text{soln})$  the density of the solution at the temperature of the measurement, and  $v_{t,\text{gas}}^o$  the molal volume of the gas ( $\text{cm}^3 \text{mol}^{-1}$ ) at the temperature of the measurement.

### SALT EFFECTS

The effect of a dissolved salt in the solvent on the solubility of a gas is often studied. The activity coefficient of a dissolved gas is a function of the concentration of all solute species (see ref. 8). At a given temperature and pressure the logarithm of the dissolved gas activity coefficient can be represented by a power series in  $C_s$ , the electrolyte concentration, and  $C_i$ , the nonelectrolyte solute gas concentration

$$\log f_i = \sum_{m,n} k_{mn} C_s^n C_i^m$$

It is usually assumed that only the linear terms are important for low  $C_s$  and  $C_i$  values when there is negligible chemical interaction between solute species.

$$\log f_i = k_s C_s + k_i C_i$$

where  $k_s$  is the salt effect parameter and  $k_i$  is the solute-solute gas interaction parameter. The dissolved gas activity is the same in the pure solvent and a salt solution in that solvent for a given partial pressure and temperature

$$a_i = f_i S_i = f_i^o S_i^o \text{ and } f_i = f_i^o \frac{S_i^o}{S_i}$$

where  $S_i$  and  $S_i^o$  are the gas solubility in the salt solution and in the pure solvent, respectively, and the  $f$ 's are the corresponding activity coefficients. It follows that  $\log f_i/f_o = \log S_i/S_i^o = k_s C_s + k_i(S_i - S_i^o)$ . When the

quantity  $(S_i - S_i^o)$  is small the second term is negligible even though  $k_s$  and  $k_i$  may be of similar magnitude. This is generally the case for gas solubilities and the equation reduces to

$$\log \frac{f_i}{f_o} = \log \frac{S_i^o}{S_i} = k_s C_s$$

which is the form of the empirical Setschenow equation in use since the 1880's. A salt that increases the activity coefficient of the dissolved gas is said to salt-out and a salt that decreases the activity coefficient of the dissolved gas is said to salt-in.

Although salt effect studies have been carried out for many years, there appears to be no common agreement of the units for either the gas solubility or the salt concentration. Both molar ( $\text{mol dm}^{-3}$ ) and molal ( $\text{mol kg}^{-1}$ ) are used for the salt concentration. The gas solubility ratio  $S_i/S_i^o$  is given as Bunsen coefficient ratio and Ostwald coefficient ratio,

which would be the same as a molar ratio; Kueunen coefficient ratio, volume dissolved in 1 g or 1 kg of solvent which would be a molal ratio; and mole fraction ratio. Recent theoretical treatments use salt concentration in  $\text{mol dm}^{-3}$  and  $S_i^0/S_i$  ratio as mole fraction ratio with each salt ion acting as a mole. Evaluations which compare the results of several workers are made in the units most compatible with present theory.

#### TEMPERATURE DEPENDENCE OF GAS SOLUBILITY

In a few cases it has been found possible to fit the mole fraction solubility at various temperatures using an equation of the form.

$$\ln x = A + B / (T/100K) + C \ln (T/100K) + DT/100K$$

It is then possible to write the thermodynamic functions  $\Delta\bar{G}_i^0$ ,  $\Delta\bar{H}_i^0$ ,  $\Delta\bar{S}_i^0$  and  $\Delta\bar{C}_{p1}^0$  for the transfer of the gas from the vapor phase at 101.325 Pa partial pressure to the (hypothetical) solution phase of unit mole fraction as:

$$\Delta\bar{G}_i^0 = -RT \ln x = -RAT - 100 RB - RCT \ln (T/100)$$

$$\Delta\bar{S}_i^0 = RA + RC \ln (T/100) + RC$$

$$\Delta\bar{H}_i^0 = -100 RB + RCT$$

$$\Delta\bar{C}_{p1}^0 = RC$$

In cases where there are solubilities at only a few temperatures it is convenient to use the simpler equations.

$$\Delta\bar{G}_i^0 = -RT \ln x = A + BT$$

in which case  $A = \Delta\bar{H}_i^0$  and  $-B = \Delta\bar{S}_i^0$ .

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COMPONENTS:  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) Water; H <sub>2</sub> O; [7732-18-5]	EVALUATOR:  Rubin Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.
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## CRITICAL EVALUATION:

The solubility of oxygen in water at atmospheric pressure has probably been the most intensively studied gas solubility system. The work started with the early and crude measurements of Bunsen in 1855 and extends to the high precision measurements of Benson, Krause, and Peterson in 1979. The solubility may be determined by strictly physical means such as measuring P, V, and T, by chemical means via some version of the Winkler method, by gas chromatography, and via electrochemical methods using some version of the Clark electrode and polarography. The correspondence between the several approaches is surprisingly good.

Since this system is of such interest to oceanographers and biologists and biochemists and limnologists and sanitary engineers and physical chemists (to name a few!), I will be presenting two sets of recommended values. The first set covers the temperature range 273 to 348K and is a smoothed composite of the work in some fifteen papers. The second set covers the range 273 to 333K and is the smoothed values of Benson, Krause, and Peterson. (Details follow.) The agreement on these solubility values to a precision of about  $\pm 0.2$  per cent leads me to recommend that the Benson, Krause, and Peterson smoothed values be taken as standard for comparison and that all workers in the field test their apparatus and methods against them, particularly the 298.15K mole fraction solubility at 101.325kPa partial pressure of gas of  $2.301 \times 10^{-5}$ . This value is 0.17 per cent higher than the smoothed value recommended in the review by Wilhelm, Wilcock, and Battino (1) and 0.30 per cent higher than the value recommended in the earlier review by Battino and Clever (2). Thus, it would be safe to state that the recommended values are reliable to at least  $\pm 0.30$  per cent.

Over forty papers with data on the O<sub>2</sub>/H<sub>2</sub>O system were screened - of these some twenty-five were considered to contain data of sufficient accuracy (comparing them against the smoothed value in reference 1) to attempt smoothing as a group. After many trials and rejecting the papers containing points about two standard deviations beyond the smoothed line, a group of fifteen papers remained which used a variety of approaches to the measurements. The 149 points used in the smoothing were obtained as follows (reference - number of data points used from that reference): 3-21, 4-37, 5-26, 6-14, 7-2, 8-15, 9-1, 10-3, 11-14, 12-1, 13-1, 14-1, 15-8, 16-3, 17-2. The fitting equation used was

$$\ln x_1 = A + B/(T/100K) + C \ln (T/100K) \quad (1)$$

By using T/100K as the variable the coefficients were all of the same order of magnitude. Increasing the order of fit to four and five constants did not improve the fit at all. The best fit for the 149 points gave

$$\ln x_1 = -66.73538 + 87.47547/(T/100K) + 24.45264 \ln (T/100K) \quad (2)$$

where  $x_1$  is the mole fraction solubility at 101.325 kPa partial pressure of gas. The standard deviation of the fit in  $x_1$  was  $\pm 0.72 \times 10^{-7}$  for a per cent deviation of  $\pm 0.36$  per cent at the middle of the temperature range of 273 to 348K. Table 1 gives smoothed values of the mole fraction at 101.325 kPa partial pressure of gas and the Ostwald coefficient at 5K intervals.

Table 1 also gives the thermodynamic functions  $\Delta \bar{G}_1^\circ$ ,  $\Delta \bar{H}_1^\circ$ , and  $\Delta \bar{S}_1^\circ$ , for the transfer of gas from the vapor phase at 101.325 kPa partial pressure to the (hypothetical) solution phase of unit mole fraction. These thermodynamic properties were calculated from the smoothing equation according to the following equations:

$$\Delta \bar{G}_1^\circ = -RAT - 100RB - RCT \ln(T/100) \quad (3)$$

$$\Delta \bar{S}_1^\circ = RA + RC \ln(T/100) + RC \quad (4)$$

continued on following page

COMPONENTS:	EVALUATOR:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Rubin Battino
(2) Water; H <sub>2</sub> O; [7732-18-5]	Department of Chemistry
	Wright State University
	Dayton, OH 45435 U.S.A.

CRITICAL EVALUATION: continued

$$\Delta \bar{H}_1^\circ = -100RB + RCT \quad (5)$$

$$\Delta C_{P1}^\circ = RC \quad (6)$$

The  $\Delta \bar{C}_{P1}^\circ$  value was constant at 203 J mol<sup>-1</sup>K<sup>-1</sup>.

TABLE 1. Smoothed values of the solubility of oxygen in water, and thermodynamic functions at 5K intervals using equation 2 at 101.325 kPa partial pressure of gas

T/K	10 <sup>5</sup> x <sub>1</sub> <sup>a</sup>	10 <sup>2</sup> L <sup>b</sup>	$\Delta \bar{G}_1^\circ /$ kJ mol <sup>-1</sup>	$\Delta \bar{H}_1^\circ /$ kJ mol <sup>-1</sup>	$\Delta \bar{S}_1^\circ /$ J mol <sup>-1</sup> K <sup>-1</sup>
273.15	3.949	4.913	23.02	-17.20	-147.3
278.15	3.460	4.384	23.75	-16.18	-143.6
283.15	3.070	3.958	24.46	-15.16	-139.9
288.15	2.756	3.614	25.15	-14.15	-136.4
293.15	2.501	3.333	25.83	-13.13	-132.9
298.15	2.293	3.104	26.48	-12.11	-129.5
303.15	2.122	2.918	27.12	-11.10	-126.1
308.15	1.982	2.766	27.74	-10.08	-122.7
313.15	1.867	2.643	28.35	- 9.06	-119.5
318.15	1.773	2.545	28.94	- 8.05	-116.3
323.15	1.697	2.468	29.51	- 7.03	-113.1
328.15	1.635	2.409	30.07	- 6.01	-110.0
333.15	1.586	2.367	30.61	- 5.00	-106.9
338.15	1.549	2.339	31.14	- 3.98	-103.9
343.15	1.521	2.325	31.65	- 2.97	-100.9
348.15	1.502	2.323	32.15	- 1.95	- 97.9

<sup>a</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.

<sup>b</sup> Ostwald coefficient.

Benson, Krause, and Peterson (4) studied the solubility of oxygen in water and attained an unprecedented precision in their work. If we fit their 37 data points using equation (1) we get

$$\ln x_1 = -64.21517 + 83.91236/(T/100K) + 23.24323 \ln(T/100K) \quad (7)$$

This is for the temperature range 273 to 333 K and it fits the data with a standard deviation in x<sub>1</sub> of ±0.36 × 10<sup>-7</sup> or ±0.17 per cent at the mid-point. However, the authors chose to fit their data to the following equation

$$\ln k = 3.71814 + 5.59617 \times 10^3/(T/K) - 1.049668 \times 10^6/(T/K)^2 \quad (8)$$

where the fugacity f = k x<sub>1</sub> and k is the Henry coefficient. They recommend this equation over the 273 to 373 K range. For unit fugacity the mole fraction solubilities calculated from this equation are given in Table 2 at 5 K intervals. The standard deviation of the fit to this equation is ±0.017 per cent. If equation 8 is written in the general form of

$$\ln k = a_0 + a_1/(T/K) + a_2/(T/K)^2 \quad (9)$$

then the thermodynamic functions are given by:

$$\Delta \bar{G}_1^\circ = R [a_0 (T/K) + a_1 + a_2/(T/K)] \quad (10)$$

continued on following page

COMPONENTS: (1) Oxygen; O <sub>2</sub> [ 7782-44-7] (2) Water; H <sub>2</sub> O; [ 7732-18-5]	EVALUATOR: Rubin Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.
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## CRITICAL EVALUATION:

continued

$$\Delta \bar{H}_1^\circ = R a_1 + 2a_2/(T/K)$$

$$\Delta \bar{S}_1^\circ = R -a_0 + a_2/(T/K)^2$$

$$\Delta \bar{Cp}_1^\circ = -2 R a_2/(T/K)^2$$

The values calculated from these equations differ little from those presented in Table 1 except, of course, for the heat capacity. Equation 13 predicts a temperature dependence which equation 6 does not.

TABLE 2. Smoothed values of the solubility of oxygen in water using equation 8 at 5K intervals and at unit fugacity

T/K	10 <sup>5</sup> x <sub>1</sub> <sup>a</sup>	T/K	10 <sup>5</sup> x <sub>1</sub> <sup>a</sup>	T/K	10 <sup>5</sup> x <sub>1</sub>
273.15	3.9583	308.15	1.9906	343.15	1.4930
278.15	3.4655	313.15	1.8743	348.15	1.4634
283.15	3.0747	318.15	1.7776	353.15	1.4403
288.15	2.7614	323.15	1.6973	358.15	1.4230
293.15	2.5078	328.15	1.6305	363.15	1.4107
298.15	2.3009	333.15	1.5753	368.15	1.4031
303.15	2.1310	338.15	1.5299	373.15	1.3996

<sup>a</sup> Mole fraction solubility at unit fugacity.

Benson, et al. (4) also analyzed the high-pressure data of Stephan, et al. (18) and calculated Henry coefficients from this data. Benson, et al., fit the Stephan, et al., data with their own and obtained equation 14 which they recommend for values above 373K. The Stephan, et al., data was

$$\ln k = -4.1741 + 1.3104 \times 10^4/(T/K) - 3.4170 \times 10^6/(T/K)^2 + 2.4749 \times 10^8/(T/K)^3 \quad (14)$$

fit to ±2.0 per cent which was within their experimental error. Table 3 contains the mole fraction solubilities calculated using equation 14 in the temperature range 373 to 563K.

TABLE 3. Smoothed values of the mole fraction solubility of oxygen in water using equation 14 at 5K intervals and 101.325 kPa partial pressure of gas.

T/K	10 <sup>5</sup> x <sub>1</sub>	T/K	10 <sup>5</sup> x <sub>1</sub>	T/K	10 <sup>5</sup> x <sub>1</sub>
373.15	1.414	438.15	1.889	503.15	3.312
378.15	1.423	443.15	1.960	508.15	3.477
383.15	1.437	448.15	2.036	513.15	3.653
388.15	1.455	453.15	2.117	518.15	3.839
393.15	1.478	458.15	2.205	523.15	4.036
398.15	1.505	463.15	2.298	528.15	4.245
403.15	1.537	468.15	2.399	533.15	4.467
408.15	1.573	473.15	2.506	538.15	4.701
413.15	1.614	478.15	2.620	543.15	4.949
418.15	1.659	483.15	2.742	548.15	4.701
423.15	1.710	488.15	2.871	553.15	5.488
428.15	1.765	493.15	3.009	558.15	5.781
433.15	1.824	498.15	3.156	563.15	6.090

continued on following page



<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>EVALUATOR:</p> <p>Rubin Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.</p>
<p>CRITICAL EVALUATION:</p> <p style="text-align: center;">continued</p> <p>Ten references (19-28) contained data of sufficient accuracy and/or historical interest to have had data sheets prepared. However, they did not meet the overall requirements of being included in the group of fifteen used for the initial smoothing.</p> <p>For completeness of coverage I am also including references to other work (29-50), most of which was of much poorer precision. Bunsen's papers, for example, are of historic interest, but his values are erratically 10-20 per cent off from modern measurements. Finally, the Klots and Benson paper (51) contains data for the ratio of <sup>32</sup>O<sub>2</sub> to <sup>34</sup>O<sub>2</sub> solubilities in water. The heavier isotope is more soluble by about 0.08 per cent.</p> <p><u>References</u></p> <ol style="list-style-type: none"> <li>1. Wilhelm, E.; Battino, R.; Wilcock, R. <i>J. Chem. Rev.</i> 1977, 77, 219-62.</li> <li>2. Battino, R.; Clever, H.L. <i>Chem. Rev.</i> 1966, 66, 395-463.</li> <li>3. Benson, B.B.; Krause, D. <i>J. Chem. Phys.</i> 1976, 64, 689-709.</li> <li>4. Benson, B.B.; Krause, D.; Peterson, M.A. <i>J. Soln. Chem.</i> 1979, 8, 655-90.</li> <li>5. Carpenter, J.H. <i>Limnol. Oceanog.</i> 1966, 11, 264-77.</li> <li>6. Douglas, E. <i>J. Phys. Chem.</i> 1964, 68, 169-74.</li> <li>7. Geffcken, G. <i>Z. Physik. Chem.</i> 1904, 49, 257-302.</li> <li>8. Klots, C.E.; Benson, B.B. <i>J. Marine Res. (Sears Found. Marine Res.)</i> 1963, 21, 48-57.</li> <li>9. Livingston, J.; Morgan, R.; Richardson, A.H. <i>J. Phys. Chem.</i>, 1930, 34, 2356-66.</li> <li>10. Murray, C.N.; Riley, J.P.; Wilson, T.R.S. <i>Deep-Sea Research</i>, 1968, 15, 237-8.</li> <li>11. Murray, C.N.; Riley, J.P. <i>Deep-Sea Research</i>, 1969, 16, 311-20.</li> <li>12. Novak, D.M.; Conway, B.E. <i>Chem. Instrumentation</i> 1974, 5, 79-90.</li> <li>13. Power, G.G. <i>J. Appl. Physiol.</i> 1968, 24, 468-74.</li> <li>14. Power, G.G.; Stegall, H. <i>J. Appl. Physiol.</i> 1970, 29, 145-9.</li> <li>15. Pray, H.A.; Stephan, E.F. <i>U.S. Atomic Energy Commission</i>, BMI-840, 1953.</li> <li>16. Steen, H. <i>Limnol. Oceanog.</i> 1958, 3, 423-6.</li> <li>17. Timofeev, W. <i>Z. Physik. Chem.</i> 1890, 6, 141-52.</li> <li>18. Stephan, E.L.; Hatfield, N.S.; Peoples, R.S.; Pray, H.A.H. <i>Battelle Memorial Institute Report BMI-1067</i>, 1956.</li> <li>19. Adeney, W.E.; Becker, H.G. <i>Royal Dublin Soc. Scientific Proc.</i> 1919, 15, 609-28.</li> <li>20. Bohr, C. <i>Z. Physik. Chem.</i> 1910, 71, 47-50.</li> <li>21. Elmore, H.L.; Hayes, T.W. <i>J. Sanit. Eng. Div. Am. Soc. Civil Engrs.</i> 1960, 86(SA4), 41-53.</li> <li>22. Fox, C.J.J. <i>Trans. Faraday Soc.</i> 1909, 5, 68-87.</li> <li>23. Morris, C.J.; Stumm, W.; Galal, H.A. <i>Proc. Am. Soc. Civil Engrs.</i> 1961, 85, 81-6.</li> <li>24. Müller, C. <i>Z. Physik. Chem.</i> 1912, 81, 483-503.</li> <li>25. Shchukarev, S.A.; Tolmacheva, T.A. <i>Zh. Strukt. Khim.</i> 1968, 9, 21-8.</li> <li>26. Wilcock, R.J.; Battino, R. <i>Nature (London)</i> 1974, 252, 614-5.</li> <li>27. Wise, D.L.; Houghton, G. <i>Biophys. J.</i> 1969, 9, 36-53.</li> <li>28. Zander, R.; Euler, R. <i>Proceedings of an Interdisciplinary Symposium held at Odense University, Denmark, 26-27 Sept. 1974</i>, Ed. H. Degn., I. Balslev, R. Brook, Elsevier Scientific Publishing Co. Amsterdam (1976), 271-6.</li> <li>29. Allen, J.A. <i>Nature</i>, 1955, 175, 83.</li> <li>30. Bunsen, R. <i>Ann.</i> 1855, 93, 1-50.</li> <li>31. Bunsen, R. <i>Phil. Mag.</i> 1855, 9, 116-30; 181-201.</li> <li>32. Bunsen, R. <i>Ann. Chim. Phys.</i> 1855, 43, 496-.</li> </ol> <p style="text-align: right;">continued on following page</p>	

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	EVALUATOR: Rubín Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.
CRITICAL EVALUATION: <p style="text-align: center;">continued</p> 33. Bunsen, R. <i>Gasometrische Methoden</i> , 2nd ed., Braunschweig 1858. 34. Cassuto, L. <i>Physik. Z.</i> 1904, 5, 233-6. 35. Christoff, A. <i>Z. Physik. Chem.</i> 1906, 55, 622-34. 36. Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. <i>J. Phys. Chem.</i> 1957, 61, 1078-82. 37. Liss, P.S.; Slater, P.G. <i>Nature-Phys.</i> 1972, 238, 64. 38. Maharajh, D.M.; Walkley, J. <i>Nature (London)</i> 1972, 236, 165. 39. Morrison, T.J.; Billett, F. <i>J. Chem. Soc.</i> 1948, 2033-5. 40. Orcutt, F.S.; SeEVERS, M.H. <i>J. Biol. Chem.</i> 1937, 117, 501-7. 41. Pogrebnaya, V.L.; Usov, A.P.; Baranov, A.V. <i>Zh. Vses. Khim. Obshchest.</i> 1972, 17, 344-5. 42. Pospisil, J.; Luzny, Z. <i>Coll. Czech. Chem. Commun.</i> 1960, 25, 589-92. 43. Schwab, G.M.; Berninger, E. <i>Z. Physik. Chem.</i> 1928, A138, 55-74. 44. Shoor, S.K. <i>Ph.D. thesis, University of Florida</i> , 1968. 45. Shoor, S.K.; Walker, R.D.; Gubbins, K.E. <i>J. Phys. Chem.</i> 1969, 73, 312-7. 46. Winkler, L.W. <i>Ber.</i> 1888, 21, 2843-54. 47. Winkler, L.W. <i>Ber.</i> 1889, 22, 1764-74. 48. Winkler, L.W. <i>Ber.</i> 1891, 24, 3602-10. 49. Winkler, L.W. <i>Z. Physik. Chem.</i> 1892, 9, 171-5. 50. Winkler, L.W. <i>Ber.</i> 1901, 34, 1408-22. 51. Klots, C.E.; Benson, B.B. <i>J. Chem. Phys.</i> 1963, 38, 890-2.	

## Oxygen Solubilities up to 200 kPa

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Timofeev, W. <i>Z. Physik. Chem.</i> <u>1890</u> , 6, 141-52.												
<b>VARIABLES:</b> T/K = 279-286 P/kPa = 101.325	<b>PREPARED BY:</b> R. Battino												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="218 485 984 628"> <thead> <tr> <th>T/K<sup>a</sup></th> <th>10<sup>5</sup> x<sub>1</sub><sup>b</sup></th> <th>10<sup>2</sup> L<sup>c</sup></th> <th>10<sup>2</sup> α<sup>d</sup></th> </tr> </thead> <tbody> <tr> <td>279.55</td> <td>3.328</td> <td>4.236</td> <td>4.1408</td> </tr> <tr> <td>285.72</td> <td>2.896</td> <td>3.767</td> <td>3.6011</td> </tr> </tbody> </table> <p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> Mole fraction solubility at 101.325 kPa (1atm) partial pressure of gas. Calculated by compiler.</p> <p><sup>c</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>d</sup> Bunsen coefficient.</p>		T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>	10 <sup>2</sup> α <sup>d</sup>	279.55	3.328	4.236	4.1408	285.72	2.896	3.767	3.6011
T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>	10 <sup>2</sup> α <sup>d</sup>										
279.55	3.328	4.236	4.1408										
285.72	2.896	3.767	3.6011										
<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> Used a Bunsen absorption apparatus as modified by Ostwald. Basically, a manometric/volumetric apparatus. Details and a drawing are given in the paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.  <b>ESTIMATED ERROR:</b> δα/α = ±0.01, estimate by compiler.  <b>REFERENCES:</b>												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Geffcken, G. <i>Z. Physik. Chem.</i> <u>1904</u> , 49, 257-302.									
<b>VARIABLES:</b> T/K = 288 - 298 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> R. Battino									
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="221 486 1063 662" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K<sup>a</sup></th> <th style="text-align: center;">10<sup>5</sup> x<sub>1</sub><sup>b</sup></th> <th style="text-align: center;">10<sup>2</sup>L<sup>c</sup></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">288.15</td> <td style="text-align: center;">2.768</td> <td style="text-align: center;">3.630<sup>d</sup></td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">2.275</td> <td style="text-align: center;">3.080<sup>e</sup></td> </tr> </tbody> </table> <p> <sup>a</sup> Temperature reported as 15 and 25°C.  <sup>b</sup> Mole fraction solubility at 101.325 kPa (1 atm) partial pressure of gas. Calculated by compiler.  <sup>c</sup> Ostwald coefficient.  <sup>d</sup> Average of the following values (10<sup>2</sup>L): 3.639, 3.640, 3.619, 3.635, 3.618, 3.643, 3.618.  <sup>e</sup> Average of the following values (10<sup>2</sup>L): 3.096, 3.074, 3.096, 3.087, 3.081, 3.081, 3.091. (Average is 3.088, although the author reported 3.080.)         </p>		T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>	288.15	2.768	3.630 <sup>d</sup>	298.15	2.275	3.080 <sup>e</sup>
T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>								
288.15	2.768	3.630 <sup>d</sup>								
298.15	2.275	3.080 <sup>e</sup>								
<b>AUXILIARY INFORMATION</b>										
<b>METHOD/APPARATUS/PROCEDURE:</b> The design of Ostwald was used. The critical gas burets and a absorption vessel were thermostatted. A manometric/volumetric procedure. Details and a drawing given in the original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared from heating pure KClO <sub>3</sub> and MnO <sub>2</sub> . Washed in dilute KOH and dried over concentrated H <sub>2</sub> SO <sub>4</sub> . (2) No comment by author.									
<b>ESTIMATED ERROR:</b> δL/L = ±0.01, estimate by compiler.										
<b>REFERENCES:</b>										

## Oxygen Solubilities up to 200 kPa

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-77] (2) Water; H <sub>2</sub> O; [7732-18-5]		Fox, C.J.J. <i>Trans. Faraday Soc.</i> <u>1909</u> , 5, 68-87.	
VARIABLES:		PREPARED BY:	
T/K = 273-316		R. Battino	
EXPERIMENTAL VALUES:			
T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coefficient <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coefficient <sup>d</sup> 10 <sup>2</sup> α
273.76	3.907	4.872	4.861
273.96	3.873	4.832	4.818
278.66	3.422	4.344	4.258
278.75	3.422	4.345	4.258
283.97	3.035	3.925	3.775
284.05	3.036	3.927	3.776
288.75	2.733	3.591	3.397
288.75	2.752	3.616	3.421
293.95	2.500	3.341	3.105
293.96	2.489	3.326	3.091
299.15	2.296	3.118	2.847
299.15	2.300	3.123	2.852
304.13	2.034	2.805	2.519
304.19	2.032	2.803	2.517
308.64	1.993	2.785	2.465
308.74	1.993	2.786	2.465
313.19	1.889	2.674	2.332
313.24	1.887	2.672	2.330
318.44	1.782	2.559	2.195
318.44	1.778	2.553	2.190
323.40	1.699	2.472	2.088
323.44	1.699	2.472	2.088
continued on following page			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
A modified form of the Estreicher (1) apparatus was used. Diagram and procedure given in paper. The water is degassed by boiling using a double flask system. The quantity of water is determined by weighing. The dry gas is introduced from a gas buret, the flask shaken and a final reading of the volume of gas absorbed is made after there are no changes. A manometer is used to take readings at different pressures. Several readings at different temperatures are taken on one loading of the absorption flask.		(1) Generated by heating KMnO <sub>4</sub> in a tube and then passing it over soda lime and P <sub>2</sub> O <sub>5</sub> .	
		(2) Distilled.	
		ESTIMATED ERROR:	
		δ <sub>α</sub> /α = ±0.004 estimated by compiler.	
		REFERENCES:	
		1. Estreicher, T. <i>Z. Physik. Chem.</i> <u>1899</u> , 31, 176.	

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-77] (2) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Fox, C.J.J. <i>Trans. Faraday Soc.</i> <u>1909</u> , 5, 68-87.
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continued

T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coefficient <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coefficient <sup>d</sup> 10 <sup>2</sup> α
274.78 <sup>e</sup>	3.799	4.755	4.727
275.33	3.726	4.673	4.636
279.35	3.367	4.284	4.189
279.75	3.342	4.258	4.158
282.68	3.116	4.011	3.876
282.76	3.116	4.012	3.876
286.80	2.855	3.727	3.550
286.90	2.844	3.714	3.536
289.87	2.691	3.549	3.344
289.90	2.680	3.534	3.330
296.95	2.391	3.226	2.967
297.05	2.383	3.216	2.957
303.01	2.140	2.941	2.651
303.03	2.147	2.951	2.660
310.66	1.950	2.740	2.409
310.69	1.947	2.737	2.406
316.40	1.818	2.596	2.241
316.44	1.817	2.595	2.240

<sup>a</sup> Original temperature reported at °C to 0.01°C.

<sup>b</sup> Mole fraction solubility at 101.325 kPa (1 atm) partial pressure of gas calculated by compiler.

<sup>c</sup> Ostwald coefficients calculated by compiler.

<sup>d</sup> Bunsen coefficients reported in original paper.

<sup>e</sup> Second series of measurements.

<sup>f</sup> Smoothing equation of author given as

$$1000 \alpha = 49.239 - 1.3440t + 0.28752 t^2 - 0.0003024 t^3$$

with t in °C.

<sup>g</sup> Author also determined the solubility of oxygen in seawater (0-28°C) and 0-20 per mille<sub>Cl</sub><sup>Cl</sup>.

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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Bohr, C. <i>Z. Physik. Chem.</i> <u>1910</u> , 71, 47-50.								
<b>VARIABLES:</b> T/K = 294 p/kPa = 101.325	<b>PREPARED BY:</b> R. Battino								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="270 493 1072 624" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K<sup>a</sup></th> <th style="text-align: center;">10<sup>5</sup> x<sub>1</sub><sup>b</sup></th> <th style="text-align: center;">10<sup>2</sup>L<sup>c</sup></th> <th style="text-align: center;">10<sup>2</sup>α<sup>d</sup></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">294.15</td> <td style="text-align: center;">2.480</td> <td style="text-align: center;">3.316</td> <td style="text-align: center;">3.079</td> </tr> </tbody> </table> <p data-bbox="139 663 1147 856"> <sup>a</sup> Temperature reported to 0.1°C.  <sup>b</sup> Mole fraction solubility at 101.325 kPa (1 atm) partial pressure of gas calculated by compiler.  <sup>c</sup> Ostwald coefficient calculated by compiler.  <sup>d</sup> Bunsen coefficient.         </p>		T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>	10 <sup>2</sup> α <sup>d</sup>	294.15	2.480	3.316	3.079
T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>	10 <sup>2</sup> α <sup>d</sup>						
294.15	2.480	3.316	3.079						
<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> The absorption measuring apparatus is described in reference (1). Paper also reports solubilities in sulfuric acid solutions.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given. <b>ESTIMATED ERROR:</b> δα/α = ±0.01, estimate by author. <b>REFERENCES:</b> 1. Bohr, C. <i>Sauerstoffaufnahme des Blutfarbstoffes.</i> Kopenhagen <u>1895</u> . Jolin, <i>Archiv f. (Anat. u.) Physiologie</i> <u>1889</u> , 265.								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Müller, C. Z. Physik. Chem. <u>1912</u> , 81, 483-503.												
<b>VARIABLES:</b> T/K = 288-289 P/kPa = 101.325	<b>PREPARED BY:</b> R. Battino												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="128 478 1163 668"> <thead> <tr> <th>T/K<sup>a</sup></th> <th>Mole Fraction<sup>b</sup> 10<sup>5</sup> x<sub>1</sub></th> <th>Ostwald Coeff.<sup>c</sup> 10<sup>2</sup>L</th> <th>Bunsen Coeff.<sup>d</sup> 10<sup>2</sup>α</th> </tr> </thead> <tbody> <tr> <td>288.45</td> <td>2.715</td> <td>3.564</td> <td>3.375</td> </tr> <tr> <td>289.35</td> <td>3.528</td> <td>3.528</td> <td>3.330</td> </tr> </tbody> </table> <p> <sup>a</sup> Temperature reported to 0.1°C.  <sup>b</sup> Mole fraction solubility at 101.325 kPa (latm) partial pressure of gas calculated by compiler.  <sup>c</sup> Ostwald coefficient calculated by compiler.  <sup>d</sup> Bunsen coefficient.         </p>		T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α	288.45	2.715	3.564	3.375	289.35	3.528	3.528	3.330
T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α										
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> Water is degassed by pumping under vacuum. The absorption vessel is about 600 cm <sup>3</sup> and is separately thermostatted from the buret gas measuring system. Both are connected by a copper capillary tube. Gas uptake is read on the volume and all liquid volumes were calibrated with mercury. Original paper contains details and a drawing. Solubilities also reported in sucrose, d-glucose, chloral hydrate, and glycerol aqueous solutions.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From the heating of KMnO <sub>4</sub> and washed in concentrated KOH solution. (2) No comment by author.												
<b>ESTIMATED ERROR:</b> $\delta\alpha/\alpha = \pm 0.01$ , estimate by compiler.													
<b>REFERENCES:</b>													



## Oxygen Solubilities up to 200 kPa

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Adeney, W. E.; Becker, H. G. <i>Royal Dublin Soc. Scientific Pro.</i> <u>1919, 15, 609-28.</u>		
<b>VARIABLES:</b> T/K = 276-308		<b>PREPARED BY:</b> R. Battino		
<b>EXPERIMENTAL VALUES:</b>				
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	10 <sup>2</sup> α <sup>d</sup> /cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>
2.5	275.7	3.529	4.431	4.390
8.8	282.0	2.982	3.830	3.710
15.5	288.7	2.580	3.389	3.206
20.2	293.4	2.379	3.174	2.955
25.2	298.4	2.203	2.985	2.732
30.3	303.5	1.990	2.739	2.465
35.1	308.3	1.835	2.562	2.270
a Calculated by compiler. b Mole fraction solubility at 101.325 kPa partial pressure of gas. c Ostwald coefficient. d Bunsen coefficient.				
<b>AUXILIARY INFORMATION</b>				
<b>METHOD/APPARATUS/PROCEDURE:</b> A manometric system using water-jacketed burets was used.		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared from heating potassium permanganate and washing the gas with caustic potash. (2) Distilled.		
		<b>ESTIMATED ERROR:</b> δα/α = ±0.02, compiler's estimate. δT/K = ±0.1		
		<b>REFERENCES:</b>		

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Water; H<sub>2</sub>O; [7732-13-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Livingston, J.; Morgan, R.; Richardson, A.H.</p> <p><i>J. Phys. Chem.</i> <u>1930</u>, 34, 2356-66.</p>																												
<p>VARIABLES:</p> <p>T/K = 298</p> <p>P/kPa = 23 - 101</p>	<p>PREPARED BY:</p> <p>R. Battino</p>																												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="276 460 1046 588"> <thead> <tr> <th>t/°C</th> <th>T<sup>a</sup>/K</th> <th>10<sup>5</sup>x<sub>1</sub><sup>a,b</sup></th> <th>10<sup>2</sup>L<sup>a,c</sup></th> <th>q'<sup>d</sup></th> </tr> </thead> <tbody> <tr> <td>25</td> <td>298</td> <td>2.304</td> <td>3.120</td> <td>0.04080</td> </tr> </tbody> </table> <p>a Calculated by compiler.</p> <p>b Mole fraction solubility at 101.325 kPa partial pressure of gas.</p> <p>c Ostwald coefficient.</p> <p>d Weight of oxygen absorbed by 1000 cm<sup>3</sup> of solvent at 25°C and a partial pressure of 760 mm Hg. Average of twelve measurements at slightly varying total pressures near 760 mm Hg.</p> <table border="1" data-bbox="394 901 848 1127"> <thead> <tr> <th>P<sub>O<sub>2</sub></sub>/mmHg</th> <th>10<sup>2</sup>q'<sup>a</sup></th> <th>10<sup>2</sup>L<sup>b</sup></th> </tr> </thead> <tbody> <tr> <td>174.7</td> <td>0.95</td> <td>3.158</td> </tr> <tr> <td>202.2</td> <td>1.07</td> <td>3.073</td> </tr> <tr> <td>240.7</td> <td>1.28</td> <td>3.088</td> </tr> <tr> <td>242.5</td> <td>1.28</td> <td>3.065</td> </tr> <tr> <td>280.7</td> <td>1.50</td> <td>3.103</td> </tr> </tbody> </table> <p style="text-align: right;">continued on following page</p>		t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	q' <sup>d</sup>	25	298	2.304	3.120	0.04080	P <sub>O<sub>2</sub></sub> /mmHg	10 <sup>2</sup> q' <sup>a</sup>	10 <sup>2</sup> L <sup>b</sup>	174.7	0.95	3.158	202.2	1.07	3.073	240.7	1.28	3.088	242.5	1.28	3.065	280.7	1.50	3.103
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	q' <sup>d</sup>																									
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<p style="text-align: center;">AUXILIARY INFORMATION</p>																													
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The Winkler method was used to determine the amount of dissolved oxygen. Details are given in the paper. For the hydrostatic pressure measurements the equilibration flask was under a pressure due to a column of water.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:</p> <p>δq'/q' = ±0.003, authors' estimate.</p> <p>REFERENCES:</p>																												

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Livingston, J.; Morgan, R.;
(2) Water; H <sub>2</sub> O; [7732-18-5]	Richardson, A.H.
	<i>J. Phys. Chem.</i> <u>1930</u> , 34, 2356-66.

continued

P <sub>O<sub>2</sub></sub> /mm Hg	10 <sup>2</sup> q <sup>a</sup>	10 <sup>2</sup> L <sup>b</sup>
300.3	1.60	3.094
349.0	1.84	3.062
364.1	1.96	3.126
396.1	2.10	3.079
413.7	2.10	3.088
433.3	2.27	3.042
440.5	2.33	3.072
446.7	2.35	3.055
458.3	2.43	3.079
478.1	2.54	3.085
504.8	2.65	3.049
511.4	2.73	3.107
539.7	2.83	3.045
559.3	2.95	3.063
577.7	3.03	3.046
610.2	3.25	3.093
614.6	3.27	3.090
639.7	3.37	3.059
649.2	3.42	3.059
738.7	3.87	3.042
741.1	3.94	3.087
741.1	3.93	3.080

<sup>a</sup> Grams of oxygen/1000 cm<sup>3</sup> solvent at the partial pressure of gas indicated. All measurements at 25°C (298 K).

<sup>b</sup> Ostwald coefficient. Calculated from

$$L = \frac{224 \times 298 \times 760 \times q}{320 \times 273 \times P_{O_2}}$$

t/°C	T <sup>a</sup> /K	P <sub>T</sub> <sup>b</sup> /mm Hg	10 <sup>2</sup> gO <sub>2</sub> /dm <sup>3</sup>	10 <sup>2</sup> q <sup>d</sup>	10 <sup>2</sup> L <sup>e</sup>
15.2	288.4	815.4	5.438	5.016	3.833
15.2	288.4	850.9	5.478	4.865	3.717
15.2	288.4	861.3	5.582	4.898	3.743
15.2	288.4	921.2	5.889	4.891	3.737
16.6	289.8	801.8	5.346	4.847	3.704
16.6	289.8	855.6	5.306	4.520	3.454
16.6	289.8	862.2	5.441	4.601	3.516
16.6	289.8	887.0	5.881	4.840	3.698
17.2	290.4	819.0	4.198	4.765	3.641
17.2	290.4	857.5	5.193	4.549	3.476
17.2	290.4	884.9	5.553	4.715	3.603
17.2	290.4	908.6	5.806	4.803	3.670
19.2	292.4	794.1	4.890	4.524	3.457
19.2	292.4	839.7	5.046	4.423	3.380
19.2	292.4	867.5	5.305	4.506	3.365
19.2	292.4	897.7	5.564	4.511	3.447
20.2	293.4	796.8	4.716	4.370	3.339
20.2	293.4	853.8	5.024	4.352	3.326
20.2	293.4	869.4	5.036	4.287	3.276
20.2	293.4	884.9	5.106	4.272	3.264
20.4	293.6	804.9	4.796	4.579	3.499
20.4	293.6	857.1	5.065	4.441	3.394

continued on following page

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Livingston, J.; Morgan, R.;
(2) Water; H <sub>2</sub> O; [7732-18-5]	Richardson, A.H.
	<i>J. Phys. Chem.</i> <u>1930</u> , 34, 2356-66.

continued

t/°C	T <sup>a</sup> /K	P <sub>T</sub> <sup>b</sup> /mm Hg	10 <sup>2</sup> gO <sub>2</sub> <sup>c</sup> /dm <sup>3</sup>	10 <sup>2</sup> q <sup>c</sup>	10 <sup>2</sup> L <sup>e</sup>
20.4	293.6	875.8	5.193	4.457	3.406
20.4	293.6	904.3	5.454	4.451	3.401
20.6	293.8	802.6	4.796	4.377	3.345
20.6	293.8	857.0	5.043	4.320	3.301
20.6	293.8	859.6	4.972	4.247	3.245
20.6	293.8	891.5	5.271	4.346	3.321
21.0	294.2	832.7	4.926	4.392	3.357
21.0	294.2	839.0	4.966	4.395	3.358
21.0	294.2	868.1	5.056	4.328	3.307
21.0	294.2	894.1	5.111	4.251	3.248
21.0	294.2	797.0	4.684	4.380	3.347
21.0	294.2	829.6	4.826	4.339	3.316
21.0	294.2	878.1	5.123	4.355	3.328
21.0	294.2	895.1	5.209	4.346	3.321
21.5	294.7	781.5	4.580	4.346	3.321
21.5	294.7	807.7	4.741	4.320	3.301
21.5	294.7	864.8	5.078	4.330	3.309
21.5	294.7	883.3	5.186	4.332	3.310

- a Calculated by compiler.
- b Total pressure. Height of a column of water plus atmospheric pressure.
- c Grams of oxygen/dm<sup>3</sup> solvent at the pressure of the measurement.
- d Grams of oxygen/dm<sup>3</sup> solvent at 1 atm (101.325 kPa) partial pressure of oxygen.
- e Ostwald coefficient.
- f All measurements at 25°C (298 K).

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Morrison, T.J.; Billett, F. J. Chem. Soc. <u>1952</u> , 3919-22.	
VARIABLES:		PREPARED BY:	
T/K - 286 - 348		R. Battino	
EXPERIMENTAL VALUES:			
T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	S <sub>0</sub> <sup>d</sup>
285.85	2.926	3.808	36.39
286.65	2.860	3.732	35.56
290.45	2.622	3.464	32.58
294.65	2.427	3.250	30.13
303.15	2.138	2.940	26.49
312.55	1.889	2.670	23.33
322.45	1.715	2.490	21.09
331.65	1.615	2.400	19.77
338.45	1.562	2.360	19.05
345.65	1.508	2.318	18.32
348.05	1.500	2.319	18.20
<p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> Mole fraction solubility at 101.325 Pa (1 atm) partial pressure of gas calculated by compiler.</p> <p><sup>c</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>d</sup> S<sub>0</sub> is the solubility in cm<sup>3</sup> at standard temperature and pressure per 1000g of water at a total gas pressure of 1 atm.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
<p>Solvent is degassed by thorough boiling. It then flows in a thin film down a glass spiral and into a buret system containing the gas to be dissolved. Equilibrium is rapidly attained. Flow rates may be varied over a wide range without affecting the solubility. The solvent serves as its own gas buret and volumes read on the burets are used to calculate the solubility. The method is described in reference (1). The present paper describes an improved degassing section based on the vapor-pump principle.</p>		<p>(1) From a cylinder and from K<sup>2</sup>MnO<sub>4</sub> gave the same results.</p> <p>(2) No comment by authors.</p>	
		ESTIMATED ERROR: δS <sub>0</sub> /S <sub>0</sub> = ±0.005, estimate of reproducibility by authors.	
		REFERENCES:	
		1. Morrison, T.J.; Billett, F. J. Chem. Soc. <u>1948</u> , 2033-5.	

COMPONENTS:		ORIGINAL MEASUREMENTS:																					
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Steen, H. <i>Limnol. Oceanog.</i> <u>1958</u> , 3, 423-6.																					
VARIABLES:		PREPARED BY:																					
T/K = 279 - 297 P/kPa = 101.325		R. Battino																					
EXPERIMENTAL VALUES:																							
T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>2</sup> L <sup>c</sup>	10 <sup>2</sup> α <sup>d</sup>																				
279.15	3.367	4.281	4.189 <sup>e</sup>																				
285.15	2.952	3.832	3.671																				
291.15	2.599	3.442	3.229																				
297.15	2.341	3.160	2.905																				
<p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> Molefraction solubility at 101.325 kPa (1 atm) partial pressure of gas. Calculated by compiler.</p> <p><sup>c</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>d</sup> Bunsen coefficient.</p> <p><sup>e</sup> Average values at each temperature. Raw values are (all α x 10<sup>2</sup>):</p> <table border="1"> <thead> <tr> <th>279.15K</th> <th>285.15K</th> <th>291.15K</th> <th>297.15K</th> </tr> </thead> <tbody> <tr> <td>4.188</td> <td>3.673</td> <td>3.229</td> <td>2.901</td> </tr> <tr> <td>4.186</td> <td>3.664</td> <td>3.231</td> <td>2.908</td> </tr> <tr> <td>4.196</td> <td>3.674</td> <td>3.222</td> <td>2.898</td> </tr> <tr> <td>4.186</td> <td>3.673</td> <td>3.235</td> <td>2.913</td> </tr> </tbody> </table>				279.15K	285.15K	291.15K	297.15K	4.188	3.673	3.229	2.901	4.186	3.664	3.231	2.908	4.196	3.674	3.222	2.898	4.186	3.673	3.235	2.913
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4.186	3.673	3.235	2.913																				
AUXILIARY INFORMATION																							
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:																					
The procedure followed was that used by Scholander (1) in his 0.5cm <sup>3</sup> analyzer. Gas-free water was prepared by boiling. Temperature was controlled to ±0.01°C and known to ±0.05°C.		No details given.																					
		ESTIMATED ERROR:																					
		δα/α = ±0.3%, estimate by author. δT/T = ±0.05K, estimate by author.																					
		REFERENCES:																					
		1. Scholander, P.F. <i>J. Biol. Chem.</i> <u>1947</u> , 167, 235-50.																					

## Oxygen Solubilities up to 200 kPa

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Elmore, H.L.; Hayes, T.W.  J. Sanit. Eng. Div. Am. Soc. Civil Engns. <u>1960</u> , 86(SA4), 41-53.			
VARIABLES:		PREPARED BY:			
T/K = 275-302		R. Battino			
EXPERIMENTAL VALUES:					
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	10 <sup>2</sup> α <sup>a,d</sup> / cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	C <sub>s</sub> <sup>e</sup>
1.81	274.96	3.750	4.697	4.666	13.874
1.82	274.97	3.756	4.704	4.673	13.894
1.83	274.98	3.765	4.716	4.685	13.930
1.85	275.00	3.761	4.711	4.680	13.914
4.99	278.14	3.480	4.409	4.330	12.851
4.99	278.14	3.464	4.388	4.310	12.791
4.99	278.14	3.479	4.407	4.328	12.845
4.99	278.14	3.453	4.375	4.297	12.753
4.99	278.14	3.456	4.379	4.301	12.764
5.09	278.24	3.457	4.381	4.300	12.762
5.09	278.24	3.470	4.398	4.318	12.813
5.09	278.24	3.467	4.394	4.313	12.800
5.09	278.24	3.465	4.391	4.311	12.792
5.29	278.44	3.458	4.386	4.303	12.771
9.19	282.34	3.107	3.995	3.865	11.439
9.29	282.44	3.104	3.993	3.862	11.428
9.29	282.44	3.104	3.993	3.862	11.430
9.39	282.54	3.103	3.993	3.860	11.423
9.39	282.54	3.100	3.989	3.856	11.410
9.39	282.54	3.099	3.987	3.854	11.405
9.59	282.74	3.104	3.997	3.861	11.421
9.59	282.74	3.114	4.009	3.873	11.457
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
<p>The determination of the amount of dissolved oxygen was via the Winkler method. The procedure and the reagents used are described in detail. The endpoint in the final titration was detected amperometrically. Equilibrium saturation was attained via two methods:</p> <p>(a) after the water was deoxygenated by bubbling nitrogen through it, the water was allowed to absorb oxygen from the overlying atmosphere with gentle stirring;</p> <p>(b) the water was first super-saturated with gaseous oxygen and then allowed to approach the saturation level under the influence of constant gentle stirring.</p>			(1) From air or from a tank.		
			(2) Distilled.		
			ESTIMATED ERROR: δC <sub>s</sub> = ±0.020, standard deviation. Estimate by authors. Ranges from ±0.032 at 2°C to ±0.008 at 29°C. δT/K = ±0.05		
			REFERENCES:		

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Elmore, H.L.; Hayes, T.W. <i>J. Sanit. Eng. Div. Am. Soc. Civil Engrs.</i> 1960, 86(SA4), 41-53.
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continued

t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	10 <sup>2</sup> α <sup>a,d</sup> / cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	C <sub>s</sub> <sup>e</sup>
15.56	288.71	2.705	3.544	3.353	9.862
15.56	288.71	2.708	3.558	3.366	9.901
15.56	288.71	2.707	3.557	3.366	9.899
15.56	288.71	2.704	3.552	3.360	9.883
15.56	288.71	2.707	3.566	3.373	9.922
15.57	288.72	2.708	3.558	3.366	9.900
20.45	293.60	2.456	3.279	3.051	8.917
20.65	293.80	2.457	3.282	3.052	8.919
20.65	293.80	2.457	3.282	3.052	8.882
20.65	293.80	2.453	3.276	3.046	8.903
20.75	293.90	2.454	3.279	3.047	9.900
20.75	293.90	2.443	3.264	3.034	8.862
20.80	293.95	2.460	3.288	3.055	8.937
20.80	293.95	2.450	3.274	3.043	8.888
20.80	293.95	2.451	3.275	3.044	8.891
20.90	294.05	2.448	3.272	3.039	8.876
20.90	294.05	2.434	3.254	3.023	8.831
20.95	294.10	2.444	3.268	3.035	8.867
22.97	296.12	2.353	3.166	2.920	8.499
22.98	296.13	2.356	3.170	2.924	8.511
22.98	296.13	2.354	3.167	2.921	8.502
23.12	296.27	2.344	3.156	2.909	8.468
23.17	296.32	2.359	3.176	2.924	8.510
23.18	296.33	2.340	3.151	2.905	8.455
29.11	302.26	2.098	2.877	2.600	7.568
29.12	302.27	2.100	2.879	2.602	7.572
29.13	302.28	2.089	2.865	2.589	7.534
29.13	302.28	2.094	2.871	2.594	7.550
29.16	302.31	2.093	2.870	2.593	7.548
29.30	302.45	2.091	2.869	2.591	7.542

a Calculated by compiler.

b Mole fraction solubility at 101.325 kPa partial pressure of gas.

c Ostwald coefficient.

d Bunsen coefficient.

e Solubility in mg O<sub>2</sub> per liter. All values reported are the means of five replicate determinations. The authors give the following smoothing curve:

$$C_s = 14.652 - 0.41022(t/°C) + 0.0079910(t/°C)^2 - 0.000077774(t/°C)^3$$

valid in the range 0 to 30°C.



COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Morris, C. J.; Stumm, W.; Galal, H.A. <i>Proc. Am. Soc. Civil Engrs.</i> <u>1961</u> , 85 81-6.			
VARIABLES:		PREPARED BY:			
T/K = 278-303		R. Battino			
EXPERIMENTAL VALUES:					
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	10 <sup>2</sup> α <sup>d,e</sup> / cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	C <sub>s</sub> <sup>d,f</sup>
5.14	278.29	3.483	4.415	4.333	12.933
7.24	280.39	3.275	4.182	4.074	12.050
9.53	282.68	3.142	4.044	3.908	11.542
9.58	282.73	3.096	3.986	3.851	11.371
9.93	283.08	3.082	3.973	3.834	11.319
14.76	287.91	2.766	3.624	3.438	10.104
18.16	291.31	2.606	3.453	3.238	9.475
18.50	291.65	2.588	3.433	3.215	9.404
19.41	292.56	2.588	3.433	3.215	9.265
23.47	296.62	2.379	3.206	2.952	8.567
25.80	298.95	2.271	3.083	2.817	8.141
29.10	302.25	2.198 <sup>g</sup>	3.013 <sup>g</sup>	2.723 <sup>g</sup>	7.813 <sup>g</sup>
<p>a Calculated by compiler.</p> <p>b Mole fraction solubility at 101.325 kPa partial pressure of gas.</p> <p>c Ostwald coefficient.</p> <p>d Determined by the chemical method.</p> <p>e Bunsen coefficient.</p> <p>f Solubility in mg O<sub>2</sub> per liter.</p> <p>g Doubtful point-author's comment.</p>					
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
In the chemical method distilled water was saturated with CO <sub>2</sub> free normal air for three days and the dissolved oxygen determined by the Winkler method. In the manometric method pure gaseous oxygen at a known pressure was brought into contact with a known volume of degassed water in a closed system. At equilibrium, the solubility was determined from a buret reading. Details of both methods are given in the original paper.			(1) Normal air freed from CO <sub>2</sub> for chemical method. No comment for physical method.		
			(2) Distilled.		
			ESTIMATED ERROR:		
			δα/α = ±0.001, authors' estimate.		
			δT/K = ±0.03		
			REFERENCES:		

## COMPONENTS:

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Water; H<sub>2</sub>O; [7732-18-5]

## EVALUATOR:

Morris, C.J.; Stumm, W.; Galal, H.A.  
*Proc. Am. Soc. Civil Engrs.*, 1961,  
 85, 81-6.

continued

t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	10 <sup>2</sup> g <sup>d,e</sup> / cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	C <sub>s</sub> <sup>d,f</sup>
11.47	284.62	2.965	3.843	3.688	10.89
14.54	287.69	2.767	3.623	3.440	10.13
15.00	288.15	2.766	3.627	3.438	10.12
15.00	288.15	2.729	3.579	3.398	9.99
17.03	290.18	2.660	3.511	3.305	9.70
22.79	295.94	2.376	3.195	2.949	8.59
22.79	295.94	2.364	3.179	2.934	8.54
22.79	295.94	2.382	3.203	2.956	8.61
22.79	295.94	2.359	3.172	2.928	8.53
22.79	295.94	2.364	3.179	2.934	8.54
26.97	300.12	2.216	3.018	2.747	7.93
26.98	300.13	2.223	3.028	2.756	7.95
29.96	303.11	2.163	2.974	2.680	7.69

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.

<sup>c</sup> Ostwald coefficient.

<sup>d</sup> Determined manometrically.

<sup>e</sup> Bunsen coefficient.

<sup>f</sup> Solubility in mg O<sub>2</sub> per liter.

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		ORIGINAL MEASUREMENTS: Klots, C. E.; Benson, B. B. <i>J. Marine Res.</i> (Sears Found. Marine Res.) <u>1963</u> , 21, 48-57.		
VARIABLES: T/K = 275-299		PREPARED BY: R. Battino		
EXPERIMENTAL VALUES:				
T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α	α(O <sub>2</sub> )/α(N <sub>2</sub> ) <sup>e</sup>
275.44	3.736	4.687	4.648	2.047
276.10	3.651	4.591	4.542	2.037
278.93	3.389	4.305	4.216	2.027
279.69	3.336	4.249	4.150	2.029
280.19	3.292	4.202	4.096	2.026
284.87	2.957	3.835	3.677	2.004
284.95	2.945	3.820	3.662	1.999
287.52	2.801	3.665	3.482	1.997
295.13	2.417	3.241	3.000	1.955
296.29	2.365	3.184	2.935	1.947
296.35	2.366	3.186	2.937	1.950
296.83	2.344	3.161	2.909	1.947
296.86	2.348	3.167	2.914	1.950
297.20	2.333	3.150	2.895	1.949
297.51	2.324	3.141	2.884	1.949
299.42	2.247	3.055	2.787	1.936
continued on following page				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE: Two bulbs of ca. 300 cm <sup>3</sup> capacity are connected by two stopcocks. Degassed water is introduced into one bulb. Dry gas is introduced into the other bulb. The volumes of both are known to better than 0.05%. The stopcocks between the bulbs are opened, about one-half the water is moved into the gas bulb and the apparatus agitated in a thermostat for up to 48 hrs. Then the bulbs are placed upright and the saturated water and the gas phase isolated. The undissolved gas is removed and its pressure, volume and temperature measured in the dry state to determine the number of moles. The moles of dissolved gas are similarly determined. Constancy of gas mass in an experiment is about 0.05%. Solubility is calculated from the known volumes and quantities.		SOURCE AND PURITY OF MATERIALS: (1) "Tank" grade with less than 0.2% nitrogen. (2) "Sterile" distilled.		
		ESTIMATED ERROR: Precision δα/α = ±0.002, author's estimate.		
		REFERENCES:		

## COMPONENTS:

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Water; H<sub>2</sub>O; [7732-18-5]

## ORIGINAL MEASUREMENTS:

Klots, C. E.; Benson, B. B.  
*J. Marine Res. (Sears Found. Marine Res.)* 1963, 21, 48-57.

continued

T/K	$\alpha(\text{O}_2)/\alpha(\text{N}_2)^f$
278.90	2.024
284.10	2.002
285.05	1.999
285.05	2.002
295.55	1.947
296.85	1.944

- a Calculated by compiler. Temperatures reported to 0.01°C.  
 b Mole fraction solubility at 101.325 Pa (1 atm) partial pressure of gas calculated by compiler.  
 c Ostwald coefficient calculated by compiler.  
 d Bunsen coefficient - data originally reported as.  
 e Ratio of solubility of O<sub>2</sub> to N<sub>2</sub> as Bunsen coefficients from a 50:50 mixture. Determined manometrically.  
 f Same as (e) but determined mass spectrometrically. The precision in the solubility ratios (authors) is about 0.2%.

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Douglas, E. <i>J. Phys. Chem.</i> <u>1964</u> , 68, 169-74.	
VARIABLES:		PREPARED BY:	
T/K = 281 - 302 P/kPa = 101.325		R. Battino	
EXPERIMENTAL VALUES:			
T/K <sup>a</sup>	Mole fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α/cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>
281.15	3.202	4.101	3.984
281.15	3.207	4.107	3.990
281.15	3.204	4.103	3.986
281.15	3.198	4.095	3.978
281.15	3.200	4.098	3.981
293.09	2.492	3.321	3.095
293.09	2.494	3.324	3.098
293.09	2.494	3.324	3.098
293.09	2.496	3.326	3.100
293.09	2.490	3.318	3.092
302.30	2.139	2.934	2.651
302.30	2.142	2.937	2.654
302.30	2.143	2.938	2.655
302.30	2.141	2.936	2.653
302.30	2.139	2.934	2.651
<p><sup>a</sup> Temperature reported to 0.01°C.</p> <p><sup>b</sup> Mole fraction solubility at 101.325 kPa (1 atm) partial pressure of gas calculated by compiler.</p> <p><sup>c</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>d</sup> Bunsen coefficient.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
The apparatus and procedures are based on the Scholander microgasometric apparatus (1). This version uses one arm with an expanded solvent reservoir. Degassed water is introduced into this reservoir and sealed over mercury. The water is then tipped into the absorption chamber. Gas is introduced and the entire apparatus is shaken in a water thermostat (controlled to 0.01K). Gas and liquid volumes are read on a micrometer syringe by displacement of mercury.		(1) No comment by author.	
		(2) Double distilled.	
		ESTIMATED ERROR:	
		δα/α = ±0.003, estimate by author.	
		δT/T = ±0.01 (to 0.02K), estimate by author	
		REFERENCES:	
		1. Scholander, P.F. <i>J. Biol. Chem.</i> <u>1947</u> , 167, 235-50.	

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Carpenter, J.H. <i>Limnol. Oceanog.</i> <u>1966</u> , <i>11</i> , 264-77.		
VARIABLES:		PREPARED BY:		
T/K = 274 - 308		R. Battino		
EXPERIMENTAL VALUES:				
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	S <sup>d</sup>
0.48	273.63	3.909	4.872	10.120
0.52	273.67	3.897	4.857	10.088
0.64	273.79	3.887	4.847	10.062
5.10	278.25	3.441	4.361	8.887 (7) <sup>e</sup>
5.21	278.36	3.430	4.349	8.858
9.89	283.04	3.068	3.954	7.894 (4) <sup>e</sup>
10.10	283.25	3.056	3.942	7.863
10.22	283.37	3.047	3.932	7.839
11.68	284.83	2.952	3.828	7.584
12.04	285.19	2.933	3.808	7.531
12.40	285.55	2.912	3.786	7.476 (8) <sup>e</sup>
14.55	287.70	2.788	3.650	7.139
14.72	287.87	2.780	3.642	7.116
14.97	288.12	2.766	3.626	7.079
14.99	288.14	2.766	3.627	7.079
15.12	288.27	2.757	3.616	7.054
15.14	288.29	2.758	3.618	7.057
20.08	293.23	2.496	3.327	6.340
20.10	293.25	2.497	3.330	6.344
25.10	298.25	2.290	3.102	5.761
25.35	298.50	2.280	3.091	5.734
25.36	298.51	2.284	3.096	5.742
29.80	302.95	2.132	2.929	5.301
continued on following page				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
Water in a plexiglass box was rocked in contact with the air. Equilibrated water is transferred to a calibrated 500 cm <sup>3</sup> bottle and the dissolved oxygen determined by the modified Winkler method described in reference (1). The precision of the titration technique is stated to be ±0.02%, but with an estimated accuracy of ±0.1%. Measurements made with 3 hr and 14 hr equilibration times agreed within ±0.1%. Details are given in reference (1). This paper also reports on oxygen solubility in seawater.		(1) From air of 20.94% oxygen content.		
		(2) No details given. Presumably distilled.		
		ESTIMATED ERROR:		
		δS/S = ±0.001, author's estimate. δT/K = ±0.01		
		REFERENCES:		
		1. Carpenter, J.H. <i>Limnol. Oceanog.</i> <u>1965</u> , <i>10</i> , 135-40.		

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Carpenter, J.H.		
(2) Water; H <sub>2</sub> O; [7732-18-5]		<i>Limnol. Oceanog.</i> 1966, 11, 264-77.		
CRITICAL EVALUATION:		continued		
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	S <sup>d</sup>
29.81	302.96	2.135	2.933	5.308
34.76	307.91	1.988	2.772	4.867
34.82	307.97	1.989	2.773	4.868
<p>a Calculated by compiler.</p> <p>b Mole fraction solubility at 101.325 kPa partial pressure of gas.</p> <p>c Ostwald coefficient.</p> <p>d Solubility in cm<sup>3</sup>/dm<sup>3</sup> of solvent corrected to 760 mm Hg total pressure, 100% relative humidity, and 20.94% oxygen. The Ostwald coefficient is then given by:</p> $L = \frac{(T/K)}{273.15} \times \frac{760S}{10 \times (760 - P_w)}$ <p>where x = % oxygen and P<sub>w</sub> = saturation vapor pressure of water.</p>				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Power, G. G. <i>J. Appl. Physiol.</i> <u>1968</u> , 24, 468-74.																																							
<b>VARIABLES:</b> T/K = 310 P/kPa = 50-95	<b>PREPARED BY:</b> C. L. Young																																							
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">T/K</th> <th style="text-align: left;">P<sub>O<sub>2</sub></sub> /mmHg</th> <th style="text-align: left;">P<sub>O<sub>2</sub></sub> /kPa</th> <th style="text-align: left;">Bunsen coefficient, α/cm<sup>3</sup>(STP)cm<sup>-3</sup> atm<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="12" style="vertical-align: top;">310.15</td> <td>398</td> <td>53.1</td> <td>0.0239</td> </tr> <tr> <td>398</td> <td>53.1</td> <td>0.0237</td> </tr> <tr> <td>398</td> <td>53.1</td> <td>0.0240</td> </tr> <tr> <td>398</td> <td>53.1</td> <td>0.0236</td> </tr> <tr> <td>398</td> <td>53.1</td> <td>0.0236</td> </tr> <tr> <td>711</td> <td>94.8</td> <td>0.0239</td> </tr> <tr> <td>371</td> <td>49.5</td> <td>0.0238</td> </tr> <tr> <td>371</td> <td>49.5</td> <td>0.0239</td> </tr> <tr> <td>395</td> <td>52.7</td> <td>0.0238</td> </tr> <tr> <td>395</td> <td>52.7</td> <td>0.0237</td> </tr> <tr> <td colspan="3"></td> <td style="text-align: right;">Average .. 0.0238 ± 0.0001</td> </tr> </tbody> </table>		T/K	P <sub>O<sub>2</sub></sub> /mmHg	P <sub>O<sub>2</sub></sub> /kPa	Bunsen coefficient, α/cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	310.15	398	53.1	0.0239	398	53.1	0.0237	398	53.1	0.0240	398	53.1	0.0236	398	53.1	0.0236	711	94.8	0.0239	371	49.5	0.0238	371	49.5	0.0239	395	52.7	0.0238	395	52.7	0.0237				Average .. 0.0238 ± 0.0001
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	<sup>a</sup> The compiler calculated an Ostwald coefficient of 0.02702 and a mole fraction solubility at 101.325 kPa partial pressure of gas of 1.925 x 10 <sup>-5</sup> from these data.																																							
<b>AUXILIARY INFORMATION</b>																																								
<b>METHOD/APPARATUS/PROCEDURE:</b> Liquid samples were equilibrated with gas and then the dissolved gas was stripped out under vacuum and measured in a manometric Van Slyke apparatus.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given. <b>ESTIMATED ERROR:</b> δT/K = ±0.03. <b>REFERENCES:</b>																																							



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Shchukarev, S.A.; Tolmacheva, T.A. <i>Zh. Strukt. Khim.</i> 1968, 9, 21-8; <i>J. Struct. Chem.</i> 1968, 9, 16-21.															
<b>VARIABLES:</b> T/K = 277-323 P/kPa = 101.325	<b>PREPARED BY:</b> R. Battino															
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="109 472 1130 740"> <thead> <tr> <th>T/K<sup>a</sup></th> <th>Molefraction<sup>b</sup> 10<sup>5</sup>x<sub>1</sub></th> <th>Ostwald Coeff.<sup>c</sup> 10<sup>2</sup>L</th> </tr> </thead> <tbody> <tr> <td>277.15</td> <td>3.573</td> <td>4.51</td> </tr> <tr> <td>285.15</td> <td>2.935</td> <td>3.81</td> </tr> <tr> <td>298.15</td> <td>2.289</td> <td>3.10</td> </tr> <tr> <td>323.15</td> <td>1.636<sup>d</sup></td> <td>2.38<sup>d</sup></td> </tr> </tbody> </table> <p data-bbox="109 760 1114 819"><sup>a</sup> Temperature reported to 1°C, but as integer values, i.e., 4, 12, 25, 50°C.</p> <p data-bbox="109 831 1088 889"><sup>b</sup> Mole fraction solubility at 101.325 kPa (1atm) partial pressure at gas calculated by compiler.</p> <p data-bbox="109 909 418 938"><sup>c</sup> Ostwald coefficient.</p> <p data-bbox="109 952 1017 1011"><sup>d</sup> This value off from smoothing curve by 3.6%, other values are within 0.5%.</p>		T/K <sup>a</sup>	Molefraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	277.15	3.573	4.51	285.15	2.935	3.81	298.15	2.289	3.10	323.15	1.636 <sup>d</sup>	2.38 <sup>d</sup>
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<b>AUXILIARY INFORMATION</b>																
<b>METHOD/APPARATUS/PROCEDURE:</b> Degassed water is transferred to an absorption vessel. The water is sealed over mercury. Gas is added and stirring accomplished with a magnetic bob. Uptake is read on a gas buret system which is thermostatted along with the absorption vessel. Details of operation and a drawing are in the original paper. The paper also reports the solubility of oxygen in water/ethanol solutions, 0-100%.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by electrolysis of NaOH solution, followed by removal of hydrogen traces, and thoroughly dried before use. No purity given. (2) Distilled.															
<b>ESTIMATED ERROR:</b> δL/L = ± 0.01, estimate by compiler																
<b>REFERENCES:</b>																

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Murray, C.N.; Riley, J.P.; Wilson, T.R.S. <i>Deep-Sea Research</i> <u>1969</u> , <i>16</i> , 297-310.																
<b>VARIABLES:</b> T/K = 297-301 P/kPa = 101.325	<b>PREPARED BY:</b> R. Battino																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="105 473 1131 705"> <thead> <tr> <th>T/K<sup>a</sup></th> <th>Mole Fraction<sup>b</sup> 10<sup>5</sup>x<sub>1</sub></th> <th>Ostwald Coeff.<sup>c</sup> 10<sup>2</sup>L</th> <th>Bunsen Coeff.<sup>d</sup> 10<sup>2</sup>α</th> </tr> </thead> <tbody> <tr> <td>286.75</td> <td>2.838</td> <td>3.704</td> <td>3.528</td> </tr> <tr> <td>298.87</td> <td>2.269</td> <td>3.079</td> <td>2.814</td> </tr> <tr> <td>301.46</td> <td>2.166</td> <td>2.963</td> <td>2.685</td> </tr> </tbody> </table> <p data-bbox="89 725 1092 924"> <sup>a</sup> Temperature reported to 0.01°C.  <sup>b</sup> Mole fraction solubility at 101.325 kPa (1atm) partial pressure of gas calculated by compiler.  <sup>c</sup> Ostwald coefficient calculated by compiler.  <sup>d</sup> Bunsen coefficient.         </p>		T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α	286.75	2.838	3.704	3.528	298.87	2.269	3.079	2.814	301.46	2.166	2.963	2.685
T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α														
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301.46	2.166	2.963	2.685														
<b>AUXILIARY INFORMATION</b>																	
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was a modification of the design by Ben-Naim and Baer (1). Degassed water is forced by centrifugal action up two outside tubes of the absorption vessel and down a center tube, contacting gas along the way. Gas uptake is read on a gas buret system. The whole apparatus is thermostatted to ±0.012°C. The degassing apparatus was a modification of the design of Battino and Evans utilizing a magnetically driven centrifugal pump.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) British Oxygen Company; contains 0.05% Ar and less than 0.1% N <sub>2</sub> . (2) Distilled. <b>ESTIMATED ERROR:</b> δT = ±0.02K, estimate by compiler δα/α = ± 0.0019, estimate of authors <b>REFERENCES:</b> 1. Ben-Naim, A.; Baer, S. <i>Trans. Faraday Soc.</i> <u>1963</u> , <i>59</i> , 2735-8. 2. Battino, R.; Evans, F.D. <i>Anal. Chem.</i> <u>1966</u> , <i>38</i> , 1627-9.																

COMPONENTS: (1) Oxygen, O <sub>2</sub> ; [7792-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		ORIGINAL MEASUREMENTS: Murray, C. N.; Riley, J. P. <i>Deep-Sea Research</i> <u>1969</u> , <i>16</i> , 311-20.		
VARIABLES: T/K = 274-303 P/kPa = 101.325		PREPARED BY: R. Battino		
EXPERIMENTAL VALUES:				
T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Bunsen Coeff. <sup>c</sup> 10 <sup>2</sup> α	Ostwald Coeff. <sup>d</sup> 10 <sup>2</sup> L	Solubility <sup>e</sup>
273.89	3.871	4.816	4.829	10.021
274.95	3.754	4.670	4.702	9.713
278.05	3.450	4.292	4.369	8.910
280.60	3.251	4.044	4.154	8.382
283.10	3.065	3.812	3.951	7.887
288.27	2.748	3.415	3.605	7.031
293.15	2.503	3.109	3.337	6.360
298.10	2.302	2.856	3.117	5.794
302.95	2.136	2.646	2.935	5.312
307.95	1.986	2.457	2.770	4.862
<p><sup>a</sup> Temperature reported to 0.01°C.</p> <p><sup>b</sup> Mole fraction solubility at 101.325 kPa (1 atm) partial pressure of gas calculated by compiler.</p> <p><sup>c</sup> Bunsen coefficient calculated from last column ("solubility") Via <math>\alpha = \frac{760 \times \text{solubility}}{10 \times X \times (760 - P_w^w)}</math> where X = 20.94 or the percentage of oxygen in the atmosphere and P<sub>w</sub><sup>w</sup> is the saturation vapor pressure of water at T.</p> <p style="text-align: right;">continued on following page</p>				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE: The chemical determination of oxygen solubility involved analyzing water saturated with air by the Winkler method. A modification of Carpenter's method (1) was used, precautions being taken to minimize the loss of iodine during the titration. Details are given in the paper including the kind of reagents used. The physical method was that of Ben-Naim and Baer (2) as modified and described by Murray, et al. (3). The apparatus uses a new degassing unit modified on the design of Battino and Evans (4). Details are given with drawings in (3). This paper also reports the solubility of oxygen in sea water of various salinities.		SOURCE AND PURITY OF MATERIALS: (1a) (Chemical Method) - from saturating water with air. (1b) (Physical Method) - 99.9% pure by mass spectrometric analysis; from the British Oxygen Company. (2) Distilled		
		ESTIMATED ERROR: δT = ±0.02K, estimate by compiler. δ(Solubility) = ±0.01 cm <sup>3</sup> O <sub>2</sub> /dm <sup>3</sup> , estimate by authors for both chemical and physical methods.		
		REFERENCES: 1. Carpenter, J.H. <i>Limnol. Oceanogr.</i> <u>1966</u> , <i>11</i> , 264-77. 2. Ben-Naim, A.; Baer, S. <i>Trans. Faraday Soc.</i> <u>1963</u> , <i>59</i> , 2735-8. 3. Murray, C.N.; Riley, J.P.; Wilson, T.R.S. <i>Deep-Sea Research</i> <u>1969</u> , <i>16</i> , 297-310.		

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Murray, C. N.; Riley, J. P. <i>Deep-Sea Research</i> <u>1969</u> , 16, 311-20.
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## CRITICAL EVALUATION:

continued

<sup>d</sup> Ostwald coefficient calculated by compiler.<sup>e</sup> Solubility as ml/l from an atmosphere of 20.94% O<sub>2</sub> and 100% relative humidity. These measurements made chemically. See method section.

T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Bunsen Coeff. <sup>c</sup> 10 <sup>2</sup> α	Ostwald Coeff. <sup>d</sup> 10 <sup>2</sup> L	Solubility <sup>e</sup>
279.05	3.374	4.198	4.289	8.71
286.75	2.838	3.528	3.704	7.270
293.30	2.492	3.095	3.323	6.33
298.87	2.269	2.814	3.079	5.711
301.46	2.166	2.685	2.963	5.423

a, b, c, d, e. Footnotes same as for previous table except that these solubilities were determined by physical means. See the methods section.

## REFERENCES:

4. Battino, R.; Evans, F. D.  
*Anal. Chem.* 1966, 38, 1627-9.

COMPONENTS:			ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]			Wise, D.L.; Houghton, L.			
(2) Water; H <sub>2</sub> O; [7732-18-5]			<i>Biochys</i> , J. <u>1969</u> , 9,36-53.			
VARIABLES:			PREPARED BY:			
T/K = 283 - 333			R. Battino			
EXPERIMENTAL VALUES:						
t/°C	T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	10 <sup>2</sup> L <sup>a,c</sup>	10 <sup>2</sup> α <sup>d</sup> / cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	S <sub>o</sub> <sup>e</sup>	
10	283.2	3.00	3.87	3.73	37.3	
20	293.2	2.49	3.32	3.09	30.9	
30	303.2	2.07	2.84	2.56	25.7	
40	313.2	1.87	2.65	2.31	23.3	
50	323.2	1.69	2.46	2.08	21.0	
60	333.2	1.57	2.34	1.92	19.5	
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.</p> <p><sup>c</sup> Ostwald coefficient.</p> <p><sup>d</sup> Bunsen coefficient.</p> <p><sup>e</sup> Solubility in cm<sup>3</sup>(STP)/1000 g of solution. Solubilities fitted to:</p> $\log_{10} S_o = -11.5783 + 1044.40(T/K) + 3.8533 \log_{10}(T/K).$						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:			
Used an adaptation of the Morrison and Billett apparatus (1), but with the gas capacity of the manometer-buret system being about 15 cm <sup>3</sup> . The storage spiral, the absorption spiral and the manometer-buret system were thermostatted in glass jackets through which water from a thermostat circulated.			(1) No details given.			
			(2) Boiled and deionized.			
			ESTIMATED ERROR:			
			δα/α = ±0.01			
			δT/K = ±0.1			
			REFERENCES:			
			1. Morrison, T.J.; Billett, F. <i>J. Chem. Soc.</i> <u>1952</u> , 3919-22.			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Power, G.G.; Stegall, H. <i>J. Appl. Physiol.</i> <u>1970</u> , 29, 145-9.								
<b>VARIABLES:</b> T/K = 310	<b>PREPARED BY:</b> C.L. Young								
<b>EXPERIMENTAL VALUES:</b>									
<table border="1"> <thead> <tr> <th data-bbox="181 501 228 525">T/K</th> <th data-bbox="286 501 615 556">Bunsen coefficient, <math>\alpha / \text{cm}^3 \text{ (STP) cm}^{-3} \text{ atm}^{-1}</math></th> <th data-bbox="623 501 689 525">S.D.<sup>a</sup></th> <th data-bbox="751 501 1027 525">No. of measurements</th> </tr> </thead> <tbody> <tr> <td data-bbox="168 633 255 656">310.15</td> <td data-bbox="386 633 488 656">0.02385</td> <td data-bbox="590 633 692 656">0.00039</td> <td data-bbox="883 633 896 656">4</td> </tr> </tbody> </table>		T/K	Bunsen coefficient, $\alpha / \text{cm}^3 \text{ (STP) cm}^{-3} \text{ atm}^{-1}$	S.D. <sup>a</sup>	No. of measurements	310.15	0.02385	0.00039	4
T/K	Bunsen coefficient, $\alpha / \text{cm}^3 \text{ (STP) cm}^{-3} \text{ atm}^{-1}$	S.D. <sup>a</sup>	No. of measurements						
310.15	0.02385	0.00039	4						
<p>a Standard deviation.</p> <p>b The compiler calculated an Ostwald coefficient of 0.02708 and a mole fraction solubility at 101.325 kPa partial pressure of gas of <math>1.930 \times 10^{-5}</math> from these data.</p>									
<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> 5 to 12 cm <sup>-3</sup> samples placed in a stirrer cell and gas, saturated with water vapor passed through water for 30-60 mins. Samples of saturated liquid withdrawn and transferred to Van Slyke apparatus. Dissolved gas removed under reduced pressure.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Matheson sample, purity better than 99.7 mole per cent. (2) No details given.								
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1$									
<b>REFERENCES:</b>									

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7732-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Novak, D.M.; Conway, B.E. <i>Chem. Instrumentation</i> <u>1974</u> , 5, 79-90.						
<b>VARIABLES:</b> T/K = 298 P/kPa = 101.325	<b>PREPARED BY:</b> R. Battino						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="230 493 989 598" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K<sup>a</sup></th> <th style="text-align: center;">10<sup>5</sup>x<sub>1</sub><sup>b</sup></th> <th style="text-align: center;">10<sup>3</sup>S<sup>c</sup></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">2.295</td> <td style="text-align: center;">1.27</td> </tr> </tbody> </table> <p data-bbox="109 624 855 656"><sup>a</sup> Temperature reported as 25°C but held to ±0.1°C.</p> <p data-bbox="109 671 1105 731"><sup>b</sup> Mole fraction solubility at 101.325 kPa (1atm) partial pressure of gas. Calculated by compiler.</p> <p data-bbox="109 747 708 779"><sup>c</sup> Solubility in units of mol dm<sup>-3</sup> atm<sup>-1</sup>.</p>		T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>3</sup> S <sup>c</sup>	298.15	2.295	1.27
T/K <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10 <sup>3</sup> S <sup>c</sup>					
298.15	2.295	1.27					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Method is based on the evaluation of the Henry's law constant $K_H$ defined by $n_s = K_H P_g$ where $n_s$ is the mass of gas in moles dissolved by unit volume of solvent at the equilibrium gas pressure $P_g$ . The solubilities were obtained by measuring the (total) pressure in the gas phase and the volumes of the liquid and gas phases. This provided sufficient information to calculate the solubility. Measurements were made at different pressures on the same quantity of gas. Equilibrium takes about 12 hr to attain. The apparatus and procedure are described in detail in the paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> <p style="text-align: center;">No details given.</p> <b>ESTIMATED ERROR:</b> $\delta T = \pm 0.1^\circ\text{C}$ $\delta S/S = \pm 0.013$ , estimate by authors <b>REFERENCES:</b>						

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wilcock, R.J.; Battino, R. <i>Nature</i> <u>1974</u>, 252, 614-5.</p>												
<p>VARIABLES:</p> <p>T/K = 298</p>	<p>PREPARED BY:</p> <p>R. Battino</p>												
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="375 456 989 635"> <thead> <tr> <th>T/K</th> <th>10<sup>5</sup>x<sub>1</sub>(O<sub>2</sub>)<sup>a</sup></th> <th>10<sup>5</sup>x<sub>1</sub>(O<sub>2</sub>/N<sub>2</sub>)<sup>b</sup></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>2.261</td> <td>1.775</td> </tr> <tr> <td>298.15</td> <td>2.251</td> <td>1.779</td> </tr> <tr> <td>298.15</td> <td>2.284</td> <td>1.757</td> </tr> </tbody> </table> <p><sup>a</sup> Mole fraction at 101.325 kPa partial pressure of gas.</p> <p><sup>b</sup> Mole fraction, but for a mixture of 49.5 mol per cent oxygen and 50.5 mol per cent nitrogen.</p>		T/K	10 <sup>5</sup> x <sub>1</sub> (O <sub>2</sub> ) <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> (O <sub>2</sub> /N <sub>2</sub> ) <sup>b</sup>	298.15	2.261	1.775	298.15	2.251	1.779	298.15	2.284	1.757
T/K	10 <sup>5</sup> x <sub>1</sub> (O <sub>2</sub> ) <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> (O <sub>2</sub> /N <sub>2</sub> ) <sup>b</sup>											
298.15	2.261	1.775											
298.15	2.251	1.779											
298.15	2.284	1.757											
<p>AUXILIARY INFORMATION</p>													
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Degassed liquid is flowed slowly through an absorption spiral containing the gas. As the gas dissolves the uptake is determined on burets. Measurements are made at constant pressure. Details are given in reference (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Distilled.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta x_1/x_1 = \pm 0.01</math>, compiler's estimate. <math>\delta T/K = \pm 0.05</math>, compiler's estimate.</p> <p>REFERENCES:</p> <p>1. Battino, R.; Evans, F.D.; Danforth, W.F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u>, 45, 830.</p>												



COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Benson, B. B.; Krause, D. Jr. J. Chem. Phys. <u>1976</u> , 64, 689-709.		
VARIABLES:		PREPARED BY:		
T/K - 274-308		R. Battino		
EXPERIMENTAL VALUES:				
t/°C	T <sup>a</sup> /K	10 <sup>5</sup> x <sub>1</sub> <sup>a,b</sup>	β <sup>c</sup> /cm <sup>3</sup> (STP) l <sup>-1</sup> atm <sup>-1</sup>	10 <sup>-4</sup> k <sup>d</sup> /atm
0.484	273.634	3.9008	48.442	2.5636
1.979	275.129	3.7442	46.503	2.6708
2.973	276.123	3.6450	45.271	2.7435
4.947	278.097	3.4632	43.013	2.8875
5.967	279.117	3.3760	41.929	2.9621
7.958	281.108	3.2166	39.946	3.1089
9.954	283.104	3.0705	38.127	3.2568
11.994	285.144	2.9345	36.432	3.4077
12.969	286.119	2.8713	35.644	3.4827
13.979	287.129	2.8110	34.891	3.5574
14.963	288.113	2.7538	34.175	3.6314
16.983	290.133	2.6445	32.809	3.7814
17.959	291.109	2.5961	32.202	3.8520
19.937	293.087	2.4999	30.999	4.0002
21.967	295.117	2.4093	29.863	4.1505
22.952	296.102	2.3688	29.354	4.2216
26.949	300.099	2.2166	27.441	4.5114
28.945	302.095	2.1496	26.596	4.6521
29.948	303.098	2.1175	26.192	4.7225
32.965	306.115	2.0289	25.073	4.9288
34.953	308.103	1.9767	24.412	5.0589
continued on following page				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
Gas-free water and the pure gas are equilibrated and volumetric samples of the liquid and gaseous phases are isolated. The gas dissolved in the water is extracted, and the number of moles determined in a special manometer. After removal of the water vapor, the number of moles in the sample of the gaseous phase is measured with the same manometer, from which the pressure (and fugacity) above the solution may be calculated. Pressures of 0.8 to 0.9 atm are used. Real gas corrections were applied.		No details given.		
		ESTIMATED ERROR:		
		δk/k = ±0.024, author's estimate.		
		REFERENCES:		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Benson, B. B.; Krause, D. Jr. <i>J. Chem. Phys.</i> <u>1976</u> , 64, 689-709.
--	--

continued

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.

<sup>c</sup> Bunsen coefficient, but per liter of solution.

<sup>d</sup> Henry's law constant in units of atmospheres. Authors give the following least squares fit with a standard deviation of ±0.024% in k:

$$\ln(1/(k/\text{atm})) = -4.0605 - 5.4167 \times 10^3/(T/K) + 10.261 \times 10^5/(T/K)^2$$

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]		Zander, R.; Euler, R. Measurement of Oxygen. [Proceedings of an Interdisciplinary Symposium Held at Odense University, Denmark, 26-27 September 1974]. Degn, H.; Balslev, I.; Brook, R.; Editors (Elsevier: Amsterdam Meth.). 1976, p. 271-6. Chem. Abstr. 1976, 85, 43420j.	
VARIABLES:		PREPARED BY:	
T/K: 310.2		R. Battino	
EXPERIMENTAL VALUES:			
Apparatus	Soly. Coeff./(ml/ml atm)	L	10 <sup>4</sup> x <sub>1</sub>
1	0.02407	0.02733	0.1715
2	0.02406	0.02732	0.1714
3	0.02418	0.02746	0.1723
<p>Three different versions of the apparatus were used.</p> <p>Measurements were at 37.0° (310.2 K).</p> <p>Solubility coefficient is the Bunsen coefficient.</p> <p>The Ostwald coefficient, L, and the mole fraction solubility, x<sub>1</sub>, at 101.325 kPa partial pressure of gas were calculated by the compiler.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
The van Slyke (1) apparatus was used with a correction for the unextracted gas applied.		No details given.	
		ESTIMATED ERROR:	
		$\delta T/K = \pm 0.1$ $\pm 1\%$ in solubility (authors)	
		REFERENCES:	
		1. Van Slyke, D.D.; Neill J.M. <i>J. Biol. Chem.</i> 1924, 61, 523.	

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (also <sup>18</sup> O solubility ratios)		Benson, B.B.; Krause, D.; Peterson, M.A.			
(2) Water; H <sub>2</sub> O; [7732-18-5]		J. Soln. Chem. <u>1979</u> , 8, 655-90.			
VARIABLES:		PREPARED BY:			
T/K = 273 - 333		R. Battino			
EXPERIMENTAL VALUES:					
t/°C	T <sup>a</sup> /K	P <sub>t</sub> <sup>b</sup> /atm	10 <sup>-4</sup> k <sup>c</sup> /atm	10 <sup>3</sup> δ <sup>d</sup> <sub>34/32</sub>	10 <sup>5</sup> x <sub>1</sub> <sup>a,e</sup>
0.046	273.196	0.8060	2.52918	0.820	3.95385
0.052	273.202	0.8067	2.52951	0.838	3.95333
1.001	274.151	0.8014	2.59725	0.810	3.85023
1.002	274.152	0.8060	2.59804	0.826	3.84906
1.998	275.148	0.8117	2.66885	0.816	3.74693
2.000	275.150	0.8111	2.66870	0.809	3.74714
3.003	276.153	0.8139	2.74085	0.820	3.64850
4.003	277.153	0.8243	2.81350	0.859	3.55429
4.997	278.147	0.8178	2.88571	0.787	3.46535
6.006	279.156	0.8307	2.95904	0.821	3.37947
7.000	280.150	0.8323	3.03224	0.795	3.29789
8.000	281.150	0.8365	3.10529	0.781	3.22031
10.001	283.151	0.8446	3.25195	0.812	3.07508
12.000	285.150	0.8501	3.40016	0.749	2.94104
13.999	287.149	0.8618	3.54772	-	2.81871
15.002	288.152	0.8744	3.62152	0.747	2.76127
16.003	289.153	0.8687	3.69497	0.774	2.70638
20.003	293.153	0.8871	3.98719	0.744	2.50803
21.998	295.148	0.8863	4.13213	0.688	2.42006
24.001	297.151	0.9135	4.27400	0.738	2.33973
24.002	297.152	0.9118	4.27381	0.718	2.33983
26.999	300.149	0.9254	4.48577	0.668	2.22927
30.001	303.151	0.9459	4.69496	0.682	2.12994
30.004	303.154	0.9361	4.69358	0.674	2.13057
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
The equilibrator is composed of concentric spheres of 1 and 2 dm <sup>3</sup> capacity. A liquid phase sample bulb and a gas phase sample bulb are calibrated as to volume. Degassed liquid is pumped through the center of the inner sphere and flows in a gentle film through the gas. After equilibrium is attained (up to 48 hr), the gas in both bulbs is extracted separately and the pressure, volume, and temperature determined in the dry state. Real gas corrections are applied. Details and drawings are given in the paper.			(1) Linde research grade. Total impurity less than 40 ppm.		
			(2) Distilled water redistilled to give a resistivity greater than 1.5 MΩ-cm.		
			ESTIMATED ERROR:		
			δk/k = ±0.00017, authors' estimate.		
			δT/K = ±0.005, authors' estimate.		
			REFERENCES:		

COMPONENTS:			ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (also <sup>18</sup> O solubility ratios)			Benson, B.B.; Krause, D.; Peterson, M.A.		
(2) Water; H <sub>2</sub> O; [7732-18-5]			J. Soln. Chem. <u>1979</u> , <i>8</i> , 655-90.		
CRITICAL EVALUATION:					
t/°C	T <sup>a</sup> /K	P <sub>t</sub> <sup>b</sup> /atm	continued		
			10 <sup>-4</sup> k <sup>c</sup> /atm	10 <sup>3</sup> δ <sup>d</sup> <sub>34/32</sub>	10 <sup>5</sup> x <sub>1</sub> <sup>a,e</sup>
33.003	306.153	0.9538	4.89287	0.655	2.04379
36.003	309.153	0.9775	5.08821	0.636	1.96533
38.998	312.148	0.9928	5.27426	0.633	1.89600
42.000	315.150	1.0170	5.45555	0.631	1.83300
44.998	318.148	1.0466	5.62631	0.625	1.77736
47.996	321.146	1.0720	5.78804	0.602	1.72770
48.000	321.150	1.0681	5.78712	0.606	1.72798
50.999	324.149	1.0925	5.94146	0.591	1.68309
53.991	327.141	1.1284	6.08549	0.561	1.64325
57.000	330.150	1.1617	6.22147	-	1.60734
57.001	330.151	1.1573	6.22310	0.568	1.60692
59.993	333.143	1.1959	6.34915	0.553	1.57501
59.998	333.148	1.1831	6.34642	0.545	1.57569
<p>a Calculated by compiler.</p> <p>b Total pressure, i.e., gas partial pressure plus saturation vapor pressure of solvent.</p> <p>c Henry's law constant; f<sub>1</sub> = kx<sub>1</sub>; units of atm/mole fraction (1 atm = 101.325kPa).</p> <p>d δ = α-1, where δ = <sup>32</sup>k/<sup>34</sup>k, or the ratio of the Henry's constants for <sup>16</sup>O<sub>2</sub> to <sup>18</sup>O<sub>2</sub> solubilities.</p> <p>e Mole fraction solubility at 101.325kPa partial pressure of gas.</p>					
T/K	ΔG°/cal mol <sup>-1</sup>	ΔH°/cal mol <sup>-1</sup>	ΔS°/cal mol <sup>-1</sup> K <sup>-1</sup>	ΔC <sub>p</sub> °/cal mol <sup>-1</sup> K <sup>-1</sup>	
283.15	5846.0	-3613	-33.41	52.03	
298.15	6327.4	-2872	-30.85	46.93	
313.15	6773.3	-2201	-28.66	42.54	
328.15	7188.7	-1592	-26.76	38.74	
<p>Authors' recommended smoothing equations are:</p> <p>1. <math>\ln(k/\text{atm}) = 3.71814 + 5.59617 \times 10^3 / (T/K) - 1.049668 \times 10^6 / (T/K)^2</math>, 273-373 K.</p> <p>2. <math>\ln(k/\text{atm}) = -4.1741 + 1.3104 \times 10^4 / (T/K) - 3.4170 \times 10^6 / (T/K)^2</math> + <math>2.4749 \times 10^8 / (T/K)^3</math>; above 373 K.</p> <p>3. <math>\ln(^{34}\text{k}/\text{atm}) = 3.71937 + 5595.45 / (T/K) - 1.049624 \times 10^6 / (T/K)^2</math>.</p>					

## COMPONENTS:

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Seawater

## EVALUATOR:

Chen-Tung A. Chen  
 School of Oceanography  
 Oregon State University  
 Corvallis, OR 97331  
 U.S.A.

## CRITICAL EVALUATION:

Many studies have been made of oxygen solubility in seawater (1-16). Unfortunately, among the early measurements (1-8) there exist serious discrepancies of as much as 4 per cent. These data often cover narrow salinity and temperature ranges, are less precise, and are sometimes subject to large systematic errors caused mainly by the loss of iodine and by the addition of oxygen from reagents (9-16). As a result, these early measurements will not be analyzed.

More recently, Carpenter (11) has made extremely careful measurements of oxygen solubility in pure water and seawater using the Winkler titration method. Subsequently, Green (10, 13) and Murray and Riley (16) also published oxygen solubility data in pure water and seawater using a similar method. The data of Carpenter and of Murray and Riley agree closely, the average difference being less than 0.01 ml/l. Green's data are of good quality but are approximately 0.1 ml/l higher than those of Carpenter and Murray and Riley in the low temperature range. Because of the excellent agreement between these two sets of data and a possible systematic error in Green's measurements (11), his data are listed in this study for comparison purposes only and are excluded from further analysis. Murray and Riley (16) also measured oxygen solubility in pure and saline waters using gasometric method. However, they neglected to correct their gasometric data for the gas dissolution effect on the volume of the aqueous phase (17). Because of this and because there are few gasometric data, these values are not included in the analysis, although they are listed in this study.

The determined values of oxygen solubility of Carpenter (11) and Murray and Riley (16) are all reported as the volume of oxygen per unit volume of water (ml/l). However, the methods of smoothing and representing the results are quite different. The results are also difficult to use because they have been tabulated, but not reported, in the form of equations. Weiss recognized this problem (17) and suggested the use of the following equation to represent the gas solubility data:

$$\ln C = A_1 + A_2(100/(T/K)) + A_3 \ln(T/100K) + A_4(T/100K) + S[B_1 + B_2(T/100K) + B_3(T/100K)^2] \dots \quad (1)$$

where C may be either the solubility in ml (STP)/l or in ml (STP)/kg from water saturated air at a total pressure of one atmosphere, T is the Kelvin temperature, the A's and B's are constants, and S is the salinity in parts per thousand.

The first four terms of eq. (1) are obtained from the integrated form of the Van't Hoff equation (18). The salinity dependence is obtained from the commonly used Setchenow relation although the choice of ST and ST<sup>2</sup> terms seems to be somewhat arbitrary. Further, the S<sup>2</sup> term is not included although Carpenter found that it was needed (11).

Chen and Carpenter (19) have since re-analyzed the data of Carpenter (11) and Murray and Riley (16). The analyses were performed by first using these two sets of data separately and then combined. It was found in all three cases that the ST<sup>2</sup> term is not significant statistically and the precision of the fit improves by approximately 10 per cent after discarding the ST<sup>2</sup> term and replacing the ST term by S/T. The ST term was found to be insignificant while the S<sup>2</sup> term is, when the S/T term is included. This confirms the finding of Carpenter. It was also found that the 1/T<sup>2</sup> term is not significant for the gas solubility in pure water, contrary to the finding of Benson and Krause (20, 21). The final equation generated from the combined data sets of Carpenter and Murray and Riley is:

continued on following page

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Seawater	EVALUATOR: Chen-Tung A. Chen School of Oceanography Oregon State University Corvallis, OR 97331 U.S.A.
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## CRITICAL EVALUATION:

continued

$$\ln C = -1268.9782 + 36063.19/(T/K) + 220.1832 \ln (T/K) - 0.351299 (T/K) + S(6.229 \times 10^{-3} - 3.5912/(T/K)) + 3.44 \times 10^{-6} S^2 \quad (2)$$

where C is the solubility in ml/l at STP. The standard deviation of eq. (2) is  $\pm 0.012$  ml/l.

Since the analytical precision of the oxygen determination has improved over the last few years, the concentrations of oxygen in the oceans are more and more frequently reported as ml or  $\mu\text{mol}$  per unit mass of seawater. To avoid the tedious work of computing the densities of seawater in order to change the units in routine use, we have also fit the data in the form of ml/kg and  $\mu\text{mol/kg}$  (17, 21, 22). The equation presented by Millero, Gonzalez and Ward (23) is used to calculate seawater densities. The best fit equations are as follows:

$$\ln C \text{ (ml/kg)} = -1286.2408 + 36607.82/(T/K) + 223.0650 \ln (T/K) - 0.354587 (T/K) + S(5.954 \times 10^{-3} - 3.7341/(T/K)) + 3.68 \times 10^{-6} S^2 \pm 0.012 \text{ ml/kg} \quad (3)$$

$$\ln C \text{ (\mu mol/kg)} = -1282.8704 + 36619.96/(T/K) + 223.1396 \ln (T/K) - 0.354707 (T/K) + S(5.957 \times 10^{-3} - 3.7353/(T/K)) + 3.68 \times 10^{-6} S^2 \pm 0.52 \text{ \mu mol/kg} \quad (4)$$

These equations are valid over the range of 9 to 35.5°C and 0 to 40‰ salinity. The factor of 22393 ml/mol was used to convert the volume of oxygen to moles.

The solubility of oxygen in marine brines has recently been investigated by Kinsman, Boardman and Borcsik (24) at 22 and 50°C up to 144 parts per thousand in chlorinity. The precision of the data probably was not much better than 4 per cent.

The effect of pressure upon the solubility of oxygen in seawater up to 102 atm has been measured by Enns, Scholander and Bradstreet (25). They reported that the equilibrium pressure increase was approximately 14 per cent at 100 atm hydrostatic pressure. They predicted that at 1000 atm the equilibrium partial pressure of oxygen would be increased nearly fourfold.

Carey and Gibson (26) measured the activity of dissolved oxygen based on its rate of reaction with the excited singlet state of pyrene-1-butyric acid and reported that it is not changed by hydrostatic pressures up to 1000 atm. They concluded that the partial pressure of dissolved oxygen will have the same relation to concentration at abyssal depths as at the surface. Carey thought it likely that neither of the above two papers gave the whole story on the pressure effect on oxygen solubility (Carey, personal communication, 1976). More recently, Taylor (27) measured the molar oxygen concentration in an artificial seawater medium in equilibrium with a high pressure oxygen-helium atmosphere. He concluded that at a partial pressure of oxygen of 1 atm or less, its concentration in the aqueous phase was adequately described by Henry's Law at total pressures of up to 600 atm. His work on seawater and pure water (28) seems to substantiate the results of Enns, Scholander and Bradstreet (25). Due to the scarcity of the data that are of satisfactory precision, meaningful equations cannot be derived

continued on following page

COMPONENTS:  (1) Oxygen; O <sub>2</sub> [7782-44-7]  (2) Seawater	EVALUATOR:  Chen-Tung A. Chen School of Oceanography Oregon State University Corvallis, OR 97331 U.S.A.
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## CRITICAL EVALUATION:

continued

to represent the oxygen solubility at high salinities and high pressures. More measurements are clearly in order.

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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Seawater (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Enns, T.; Scholander, P. F.; Bradstreet, E. D. <i>J. Phys. Chem.</i> <u>1965</u> , 69, 389-91.			
<b>VARIABLES:</b> T/K = 274-298 P/MPa (hydrostatic) = 0-10		<b>PREPARED BY:</b> Chen-Tung A. Chen			
<b>EXPERIMENTAL VALUES:</b>					
t/°C	T <sup>a</sup> /K	P <sup>b</sup> =0 (0 MPa)	P <sup>b</sup> =34 atm (3.45 MPa)	P <sup>b</sup> = 68 atm (6.89 MPa)	P <sup>b</sup> =102 atm (10.34 MPa)
Distilled Water					
0.5	273.7	682			789
25	298.2	734.5	771	805	839.5
25	298.2	781	819	855	892
25	298.2	359	373	390	410.5
25	298.2	443	464	484	508
Seawater					
25	298.2	737	775	806	842
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Hydrostatic pressure.</p> <p><sup>c</sup> The values in the table are the oxygen equilibrium pressures in units of mm Hg. The table shows the effect of hydrostatic pressure on the oxygen equilibrium pressure.</p>					
AUXILIARY INFORMATION					
<b>METHOD/APPARATUS/PROCEDURE:</b> Water was gas-extracted before the experiment. Oxygen at the desired initial pressure was dissolved in it at controlled temperature. The equilibrium vessel was shaken for 0.5 to 1 hr during the oxygen uptake. The solution was then transferred to a syringe which has a teflon tubing attached to it. Pressure was then measured by a null point measurement of the pressure developed within the teflon tube.			<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given.		
			<b>ESTIMATED ERROR:</b>		
			<b>REFERENCES:</b>		

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Green, E. J.			
(2) Seawater				Ph. D. thesis, Massachusetts Institute of Technology, 1965.			
VARIABLES:				PREPARED BY:			
T/K = 274-308 Salinity				Chen-Tung A. Chen			
EXPERIMENTAL VALUES:							
Chlor- inity	t/°C	T <sup>a</sup> /K	10 <sup>3</sup> α/ cm(STP) cm <sup>-3</sup> atm <sup>-1</sup>	Chlor- inity	t/°C	T <sup>a</sup> /K	10 <sup>3</sup> α/ cm(STP) cm <sup>-3</sup> atm <sup>-1</sup>
			48.633				30.066
			48.598				29.938
			48.669				29.945
0	0.59	273.74	48.661				30.026
			48.665				29.996
			48.618				29.981
			43.118				29.913
			42.890				30.140
			42.932				30.072
0	5.03	278.18	42.920	0	22.02	295.17	30.131
			42.972				30.071
			42.857				30.049
			34.299				30.074
			34.228				30.083
			34.244				29.990
0	15.09	288.24	34.208				30.092
			34.153				30.080
			34.356				30.103
			30.061				30.156
			30.242				30.137
			30.177				30.090
0	22.02	295.17	30.059	0	22.05	295.20	30.126
			30.086				30.061
							30.118
							30.101
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Distilled and seawater were simultaneously saturated with air with two 12-l round bottom long-neck flasks inclined at a 45° angle and arranged to rotate about their axes of symmetry. A thin film of water was drawn over the inside surface of the flask by its rotation. The reagents (MnCl <sub>2</sub> ·4H <sub>2</sub> O, NaI, NaOH, H <sub>2</sub> SO <sub>4</sub> ) were added to the equilibrated water (after at least 8 hours of rotation) and the thiosulfate titration end point determined by the Amperometric technique using a Keithley microammeter. A modified Winkler method was used.							
				ESTIMATED ERROR: δT/K = ±0.01 δCl% < ±0.028% δα/α = ±0.0027			
				REFERENCES: 1. Green, E.J., Ph.D. thesis Massachusetts Institute of Technology, 1965. 2. Green, E.J.; Carritt, D.E., J. Mar. Res. 1967, 25, 140.			

COMPONENTS:				EVALUATOR:			
(1) Oxygen; O <sub>2</sub> ; 7782-44-7				Green, E. J.			
(2) Seawater				Ph.D. thesis, Massachusetts Institute of Technology, 1965.			
CRITICAL EVALUATION:							
continued							
Chlor- inity	t/°C	T <sup>a</sup> /K	10 <sup>3</sup> <sub>α</sub> / cm(STP)cm <sup>-3</sup> atm <sup>-1</sup>	Chlor- inity	t/°C	T <sup>a</sup> /K	10 <sup>3</sup> <sub>α</sub> / cm(STP)cm <sup>-3</sup> atm <sup>-1</sup>
0	24.92	298.07	28.494 28.549 28.730 28.682 28.670 28.661	17.551	15.09	288.24	28.177 28.161 28.206 28.162 28.203 28.067
0	34.81	307.96	24.086 24.129 24.132 24.181 24.085 24.199	17.562	34.81	307.96	20.172 20.197 20.194 20.231 20.200 20.246
6.349	22.02	295.17	28.099 28.139 28.165 28.262	17.632	24.92	298.07	23.652 23.865 23.901 23.905
12.412	22.02	295.17	26.324 26.263 26.214 26.269 26.263 26.245	24.339	22.02	295.20	23.856 23.770 23.323 23.375 23.378 23.391
17.419	5.03	278.18	34.860 34.930 34.890 34.695 34.723 34.821	30.804	22.02	295.20	21.965 21.912 21.874 21.825 21.930 21.855
17.464	0.59	273.74	39.022 39.092 39.051 39.099 39.079 39.132				
17.487	22.02	295.17	24.961 25.108 25.091				

<sup>a</sup> Calculated by compiler.

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Carpenter, J. H.			
(2) Seawater				<i>Limnol. Oceanog.</i> 1966, 11, 264-77.			
VARIABLES:				PREPARED BY:			
T/K = 274-309 Chlorinity				Chen-Tung A. Chen			
EXPERIMENTAL VALUES:							
Chlorinity /‰	t/°C	T <sup>a</sup> /K	S <sup>b</sup> / (ml/liter)	Chlorinity /‰	t/°C	T <sup>a</sup> /K	S <sup>b</sup> / (ml/liter)
	0.48	273.63	10.120		12.38	285.53	7.469
	0.52	273.67	10.088		12.40	285.55	7.476
	0.64	273.79	10.062		12.40	285.55	7.485
	5.02	278.17	8.898		12.41	285.56	7.465
	5.07	275.22	8.903		12.41	285.56	7.473
	5.08	275.23	8.898		12.43	285.58	7.462
	5.10	275.25	8.890		14.55	287.70	7.139
	5.11	275.26	8.875		14.72	287.87	7.116
	5.13	275.28	8.884		14.97	288.12	7.078
0.0	5.18	278.33	8.862	0.0	14.99	288.14	7.079
	5.21	278.36	8.858		15.12	288.27	7.054
	9.85	283.00	7.894		15.14	288.29	7.057
	9.86	283.01	7.897		20.08	293.23	6.340
	9.89	283.04	7.899		20.10	293.25	6.344
	9.94	283.09	7.884		25.10	298.25	5.761
	10.10	283.25	7.863		25.35	298.50	5.734
	10.22	283.37	7.839		25.36	298.51	5.742
	11.68	284.83	7.584		29.80	302.95	5.301
	12.04	285.19	7.531		29.81	302.96	5.308
	12.36	285.51	7.483		34.76	307.91	4.867
	12.37	285.52	7.491		34.82	307.97	4.868
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
The sample was contained in a plexi-glass (perspex) box which was placed on a frame that could be rocked to mix air and liquid. The equilibrated water was transferred to a pyrex bottle and the reagents (MnCl <sub>2</sub> ·4H <sub>2</sub> O, NaI, NaOH, H <sub>2</sub> SO <sub>4</sub> ) added. The resulting solution was then titrated with thiosulfate solution with the iodine endpoint detected by a Beckman DU spectrophotometer at 320 and 350 μm. The method was a modified Winkler method with a weight photometric titration. See references.				(1) From air collected in the country 32 km west of Baltimore, MD. 20.94% oxygen.			
				ESTIMATED ERROR:			
				δT/K = ±0.01 δS/S = ±0.001, author's estimate			
				REFERENCES:			
				(1) Carpenter, J. H. <i>Limnol. Oceanog.</i> 1965, 10, 135.			
				(2) Carpenter, J. H. <i>Limnol. Oceanog.</i> 1966, 11, 264.			
				(3) Carritt, D. E.; Carpenter, J. H. <i>J. Mar. Res.</i> 1966, 24, 286.			

COMPONENTS:				EVALUATOR:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Carpenter, J. H.			
(2) Seawater				<i>Limnol. Oceanog.</i> 1966, 11, 264-77.			
EXPERIMENTAL VALUES:				continued			
Chlorinity /‰	t/°C	T <sup>a</sup> /K	S <sup>b</sup> / (ml/liter)	Chlorinity /‰	t/°C	T <sup>a</sup> /K	S <sup>b</sup> / (ml/liter)
4.99	35.43 35.45 35.45	308.58 308.60 308.60	4.597 4.596 4.597		0.62 0.55 5.39 5.37	273.77 273.70 278.54 278.52	8.331 8.315 7.408 7.401
	20.08 20.09 25.02	293.23 293.24 298.17	6.017 6.017 5.475	15.00	5.37 10.16 10.20 14.10	278.52 283.31 283.35 287.25	7.401 6.618 6.613 5.982
5.07	25.05 30.04 30.09 35.18	298.20 303.19 303.24 308.33	5.475 5.008 4.992 4.592		14.97 20.15 20.11 25.24 25.27	288.12 293.30 293.26 298.39 298.42	5.971 5.396 5.393 4.924 4.922
	0.48 0.49 5.28 5.29	273.63 273.64 278.43 278.44	9.447 9.443 8.335 8.336	15.18	29.99 30.01 35.50 35.50	303.14 303.16 308.65 308.65	4.542 4.542 4.162 4.162
	10.15 10.19 14.94 14.95	283.30 283.34 288.09 288.10	7.398 7.386 6.663 6.654		0.41 0.44 1.09 9.88 35.53 35.58	273.56 273.59 274.24 283.03 308.68 308.73	7.863 7.856 7.729 6.292 3.961 3.963
10.02	35.48 35.56	308.63 308.71	4.363 4.361	20.32			
	0.60 0.64 5.30 5.35	273.75 273.79 278.45 278.50	8.886 8.851 7.883 7.873		20.18 20.18 25.23 25.25	293.33 293.33 298.38 298.40	5.115 5.117 4.688 4.685
10.13	10.17 10.14 15.02	283.32 283.29 288.17	6.994 6.993 6.288	20.37	29.98 29.99 29.99	303.13 303.14 303.14	4.300 4.304 4.304
	20.12 20.14 25.19 25.23	293.27 293.29 298.34 298.38	5.666 5.667 5.154 5.157		5.34 5.34 10.18 10.20	278.49 278.49 283.33 283.35	6.919 6.916 6.196 6.184
10.49	29.97 29.92	303.12 303.07	4.753 4.748	20.88	14.97 15.02	288.12 288.17	5.602 5.590

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Solubilities of oxygen in seawater assuming an oxygen volume of 22,400 ml/mol at STP. Observations were corrected by author to 101.325 kPa total pressure including water vapor and 20.94% oxygen excluding water vapor on the basis of individual gas analyses.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Seawater	<b>ORIGINAL MEASUREMENTS:</b> Murray, C. N.; Riley, J. P. <i>Deep-Sea Research</i> , <u>1969</u> , <i>16</i> , 311-20.																																								
<b>VARIABLES:</b> T/K = 279-301 Salinity	<b>PREPARED BY:</b> Chen-Tung A. Chen																																								
<b>EXPERIMENTAL VALUES:</b> Physically determined values of oxygen solubility in ml/l (from an atmosphere of 20.94% O <sub>2</sub> and 100% relative humidity). <table border="1" data-bbox="125 568 1190 1058"> <thead> <tr> <th>t/°C</th> <th>T<sup>a</sup>/K</th> <th>Salinity/(‰)</th> <th>O<sub>2</sub>/(ml/l)</th> </tr> </thead> <tbody> <tr><td>5.90</td><td>279.05</td><td>0.000</td><td>8.71</td></tr> <tr><td>5.90</td><td>279.05</td><td>32.995</td><td>7.03</td></tr> <tr><td>13.60</td><td>286.75</td><td>0.000</td><td>7.27</td></tr> <tr><td>13.70</td><td>286.85</td><td>31.981</td><td>5.96</td></tr> <tr><td>20.00</td><td>293.15</td><td>36.725</td><td>5.11</td></tr> <tr><td>20.15</td><td>293.30</td><td>0.000</td><td>6.33</td></tr> <tr><td>25.72</td><td>298.87</td><td>0.000</td><td>5.71</td></tr> <tr><td>24.65</td><td>297.80</td><td>34.261</td><td>4.77</td></tr> <tr><td>28.31</td><td>301.46</td><td>0.000</td><td>5.42</td></tr> </tbody> </table> <p><sup>a</sup> Calculated by compiler.</p>		t/°C	T <sup>a</sup> /K	Salinity/(‰)	O <sub>2</sub> /(ml/l)	5.90	279.05	0.000	8.71	5.90	279.05	32.995	7.03	13.60	286.75	0.000	7.27	13.70	286.85	31.981	5.96	20.00	293.15	36.725	5.11	20.15	293.30	0.000	6.33	25.72	298.87	0.000	5.71	24.65	297.80	34.261	4.77	28.31	301.46	0.000	5.42
t/°C	T <sup>a</sup> /K	Salinity/(‰)	O <sub>2</sub> /(ml/l)																																						
5.90	279.05	0.000	8.71																																						
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28.31	301.46	0.000	5.42																																						
<b>AUXILIARY INFORMATION</b>																																									
<b>METHOD/APPARATUS/PROCEDURE:</b> Saturation of samples with oxygen was carried out by stirring at such a rate that a vortex of ~ 3 cm in length was formed. The ratio of the volume of seawater (measured by weight) gives the solubility.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) > 99.9% purity.  <b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.02$ $\delta S \text{‰} = \pm 0.02$ $\delta O_2 = \pm 0.01 \text{ ml/l}$  <b>REFERENCES:</b> 1. Murray, C. N.; Riley, J. P.; Wilson, T. R. S. <i>Deep-Sea Research</i> , <u>1969</u> , <i>16</i> , 297. 2. Murray, C. N.; Riley, J. P. <i>Deep-Sea Research</i> , <u>1969</u> , <i>16</i> , 311.																																								

COMPONENTS:			ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]			Murray, C. N.; Riley, J. P.		
(2) Seawater			Deep-sea Research, <u>1969</u> , 16, 311-20.		
VARIABLES:			PREPARED BY:		
T/K = 274-308 Salinity			Chen-Tung A. Chen.		
EXPERIMENTAL VALUES:					
Chemically determined values of oxygen solubility in ml/l. (from an atmosphere of 20.94% O <sub>2</sub> and 100% relative humidity).					
t/°C (T <sup>a</sup> /K)	Salinity/ (‰)	O <sub>2</sub> / (ml/l)	t/°C (T <sup>a</sup> /K)	Salinity/ (‰)	O <sub>2</sub> / (ml/l)
	0.000	10.021		0.000	7.031
	5.962	9.622		10.090	6.618
0.74	11.418	9.241	15.12	15.084	6.395
(273.89)	19.999	8.743	(288.27)	20.774	6.172
	36.103	7.834		29.102	5.863
	0.000	9.713		0.000	6.360
	7.520	9.249		10.090	5.971
1.80	14.480	8.791	20.00	15.446	4.788
(274.95)	24.459	8.232	(293.15)	28.781	5.362
	29.148	8.022		39.020	5.045
	0.000	8.910		0.000	5.794
	11.577	8.281		8.712	5.464
4.90	17.508	7.959	24.95	12.646	5.348
(278.05)	25.870	7.571	(298.10)	22.169	5.098
	36.989	7.022		33.894	4.765
	0.000	8.382		0.000	5.312
	9.680	7.891		8.682	5.064
7.45	17.663	7.470	29.80	16.690	4.831
(280.60)	25.243	7.140	(302.95)	25.435	4.611
	31.513	6.836		33.626	4.400
	37.882	6.561		39.120	4.254
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Air saturated sample was introduced at the top of a helix (diameter 7 cm; length 360 cm.) at a rate of ≈ 4 ml/min to ensure that the sample was saturated, but not super-saturated. Thiosulfate was used to titrate the solution after the reagents (MnCl <sub>2</sub> ·4H <sub>2</sub> O, NaI, NaOH, H <sub>2</sub> SO <sub>4</sub> ) had been added. The end point was determined photometrically with an EEL Quantitrator fitted with an Ilford 608 filter. Starch was used as the end point indicator. Used a modified Winkler method. See references.			(1) From air.		
			ESTIMATED ERROR:		
			$\delta T/K = \pm 0.02$ $\delta S\% = \pm 0.02\%$ $\delta O_2/(ml/l) = \pm 0.01$		
			REFERENCES:		
			1. Murry, C. N.; Riley, J. P.; Wilson, T. R. S. <i>Deep-Sea Research</i> , <u>1968</u> , 15, 237.		
			2. Murry, C. N.; Riley, J. P. <i>Deep-Sea Research</i> <u>1969</u> , 16, 311.		

COMPONENTS:			EVALUATOR:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]			Murray, C. N.; Riley, J. P.		
(2) Seawater			Deep-Sea Research, <u>1969</u> , 16, 311-20.		
EXPERIMENTAL VALUES:					
continued					
t/°C (T <sup>a</sup> /K)	Salinity/ (‰)	O <sub>2</sub> (ml/l)	t/°C (T <sup>a</sup> /K)	Salinity (‰)	O <sub>2</sub> / (ml/l)
	0.000	7.887		0.000	4.862
	10.566	7.364		8.569	4.641
9.95	17.508	7.045	34.80	14.019	4.528
(283.10)	23.355	6.775	(307.95)	23.651	4.293
	31.935	6.445		34.205	4.067
	40.201	6.110			



COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [ 7782-44-7 ]				Kinsman, D.J.J.; Boardman, M.;			
(2) Artificial Seawater				Borcsik, M.			
				Symposium. Salt. 4th, 1973 (pub. 1973), 1, 325-7.			
VARIABLES:				PREPARED BY:			
T/K = 293-323				Chen-Tung A. Chen			
Chlorinity							
EXPERIMENTAL VALUES:							
t/°C	T <sup>a</sup> /K	Cl/‰	O <sub>2</sub> <sup>b</sup> (mg/kg water)	t/°C	T <sup>a</sup> /K	Cl/‰	O <sub>2</sub> <sup>b</sup> (mg/kg water)
22.5	295.7	18.57	7.15	23.0	296.2	122.51	2.63
23.0	296.2	18.59	7.28	22.5	295.7	122.53	2.60
23.75	296.9	18.76	6.91	23.75	296.9	123.6	2.63
22.0	295.2	18.81	6.83	21.0	294.2	128.19	2.40
21.0	294.2	20.45	7.01	22.0	295.2	128.84	2.48
22.0	295.2	20.60	7.12				
23.0	296.2	37.88	6.06				
22.5	295.7	38.16	5.78				
22.0	295.2	38.31	5.67				
23.75	296.9	38.54	5.69				
21.0	294.2	41.24	5.71				
22.0	295.2	41.54	5.85				
23.0	296.2	59.60	4.69				
22.5	295.7	60.14	4.65				
22.0	295.2	60.27	4.57				
23.75	296.9	61.23	4.57				
21.0	294.2	64.35	4.48				
22.0	295.2	64.63	4.56				
23.0	296.2	98.31	3.36				
22.0	295.2	98.48	3.60				
22.5	295.7	98.53	3.33				
23.75	296.9	99.04	3.31				
21.0	294.2	104.60	3.10				
22.0	295.2	105.54	3.17				
22.0	295.2	121.69	2.58				
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Standard Winkler Method.				Oxygen: air			
				Marine brines: unspecified			
				ESTIMATED ERROR:			
				δT = 2°C			
				δO <sub>2</sub> < 4%			
				REFERENCES:			
				1. Kinsman, D. J. <i>Private communication, 1981.</i>			

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Artificial Seawater	EVALUATOR: Kinsman, D.J.J.; Boardman, M.; Borcsik, M. <i>Symp. Salt. 4th, 1973</i> (pub. 1973), 1, 325-7.
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CRITICAL EVALUATION: continued

Cl/‰	O <sub>2</sub> <sup>b</sup> (mg/kg <sup>b</sup> water)	Cl/‰	O <sub>2</sub> <sup>b</sup> (mg/kg <sup>b</sup> water)
t/°C = 50 (323K)			
18.20	5.03	96.08	2.63
18.90	4.94	97.04	2.61
20.25	4.98	104.14	2.55
20.74	4.90	104.80	2.55
24.29	4.78	111.47	2.48
25.80	4.73	118.34	2.34
27.85	4.63	119.96	2.27
38.43	4.22	121.45	2.08
39.67	4.20	127.85	2.14
41.14	4.18	128.67	2.09
41.21	4.196	137.13	1.88
51.85	3.80	140.79	1.89
54.89	3.73	144.35	1.79
58.52	3.59		
63.65	3.40		
64.45	3.32		
74.78	3.43		
65.69	3.35		
81.51	2.99		
84.13	2.88		
90.23	2.85		

<sup>a</sup> Calculated by compiler.

<sup>b</sup> The oxygen partial pressure was 0.2 atm.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Seawater	<b>ORIGINAL MEASUREMENTS:</b> Taylor, C. D. <i>Undersea Biomed. Res.</i> 1979, 6, 147-54.																																																
<b>VARIABLES:</b> T/K = 293 P/MPa (Hydrostatic) = 1-61	<b>PREPARED BY:</b> Chen-Tung A. Chen, R. Battino																																																
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">Oxygen Partial Pressure/atm</th> <th style="text-align: left;">Hydrostatic Pressure/atm</th> <th style="text-align: right;">O<sub>2</sub>/ (<math>\mu</math>mole/liter)</th> </tr> </thead> <tbody> <tr> <td>0.036 (3.6 kPa)<sup>b</sup></td> <td>80 (8.1 MPa)<sup>c</sup></td> <td style="text-align: right;">40</td> </tr> <tr> <td>0.036 (3.6 kPa)</td> <td>160 (16.2 MPa)</td> <td style="text-align: right;">60</td> </tr> <tr> <td>0.036 (3.6 kPa)</td> <td>580 (58.8 MPa)</td> <td style="text-align: right;">180</td> </tr> <tr> <td>0.065 (6.6 kPa)</td> <td>200 (20.3 MPa)</td> <td style="text-align: right;">170</td> </tr> <tr> <td>0.065 (6.6 kPa)</td> <td>400 (40.5 MPa)</td> <td style="text-align: right;">260</td> </tr> <tr> <td>0.065 (6.6 kPa)</td> <td>600 (60.8 MPa)</td> <td style="text-align: right;">420</td> </tr> <tr> <td>0.094 (9.5 kPa)</td> <td>200 (20.3 MPa)</td> <td style="text-align: right;">220</td> </tr> <tr> <td>0.094 (9.5 kPa)</td> <td>400 (40.5 MPa)</td> <td style="text-align: right;">380</td> </tr> <tr> <td>0.094 (9.5 kPa)</td> <td>570 (57.8 MPa)</td> <td style="text-align: right;">580</td> </tr> <tr> <td>0.12 (12 kPa)</td> <td>200 (20.3 MPa)</td> <td style="text-align: right;">250</td> </tr> <tr> <td>0.12 (12 kPa)</td> <td>440 (44.6 MPa)</td> <td style="text-align: right;">560</td> </tr> <tr> <td>0.12 (12 kPa)</td> <td>600 (60.8 MPa)</td> <td style="text-align: right;">740</td> </tr> <tr> <td>0.15 (15 kPa)</td> <td>100 (10.1 MPa)</td> <td style="text-align: right;">180</td> </tr> <tr> <td>0.15 (15 kPa)</td> <td>200 (20.3 MPa)</td> <td style="text-align: right;">320</td> </tr> <tr> <td>0.15 (15 kPa)</td> <td>300 (30.4 MPa)</td> <td style="text-align: right;">460</td> </tr> </tbody> </table> <p><sup>a</sup> Oxygen solubility values at 20°C (293K) estimated from Figure 3 given in the paper. Data were presented as average of duplicate analyses.</p> <p><sup>b</sup> Calculated in kPa by compiler.</p> <p><sup>c</sup> Calculated in MPa by compiler.</p> <p style="text-align: right;">continued on following page</p>		Oxygen Partial Pressure/atm	Hydrostatic Pressure/atm	O <sub>2</sub> / ( $\mu$ mole/liter)	0.036 (3.6 kPa) <sup>b</sup>	80 (8.1 MPa) <sup>c</sup>	40	0.036 (3.6 kPa)	160 (16.2 MPa)	60	0.036 (3.6 kPa)	580 (58.8 MPa)	180	0.065 (6.6 kPa)	200 (20.3 MPa)	170	0.065 (6.6 kPa)	400 (40.5 MPa)	260	0.065 (6.6 kPa)	600 (60.8 MPa)	420	0.094 (9.5 kPa)	200 (20.3 MPa)	220	0.094 (9.5 kPa)	400 (40.5 MPa)	380	0.094 (9.5 kPa)	570 (57.8 MPa)	580	0.12 (12 kPa)	200 (20.3 MPa)	250	0.12 (12 kPa)	440 (44.6 MPa)	560	0.12 (12 kPa)	600 (60.8 MPa)	740	0.15 (15 kPa)	100 (10.1 MPa)	180	0.15 (15 kPa)	200 (20.3 MPa)	320	0.15 (15 kPa)	300 (30.4 MPa)	460
Oxygen Partial Pressure/atm	Hydrostatic Pressure/atm	O <sub>2</sub> / ( $\mu$ mole/liter)																																															
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<b>AUXILIARY INFORMATION</b>																																																	
<b>METHOD/APPARATUS/PROCEDURE:</b> Air-equilibrated artificial seawater was contained in a polycarbonate vessel housed in a stainless steel pressure cylinder. Oxygen-helium mixture was used in flushing gas and the partial pressure of it was monitored by a membrane-covered oxygen polarographic electrode. Flushing was continued until the partial O <sub>2</sub> pressure remained constant for at least 5 minutes, then the aqueous and gaseous phases were allowed to equilibrate with stirring at 20°C for at least two hours prior to analysis by the Winkler method using undecompressed subsamples. Details also given in reference 1.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Union Carbide, 99.5% purity (2) Artificial seawater: 4% Seven Seas Marine Mix; 0.1% Tris-base; 0.05% ammonium sulfate; pH 7.2-7.4. <b>ESTIMATED ERROR:</b> $\delta O_2 < 12\%$ , author's estimate <b>REFERENCES:</b> 1. Taylor, C.D. <i>Appl. Environ. Microbiol.</i> 1979, 37, 42-9.																																																

## COMPONENTS:

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Seawater

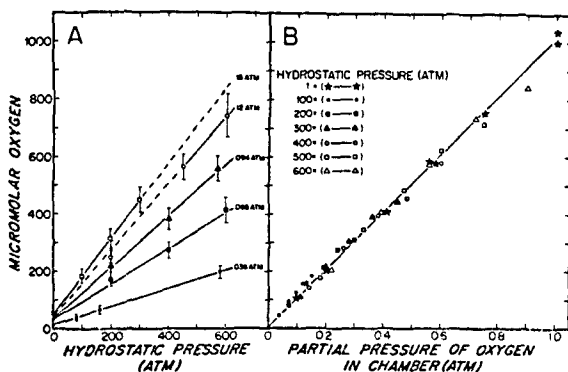
## EVALUATOR:

Taylor, C. D.

*Undersea Biomed. Res.* 1979, 6,  
 147-54.

## CRITICAL EVALUATION:

continued



Data presented only in graphical form. Solubilities determined at 20°C (293K). The solubility is given in micromoles of oxygen per liter of seawater. In A the oxygen partial pressure is given for each line. The error bars are estimated from duplicate analyses. The starred data points in B were obtained from separate experiments conducted in bottles. Oxygen partial pressures were determined using a membrane-covered oxygen polarographic electrode.

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Electrolyte(s)</p> <p>(3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>EVALUATOR:</p> <p>H. L. Clever          Department of Chemistry          Emory University          Atlanta, GA 30322 USA</p> <p>1981, April</p>
<p>CRITICAL EVALUATION:</p> <p style="text-align: center;">An Evaluation of the Solubility of Oxygen in Aqueous Electrolyte Solutions.</p> <p>Not enough workers have measured the solubility of oxygen in any one aqueous electrolyte system over common ranges of concentration and temperature to recommend solubility values. Most of the available data are classed as tentative.</p> <p>In order to have a common basis for comparison, where possible the solubility data have been converted to Setschenow salt effect parameters at an oxygen partial pressure of 101.325 kPa in the form</p> $k_{sc\alpha}/\text{dm}^3 \text{ mol}^{-1} = (1/(c_2/\text{mol dm}^{-3})) \log(\alpha^\circ/\alpha)$ <p>where <math>c_2</math> is the electrolyte concentration in mol dm<sup>-3</sup>, and <math>\alpha^\circ</math> and <math>\alpha</math> are the Bunsen coefficients in pure water and electrolyte solution, respectively. The Ostwald coefficient ratio, <math>L^\circ/L</math>, will give the same value, but the salt effect parameter is symbolized, <math>k_{scL}</math>. Both ratios are equivalent to a molar gas solubility ratio, <math>c_1^\circ/c_1</math>, thus</p> $k_{sc\alpha} = k_{scL} = k_{scc} = (1/(c_2/\text{mol dm}^{-3})) \log (c_1^\circ/\text{sat}/c_1/\text{sat})$ <p>Other forms of the salt effect parameter will be found on the data sheets that follow this discussion. They include</p> $k_{sms}/\text{kg mol}^{-1} = (1/(m_2/\text{mol kg}^{-1})) \log(s^\circ/s)$ $k_{scx}/\text{dm}^3 \text{ mol}^{-1} = (1/(c_2/\text{mol dm}^{-3})) \log(x^\circ/x)$ $k_{smx}/\text{kg mol}^{-1} = (1/(m_2/\text{mol kg}^{-1})) \log(x^\circ/x)$ <p>where <math>m_2</math> is the electrolyte molality, <math>s^\circ/s</math> is the Kuenen coefficient ratio, and <math>x^\circ/x</math> is the mole fraction gas solubility ratio usually calculated with respect to all ions in the solution. The Kuenen coefficient, <math>s</math>, is referenced to 1 g of water whether it is for pure water or the electrolyte solution. Thus the <math>s^\circ/s</math> ratio is equal to a gas molality ratio <math>m_1^\circ/m_1</math>.</p> <p>The density data required to convert the salt effect parameter from one form to another were taken from the <i>International Critical Tables</i>, McGraw-Hill Co., Inc., 1928, Vol. III.</p> <p>The activity coefficient of the dissolved oxygen, <math>y_1</math>, is a function of the concentration of all solute species, which in the present systems are the electrolyte and the nonelectrolyte. At a given temperature <math>\log y_1</math> can be represented as a power series in <math>c_1</math> and <math>c_2</math></p> $\log y_1 = \sum_{nm} k_{nm} c_1^n c_2^m$ <p>If it is assumed that for low concentrations of both nonelectrolyte, <math>c_1</math>, and electrolyte, <math>c_2</math>, the only important terms are the linear ones,</p> $\log y_1 = k_1 c_1 + k_2 c_2$ <p>The expression has been experimentally verified for moderately dilute solutions in which there is no chemical interaction between the solute species.</p>	

The measurements of the nonelectrolyte solubility in pure water,  $c_{1,\text{sat}}^{\circ}$ , and in a salt solution,  $c_{1,\text{sat}}$ , give directly the activity coefficient of the nonelectrolyte. Long and McDevit (7) show that

$$\log(y_1/y_1^{\circ}) = \log(c_{1,\text{sat}}^{\circ}/c_{1,\text{sat}}) = k_1(c_{1,\text{sat}} - c_{1,\text{sat}}^{\circ}) + k_2 c_2$$

And if the nonelectrolyte solubility values are low, as they generally are for a gas, the term in  $k_1$  can be neglected, even though  $k_1$  is similar in magnitude to  $k_2$ . Thus for low nonelectrolyte concentration

$$\log(y_1/y_1^{\circ}) = \log(c_{1,\text{sat}}^{\circ}/c_{1,\text{sat}}) = k_2 c_2$$

The solubility data which are evaluated in this section do not always meet the requirements set forth above. Thus, the experimental Setschenow salt effect parameters,  $k_s$ , may not be equivalent to the theoretically important salt effect parameter,  $k_2$ .

A plot of  $\log(\alpha^{\circ}/\alpha)$  vs.  $c_2$  is usually linear over moderate concentrations of the electrolyte. However, curvature of the plot is often seen at above moderate concentrations, and in extreme cases one observes regions of both salting-out and salting-in over different concentration regions of the same isotherm, e.g.  $\text{O}_2 + \text{HNO}_3 + \text{H}_2\text{O}$  at 333 K.

The salt effect parameters,  $k_{\text{sca}}/\text{dm}^3 \text{ mol}^{-1}$ , are presented by several methods in the evaluation.

In the first method  $k_{\text{sca}}$  values are calculated for each experimental determination, and a graph is prepared of  $k_{\text{sca}}$  vs.  $c_2$ . If the plot is linear and of zero slope,  $k_{\text{sca}}$  is taken to be independent of concentration. In such cases an average value of  $k_{\text{sca}}$  is given. If the plot is linear, but of non-zero slope,  $k_{\text{sca}}$  is fitted to a linear equation in  $c_2$ .

In the second method a graph is prepared of  $\log(\alpha^{\circ}/\alpha)$  vs.  $c_2$ . A linear plot shows no concentration dependence of the salt effect parameter and the slope is  $k_{\text{sca}}$ . Recently Yasunischi (33,34) has fitted such plots that show curvature to a function

$$\log(\alpha^{\circ}/\alpha) = k_{\text{sca}}^{\circ} c_2 / (1 + k'_{\text{sca}} c_2)$$

In a sense the first method, in which the salt effect parameter is given by a linear function of concentration,  $k_{\text{sca}} = a + bc_2$ , is equivalent to

$$\log(\alpha^{\circ}/\alpha) = (a + bc_2)c_2 = ac_2 + bc_2^2$$

however, the constants should be redetermined from the  $\log(\alpha^{\circ}/\alpha)$  and  $c_2$  data.

Salt effects on the solubility of oxygen have been studied at both large partial pressures of oxygen and at atmospheric pressure. In general  $k_{\text{sca}}$  values are calculated for only the atmospheric pressure measurements. An exception are the data of Bruhn, Gerlach, and Pawlek (17) who gave  $\alpha/\alpha^{\circ}$  ratio's for their measurements at high pressure.

The use of a salt effect parameter of the Setschenow type should not be taken to mean that it is necessarily the best way to represent the salt effect data. It is used here as a convenient parameter in the comparison of data from several sources.

The solubility of oxygen in water was usually taken from the paper under evaluation for the calculation of the salt effect parameter. The reason for using the water solubility value of the author, rather than the recommended value from this volume, is that systematic errors in a given author's work may cancel in the  $\alpha^{\circ}/\alpha$  ratio.

Studies of the solubility of oxygen in aqueous electrolyte solutions appear in over 30 papers. The seven papers which report salt effect data on oxygen solubility in four or more electrolyte solutions are discussed below. The papers which report data on only one or two systems are discussed with the system.

Geffcken (1) measured the solubility of oxygen in aqueous solutions of HCl, H<sub>2</sub>SO<sub>4</sub>, HNO<sub>3</sub>, NaOH, NaCl, KOH, and K<sub>2</sub>SO<sub>4</sub> at several concentrations up to about 2 mol dm<sup>-3</sup>. His average values of the Ostwald coefficient of oxygen in water of 0.03630 at 288.15 K and 0.03080 at 298.15 K were used to calculate the  $k_{scL}$  values from his data. The  $k_{scL}$  values from his work usually show a small decrease in magnitude as the electrolyte concentration increases. In general Geffcken's measurement compare well with more modern measurements, and they are classed as tentative.

MacArthur (4) measured the solubility of atmospheric oxygen in fifteen aqueous electrolytes. He analyzed 250 cm<sup>3</sup> samples of air saturated solution for oxygen by a modified Winkler procedure. The salt effect parameters calculated from his data are equivalent to  $k_{scL}$  or  $k_{sca}$  values. The solubility values may be in error by as much as 10 per cent. Some of the aqueous electrolyte density values appear to be in error. The salt effect parameters show more than average scatter as a function of electrolyte concentration. In spite of the defects, some of the salt effect values compare well with more modern measurements. The data are classed as doubtful or tentative depending on the system.

Eucken and Hertzberg (6) measured the Ostwald coefficient of the solubility of oxygen in aqueous solutions of MgCl<sub>2</sub>, LiCl, NaCl, and KCl at several temperatures and two or three electrolyte concentrations up to about 2.5 mol kg<sup>-1</sup>. Some doubt was cast on their work because of the poor agreement of their argon solubility values at 273.15 K with other workers values. However, the oxygen data appears reliable, and they are classed as tentative.

Bruhn, Gerlach and Pawlek (17) measured the solubility of oxygen in aqueous solutions of H<sub>2</sub>SO<sub>4</sub>, NH<sub>4</sub>OH, (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, CuSO<sub>4</sub>, NiSO<sub>4</sub>, CoSO<sub>4</sub>, and NaOH, usually at concentrations of 0.5, 1.0 and 1.5 mol dm<sup>-3</sup>, under pressure and up to temperatures of 523 K. They did not measure the solubility of oxygen in water but they did their own evaluation of the oxygen solubility in water from literature data. They reported a Bunsen coefficient,  $\alpha/\text{cm}^3(\text{STP})\text{cm}^{-3}\text{atm}^{-1}$ , and the  $\alpha/\alpha^\circ$  ratio where  $\alpha^\circ$  is the Bunsen coefficient in water. From the reported  $\alpha$  and  $\alpha/\alpha^\circ$  values one can deduce the solubility values of oxygen in water used by them are:

$T/\text{K}$	$\alpha^\circ/\text{cm}^3(\text{STP})\text{cm}^{-3}\text{atm}^{-1}$	$T/\text{K}$	$\alpha^\circ/\text{cm}^3(\text{STP})\text{cm}^{-3}\text{atm}^{-1}$
298.15	0.02831	398.15	0.01775
323.15	0.02092	423.15	0.01959
348.15	0.01797	473.15	0.02690
373.15	0.01705	523.15	0.03782

The authors obtained smooth curves when they plotted  $\alpha/\alpha^\circ$  vs.  $c_2$ . However, the salt effect parameters,  $k_{sca}/\text{dm}^3\text{mol}^{-1}$ , calculated from the inverse of the  $\alpha/\alpha^\circ$  ratios scattered badly and do not appear to correlate well with either electrolyte concentration or temperature. Some of the scatter may be due to the choice of  $\alpha^\circ$  values, and some may be due to the difficulties encountered in making solubility measurements at high pressure. The tabulated values of  $k_{sca}$  are the average of the measured values at all concentrations. The data are classed as tentative, however, they scatter more widely and are greater in magnitude than the values obtained by other workers.

Khomutov and Konnik (30) measured the solubility of oxygen from air, at 101 kPa (1 atm) at 298.15 K in forty four aqueous alkali metal salt solutions. They usually measured the oxygen solubility at 6 to 8 electrolyte concentrations up to either 0.5 or 1.2 mol dm<sup>-3</sup>. The air saturated solutions were analyzed for oxygen by the Winkler method with an accuracy of ±0.05 mg dm<sup>-3</sup>. The solubility of oxygen ranged from 2.8 to 8.15 mg dm<sup>-3</sup> and the maximum error was stated to be ±1.8 per cent. They did not report numerical data, but they presented graphs of all 44 systems of log(solubility, mg dm<sup>-3</sup>) vs.  $c_2$ . Except for the lithium salts, the linearity of the log (solubility) vs.  $c_2$  plots was quite good. They did present a table of salt effect constants which appear to be the equivalent of  $k_{sca}$  values. The salt effect parameters are classed as tentative.

Yasunischī (33, 34) measured the solubility of oxygen at a partial pressure of 101.325 kPa (1 atm) in 13 aqueous electrolyte solutions at temperatures of 288.15, 298.15 and 308.15 K and at electrolyte concentrations of about 1 to 6.4 mol dm<sup>-3</sup> depending on the electrolyte. He used an apparatus similar to that of Horvutī. He tabulated both the solubility data and his value of  $k_{scl}$  from a fit to the log L°/L and  $c_2$  data. When the log L°/L vs.  $c_2$  showed a definite curvature he fitted the data to an empirical relation

$$\log(L^\circ/L) = k_{scl}^\circ c_2 / (1 + k_{scl}' c_2)$$

The solubility values were calculated taking into account the vapor pressure of the solvent and the increase in solution volume due to the dissolved gas. The results are classed as tentative, but should be preferred over the data of others where there is a choice.

Oxygen solubility measurements have been reported in over 70 aqueous electrolyte systems. Unless otherwise stated, the salt effect parameters are for a one mole dm<sup>-3</sup> electrolyte solution at an oxygen partial pressure of 101.325 kPa.

The systems are given in the order of the standard arrangement for inorganic compounds used in the U. S. National Bureau of Standards publications. The number before each system is the standard order number for the electrolyte.

#### 10(1) Oxygen + Hydrochloric acid [7647-01-0] + Water

Geffcken (1) measured the solubility of oxygen in aqueous hydrochloric acid at six acid concentrations up to 1.982 mol dm<sup>-3</sup> at 288.15 and 298.15 K. The  $k_{sca}$  values scatter with no definite trend with acid concentration. The average values are taken as the tentative values

$T/K$	288.15	298.15
$k_{sca}/\text{dm}^3\text{mol}^{-1}$	0.0440	0.0307
standard deviation, $\sigma$	±0.0020	±0.0014

#### 14(1) Oxygen + Sulfuric acid [7664-93-9] + Water

There are six reports on the solubility of oxygen in aqueous sulfuric acid solution. Three were carried out at atmospheric pressure near the turn of the century. Three were carried out at pressures up to 15 atm and reported in 1965 and 1967. Geffcken (1) measured the solubility of oxygen in ten solutions up to concentrations of 2.65 mol dm<sup>-3</sup> at temperatures of 288.15 and 298.15 K. Christoff (2) made measurements in two solutions at 293.15 K and Bohr (3) made measurements of oxygen solubility in eight solutions at concentrations between 2.45 and 17.9 mol dm<sup>-3</sup> at temperatures near 294 K. The three authors' data were converted to salt effect parameters,  $k_{sca}'$ , which are given in the following table. The salt effect parameter values form a consistent pattern. The data are classed as tentative.



Bruhn, Gerlach, and Pawlek (17) measured the solubility of oxygen in 0.5, 1.0, and 1.5 mol dm<sup>-3</sup> sulfuric acid solutions at five temperatures between 323 and 523 K. They report Bunsen coefficients and  $\alpha/\alpha^\circ$  ratios. The  $\alpha/\alpha^\circ$  values have been converted to  $k_{sc\alpha}$  values. The average of the three values at each temperature are given in the table. The  $k_{sc\alpha}$  values show little variation with temperature. There is some indication of a decrease in  $k_{sc\alpha}$  value as the acid concentration increases, but the trend is obscured by the random scatter of the data. The data are classed as tentative.

Sulfuric Acid Concentration $c_2/\text{mol dm}^{-3}$	Salt Effect Parameters, $k_{sc\alpha}/\text{dm}^3 \text{ mol}^{-1}$			
	Geffcken 288.15 K	Christoff 293.15 K	Bohr 294.2 K <sup>1</sup>	Geffcken 298.15 K
0.245	0.134			0.115
0.264	0.120			0.114
0.489	0.109			0.099
0.509	0.103			0.098
0.915	0.102			0.085
0.948	0.105			0.087
1.474	0.100			0.088
1.756	0.102			0.083
2.45	---		0.082	---
2.476	0.090		---	---
2.647	0.092		---	0.078
4.45			0.068	
4.63		0.063	---	
5.35		---	0.063	
9.52		0.038	---	
10.2			0.041	
12.4			0.039	
14.8			0.030	
17.2			0.011	
17.9			0.003	

Bruhn, Gerlach, and Pawlek

	323 K	373 K	423 K	473 K	523 K
1.0	0.088	0.102	0.102	0.105	0.100
	±0.013	±0.010	±0.015	±0.023	---

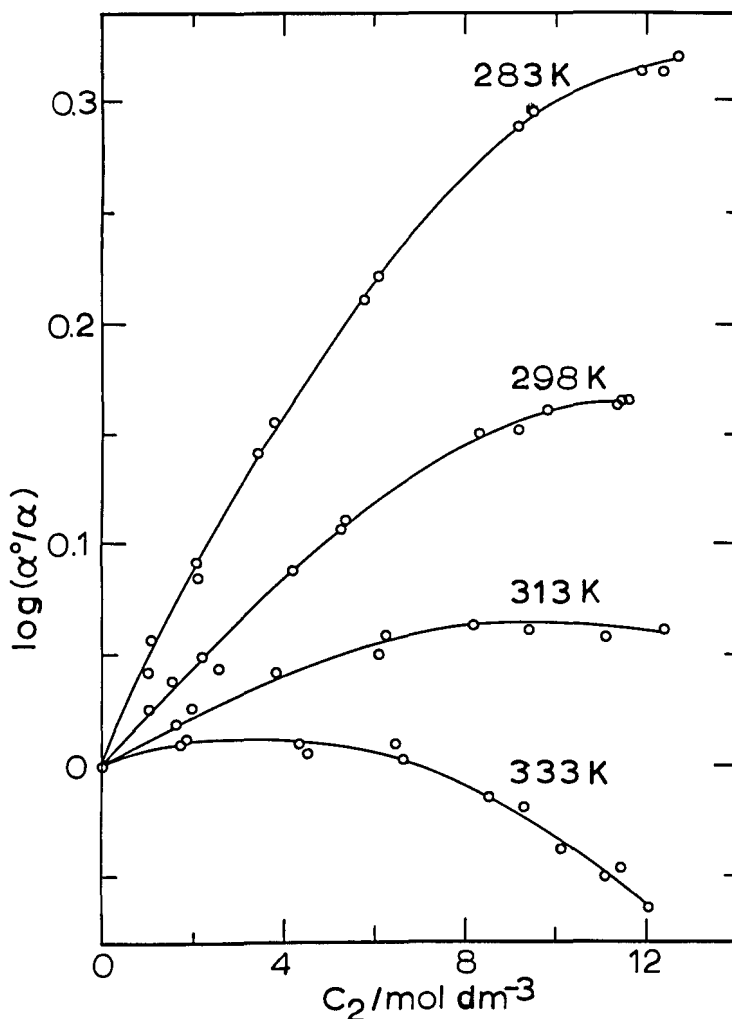
<sup>1</sup> Temperature ranges from 293.95 to 294.65, see data sheet.

Klyueva (19) and Turchinov (20) measured oxygen solubilities in aqueous sulfuric acid solution at several pressures. Klyueva measured the oxygen solubility at oxygen partial pressures of 2.5 and 10 atm at six temperatures between 323 and 473 K in water and at 10 atm in 0.0125 mol dm<sup>-3</sup> sulfuric acid solution saturated with either Ni<sub>3</sub>S<sub>2</sub>, Cu<sub>2</sub>S or Co<sub>4</sub>S<sub>3</sub>. The sulfuric acid metal sulfide solutions decrease the oxygen solubility to less than 50 per cent its solubility in water. The sulfide concentrations are not given. Turchinov (20) measured the oxygen solubility at oxygen partial pressures of 5, 10 and 15 atm at 383 K in four sulfuric acid solutions up to a concentration of 2.30 mol dm<sup>-3</sup>. Values of  $k_{sc\alpha}$  were calculated. At concentrations of 0.756 and 1.275 mol dm<sup>-3</sup> H<sub>2</sub>SO<sub>4</sub> the values scatter badly and they are much smaller than the values of Bruhn, Gerlach and Pawlek at similar temperatures. At the two higher acid concentrations the values of  $k_{sc\alpha}$  are 0.111 ± 0.009 at 1.785 mol dm<sup>-3</sup> and 0.214 ± 0.006 at 2.30 mol dm<sup>-3</sup>. The first value agrees within experimental error with the Bruhn, *et al.* value, but the second value appears large for such a small increase in acid concentration.

## 18(1) Oxygen + Nitric acid [7697-37-2] + Water

Both Geffcken (1) and Pogrebnyaya, Usov, Baranov, and Machigin (31) have measured the solubility of oxygen in aqueous nitric acid at an oxygen partial pressure near one atm (101 kPa). Geffcken made five to six measurements at acid concentrations up to near 2 mol dm<sup>-3</sup> at 288.15 and 298.15 K. Pogrebnyaya *et al.* made up to 13 measurements at acid concentrations up to 12.5 mol dm<sup>-3</sup> at seven temperatures between 283.15 and 333.15 K.

Both data sets were converted to salt effect parameters,  $k_{sca}$ . The  $\log(\alpha^0/\alpha)$  vs.  $c_2$  plots are reasonably linear up to concentrations of 3 to 4 mol dm<sup>-3</sup> but show definite curvature at the larger acid concentrations. At 323 and 333 K the nitric acid salts-in oxygen starting at about 10 mol dm<sup>-3</sup> and 8.5 mol dm<sup>-3</sup> respectively. A graph of  $\log(\alpha^0/\alpha)$  vs.  $c_2$  at temperatures of 283, 298, 313 and 333 K from the data of Pogrebnyaya *et al.* (31) is shown.



Values of  $k_{sca}$  to use at acid concentrations from 0 to 2 mol dm<sup>-3</sup> acid are given below. All except the 288.15 K value were calculated from the data of Pogrebnyaya *et al.* and they are classed as tentative.

$T/K$	$k_{s\alpha}/\text{dm}^3 \text{ mol}^{-1}$	$T/K$	$k_{s\alpha}/\text{dm}^3 \text{ mol}^{-1}$
283.15	0.0440	303.15	0.0175
288.15	0.0340 <sup>1</sup>	313.15	0.0115
293.15	0.0255	323.15	0.0090
298.15	0.0240 <sup>2</sup>	333.15	0.0050

<sup>1</sup> Geffcken's value.

<sup>2</sup> Geffcken's value is 0.0176.

Pogrebnyaya *et al.* give one value of  $k_{sux}$  of 0.017 at 298.15 K. The solubility ratio  $x^\circ/x$  was calculated with respect to molecular nitric acid,  $\text{HNO}_3$ . Inspection of the data shows that  $k_{sux}$  values salt-in over most of the acid concentration range at both 323 and 333 K. The temperature coefficient of mole fraction solubility changes sign at about 16 mol percent nitric acid. At lower mole fractions oxygen solubility decreases with temperature, at higher nitric acid concentration oxygen solubility increases with temperature.

Another paper of Pogrebnyaya, Usov, and Baranov (27) which may contain additional data was not available to us.

Other measurements of the solubility of oxygen in nitric acid solution were carried out at higher oxygen partial pressure. They are classed as tentative. In 1955 both Robertson, Mason and Corcoran (10) and Sprague (11) reported oxygen solubility in pure nitric acid and in nitric acid containing up to 31 weight per cent water. More recently Shapka and Atroshchenko (25, 29) and Pogrebnyaya, Usov and Baranov (32) reported oxygen solubility in nitric acid solutions over wide ranges of composition, temperature and pressure. The data are presented on data sheets following this section. No attempt was made to treat the data in terms of salt effect parameters. The data of Pogrebnyaya, Usov and Baranov (32) are preferred not because there is evidence they are more accurate, but because they cover the greatest range of concentration, temperature and pressure in one self-consistent study.

18(2) Oxygen + Nitric acid [7697-37-2] + Nitrogen dioxide/  
Dinitrogen tetroxide

Both Robertson, Mason, and Corcoran (10) and Sprague report the solubility of oxygen in nitric acid containing  $\text{NO}_2/\text{N}_2\text{O}_4$ . The studies were carried out at different compositions and temperatures, and cannot be compared. Both are classed as tentative.

18(3) Oxygen + Ammonium hydroxide [1336-21-6] + Water

Bruhn, Gerlach, and Pawlek (17) measured the solubility of oxygen in aqueous solutions of ammonium hydroxide at concentrations of 2.87, 5.63 and 8.28 mol  $\text{dm}^{-3}$  at temperatures up to 423.15 K. Ammonium hydroxide shows only a small salt effect. The data shows no discernible trend with either concentration or temperature. The tentative salt effect parameter values are the average of the three values at each temperature.

$T/K$	323.15	348.15	373.15	423.15
$k_{s\alpha}/\text{dm}^3 \text{ mol}^{-1}$	0.0063	0.0057	0.0088	0.0045
standard deviation, $\sigma$	$\pm 0.0012$	$\pm 0.0027$	$\pm 0.0033$	$\pm 0.0013$

## 18(4) Oxygen + Ammonium sulfate [7783-20-2] + Water

Bruhn, Gerlach, and Pawlek (17) measured the solubility of oxygen in aqueous ammonium sulfate solutions of concentrations 0.25, 0.75, 1.5 and 3.0 mol dm<sup>-3</sup> at temperatures up to 473.15 K. The tentative salt effect parameter values are the average of the four values at each temperature. There is no discernible trend of the salt effect parameters with either concentration or temperature.

<i>T</i> /K	298.15	323.15	373.15	423.15	473.15
$k_{sca}/\text{dm}^3\text{mol}^{-1}$	0.212	0.196	0.203	0.193	0.198
standard deviation, $\sigma$	$\pm 0.021$	$\pm 0.031$	$\pm 0.035$	$\pm 0.040$	$\pm 0.036$

## 18(5) Oxygen + Tetraethylammonium bromide [71-91-0] + Water

Morrison and Johnstone (9) measured the solubility of oxygen in water and in one mol kg<sup>-1</sup> aqueous tetraethylammonium bromide solution at 298.15 K. The work is classed as tentative. The salt effect parameter is  $k_{sms} = -0.046$  or  $k_{smx} = -0.031$ . The  $k_{sca}$  value is probably of similar magnitude. Oxygen is salted-in.

## 29(1) Oxygen + Hydrated aluminum oxide [1333-84-6] + Water

The data of Shkol'nikova (13) are classed as tentative. The solubility of oxygen in water was not measured. No salt effect parameters were calculated for the colloidal solutions.

## 29(2) Oxygen + Aluminum chloride [7446-70-0] + Water

Yasunischi (34) measured the solubility of oxygen in 12 aqueous solutions of aluminum chloride up to 2.204 mol dm<sup>-3</sup> at 298.15 K. The work is classed as tentative. The salt effect parameter shows a definite concentration dependence above 1.7 mol dm<sup>-3</sup> AlCl<sub>3</sub>. Yasunischi suggests that up to 1.7 mol dm<sup>-3</sup>

$$\log(L^\circ/L) = \log(\alpha^\circ/\alpha) = (k_{sca}/\text{dm}^3\text{mol}^{-1})(c_2/\text{mol dm}^{-3}) = 0.274 c_2$$

over the entire concentration range

$$\log(L^\circ/L) = \log(\alpha^\circ/\alpha) = 0.303 c_2/(1 + 0.0859 c_2)$$

## 29(3) Oxygen + Aluminum sulfate [10043-01-3] + Water

Yasunischi (34) measured the solubility of oxygen in nine aluminum sulfate solutions over the 0 to 0.812 mol dm<sup>-3</sup> concentration range at 298.15 K. The work is classed as tentative. The salt effect parameter is independent of concentration and is  $k_{sca} = k_{scl} = 0.745 \text{ dm}^3\text{mol}^{-1}$ .

## 36(1) Oxygen + Copper (II) sulfate [7758-98-7] + Water

Bruhn, Gerlach, and Pawlek (17) measured the solubility of oxygen in aqueous copper (II) sulfate of 0.5, 1.0 and 1.5 mol dm<sup>-3</sup> and temperatures up to 523 K. There is some tendency for the  $k_{sca}$  value to decrease with concentration at each temperature. However, the tentative salt effect parameters below were obtained by averaging the values of the three concentrations.

<i>T</i> /K	298	323	373	423	473	523
$k_{sca}/\text{dm}^3\text{mol}^{-1}$	0.114	0.123	0.106	0.119	0.122	0.103
standard deviation, $\sigma$	$\pm 0.014$	$\pm 0.018$	$\pm 0.019$	$\pm 0.018$	$\pm 0.011$	$\pm 0.003$

## 39(1) Oxygen + Nickel sulfate [7786-81-4] + Water

Bruhn, Gerlach, and Pawlek (17) measured the solubility of oxygen in aqueous nickel sulfate at 0.5, 1.0 and 1.5 mol dm<sup>-3</sup> and temperatures up to 423 K. There is a tendency of the salt effect parameters decreasing with concentration at most of the temperatures. However, the tentative salt effect parameters below were obtained by averaging the values at the three concentrations.

T/K	298	323	373	398	423
$k_{sca}/\text{dm}^3\text{mol}^{-1}$	0.113	0.116	0.112	0.115	0.122
standard deviation, $\sigma$	$\pm 0.013$	$\pm 0.009$	$\pm 0.025$	$\pm 0.009$	$\pm 0.020$

## 40(1) Oxygen + Cobalt (II) sulfate [10124-43-3] + Water

Bruhn, Gerlach, and Pawlek (17) measured the solubility of oxygen in aqueous cobalt (II) sulfate at 0.5, 1.0 and 1.5 mol dm<sup>-3</sup> at temperatures up to 423 K. There is a tendency of the salt effect parameter to decrease with concentration at each temperature. However, the salt effect parameters were obtained by averaging the values at the three concentrations.

T/K	298	323	373	398	423
$k_{sca}/\text{dm}^3\text{mol}^{-1}$	0.115	0.128	0.105	0.113	0.117
standard deviation, $\sigma$	$\pm 0.015$	$\pm 0.022$	$\pm 0.006$	$\pm 0.025$	---

## 41(1) Oxygen + Hydrated iron oxide [12259-21-1] + Water

The data of Shkol'nikova (13) are classed as tentative. She made no solubility measurements in pure water. No salt effect parameters were calculated for the colloidal solutions.

48(1) Oxygen + Manganese chloride (MnCl<sub>2</sub>) [7773-01-5] + Water48(2) Oxygen + Manganese sulfate (MnSO<sub>4</sub>) [7785-87-7] + Water

Murray, Riley and Wilson (22) measured the solubility of oxygen in 2.69 mol dm<sup>-3</sup> MnCl<sub>2</sub> and in 2.43 mol dm<sup>-3</sup> MnSO<sub>4</sub> at 298.7 K. The two measurements were converted to tentative salt effect parameters of:

$$k_{sca} = 0.202 \text{ for MnCl}_2, \text{ and}$$

$$k_{sca} = 0.194 \text{ for MnSO}_4.$$

88(1) Oxygen + Uranyl fluoride (UO<sub>2</sub>F<sub>2</sub>) [13536-84-0] + Water88(2) Oxygen + Uranyl sulfate (UO<sub>2</sub>SO<sub>4</sub>) [1314-64-3] + Water

## 88(3) Oxygen + Uranyl sulfate + Sulfuric acid + Copper (II) sulfate + Water

These systems were studied at high pressure. The evaluator made no attempt to convert the data into salt effect parameters. The data are classed as tentative.

Stephan, Hatfield, Peoples, and Pray (12) reported the solubility of oxygen in water and solutions containing 40, 100, and 243 g dm<sup>-3</sup> of uranium as UO<sub>2</sub>F<sub>2</sub> at temperatures of 373.15, 408.15, and 435.93 K over oxygen partial pressure ranges of 1.34 to 10.6 MPa.

Pray and Stephan (8), and Stephan, Hatfield, Peoples and Pray (12) reported the solubility of oxygen in water and in solutions containing 40, 100, and 243 g uranium as UO<sub>2</sub>SO<sub>4</sub> at temperatures of 373.15, 408.15 and 435.93 K in both references and at additional temperatures of 477.59, 533.15, and 560.93 K in the second reference (12). The oxygen partial pressures ranged from 1.0 to 17.5 MPa. The complete data set appears in reference 12.

Anderson, Keeler and Klach (15) measured the solubility of oxygen in water and two solutions, one of which was  $0.02 \text{ mol dm}^{-3} \text{ UO}_2\text{SO}_4$ ,  $0.005 \text{ mol dm}^{-3} \text{ H}_2\text{SO}_4$  and  $0.005 \text{ mol dm}^{-3} \text{ CuSO}_4$ . The second solution was  $0.04 \text{ mol dm}^{-3} \text{ UO}_2\text{SO}_4$ ,  $0.01 \text{ mol dm}^{-3} \text{ H}_2\text{SO}_4$  and  $0.01 \text{ mol dm}^{-3} \text{ CuSO}_4$ . The authors saw no evidence of salting out by these relatively dilute solutions over the 373 to 573 K and 386 to 5190 kPa temperature and pressure ranges.

### 93(1) Oxygen + Magnesium chloride [7786-30-3] + Water

Both MacArthur (4) and Yasunischi (34) have measured the solubility of oxygen in aqueous  $\text{MgCl}_2$  solutions at 298.15 K. Eucken and Hertzberg (6) made measurements at 273.15 and 293.15 K. Their measurements are summarized in the table below.

The Eucken and Hertzberg salt effect parameters show little scatter at each temperature. They are classed as tentative.

At 298.15 K MacArthur's values fall into two distinct regions, salting out more between 0 and  $1 \text{ mol dm}^{-3}$  than between 2 and  $5 \text{ mol dm}^{-3}$ . Yasunischi fitted his data up to  $2.5 \text{ mol dm}^{-3}$  to  $\log(\alpha^\circ/\alpha) = k_{\text{sc}\alpha}^\circ c_2$ , and over the entire concentration range to  $\log(\alpha^\circ/\alpha) = k_{\text{sc}\alpha}^\circ c_2 / (1 + k'_{\text{sc}\alpha} c_2)$ .

MacArthur's data are classed as doubtful, and Yasunischi's data are classed tentative.

T/K	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameters	
			$k_{\text{sc}\alpha}^\circ/\text{dm}^3\text{mol}^{-1}$	$k'_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1}$
273.15	4	0 - 1.64	0.290	
293.15	4	0 - 1.84	0.267	
298.15	5	0 - 1	0.258 <sup>2</sup>	
	3	2 - 5	0.211 <sup>2</sup>	
298.15	8	0 - 2.5	0.200	
	11	0 - 3.9	0.222	0.0566

<sup>1</sup> Includes determination in pure water.

<sup>2</sup> MacArthur's values.

### 93(2) Oxygen + Magnesium sulfate [7487-88-9] + Water

Yasunischi (34) measured the solubility of oxygen in aqueous magnesium sulfate solutions up to concentrations of  $2.608 \text{ mol dm}^{-3}$  at temperatures of 288.15, 298.15 and 308.15 K. He found that  $\log(\alpha^\circ/\alpha)$  vs.  $c_2$  was linear up to concentrations between 1.3 and  $1.7 \text{ mol dm}^{-3}$ . For the entire concentration range the data were better fitted by

$$\log(\alpha^\circ/\alpha) = k_{\text{sc}\alpha}^\circ c_2 / (1 + k'_{\text{sc}\alpha} c_2)$$

The constants, which are classed as tentative, are summarized in the following table.

T/K	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameters	
			$k_{\text{sc}\alpha}^\circ/\text{dm}^3\text{mol}^{-1}$	$k'_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1}$
288.15	9	0 - 1.3	0.290	
	17	0 - 2.5	0.288	-0.0012
298.15	7	0 - 1.7	0.273	
	14	0 - 2.4	0.250	-0.0583
308.15	8	0 - 1.7	0.280	
	12	0 - 2.6	0.293	-0.0359

<sup>1</sup> Includes determination in pure water.

## 94(1) Oxygen + Calcium chloride [10043-52-4] + Water

Both MacArthur (4) and Yasunischi (34) measured the solubility of oxygen in aqueous calcium chloride solutions up to concentrations of  $5 \text{ mol dm}^{-3}$  at 298.15 K. MacArthur worked with air saturated solutions at 101 kPa (1 atm) while Yasunischi worked with oxygen at a partial pressure of 101 kPa (1 atm). The two data sets show similar features but the Yasunischi data are preferred because he made more measurements that showed less scatter. Their results are summarized in the following table.

$T/K$	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameters	
			$k_{\text{sc}\alpha}^{\circ}/\text{dm}^3\text{mol}^{-1}$	$k'_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1}$
298.15	3	0 - 1	0.191 <sup>2</sup>	
	1	5	0.087 <sup>2</sup>	
	11	0 - 2.7	0.204	
	14	0 - 4.5	0.226	0.0523

<sup>1</sup> Includes determination in pure water.

<sup>2</sup> MacArthur's values.

## 94(2) Oxygen + Calcium nitrate [10124-37-5] + Water

Yasunischi (34) measured the solubility of oxygen in seven aqueous calcium nitrate solutions at concentrations up to  $2.4 \text{ mol dm}^{-3}$  at 298.15 K. The tentative salt effect parameter is  $k_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1} = 0.194$ .

## 96(1) Oxygen + Barium chloride [10361-37-2] + Water

MacArthur (4) measured the solubility of oxygen in four air saturated aqueous barium chloride solutions up to concentrations of  $1 \text{ mol dm}^{-3}$  at 298.15 K. Yasunischi (34) measured the solubility of oxygen in seven oxygen saturated solutions up to concentrations of  $1.54 \text{ mol dm}^{-3}$  at 298.15 K. The values of the salt effect parameters are

$$\text{MacArthur } k_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1} = 0.270$$

$$\text{Yasunischi } k_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1} = 0.212$$

The value of Yasunischi is preferred.

- 98(1) Oxygen + Lithium hydroxide [1310-65-2] + Water
- 98(2) Oxygen + Lithium fluoride [7789-24-4] + Water
- 98(3) Oxygen + Lithium chloride [7447-41-8] + Water
- 98(4) Oxygen + Lithium perchlorate [7791-03-9] + Water
- 98(5) Oxygen + Lithium bromide [7550-35-8] + Water
- 98(6) Oxygen + Lithium iodide [10377-51-2] + Water
- 98(7) Oxygen + Lithium sulfate [10377-48-7] + Water
- 98(8) Oxygen + Lithium nitrate [7790-69-4] + Water
- 98(9) Oxygen + Lithium carbonate [554-13-2] + Water

Khomutov and Konnik (30) measured the solubility of oxygen in the air saturated lithium salt solutions above at 298.15 K by a chemical method. The solubility values are presented graphically as  $\log(\text{solubility}/\text{mg dm}^{-3})$  vs.  $c_2/\text{mol dm}^{-3}$ , and the salt effect parameters, equivalent to  $k_{\text{sc}\alpha}$ , are tabulated.

In addition the solubility of oxygen in aqueous LiCl was measured by Eucken and Hertzberg (6) at 273.15 and 293.15 K and by MacArthur (4) at 298.15 K.

The most interesting feature of the solubility of oxygen in lithium salt solutions is the observation of Khomutov and Konnik of two linear regions of salt effects for the hydroxide, fluoride, chloride, perchlorate, bromide and nitrate of lithium. Between concentrations of 0 and about  $0.07 \text{ mol dm}^{-3}$  (0.01 for LiF) the lithium salts "salt-out" more than they do at concentrations between 0.15 and  $1.2 \text{ mol dm}^{-3}$ . Two of the salts, LiF and  $\text{LiNO}_3$  "salt-out" in the low concentration region and "salt-in" in the high concentration region. LiI,  $\text{Li}_2\text{SO}_4$  and  $\text{Li}_2\text{CO}_3$  show a concentration independent salt effect parameter over the entire concentration range studied. This is a very interesting observation which deserves further study.

Neither Eucken and Hertzberg or MacArthur carried out studies at a low enough LiCl concentration to observe the effect. All of the results are summarized in the following table. At 298.15 K the results of Khomutov and Konnik are preferred over the result of MacArthur. All of the values are classed as tentative.

$T/\text{K}$	Electrolyte	Number of Determinations <sup>1</sup>	Range of Concentration, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter $k_{\text{sc}\alpha}/\text{dm}^3\text{mol}^{-1}$
298.15	LiOH	4	0 - 0.07	0.332
		5	0.015 - 1.2	0.091
	LiF	3	0 - 0.01	0.725
		5	0.04 - 0.10	-0.385
273.15 293.15 298.15	LiCl	4	0 - 2.32	0.163 <sup>2</sup>
		4	0 - 1.94	0.140 <sup>2</sup>
		6	0 - 2	0.100 <sup>3</sup>
		4	0 - 0.07	0.112
		6	0.15 - 1.2	0.070
298.15	LiClO <sub>4</sub>	3	0 - 0.07	0.218
		5	0.15 - 1.2	0.066
	LiBr	4	0 - 0.07	0.252
		5	0.15 - 1.2	0.084
		6	0 - 0.65	0.163
	Li <sub>2</sub> SO <sub>4</sub>	7	0 - 1.2	0.244
	LiNO <sub>3</sub>	(?)	0 - 0.07	0.196
		5	0.15 - 1.2	-0.040
Li <sub>2</sub> CO <sub>3</sub>	7	0 - 0.12	0.254	

<sup>1</sup> Includes value in pure water.

<sup>2</sup> Eucken and Hertzberg's values.

<sup>3</sup> MacArthur's value, there are two additional measurements at 3 and 4  $\text{mol dm}^{-3}$  LiCl, for which  $k_{\text{sc}\alpha}$  is 0.156 and 0.178 respectively. The two values are classed as doubtful.

#### 99(1) Oxygen + Sodium hydroxide [1310-73-2] + Water

Geffcken (4), Khomutov and Konnik (30), and Yasunischi (34) measured the solubility of oxygen in aqueous NaOH solutions around room temperature, and Bruhn, Gerlach, and Pawlek (17) measured the solubility in 0.5, 1.0, and  $1.5 \text{ mol dm}^{-3}$  solutions at five temperatures between 323 and 523 K.

Recently Broden and Simonson (36) have measured the solubility of oxygen in water and in 0.01 and  $0.10 \text{ mol dm}^{-3}$  NaOH. Their results are presented by graphs and fitted equations. The results indicate that oxygen is salted-out more effectively by 0.01 and  $0.10 \text{ mol dm}^{-3}$  NaOH, in that the slope of  $\log(a^0/a)$  vs.  $c_2$  is much larger up to 0.1 than at higher molarities. This reinforces the observation of Khomutov and Konnik of a larger salt effect parameter for certain lithium salts at concentrations below  $0.07 \text{ mol dm}^{-3}$  than at larger concentrations. Broden and Simonson carried out their measurements at 323, 348, 373, 398, and 423 K and pressures of 1, 2, 3, 4, and 5 MPa.



The results are summarized below.

T/K	Salt Effect Parameter, $k_{sca}/\text{dm}^3 \text{ mol}^{-1}$			
	Geffcken	Khomutov, Konnik	Yasunischi	Bruhn, Gerlach and Pawlek
288.15	0.190		0.158	
298.15	0.180	0.180	0.160	
308.15			0.167	
323				0.185
373				0.171
423				0.187
473				0.187
523				0.167

Yasunischi also fitted his data to the relationship

$$\log(\alpha^\circ/\alpha) = k_{sca}^\circ c_2 / (1 + k'_{sca} c_2)$$

with the constants

T/K	$k_{sca}^\circ$	$k'_{sca}$
288.15	0.171	0.0181
298.15	0.164	0.0049
308.15	0.181	0.0310

There is some concern that Yasunischi's parameters do not follow a more consistent pattern as the temperature increases. His data do cover a larger concentration range, up to  $6.4 \text{ mol dm}^{-3}$ , than do the data of the others. Geffcken's measurements go to  $2 \text{ mol dm}^{-3}$ , Khomutov and Konnik to  $1.2 \text{ mol dm}^{-3}$ , and Bruhn *et al.* are at 0.5, 1.0, and  $1.5 \text{ mol dm}^{-3}$ .

The data are classed as tentative with no reason to prefer one data set over another.

Broden and Simonson discuss in detail the salting out by NaOH at 373 K. The value of  $k_{sca}$  in the limiting slope region from 0 to  $0.1 \text{ mol dm}^{-3}$  is 0.65 which is much larger than any of the values in the table above. They discuss in more detail the  $\text{NaHCO}_3$  system which also exhibits the effect, and they point out that  $\text{NaNO}_3$  does not show the effect, but gives a "normal" salt effect parameter at all concentrations.

#### 99(2) Oxygen + Sodium fluoride [7681-49-4] + Water

Khomutov and Konnik (30) measured the solubility of oxygen in six aqueous sodium fluoride solutions at concentrations up to  $0.6 \text{ mol dm}^{-3}$  at 298.15 K. The salt effect parameter is  $k_{sca}/\text{dm}^3 \text{ mol}^{-1} = 0.284$ . It is classed as tentative.

#### 99(3) Oxygen + Sodium chloride [7647-14-5] + Water

Geffcken (1), MacArthur (4), Eucken and Hertzberg (6), and Khomutov and Konnik (30) report measurement of the solubility of oxygen in aqueous sodium chloride solution. Mishnina, Avdeeva, and Bozhovakaya (14) present an extensive table of smoothed solubility data for the system. The source of their data is not clear to us. Recently Cramer (35) made extensive measurements of the solubility of oxygen in aqueous sodium chloride and in several brines at high temperature and pressure. He reports Henry's constants in water and aqueous sodium chloride of 0.87, 2.97 and  $5.69 \text{ mol kg}^{-1}$  up to temperatures of 570 K. His Henry's constants are of the form  $K/\text{MPa} = (P_1/\text{MPa})/X_1$ . No attempt was made to convert his data into salt effect parameters.

The salt effect parameters are summarized in the following table. The values of Geffcken and of Eucken and Hertzberg agree well at 288.15 K. The values of Geffcken, of MacArthur, and of Khomutov and Konnik agree well at 298.15 K. The smoothed values of Mishnina *et al.* appear to be greater than the other values at all temperatures. Mishnina *et al.* did give values up to saturation, about 5.4 mol dm<sup>-3</sup> NaCl. None of the experimental data known to us go above 2.5 mol dm<sup>-3</sup>.

All of the data are classed as tentative with no preference given to any one laboratories results. The data of Cramer appear to be very useful and deserve further analysis.

T/K	Salt Effect Parameter, $k_{sca}/\text{dm}^3 \text{mol}^{-1}$				
	Geffcken	MacArthur	Eucken Hertzberg	Khomutov Konnik	Mishnina, Avdeeva Bozhovahoya
273.15			0.169		0.180
278.15					0.168
283.15					0.160
288.15	0.148		0.150		0.156
293.15			0.145		0.149
298.15	0.141	0.138	0.145	0.136	0.145
303.15					0.139

93(4) Oxygen + Sodium perchlorate [7601-89-0] + Water

93(5) Oxygen + Sodium bromide [7647-15-6] + Water

93(6) Oxygen + Sodium iodide [7681-82-5] + Water

Both Khomutov and Konnik (30) and MacArthur (4) measured the solubility of oxygen in air saturated solutions of the above solutions at 298.15 K by a chemical method. MacArthur measured solubilities only in the sodium bromide solutions. The salt effect parameters are given in the following table. All are classed as tentative, but Khomutov and Konnik's result is preferred for the sodium bromide solutions.

T/K	Electrolyte	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{dm}^3 \text{mol}^{-1}$	Salt Effect Parameter $k_{sca}/\text{dm}^3 \text{mol}^{-1}$
298.15	NaClO <sub>4</sub>	8	0 - 1.2	0.160
	NaBr	8	0 - 1.2	0.131
		9	0 - 6	0.115 <sup>2</sup>
	NaI	8	0 - 1.2	0.120

<sup>1</sup> Includes determination in pure water.

<sup>2</sup> MacArthur's value.

93(7) Oxygen + Sodium iodide [7681-82-5] +  
Sodium hydroxide [1310-73-2] + Water

Murray, Riley and Wilson (22) measured the solubility of oxygen in concentrated solutions of NaI + NaOH at 298.65 K. A salt effect parameter was calculated for the combined electrolyte concentration.

T/K	NaI $c_2/\text{mol dm}^{-3}$	NaOH $c_3/\text{mol dm}^{-3}$	Total Concentration	Salt Effect Parameter $k_{sca}/\text{dm}^3 \text{mol}^{-1}$
298.65	4	8	12	0.181
	6	10	16	0.129

The results appear consistent with the salt effect parameters for the two electrolytes determined at lower concentrations.

## 93(8) Oxygen + Sodium sulfite [7757-83-7] + Water

Gestrich and Pontow (28) measured the solubility of oxygen in aqueous solutions of a 38:1 ratio of  $\text{Na}_2\text{SO}_3$  and  $\text{Na}_2\text{S}_2\text{O}_5$  at concentrations up to  $1.2 \text{ mol dm}^{-3}$  and temperatures of 273.15, 288.15, 298.15, and 303.15 K. Yasunischi (33) estimated the solubility at  $0.1 \text{ mol dm}^{-3}$  intervals up to  $1.0 \text{ mol dm}^{-3}$  from his measurements of the solubility of oxygen in sodium sulfate and of nitrogen in sodium sulfite and sodium sulfate solutions. Both worker's results were recalculated as  $k_{\text{sc}\alpha}/\text{dm}^3 \text{ mol}^{-1}$  values which are in the following table.

$T/\text{K}$	Salt Effect Parameter, $k_{\text{sc}\alpha}/\text{dm}^3 \text{ mol}^{-1}$	
	Gestrich, Pontow	Yasunischi
273.15	0.37	
288.15	0.39	
298.15	0.39	0.36
303.15	0.32	

The  $\log(\alpha^\circ/\alpha)$  vs.  $c_2$  plots of Gestrich and Pontow show some scatter. Yasunischi's  $k_{\text{sc}\alpha}$  values vary smoothly from a value of 0.43 at  $0.1 \text{ mol dm}^{-3}$  to the 0.36 value at  $1.0 \text{ mol dm}^{-3}$   $\text{Na}_2\text{SO}_3$ . The system reacts slowly with oxygen. The results are classed as tentative.

## 99(9) Oxygen + Sodium sulfate [7757-82-6] + Water

MacArthur (4) and Khomutov and Konnik (30) have measured the solubility of oxygen in air saturated aqueous sodium sulfate at 298.15 K. Yasunischi (33) has measured the solubility of oxygen in the system at 288.15, 298.15, and 308.15 K. Linek and Mayrhoferova (24) have measured the solubility of oxygen in aqueous sodium sulfate solutions at 293.15 K.

Yasunischi found definite curvature in plots of  $\log(L^\circ/L)$ . Agreement among the work on this system is not good. All of the data, summarized in the following table, are classed as tentative.

$T/\text{K}$	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter	
			$k_{\text{sc}\alpha}^\circ/\text{dm}^3 \text{ mol}^{-1}$	$k'_{\text{sc}\alpha}/\text{dm}^3 \text{ mol}^{-1}$
288.15	8	0 - 0.9	0.420	0.251
293.15	5	0 - 1.0	0.355 <sup>b</sup>	
298.15	12	0 - 1.5	0.398	0.183
		0 - 0.5	0.325 <sup>2</sup>	
308.15	6	0 - 1.2	0.376 <sup>3</sup>	
		0 - 1.7	0.420	0.231

<sup>1</sup> Includes determination in pure water.

<sup>2</sup> MacArthur's value, another value at  $1 \text{ mol dm}^{-3}$  would have decreased the value to 0.29.

<sup>3</sup> Khomutov and Konnik's value.      <sup>b</sup> Linek and Mayrhoferova's value.

## 99(10) Oxygen + Sodium sulfate [7757-82-6] + Sulfuric acid [7664-93-9] + Water

The single measurement of Kobe and Kenton (5) is classed as tentative.

## 99(11) Oxygen + Sodium sulfate [7757-82-6] + Sodium dithionite [7775-14-6] + Sodium hydroxide [1310-73-2] + Water

The work of Jhaveri and Sharma (21) on this system is classed as tentative.

- 99(12) Oxygen + Sodium nitrate [7631-99-4] + Water  
 99(13) Oxygen + Sodium phosphate [7601-54-9] + Water  
 99(14) Oxygen + Sodium bicarbonate [144-55-8] + Water  
 99(15) Oxygen + Sodium carbonate [497-19-8] + Water

Khomutov and Konnik (30), Yasunischi (34), and Broden and Simonson (36) report the solubility of oxygen in aqueous sodium nitrate solutions. Broden and Simonson do not observe larger salt effect parameters at low concentration than at high concentrations as they did for NaOH and NaHCO<sub>3</sub>. Khomutov and Konnik's value accords better with Broden and Simonson's values than does the value of Yasunischi. All are classed as tentative.

The salt effect parameter for aqueous sodium phosphate of Khomutov and Konnik is classed as tentative.

Broden and Simonson (36) measured the solubility of oxygen in water and in 0.1 and 0.5 mol dm<sup>-3</sup> sodium bicarbonate at five temperature between 323 and 423 K and at pressures of 1, 2, 3, 4, and 5 MPa. They find that the salt effect parameter is much larger in the 0 to 0.1 mol dm<sup>-3</sup> NaHCO<sub>3</sub> region than the 0.5 mol dm<sup>-3</sup> region. At 323 K the limiting value is about  $k_{SC\alpha}/dm^3 mol^{-1}$  0.3 at all pressures, but it changes with pressure at higher temperatures. Between concentrations of 0.1 and 0.5 the value is more normal and averages about 0.14. Both the solubilities and the salt effect parameters are presented graphically in the paper.

Both Khomutov and Konnik (30) and Yasunischi (34) have measured the oxygen solubility in aqueous sodium carbonate solutions. The agreement between the two is poor. There is no reason to prefer one set of data over the other, and both are classed as tentative.

T/K	Electrolyte	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/mol dm^{-3}$	Salt Effect Parameter $k_{SC\alpha}/dm^3 mol^{-1}$
298.15	NaNO <sub>3</sub>	8	0 - 1.2	0.124 <sup>2</sup>
		9	0 - 5.1	0.109 <sup>3</sup>
		4	0 - 1.0	0.110 <sup>4</sup>
323		4	0 - 1.0	0.080 <sup>4</sup>
373		4	0 - 1.0	0.065 <sup>4</sup>
423		4	0 - 1.0	0.065 <sup>4</sup>
298.15	Na <sub>3</sub> PO <sub>4</sub>	8	0 - 0.6	0.652 <sup>2</sup>
288.15	Na <sub>2</sub> CO <sub>3</sub>	7	0 - 1.3	0.356 <sup>3</sup>
298.15		10	0 - 2.1	0.338 <sup>3</sup>
298.15		7	0 - 1.0	0.464 <sup>4</sup>
308.15		9	0 - 3	0.353 <sup>3</sup>

<sup>1</sup> Includes determination in pure water. <sup>2</sup> Khomutov and Konnik's values.

<sup>3</sup> Yasunischi's values

<sup>4</sup> Broden and Simonson's values.

- 99(1) Oxygen + Sodium acetate [127-09-3] + Water

Guseva, Konnik, Saifi, Kuz'min, and Mordukhovich (26) measured the solubility of oxygen in aqueous solutions and in 0.1 mol dm<sup>-3</sup> sodium acetate solutions at various pH's between 0 and 14. The pH was adjusted by addition of small amounts of either KOH or H<sub>2</sub>SO<sub>4</sub>. The evaluator made no attempt to convert the results to salt effect parameters. The work is classed as tentative.

- 100(1) Oxygen + Potassium hydroxide [1310-58-3] + Water

The solubility of oxygen in aqueous potassium hydroxide has been reported from five laboratories. Geffcken (1) measured the solubility in four solutions at concentrations up to 1.17 mol dm<sup>-3</sup> at 288.15 and 298.15 K. MacArthur (4) measured the solubility in solutions up to 4 mol dm<sup>-3</sup> at 298.15 K. Knaster and Apel'baum (16) measured the solubility in 1, 4, 7 and 10 mol dm<sup>-3</sup> KOH at temperatures of 244.15, 318.15, and 348.15 K. Shoor, Walker, and Gubbins (23) measured the solubility up to 16 mol dm<sup>-3</sup> KOH at the temperatures 298.15, 313.15, 333.15, 353.15 and 373.15 K. Khomutov and Konnik (30) made measurements up to 0.8 mol dm<sup>-3</sup> at 298.15 K.

The salt effect parameters are summarized in the following table.

T/K	Salt Effect Parameter, $k_{sc\alpha}/\text{dm}^3 \text{ mol}^{-1}$				
	Geffcken	MacArthur	Knaster Apel'baum <sup>1</sup>	Shoor, Walker, Gubbins <sup>2</sup>	Khomutov, Konnik
288.15	0.190				
294.15			0.160		
298.15	0.177	0.130		0.180	0.176
313.15				0.168	
318.15			0.160		
333.15				0.159	
348.15			0.160		
353.15				0.157	
373.15				0.155	

<sup>1</sup> The evaluator's judgement of the data, which scatters as individual  $k_{sc\alpha}$  values.

<sup>2</sup> Shoor *et al.* give their parameter as  $k_{scx}/\text{dm}^3 \text{ mol}^{-1} = (1/(c_2/\text{mol dm}^{-3}) \log(x^\circ/x))$  where the  $x^\circ/x$  ratio is the mole fraction ratio. It may not differ much from the  $\alpha^\circ/\alpha$  ratio.

MacArthur's value should be rejected. The others are classed as tentative.

#### 100(2) Oxygen + Potassium fluoride [7789-23-3] + Water

Khomutov and Konnik (30) measured the solubility of oxygen in six air saturated aqueous potassium fluoride solutions at concentrations up to  $0.6 \text{ mol dm}^{-3}$  at 298.15 K. The salt effect parameter,  $k_{sc\alpha}/\text{dm}^3 \text{ mol}^{-1} = 0.203$  is classed as tentative.

#### 100(3) Oxygen + Potassium chloride [7447-40-7] + Water

Four laboratories have reported on the solubility of oxygen in aqueous potassium chloride. MacArthur (4) and Khomutov and Konnik (30) measured the solubility of oxygen in air saturated solutions at concentrations up to 4 and to  $1.2 \text{ mol dm}^{-3}$  respectively at 298.15 K. Eucken and Hertzberg (6) measured the solubility up to concentrations of 2.56 and  $1.52 \text{ mol dm}^{-3}$  at 273.15 and 293.15 K, respectively. Yasunischi (34) made measurements up to concentrations of  $4.1 \text{ mol dm}^{-3}$  at 288.15, 298.15, and 308.15 K.

At concentrations below  $3.2 \text{ mol dm}^{-3}$  Yasunischi considered  $\log(\alpha^\circ/\alpha)$  *vs.*  $c_2$  to be linear, however he gave a two constant equation to fit his data over the entire concentration range.

The salt effect parameters are summarized in the following table.

T/K	Salt Effect Parameter, $k_{sc\alpha}/\text{dm}^3 \text{ mol}^{-1}$			
	MacArthur	Eucken, Hertzberg	Khomutov, Konnik	Yasunischi <sup>1</sup>
273.15		0.178		
288.15				0.106
293.15		0.151		
298.15	0.128		0.129	0.095
308.15				0.087

<sup>1</sup> For use up to  $3.3 \text{ mol dm}^{-3}$  KCl.

For the entire concentration range Yasunischi gives

T/K	Salt Effect Parameter	
	$k_{sc\alpha}^{\circ}/\text{dm}^3\text{mol}^{-1}$	$k'_{sc\alpha}/\text{dm}^3\text{mol}^{-1}$
288.15	0.105	-0.0022
298.15	0.103	0.0378
308.15	0.092	0.0291

The data clearly fall into two groups. The data of MacArthur, Eucken and Hertzberg, and Khomutov and Konnik make one self-consistent group. Yasunischi's data makes up the other group. At present neither group can be preferred. The data are classed as tentative.

- 100(4) Oxygen + Potassium perchlorate [7778-74-7] + Water  
 100(5) Oxygen + Potassium bromide [7758-02-3] + Water  
 100(6) Oxygen + Potassium iodide [7681-11-0] + Water

MacArthur (4) measured the solubility of oxygen in air saturated aqueous KBr and KI solutions, and Khomutov and Konnik (30) measured the solubility of oxygen in air saturated  $\text{KClO}_4$ , KBr and KI solutions. Both worked at a temperature of 298.15 K and analyzed the saturated solutions by a modified Winkler chemical method. Their results agree well, but the MacArthur measurements show more random scatter, thus the Khomutov and Konnik values are preferred. The MacArthur value of  $k_{sc\alpha}$  for KI given below uses the six data points up to a concentration of  $2 \text{ mol dm}^{-3}$ . When the datum of the seventh determination at  $5 \text{ mol dm}^{-3}$  KI is added the  $k_{sc\alpha}$  value increases to 0.101.

T/K	Electrolyte	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter $k_{sc\alpha}/\text{dm}^3 \text{mol}^{-1}$
298.15	$\text{KClO}_4$	8	0 - 0.12	0.150
		5	0 - 1.2	0.117
	4	0 - 4	0.123 <sup>2</sup>	
	KI	7	0 - 1.2	0.093
		7	0 - 5	0.092 <sup>2</sup>

<sup>1</sup> Includes measurement in pure water.

<sup>2</sup> MacArthur's values.

- 100(7) Oxygen + Potassium sulfate [7778-80-5] + Water

Three laboratories report data on this system. Geffcken (1) made measurements at both 288.15 and 298.15 K temperatures. Both MacArthur (4) and Khomutov and Konnik report measurements at 298.15 K. Their results, obtained from the slope of  $\log(\alpha^{\circ}/\alpha)$  vs.  $c_2$  plots, are in the table below.

The data are classed as tentative. At 298.15 K the agreement in the results of Geffcken and MacArthur may be misleading as MacArthur's individual data points scatter badly, while Geffcken's results fall on the line. There appears to be no reason to prefer either the Geffcken or the Khomutov and Konnik data.

T/K	Electrolyte	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter $k_{\text{sc}\alpha}/\text{dm}^3 \text{ mol}^{-1}$
288.15	K <sub>2</sub> SO <sub>4</sub>	5	0 - 0.5	0.375 <sup>2</sup>
298.15	K <sub>2</sub> SO <sub>4</sub>	4	0 - 0.5	0.345 <sup>2</sup>
	K <sub>2</sub> SO <sub>4</sub>	4	0 - 0.5	0.345 <sup>3</sup>
	K <sub>2</sub> SO <sub>4</sub>	5	0 - 0.6	0.297 <sup>4</sup>

<sup>1</sup> Includes measurement in pure water.

<sup>2</sup> Geffcken

<sup>3</sup> MacArthur

<sup>4</sup> Khomutov and Konnik

100(8) Oxygen + Potassium nitrate [7757-79-1] + Water

100(9) Oxygen + Potassium phosphate [7778-53-2] + Water

100(10) Oxygen + Potassium carbonate [584-08-7] + Water

Khomutov and Konnik (30) measured the solubility of oxygen in air saturated potassium salt solutions at 298.15 K by a chemical method. They presented the solubility values on a graph and tabulated the salt effect parameter, which was equivalent to  $k_{\text{sc}\alpha}$ , for each salt. MacArthur (4)

measured the solubility of oxygen in several air saturated potassium nitrate solutions at 298.15 K by a chemical method. The salt effect parameter of Khomutov and Konnik and of MacArthur for potassium nitrate agree within 3 per cent. The data for these solutions are classed as tentative.

T/K	Electrolyte	Number of Determinations <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter $k_{\text{sc}\alpha}/\text{dm}^3 \text{ mol}^{-1}$
298.15	KNO <sub>3</sub>	6	0 - 1.2	0.105
		5	0 - 2	0.102 <sup>2</sup>
	K <sub>3</sub> PO <sub>4</sub>	7	0 - 0.6	0.507
	K <sub>2</sub> CO <sub>3</sub>	7	0 - 1.2	0.379

<sup>1</sup> Includes measurement in pure water.

<sup>2</sup> MacArthur's value.

101(1) Oxygen + Rubidium hydroxide [1310-82-3] + Water

101(2) Oxygen + Rubidium fluoride [13446-74-7] + Water

101(3) Oxygen + Rubidium chloride [7791-11-9] + Water

101(4) Oxygen + Rubidium perchlorate [13510-42-4] + Water

101(5) Oxygen + Rubidium bromide [7789-39-1] + Water

101(6) Oxygen + Rubidium iodide [7790-29-6] + Water

101(7) Oxygen + Rubidium sulfate [7488-54-2] + Water

101(8) Oxygen + Rubidium nitrate [13126-12-0] + Water

Khomutov and Konnik (30) measured the solubility of oxygen in air saturated rubidium salt solutions by a chemical method at 298.15 K. Their solubility values were presented on a graph and the salt effect parameter for each salt was tabulated. The salt effect parameters are classed as tentative. MacArthur (4) measured the solubility of oxygen in air saturated 0.125 mol dm<sup>-3</sup> rubidium chloride at 298.15 K. The value of the salt effect parameter is classed as tentative. The salt effect parameter of Khomutov and Konnik for rubidium chloride solutions is preferred because they made measurements of the oxygen solubility in solutions of several RbCl concentrations with consistent results.

$T/K$	Electrolyte	Number of Measurements <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter $k_{sca}/\text{dm}^3 \text{ mol}^{-1}$
298.15	RbOH	8	0 - 0.5	0.168
	RbF	8	0 - 0.5	0.146
	RbCl	7	0 - 0.5	0.120
		2	0 - 0.125	0.079 <sup>2</sup>
	RbClO <sub>4</sub>	8	0 - 0.1	0.150
	RbBr	7	0 - 0.5	0.104
	RbI	8	0 - 0.5	0.086
	Rb <sub>2</sub> SO <sub>4</sub>	8	0 - 0.3	0.290
	RbNO <sub>3</sub>	5	0 - 0.5	0.096

<sup>1</sup> Includes measurement in pure water.

<sup>2</sup> MacArthur's value.

- 102(1) Oxygen + Cesium hydroxide [21351-79-1] + Water  
 102(2) Oxygen + Cesium fluoride [13400-13-0] + Water  
 102(3) Oxygen + Cesium chloride [7647-17-8] + Water  
 102(4) Oxygen + Cesium bromide [7787-69-1] + Water  
 102(5) Oxygen + Cesium iodide [7789-17-5] + Water  
 102(6) Oxygen + Cesium sulfate [10294-54-9] + Water  
 102(7) Oxygen + Cesium nitrate [7789-18-6] + Water

Khomutov and Konnik(30) measured the solubility of oxygen in air saturated cesium salt solutions by the Winkler chemical method at 298.15 K. Their solubility values were presented on a graph and the salt effect parameter for each salt was tabulated. MacArthur (4) measured the solubility of oxygen in air saturated 0.125 mol dm<sup>-3</sup> cesium chloride solution by a chemical method at 298.15 K. The value is classed as tentative. The salt effect parameter of Khomutov and Konnik for cesium chloride solutions is preferred because they made more measurements over a range of salt concentrations with consistent results.

$T/K$	Electrolyte	Number of Measurements <sup>1</sup>	Concentration Range, $c_2/\text{mol dm}^{-3}$	Salt Effect Parameter $k_{sca}/\text{dm}^3 \text{ mol}^{-1}$
298.15	CsOH	8	0 - 0.5	0.158
	CsF	8	0 - 0.5	0.114
	CsCl	8	0 - 0.5	0.098
		2	0 - 0.125	0.067 <sup>2</sup>
	CsBr	6	0 - 0.5	0.078
	CsI	8	0 - 0.5	0.062
	Cs <sub>2</sub> SO <sub>4</sub>	9	0 - 0.45	0.225
	CsNO <sub>3</sub>	6	0 - 0.5	0.066

<sup>1</sup> Includes measurement in pure water.

<sup>2</sup> MacArthur's value.

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1979, *82*, 487.

<b>COMPONENTS:</b> (1) Oxygen, O <sub>2</sub> ; [7782-44-7] (2) Hydrochloric acid; HCl; [7647-01-0] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Geffcken, G. Z. Phys. Chem. <u>1904</u> , 49, 257-302.	
<b>VARIABLES:</b> T/K = 288-298 Concentration	<b>PREPARED BY:</b> C. L. Young; R. Battino	
<b>EXPERIMENTAL VALUES:</b>		
T/K	Conc of acid/mol dm <sup>3</sup> (soln)	Ostwald coefficient, L
288.15	0.578 0.579 1.170 1.176 1.736 1.982	0.03431 0.03410 0.03217 0.03209 0.03069 0.02988
298.15	0.578 0.578 1.170 1.176 1.736 1.982	0.02963 0.02960 0.02817 0.02833 0.02733 0.02674
<b>AUXILIARY INFORMATION</b>		
<b>METHOD /APPARATUS/PROCEDURE:</b> Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried. (3) Degassed.	
	<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1$ ; $\delta L = \pm 1\%$ . (estimated by compiler).	
	<b>REFERENCES:</b>	

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Geffcken, G.		
(2) Sulfuric acid; H <sub>2</sub> SO <sub>4</sub> ; [7664-93-9]		Z. Phys. Chem. <u>1904</u> , 49, 257-302.		
(3) Water; H <sub>2</sub> O; [7732-18-5]				
VARIABLES:		PREPARED BY:		
T/K = 288-298 Concentration		C.L. Young, R. Battino		
EXPERIMENTAL VALUES:				
T/K	Conc of acid/mol dm <sup>3</sup> (soln)	Ostwald coefficient, L		
288.15	0.2445	0.03366		
	0.2635	0.03375		
	0.4885	0.03210		
	0.5085	0.03217		
	0.9480	0.02886		
	0.9145	0.02930		
	1.4735	0.02584		
	1.7560	0.02399		
	2.4755	0.02174		
	2.6465	0.02067		
	298.15	0.2445	0.02887	
		0.2635	0.02875	
		0.4885	0.02757	
0.5085		0.02745		
0.9480		0.02545		
0.9145		0.02577		
1.4735		0.02285		
1.7560		0.02198		
2.6465	0.01918			
AUXILIARY INFORMATION				
METHOD /APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.		(1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried.		
		(3) Degassed.		
		ESTIMATED ERROR:		
		δT/K = ±0.1; δL = ±1%. (estimated by compiler).		
		REFERENCES:		

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Sulfuric acid; H<sub>2</sub>SO<sub>4</sub>; [7664-93-9]</p> <p>(3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Christoff, A.</p> <p><i>Z. Phys. Chem.</i> <u>1906</u>, 55, 622-34.</p>																	
<p>VARIABLES:</p> <p>T/K = 293.15</p> <p>P/kPa = Atmospheric</p> <p>H<sub>2</sub>SO<sub>4</sub>/wt % = 0 - 95.6</p>	<p>PREPARED BY:</p> <p>M. E. Derrick</p> <p>H. L. Clever</p>																	
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="279 522 1076 743"> <thead> <tr> <th>T/K</th> <th>H<sub>2</sub>SO<sub>4</sub>/wt %</th> <th>m<sub>H<sub>2</sub>SO<sub>4</sub></sub>/mol kg<sup>-1</sup></th> <th>Ostwald Coefficient L x 10<sup>2</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="4">293.15</td> <td>0.0</td> <td>0.0</td> <td>3.046</td> </tr> <tr> <td>35.82</td> <td>5.690</td> <td>1.561</td> </tr> <tr> <td>61.62</td> <td>16.37</td> <td>1.330</td> </tr> <tr> <td>95.6</td> <td>222.</td> <td>3.166</td> </tr> </tbody> </table>		T/K	H <sub>2</sub> SO <sub>4</sub> /wt %	m <sub>H<sub>2</sub>SO<sub>4</sub></sub> /mol kg <sup>-1</sup>	Ostwald Coefficient L x 10 <sup>2</sup>	293.15	0.0	0.0	3.046	35.82	5.690	1.561	61.62	16.37	1.330	95.6	222.	3.166
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<p>AUXILIARY INFORMATION</p>																		
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus was an Ostwald type (1) with a lead capillary tube through which the gas flows to the absorption flask, the gas buret, and the gasometer.</p> <p>The acid solution was degassed by boiling under reflux. The author estimates a one per cent change in the acid concentration due to the degassing procedure. The adsorption flask was filled with solvent, the gas was introduced, and the system shaken until equilibrium was reached.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Prepared by heating KClO<sub>3</sub>.</p> <p>(2) Sulfuric acid. Merck (Darmstadt). Specific gravity 1.271, 1.523, and 1.839 for 35.82, 61.61, and 95.6 wt per cent, respectively.</p> <p>(3) Water. Distilled.</p> <p>ESTIMATED ERROR:</p> <p>δT/K = 0.02 for acid = 0.5 for gas</p> <p>Barometric fluctuations stated to be negligible.</p> <p>REFERENCES:</p> <p>1. Ostwald, W. <i>Lehrbuch der allgem. Chemie</i> (2 Aufl.), 1, 615.</p>																	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7732-44-7] (2) Sulfuric acid; H <sub>2</sub> SO <sub>4</sub> ; [7664-93-9 ] (3) Water; H <sub>2</sub> O; 7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Bohr, C. <i>Z. Physik. Chem.</i> <u>1910</u> , <i>71</i> , 47-50.																																								
<b>VARIABLES:</b> T/K = 294 P/kPa = 101.325 c/N = 0 - 36	<b>PREPARED BY:</b> R. Battino																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="185 518 1243 950"> <thead> <tr> <th>T/K<sup>a</sup></th> <th>Normality<sup>b</sup></th> <th>Ostwald Coeff.<sup>c</sup> 10<sup>2</sup>L</th> <th>Bunsen Coeff.<sup>d</sup> 10<sup>2</sup>α</th> </tr> </thead> <tbody> <tr><td>294.05</td><td>0.0</td><td>3.34</td><td>3.10</td></tr> <tr><td>294.05</td><td>4.9</td><td>2.10</td><td>1.95</td></tr> <tr><td>294.05</td><td>8.9</td><td>1.67</td><td>1.55</td></tr> <tr><td>294.35</td><td>10.7</td><td>1.54</td><td>1.43</td></tr> <tr><td>294.25</td><td>20.3</td><td>1.28</td><td>1.19</td></tr> <tr><td>294.65</td><td>24.8</td><td>1.11</td><td>1.03</td></tr> <tr><td>293.95</td><td>29.6</td><td>1.26</td><td>1.17</td></tr> <tr><td>294.05</td><td>34.3</td><td>2.16</td><td>2.01</td></tr> <tr><td>294.25</td><td>35.8</td><td>2.96</td><td>2.75</td></tr> </tbody> </table> <p> <sup>a</sup> Temperature reported to 0.1°C.  <sup>b</sup> Normality of sulfuric acid solution in g-equiv per liter.  <sup>c</sup> Ostwald coefficient calculated by compiler.  <sup>d</sup> Bunsen coefficient.         </p>		T/K <sup>a</sup>	Normality <sup>b</sup>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α	294.05	0.0	3.34	3.10	294.05	4.9	2.10	1.95	294.05	8.9	1.67	1.55	294.35	10.7	1.54	1.43	294.25	20.3	1.28	1.19	294.65	24.8	1.11	1.03	293.95	29.6	1.26	1.17	294.05	34.3	2.16	2.01	294.25	35.8	2.96	2.75
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<p>VARIABLES:</p> <p style="text-align: center;">T/K = 323-523  Concentration</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C.L. Young</p>																																
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<p>METHOD: /APPARATUS/PROCEDURE:</p> <p>Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p style="text-align: center;">No details given.</p> <hr/> <p>ESTIMATED ERROR:</p> <p style="text-align: center;">δT/K = ±2; δα = ±2%.  (estimated by compiler).</p> <hr/> <p>REFERENCES:</p> <p>1. Pray, H.A.; Stephan, E.L.  <i>Battelle Memorial Institute Report BMI-840, 1953.</i></p>																																

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfuric acid; H <sub>2</sub> SO <sub>4</sub> ; [7664-93-9] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Turchinov, V.V. <i>Nauch. Tr., Irkutsk. Irkutsk. Gos. Nauch.-Issled. Inst. Redk. Tsvet. Metal., 1967, (16), 293-9.</i> <i>Chem. Abstr. 1969, 70, 61694Z.</i>																																																																				
<b>VARIABLES:</b> T/K = 383 P <sub>O<sub>2</sub></sub> /MPa = 0.5-1.5 Concentration	<b>PREPARED BY:</b> V. Katovic																																																																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; text-align: center;"> <thead> <tr> <th colspan="2">C<sub>H<sub>2</sub>SO<sub>4</sub></sub>/</th> <th>P<sub>O<sub>2</sub></sub><sup>a</sup>/atm</th> <th>S<sup>b</sup></th> </tr> <tr> <th colspan="2">gℓ<sup>-1</sup> mole ℓ<sup>-1</sup></th> <th></th> <th></th> </tr> </thead> <tbody> <tr><td>0</td><td>0</td><td>5</td><td>0.09</td></tr> <tr><td>0</td><td>0</td><td>10</td><td>0.175</td></tr> <tr><td>0</td><td>0</td><td>15</td><td>0.275</td></tr> <tr><td>75</td><td>0.756</td><td>5</td><td>0.085</td></tr> <tr><td>75</td><td>0.756</td><td>10</td><td>0.17</td></tr> <tr><td>75</td><td>0.756</td><td>15</td><td>0.255</td></tr> <tr><td>125</td><td>1.275</td><td>5</td><td>0.069</td></tr> <tr><td>125</td><td>1.275</td><td>10</td><td>0.154</td></tr> <tr><td>125</td><td>1.275</td><td>15</td><td>0.24</td></tr> <tr><td>175</td><td>1.785</td><td>5</td><td>0.055</td></tr> <tr><td>175</td><td>1.785</td><td>10</td><td>0.115</td></tr> <tr><td>175</td><td>1.785</td><td>15</td><td>0.175</td></tr> <tr><td>225</td><td>2.30</td><td>5</td><td>0.03</td></tr> <tr><td>225</td><td>2.30</td><td>10</td><td>0.055</td></tr> <tr><td>225</td><td>2.30</td><td>15</td><td>0.087</td></tr> </tbody> </table> <p><sup>a</sup> Partial pressure of oxygen.</p> <p><sup>b</sup> Solubility of oxygen in ml (at standard temperature and pressure) per ml of solution at given pressure.</p>		C <sub>H<sub>2</sub>SO<sub>4</sub></sub> /		P <sub>O<sub>2</sub></sub> <sup>a</sup> /atm	S <sup>b</sup>	gℓ <sup>-1</sup> mole ℓ <sup>-1</sup>				0	0	5	0.09	0	0	10	0.175	0	0	15	0.275	75	0.756	5	0.085	75	0.756	10	0.17	75	0.756	15	0.255	125	1.275	5	0.069	125	1.275	10	0.154	125	1.275	15	0.24	175	1.785	5	0.055	175	1.785	10	0.115	175	1.785	15	0.175	225	2.30	5	0.03	225	2.30	10	0.055	225	2.30	15	0.087
C <sub>H<sub>2</sub>SO<sub>4</sub></sub> /		P <sub>O<sub>2</sub></sub> <sup>a</sup> /atm	S <sup>b</sup>																																																																		
gℓ <sup>-1</sup> mole ℓ <sup>-1</sup>																																																																					
0	0	5	0.09																																																																		
0	0	10	0.175																																																																		
0	0	15	0.275																																																																		
75	0.756	5	0.085																																																																		
75	0.756	10	0.17																																																																		
75	0.756	15	0.255																																																																		
125	1.275	5	0.069																																																																		
125	1.275	10	0.154																																																																		
125	1.275	15	0.24																																																																		
175	1.785	5	0.055																																																																		
175	1.785	10	0.115																																																																		
175	1.785	15	0.175																																																																		
225	2.30	5	0.03																																																																		
225	2.30	10	0.055																																																																		
225	2.30	15	0.087																																																																		
<b>AUXILIARY INFORMATION</b>																																																																					
<b>METHOD/APPARATUS/PROCEDURE:</b> Sulfuric acid (400 ml) was degassed by bubbling with oxygen. The oxygen pressure was increased to desired value and the temperature was raised to 110°C. After stirring for 30 minutes, 20 ml of solution was transferred into a measuring device and cooled to room temperature. Volumes of oxygen and liquid were measured using burets.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.																																																																				
<b>ESTIMATED ERROR:</b> δS/S = ±0.02, author's estimate.																																																																					
<b>REFERENCES:</b>																																																																					

COMPONENTS:		ORIGINAL MEASUREMENTS:				
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Klyueva, A.V.				
(2) Sulfuric acid; H <sub>2</sub> SO <sub>4</sub> ; [7664-93-9]		Tr. Ural. Politekh. Inst., 1967, No. 155, 39-44.				
(3) Water; H <sub>2</sub> O; [7732-18-5]		Chem. Abstr. 1969, 70, 23521e.				
VARIABLES:		PREPARED BY:				
T/K = 50-200		V. Katovic				
P/kPa = 202-1013						
EXPERIMENTAL VALUES:						
Solubility of oxygen <sup>a</sup> in water						
P <sub>O<sub>2</sub></sub> <sup>b</sup> /atm	50°C (323K)	100°C (373K)	125°C (398K)	150°C (423K)	175°C (448K)	200°C (473K)
2	-	0.0118	0.00685	0.00593	-	-
5	0.02347	0.01436	0.00913	0.00926	0.00973	0.00973
10	-	0.02667	0.0131	0.01014	0.01134	0.01240
<sup>a</sup> Solubility of oxygen in mg O <sub>2</sub> per ml H <sub>2</sub> O.						
<sup>b</sup> Partial pressure of oxygen.						
Solubility of oxygen <sup>b</sup> in 0.0125M sulfuric acid (P <sub>O<sub>2</sub></sub> /10 atm)						
Sulfide <sup>a</sup>	100°C (373K)	125°C (398K)	150°C (423K)	175°C (448K)	200°C (473)	
Ni <sub>3</sub> S <sub>2</sub>	0.00917	0.00730	0.00561	0.00718	0.00633	
Cu <sub>2</sub> S	0.00956	0.00825	0.00621	0.0059	0.0057	
Co <sub>4</sub> S <sub>3</sub>	0.00941	0.00653	0.0059	0.00483	0.00479	
<sup>a</sup> Amounts not given.						
<sup>b</sup> Solubility of oxygen in mg O <sub>2</sub> per ml solution.						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:			
Oxygen was determined by the Winkler method.			No details given.			
			ESTIMATED ERROR:			
			REFERENCES:			



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Geffcken, G. <i>Z. Phys. Chem.</i> <u>1904</u> , 49, 257-302.																												
<b>VARIABLES:</b> T/K = 288-298 Concentration	<b>PREPARED BY:</b> C.L. Young; R. Battino.																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Conc of acid/mol dm<sup>3</sup> (soln)</th> <th style="text-align: center;">Ostwald coefficient, <i>L</i></th> </tr> </thead> <tbody> <tr> <td rowspan="5" style="vertical-align: top;">288.15</td> <td>0.492</td> <td>0.03478</td> </tr> <tr> <td>0.494</td> <td>0.03490</td> </tr> <tr> <td>1.00</td> <td>0.03354</td> </tr> <tr> <td>1.008</td> <td>0.03365</td> </tr> <tr> <td>1.88</td> <td>0.03175</td> </tr> <tr> <td rowspan="5" style="vertical-align: top;">298.15</td> <td>1.901</td> <td>0.03166</td> </tr> <tr> <td>0.492</td> <td>0.03021</td> </tr> <tr> <td>0.494</td> <td>0.03016</td> </tr> <tr> <td>1.00</td> <td>0.02954</td> </tr> <tr> <td>1.008</td> <td>0.02964</td> </tr> <tr> <td></td> <td>1.88</td> <td>0.02853</td> </tr> </tbody> </table>		T/K	Conc of acid/mol dm <sup>3</sup> (soln)	Ostwald coefficient, <i>L</i>	288.15	0.492	0.03478	0.494	0.03490	1.00	0.03354	1.008	0.03365	1.88	0.03175	298.15	1.901	0.03166	0.492	0.03021	0.494	0.03016	1.00	0.02954	1.008	0.02964		1.88	0.02853
T/K	Conc of acid/mol dm <sup>3</sup> (soln)	Ostwald coefficient, <i>L</i>																											
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<b>AUXILIARY INFORMATION</b>																													
<b>METHOD /APPARATUS/PROCEDURE:</b> Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried. (3) Degassed. <b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1$ ; $\delta L = \pm 1\%$ . (estimated by compiler). <b>REFERENCES:</b>																												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid· HNO <sub>3</sub> ; [7697-37-2] (3) Nitrogen oxide; NO <sub>2</sub> ; [10102-44-0] (4) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Robertson, G.D., Jr.; Mason, D.M.; Corcoran, W.H. <i>Ind. Eng. Chem.</i> <u>1955</u> , 47, 1470-2.																																																
<b>VARIABLES:</b> T/K = 310.9 - 361.0 Pressure Composition	<b>PREPARED BY:</b> R. Battino																																																
<b>EXPERIMENTAL VALUES:</b> <table style="width:100%; border:none;"> <thead> <tr> <th style="text-align:center;">t/°C</th> <th style="text-align:center;">T/K</th> <th style="text-align:center;"><math>10^3 \alpha / \text{mol dm}^{-3} \text{ atm}^{-1}</math></th> </tr> </thead> </table>		t/°C	T/K	$10^3 \alpha / \text{mol dm}^{-3} \text{ atm}^{-1}$																																													
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<table style="width:100%; border:none;"> <thead> <tr> <th colspan="3" style="text-align:center;">HNO<sub>3</sub></th> </tr> </thead> <tbody> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">5.55</td> </tr> <tr> <td style="text-align:center;">54.4</td> <td style="text-align:center;">327.6</td> <td style="text-align:center;">5.80</td> </tr> <tr> <td colspan="3" style="text-align:center;">85 wt. per cent HNO<sub>3</sub> + 15 wt. per cent NO<sub>2</sub></td> </tr> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">3.60</td> </tr> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">3.73</td> </tr> <tr> <td style="text-align:center;">54.4</td> <td style="text-align:center;">327.6</td> <td style="text-align:center;">3.84</td> </tr> <tr> <td style="text-align:center;">54.4</td> <td style="text-align:center;">327.6</td> <td style="text-align:center;">3.86</td> </tr> <tr> <td colspan="3" style="text-align:center;">94 wt. per cent HNO<sub>3</sub> + 6 wt. per cent H<sub>2</sub>O</td> </tr> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">4.44</td> </tr> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">4.16</td> </tr> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">4.17</td> </tr> <tr> <td style="text-align:center;">37.7</td> <td style="text-align:center;">310.9</td> <td style="text-align:center;">4.05</td> </tr> <tr> <td style="text-align:center;">54.4</td> <td style="text-align:center;">327.6</td> <td style="text-align:center;">4.26</td> </tr> <tr> <td style="text-align:center;">71.1</td> <td style="text-align:center;">344.3</td> <td style="text-align:center;">4.98</td> </tr> <tr> <td style="text-align:center;">87.8</td> <td style="text-align:center;">361.0</td> <td style="text-align:center;">5.63</td> </tr> </tbody> </table>		HNO <sub>3</sub>			37.7	310.9	5.55	54.4	327.6	5.80	85 wt. per cent HNO <sub>3</sub> + 15 wt. per cent NO <sub>2</sub>			37.7	310.9	3.60	37.7	310.9	3.73	54.4	327.6	3.84	54.4	327.6	3.86	94 wt. per cent HNO <sub>3</sub> + 6 wt. per cent H <sub>2</sub> O			37.7	310.9	4.44	37.7	310.9	4.16	37.7	310.9	4.17	37.7	310.9	4.05	54.4	327.6	4.26	71.1	344.3	4.98	87.8	361.0	5.63
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<b>AUXILIARY INFORMATION</b>																																																	
<b>METHOD/APPARATUS/PROCEDURE:</b> A sample of acid and oxygen was confined in a 3 mm i.d. precision-bore glass tube by Fluorolube S. The system was pressurized to ca. 40 atm by adjusting the volume and then agitated. The pressure was lowered to ca. 22 atm while continuing agitation. At equilibrium the solubility was determined from measurements of the liquid and gas phase volumes and the total pressure.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Commercial grade. (2) Prepared as in reference 1. (3) No details given.  <b>ESTIMATED ERROR:</b> $\delta P / \text{atm} = 0 \pm 0.005$ (authors) $\delta T / K = \pm 0.05$ (authors) $\delta \alpha / \alpha = \pm 0.04$ (compiler)  <b>REFERENCES:</b> 1. Reamer, H.H.; Corcoran, W.H.; Sage, B.H. <i>Ind. Eng. Chem.</i> <u>1953</u> , 45, 2699-704.																																																

COMPONENTS:				ORIGINAL MEASUREMENTS:				
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Шапка, A.V.; Atroshchenko, A.V.				
(2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2]				Izv. Vyssh. Ucheb. Zavod., Khim. Khim. Tekhnol. 1971, 14, 1386-8.				
(3) Water; H <sub>2</sub> O; [7732-18-5]				Chem. Abstr. 1972, 76, 28296u.				
VARIABLES:				PREPARED BY:				
T/K = 291-333 P/MPa = 1.1-5.2 Concentration				V. Katovic				
EXPERIMENTAL VALUES:								
C <sub>HNO<sub>3</sub></sub> /%	t/°C	T <sup>a</sup> /K	P/atm	P/atm	P/atm	P/atm	P/atm	
			11 s <sup>b</sup>	21 s <sup>b</sup>	31 s <sup>b</sup>	41 s <sup>b</sup>	51 s <sup>b</sup>	
30	18	291	0.182	0.422	0.606	0.780	1.044	
30	18	291	0.199	0.422	0.609	0.771	1.002	
30	40	313	0.140	0.417	0.565	0.720	0.879	
30	40	313	0.173	0.417	0.602	0.712	0.890	
30	60	333	0.142	0.335	0.507	0.626	0.788	
30	60	333	0.142	0.335	0.523	0.680	0.885	
50	18	291	0.280	0.372	0.681	0.870	1.130	
50	18	291	0.331	0.529	0.760	0.986	1.183	
50	40	313	0.183	0.424	0.699	0.806	0.988	
50	40	313	0.218	0.434	0.644	0.803	0.914	
50	60	333	0.398	0.596	0.806	0.908	1.027	
50	60	333	0.398	0.600	0.708	0.906	1.016	
60	18	291	0.37	0.530	0.733	0.935	1.019	
60	18	291	0.34	0.527	0.737	0.960	0.975	
60	40	313	0.468	0.427	0.827	0.991	1.200	
60	40	313	0.370	0.454	0.750	1.000	1.090	
60	60	333	0.315	0.630	0.840	0.980	0.910	
60	60	333	0.320	0.620	0.770	0.910	0.943	
70	18	291	0.276	0.464	0.750	1.070	1.180	
70	18	291	0.312	0.490	0.785	1.080	1.220	
70	40	313	0.274	0.590	0.820	0.970	1.020	
continued on following page								
AUXILIARY INFORMATION								
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:				
Solubilities determined by an apparatus described in the paper. The technique involved measuring volumes on burets.				No details given.				
				ESTIMATED ERROR:				
				δS/S = ±0.03, compiler's estimate.				
				REFERENCES:				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>EVALUATOR:</b> Shapka, A.V., Atroshchenko, A.V. <i>Izv. Vyssh. Ucheb. Zavod., Khim. Khim. Tekhnol.</i> <u>1971</u> , 14, 1386-8. <i>Chem. Abstr.</i> <u>1972</u> , 76, 28296u.
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## CRITICAL EVALUATION:

continued

C <sub>HNO<sub>3</sub></sub> /%	t/°C	T <sup>a</sup> /K	P/atm	P/atm	P/atm	P/atm	P/atm
			<u>11</u>	<u>21</u>	<u>31</u>	<u>41</u>	<u>51</u>
			s <sup>b</sup>	s <sup>b</sup>	s <sup>b</sup>	s <sup>b</sup>	s <sup>b</sup>
70	40	313	0.310	0.710	0.880	0.975	1.000
70	60	333	0.346	0.590	0.900	1.120	1.390
70	60	333	0.346	0.620	0.900	1.160	1.270

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Solubility in ℓ O<sub>2</sub>(STP)/ℓ solution.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Pogrebnaya, V.L.; Usov, A.P.; Baranov, A.V.; Machigin, A.A. Izv. Vyssh. Uchebn. Zavod., Khim. Khim. Tekhnol. 1972, 15(1), 16-20. Chem. Abstr. 1972, 76, 132165m.																																																																																												
<b>VARIABLES:</b> T/K = 283-333 P/kPa = 101 Concentration	<b>PREPARED BY:</b> V. Katovic																																																																																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th colspan="2" style="text-align: center;">Concentration of acid</th> <th colspan="2" style="text-align: center;">Solubility of oxygen</th> </tr> <tr> <th style="text-align: center;">wt %</th> <th style="text-align: center;">mole %</th> <th style="text-align: center;">10<sup>3</sup>α<sup>a</sup></th> <th style="text-align: center;">10<sup>5</sup>x<sub>1</sub><sup>b</sup></th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">10°C</td> </tr> <tr><td style="text-align: center;">0.0</td><td style="text-align: center;">0.0</td><td style="text-align: center;">38.1</td><td style="text-align: center;">3.07</td></tr> <tr><td style="text-align: center;">6.1</td><td style="text-align: center;">1.8</td><td style="text-align: center;">34.5</td><td style="text-align: center;">2.80</td></tr> <tr><td style="text-align: center;">6.5</td><td style="text-align: center;">2.0</td><td style="text-align: center;">33.9</td><td style="text-align: center;">2.75</td></tr> <tr><td style="text-align: center;">12.2</td><td style="text-align: center;">3.8</td><td style="text-align: center;">30.9</td><td style="text-align: center;">2.53</td></tr> <tr><td style="text-align: center;">12.3</td><td style="text-align: center;">3.8</td><td style="text-align: center;">31.4</td><td style="text-align: center;">2.57</td></tr> <tr><td style="text-align: center;">19.4</td><td style="text-align: center;">6.4</td><td style="text-align: center;">27.5</td><td style="text-align: center;">2.29</td></tr> <tr><td style="text-align: center;">21.3</td><td style="text-align: center;">7.2</td><td style="text-align: center;">26.7</td><td style="text-align: center;">2.23</td></tr> <tr><td style="text-align: center;">30.6</td><td style="text-align: center;">11.2</td><td style="text-align: center;">23.5</td><td style="text-align: center;">2.03</td></tr> <tr><td style="text-align: center;">32.1</td><td style="text-align: center;">11.9</td><td style="text-align: center;">22.9</td><td style="text-align: center;">1.98</td></tr> <tr><td style="text-align: center;">44.8</td><td style="text-align: center;">18.8</td><td style="text-align: center;">19.6</td><td style="text-align: center;">1.79</td></tr> <tr><td style="text-align: center;">46.2</td><td style="text-align: center;">19.7</td><td style="text-align: center;">19.3</td><td style="text-align: center;">1.78</td></tr> <tr><td style="text-align: center;">55.3</td><td style="text-align: center;">26.1</td><td style="text-align: center;">18.5</td><td style="text-align: center;">1.81</td></tr> <tr><td style="text-align: center;">57.1</td><td style="text-align: center;">27.5</td><td style="text-align: center;">18.5</td><td style="text-align: center;">1.83</td></tr> <tr><td style="text-align: center;">58.4</td><td style="text-align: center;">28.6</td><td style="text-align: center;">17.8</td><td style="text-align: center;">1.78</td></tr> <tr> <td colspan="4" style="text-align: center;">20°C</td> </tr> <tr><td style="text-align: center;">0.0</td><td style="text-align: center;">0.0</td><td style="text-align: center;">30.9</td><td style="text-align: center;">2.49</td></tr> <tr><td style="text-align: center;">6.9</td><td style="text-align: center;">2.1</td><td style="text-align: center;">29.0</td><td style="text-align: center;">2.36</td></tr> <tr><td style="text-align: center;">9.1</td><td style="text-align: center;">2.8</td><td style="text-align: center;">28.2</td><td style="text-align: center;">2.31</td></tr> <tr><td style="text-align: center;">15.1</td><td style="text-align: center;">4.9</td><td style="text-align: center;">26.6</td><td style="text-align: center;">2.21</td></tr> <tr><td style="text-align: center;">16.1</td><td style="text-align: center;">5.2</td><td style="text-align: center;">26.1</td><td style="text-align: center;">2.18</td></tr> </tbody> </table> <p style="text-align: right;">continued on following page</p>		Concentration of acid		Solubility of oxygen		wt %	mole %	10 <sup>3</sup> α <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>	10°C				0.0	0.0	38.1	3.07	6.1	1.8	34.5	2.80	6.5	2.0	33.9	2.75	12.2	3.8	30.9	2.53	12.3	3.8	31.4	2.57	19.4	6.4	27.5	2.29	21.3	7.2	26.7	2.23	30.6	11.2	23.5	2.03	32.1	11.9	22.9	1.98	44.8	18.8	19.6	1.79	46.2	19.7	19.3	1.78	55.3	26.1	18.5	1.81	57.1	27.5	18.5	1.83	58.4	28.6	17.8	1.78	20°C				0.0	0.0	30.9	2.49	6.9	2.1	29.0	2.36	9.1	2.8	28.2	2.31	15.1	4.9	26.6	2.21	16.1	5.2	26.1	2.18
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<b>METHOD/APPARATUS/PROCEDURE:</b> Solubilities determined using an apparatus described in the paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Obtained by electrolysis. (2) No details given.  <b>ESTIMATED ERROR:</b> δα/α = ±0.03, authors' estimate. δT/K = ±0.1  <b>REFERENCES:</b>																																																																																												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>EVALUATOR:</b> Pogrebnaya, V.L.; Usov, A.P.; Baranov, A.V.; Machigin, A.A. <i>Izv. Vyssh. Uchebn. Zavod., Khim.</i> <i>Khim. Tekhnol.</i> 1972, 15(1), 16-20 <i>Chem. Abstr.</i> 1972, 76,132165m.
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Concentration of acid		Solubility of oxygen	
wt %	mole %	10 <sup>3</sup> α <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>
21.7	7.3	25.0	2.10
21.1	7.0	24.6	2.08
31.1	11.4	22.3	1.94
33.2	12.4	22.0	1.93
40.7	16.4	20.3	1.84
41.4	16.8	20.0	1.82
56.8	27.3	19.0	1.91
58.1	28.4	19.2	1.75
58.7	28.9	18.8	1.91
25°C			
0.0	0.0	28.5	2.29
6.6	2.0	26.8	2.19
9.4	2.9	26.1	2.15
12.8	4.0	25.5	2.11
15.0	4.7	25.8	2.08
23.4	8.0	23.3	1.98
28.5	10.2	22.3	1.93
28.7	10.3	22.1	1.91
41.7	17.0	20.2	1.85
45.3	19.1	20.1	1.87
47.9	20.8	19.7	1.86
53.8	24.9	19.6	1.93
54.2	25.3	19.5	1.93
54.8	25.7	19.5	1.94
30°C			
0.0	0.0	26.2	2.12
6.9	2.1	25.0	2.05
8.0	2.4	24.6	2.02
13.1	4.1	23.9	1.98
23.4	8.0	22.4	1.91
25.1	8.7	21.9	1.88
32.1	11.9	20.8	1.83
35.5	13.6	20.5	1.83
42.4	17.4	19.8	1.82
44.3	18.5	19.9	1.86
49.6	22.0	20.0	1.92
54.0	25.4	20.2	2.00
54.1	25.2	19.9	1.97
57.3	27.7	20.0	2.04
40°C			
0.0	0.0	23.0	1.86
9.6	2.9	22.1	1.83
10.3	3.2	21.9	1.81
12.0	3.7	21.7	1.81
20.4	6.8	21.0	1.79
20.9	7.0	20.9	1.78
21.5	7.3	20.6	1.76
32.4	12.0	20.5	1.81
33.1	12.4	20.1	1.79
41.5	16.8	19.9	1.84
46.7	20.0	20.0	1.90
53.3	24.6	20.1	2.00
57.8	28.1	21.0	2.16
58.3	28.5	20.0	2.13

continued on following page

COMPONENTS:	EVALUATOR:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Pogrebnyaya, V.L.; Usov, A.P.;
(2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2]	Baranov, A.V.; Machigin, A.A.
(3) Water; H <sub>2</sub> O; [7732-18-5]	Izv. Vyssh. Uchbn. Zavod., Khim. Khim. Tekhnol. 1972, 15 (1), 16-20. Chem. Abstr. 1972, 76, 132165m.

CRITICAL EVALUATION: continued

Concentration of acid		Solubility of oxygen	
wt %	mole %	10 <sup>3</sup> α <sup>a</sup>	10 <sup>5</sup> x <sub>1</sub> <sup>b</sup>
50°C			
0.0	0.0	21.0	1.71
5.9	1.8	20.6	1.70
7.2	2.2	20.5	1.69
14.3	4.6	20.0	1.68
14.9	4.8	20.5	1.73
22.7	7.7	20.2	1.74
23.4	8.0	20.0	1.73
33.4	12.5	19.8	1.77
34.3	13.0	19.5	1.76
35.1	13.4	19.7	1.78
52.3	23.9	21.0	2.09
53.4	24.7	20.7	2.08
57.6	28.0	21.3	2.21
58.8	29.0	22.2	2.33
60°C			
0.0	0.0	19.4	1.59
10.6	3.3	19.0	1.59
11.4	3.6	18.9	1.59
22.1	7.5	19.4	1.68
24.7	8.6	19.0	1.66
25.6	8.9	19.2	1.68
34.8	13.2	19.0	1.72
35.3	13.5	19.3	1.76
43.9	18.3	20.1	1.92
47.2	20.4	20.3	1.97
50.4	22.5	21.2	2.11
54.5	25.5	21.8	2.23
55.9	26.6	21.6	2.23
58.3	28.6	22.5	2.37

a Bunsen coefficient.

b Mole fraction solubility at 101 kPa partial pressure of gas. Mole fraction is for O<sub>2</sub>, HNO<sub>3</sub>, and H<sub>2</sub>O as components.

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (3) Water; H <sub>2</sub> O; [7732-18-5]				Shapka, A. V.; Atroshchenko, A. V. <i>Zh. Prikl. Khim.</i> 1973, 46, 2759-61. <i>J. Appl. Chem. USSR (Engl. trans.)</i> 1973, 46, 2915-7.			
VARIABLES:				PREPARED BY:			
T/K - 291-332 P/bar = 11-52 Concentration				C. L. Young			
EXPERIMENTAL VALUES:							
T/K	P <sup>a</sup> /bar	Conc. <sup>b</sup> of nitric acid, %	Solubility <sup>c</sup>	T/K	P <sup>a</sup> /bar	Conc. <sup>b</sup> of nitric acid, %	Solubility <sup>c</sup>
291.15	11.1	80	0.41	313.15	41.5	90	2.37
	21.1		0.84		51.7		2.93
	31.4		1.27	333.15	11.1		0.74
	41.5		1.70		21.1		1.35
	51.7		2.12		31.4		1.96
313.15	11.1		0.47		41.5		2.58
	21.1		0.96		51.7		3.18
	31.4		1.44	291.15	11.1	98	0.97
	41.5		1.92		21.1		1.80
	51.7		2.40		31.4		2.63
333.15	11.1		0.57		41.5		3.45
	21.1		1.05		51.7		4.27
	31.4		1.55	313.15	11.1		1.10
	41.5		2.17		21.1		2.0
	51.7		2.70		31.4		2.89
291.15	11.1	90	0.57		41.5		3.78
	21.1		1.05		51.7		4.65
	31.4		1.55	333.15	11.1		1.35
	41.5		2.03		21.1		2.35
	51.7		2.51		31.4		3.34
313.15	11.1		0.67		41.5		4.32
	21.1		1.24		51.7		5.29
	31.4		1.80				
Continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Static cell fitted with stirrer. Oxygen admitted at pressure of 100 atmospheres with periodic stirring. Pressure reduced to required pressure and solution rapidly stirred. After equilibration liquid sample withdrawn and analysed volumetrically. Details in source.				No details given.			
				ESTIMATED ERROR: $\delta T/K = \pm 1$ ; $\delta P/\text{bar} = \pm 0.3$ ; $\delta \alpha = \pm 2\%$ (estimated by compiler).			
				REFERENCES:			



<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7797-37-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>EVALUATOR:</b>  Shapka, A.V.; Atroshchenko. A.V. <i>Zh. Prikl. Khim.</i> <u>1973</u> , 46, 2759-61. <i>J. Appl. Chem. USSR (Engl. trans.)</i> <u>1973</u> , 46, 2915-7.
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**CRITICAL EVALUATION:**

continued

- a Pressure reported as 11, 21, 31, 41, 51 atm.
- b Although the authors do not identify the %, it appears to be wt %.
- c Solubility is in dm<sup>3</sup>(STP) dm<sup>-3</sup> at the pressure of the measurement. Divide by the pressure (in atm) to obtain the Bunsen coefficient.

EXPERIMENTAL VALUES:				EXPERIMENTAL VALUES:			
T/K	P <sup>a</sup> /bar	Conc. of nitric acid, wt-%	Solubility <sup>b</sup>	T/K	P <sup>a</sup> /bar	Conc. of nitric acid, wt-%	Solubility <sup>b</sup>
293.15	10.1	11	0.215	333.15	10.1	11	0.154
	20.2		0.477		20.2		0.343
	30.4		0.703		30.4		0.509
	40.5		0.924		40.5		0.683
	50.7		1.169		50.7		0.848
	60.8		1.374		60.8		1.003
303.15	10.1		0.209	353.15	10.1		0.165
	20.2		0.426		20.2		0.316
	30.4		0.633		30.4		0.484
	40.5		0.838		40.5		0.629
	50.7		1.022		50.7		0.796
	60.8		1.226		60.8		0.911
313.15	10.1		0.198	293.15	10.1	21	0.227
	20.2		0.398		20.2		0.439
	30.4		0.578		30.4		0.659
	40.5		0.764		40.5		0.840
	50.7		0.948		50.7		1.058
	60.8		1.11		60.8		1.264
323.15	10.1		0.192	303.15	10.1		0.185
	20.2		0.376		20.2		0.414
	30.4		0.535		30.4		0.581
	40.5		0.705		40.5		0.775
	50.7		0.892		50.7		0.951
	60.8		1.049				

Continued on following page

## AUXILIARY INFORMATION

## METHOD/APPARATUS/PROCEDURE:

Static cell of 1 l capacity fitted with electromagnetic stirrer. Temperature measured with mercury thermometer and pressure with a Bourdon gauge. Liquid sample analysed by stripping out oxygen and measuring amount volumetrically. Details in source.

## SOURCE AND PURITY OF MATERIALS:

No details given.

## ESTIMATED ERROR:

 $\delta T/K = \pm 0.2$ ;  $\delta P/\text{bar} = \pm 0.3$ ; $\delta \alpha = \pm 4\%$  (estimated by compiler).

## REFERENCES:

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Pogrebnyaya, V. L.; Usov, A. P.;			
(2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2]				Baranov, A. V.			
(3) Water; H <sub>2</sub> O; [7732-18-5]				<i>Zhur. Prikl. Khim.</i> 1977, 50, 12-16.			
				<i>J. Appl. Chem. USSR (Engl. trans.)</i>			
				1977, 50, 10-13			
EXPERIMENTAL VALUES:				continued			
T/K	P <sup>a</sup> /bar	Conc. of nitric acid, wt-%	Solubility <sup>b</sup>	T/K	P <sup>a</sup> /bar	Conc. of nitric acid, wt-%	Solubility <sup>b</sup>
303.15	60.8	21	1.135	353.15	50.7	30	0.826
313.15	10.1		0.189		60.8		1.002
	20.2		0.371	293.15	10.1	42	0.190
	30.4		0.566		20.2		0.367
	40.5		0.579		30.4		0.538
	50.7		0.724		40.5		0.708
	60.8		1.099		50.7		0.888
323.15	10.1		0.168		60.8		1.069
	20.2		0.353	303.15	10.1		0.186
	30.4		0.550		20.2		0.354
	40.5		0.687		30.4		0.533
	50.7		0.859		40.5		0.698
	60.8		1.062		50.7		0.896
333.15	10.1		0.168		60.8		0.988
	20.2		0.383	313.15	10.1		0.178
	30.4		0.529		20.2		0.354
	40.5		0.686		30.4		0.529
	50.7		0.840		40.5		0.698
	60.8		0.976		50.7		0.896
353.15	10.1		0.179		60.8		0.988
	20.2		0.335	323.15	10.1		0.185
	30.4		0.495		20.2		0.355
	40.5		0.661		30.4		0.527
	50.7		0.833		40.5		0.718
	60.8		0.966		50.7		0.886
293.15	10.1	30	0.237		60.8		1.014
	20.2		0.406	333.15	10.1		0.177
	30.4		0.602		20.2		0.370
	40.5		0.806		30.4		0.515
	50.7		0.978		40.5		0.703
	60.8		1.164		50.7		0.891
303.15	10.1		0.186		60.8		1.036
	20.2		0.381	353.15	10.1		0.211
	30.4		0.588		20.2		0.383
	40.5		0.777		30.4		0.572
	50.7		0.931		40.5		0.793
	60.8		1.078		50.7		0.896
313.15	10.1		0.244		60.8		1.056
	20.2		0.402	293.15	10.1	53	0.200
	30.4		0.561		20.2		0.369
	40.5		0.719		30.4		0.527
	50.7		0.886		40.5		0.689
	60.8		1.053		50.7		0.886
323.15	10.1		0.209		60.8		1.039
	20.2		0.374	303.15	10.1		0.186
	30.4		0.539		20.2		0.365
	40.5		0.722		30.4		0.536
	50.7		0.895		40.5		0.671
	60.8		1.007		50.7		0.861
333.15	10.1		0.165		60.8		1.033
	20.2		0.350	313.15	10.1		0.195
	30.4		0.547		20.2		0.394
	40.5		0.691		30.4		0.561
	50.7		0.858		40.5		0.714
	60.8		1.037		50.7		0.856
353.15	10.1		0.179		60.8		1.048
	20.2		0.353	323.15	10.1		0.207
	30.4		0.513		20.2		0.389
	40.5		0.682				

Continued on following page

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Pogrebnaya, V. L.; Usov, A. P.;			
(2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2]				Baranov, A. V.			
(3) Water; H O; [7732-18-5]				<i>Zhur. Prikl. Khim.</i> 1977, 50, 12-16. <i>J. Appl. Chem. USSR (Engl. trans.)</i> 1977, 50, 10-13			
EXPERIMENTAL VALUES:				continued			
T/K	a P/bar	Conc. of nitric acid, wt-%	Solubility <sup>b</sup>		P <sup>a</sup> /bar	Conc. of nitric acid, wt-%	Solubility <sup>b</sup>
323.15	30.4	53	0.581	313.15	20.2	85	0.85
	40.5		0.731		30.4		1.48
	50.7		0.945		40.5		1.69
	60.8		1.078		50.7		1.94
333.15	10.1		0.204	323.15	60.8		2.20
	20.2		0.396		10.1		0.66
	30.4		0.604		20.2		0.89
	40.5		0.787		30.4		1.307
	50.7		0.969		40.5		1.748
	60.8		1.078		50.7		2.133
293.15	10.1	70	0.225	333.15	60.8		2.538
	20.2		0.425		20.2		0.99
	30.4		0.631		30.4		1.460
	40.5		0.839		40.5		1.950
	50.7		1.057		50.7		2.379
	60.8		1.243		60.8		2.780
303.15	10.1		0.234	353.15	20.2		1.101
	20.2		0.448		30.4		1.619
	30.4		0.671		40.5		2.116
	40.5		0.856	293.15	10.1	99	0.761
	50.7		1.082		20.2		1.498
	60.8		1.289		30.4		2.191
313.15	10.1		0.259		40.5		3.017
	20.2		0.513		50.7		3.594
	30.4		0.764		60.8		4.398
	40.5		0.970	303.15	10.1		0.741
	50.7		1.174		20.2		1.539
	60.8		1.443		30.4		2.246
323.15	10.1		0.255		40.5		2.994
	20.2		0.526		50.7		3.219
	30.4		0.792		60.8		4.481
	40.5		1.048	313.15	10.1		0.789
	50.7		1.309		20.2		1.709
	60.8		1.508		30.4		2.391
333.15	20.2		0.557		40.5		3.119
	30.4		0.829		50.7		3.841
	40.5		1.070		60.8		4.739
	50.7		1.320	323.15	10.1		0.847
	60.8		1.576		20.2		1.776
353.15	10.1		0.311		30.4		2.516
	20.2		0.688		40.5		3.452
	30.4		1.011		50.7		4.273
	60.8		1.774		60.8		4.774
293.15	20.2	85	0.75	333.15	10.1		0.877
	30.4		1.086		20.2		1.733
	40.5		1.438		30.4		2.451
	50.7		1.794		40.5		3.503
	60.8		2.154		50.7		4.191
303.15	20.2		0.74		60.8		4.993
	30.4		1.17	353.15	10.1		0.984
	40.5		1.45		20.2		1.895
	50.7		1.82		30.4		2.793
	60.8		2.23				

<sup>a</sup> Pressure in original paper as 10, 20, 30, 40, 50, 60 atm.

<sup>b</sup> Solubility is in liters of O<sub>2</sub> per liter of solution under the oxygen pressure listed.

COMPONENTS:			ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (3) Dinitrogen Tetroxide; N <sub>2</sub> O <sub>4</sub> ; [10544-72-6] (4) Water; H <sub>2</sub> O; [7732-18-5]			Sprague, R.W. <i>Ind. Eng. Chem.</i> <u>1955</u> , 47, 2396-8.			
VARIABLES:			PREPARED BY:			
Composition T/K = 298			R. Battino			
EXPERIMENTAL VALUES:						
All measurements at 25°C						
%HNO <sub>3</sub>	%N <sub>2</sub> O <sub>4</sub>	%H <sub>2</sub> O	10 <sup>2</sup> α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>	10 <sup>2</sup> /cm <sup>3</sup> (STP) O <sub>2</sub> g <sup>-1</sup>	10 <sup>3</sup> /moles O <sub>2</sub> lit <sup>-1</sup> atm <sup>-1</sup>	10 <sup>4</sup> /moles O <sub>2</sub> g <sup>-1</sup> atm <sup>-1</sup>
100	0	0	6.59	4.37	2.94	1.95
93.94	0	6.06	4.57	3.08	2.04	1.37
90.10	0	9.90	2.99	2.03	1.33	0.904
85.15	0	14.85	1.86	1.27	0.828	0.566
80.97	0	19.03	1.58	1.08	0.703	0.483
69.11	0	30.89	1.99	1.42	0.886	0.632
92.52	7.48	0	6.59	4.30	2.94	1.92
88.69	11.31	0	6.00	3.72	2.67	1.66
85.64	14.36	0	4.26	2.68	1.90	1.20
79.99	20.01	0	3.82	2.44	1.71	1.09
0	0	100	2.3			
a All compositions are in weight per cent. b α is the Bunsen coefficient. c In the fifth column g refers to grams of solvent or solution. d The sixth and seventh columns are Henry's law constants in the units indicated. e All values are the author's.						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:			
A borosilicate glass cell of volume ca. 25cm <sup>3</sup> and with graduated end sections was used. A sample of acid was weighed into the cell and frozen solid. A magnetically-driven stirrer sealed in glass did the stirring. The liquids were confined over perfluorinated kerosine. Gas was introduced. Pressures were read on a Heise gage to 0.5 psi, and volumes to ±0.001 cm <sup>3</sup> . After equilibration the solubility was determined by measuring the pressure and the gas and liquid volumes.			(1) "Used directly from the cylinder." (2) Prepared by low-pressure distillation from potassium nitrate and concentrated sulfuric acid and condensed at dry ice-alcohol temperature. (3) Prepared by the method of Whittaker et al. (1). (4) Distilled. 1 to 2 ppm conductive materials.			
			ESTIMATED ERROR:			
			δα/α = ±0.2 (compiler's estimates).			
			REFERENCES:			
			1. Whittaker, A.G.; Sprague, R.W.; Skolnik, S.; Smith, G.B.L. <i>J. Am. Chem. Soc.</i> <u>1952</u> , 74, 4794-7.			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ammonium hydroxide; NH <sub>4</sub> OH; [1336-21-6] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Bruhn, G.; Gerlach, J.; Pawlek, F. <i>Z. Anorg. Allgem. Chem.</i> <u>1965</u> , 337, 68-79.																															
<b>VARIABLES:</b>  T/K = 323-423	<b>PREPARED BY:</b>  C.L. Young																															
<b>EXPERIMENTAL VALUES:</b>																																
<table border="1"> <thead> <tr> <th data-bbox="159 486 207 511">T/K</th> <th data-bbox="334 486 698 511">Conc of hydroxide/mol l<sup>-1</sup></th> <th data-bbox="800 486 1080 537">Bunsen coefficient, α/cm<sup>3</sup>(STP)cm<sup>-3</sup> atm<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td data-bbox="132 570 221 595" rowspan="3">323.15</td> <td data-bbox="484 570 540 595">2.87</td> <td data-bbox="873 570 975 595">0.02025</td> </tr> <tr> <td data-bbox="484 595 540 621">5.63</td> <td data-bbox="873 595 975 621">0.01908</td> </tr> <tr> <td data-bbox="484 621 540 646">8.28</td> <td data-bbox="873 621 975 646">0.01840</td> </tr> <tr> <td data-bbox="132 652 221 678" rowspan="3">348.15</td> <td data-bbox="484 652 540 678">2.87</td> <td data-bbox="873 652 975 678">0.01765</td> </tr> <tr> <td data-bbox="484 678 540 703">5.63</td> <td data-bbox="873 678 975 703">0.01619</td> </tr> <tr> <td data-bbox="484 703 540 729">8.28</td> <td data-bbox="873 703 975 729">0.01593</td> </tr> <tr> <td data-bbox="132 735 221 760" rowspan="3">373.15</td> <td data-bbox="484 735 540 760">2.87</td> <td data-bbox="873 735 975 760">0.01570</td> </tr> <tr> <td data-bbox="484 760 540 785">5.63</td> <td data-bbox="873 760 975 785">0.01575</td> </tr> <tr> <td data-bbox="484 785 540 811">8.28</td> <td data-bbox="873 785 975 811">0.01469</td> </tr> <tr> <td data-bbox="132 817 221 842" rowspan="3">423.15</td> <td data-bbox="484 817 540 842">2.87</td> <td data-bbox="873 817 975 842">0.01918</td> </tr> <tr> <td data-bbox="484 842 540 868">5.63</td> <td data-bbox="873 842 975 868">0.01833</td> </tr> <tr> <td data-bbox="484 868 540 893">8.28</td> <td data-bbox="873 868 975 893">0.01760</td> </tr> </tbody> </table>		T/K	Conc of hydroxide/mol l <sup>-1</sup>	Bunsen coefficient, α/cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	323.15	2.87	0.02025	5.63	0.01908	8.28	0.01840	348.15	2.87	0.01765	5.63	0.01619	8.28	0.01593	373.15	2.87	0.01570	5.63	0.01575	8.28	0.01469	423.15	2.87	0.01918	5.63	0.01833	8.28	0.01760
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<b>AUXILIARY INFORMATION</b>																																
<b>METHOD/APPARATUS/PROCEDURE:</b>  Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details given.  <b>ESTIMATED ERROR:</b>  δT/K = ±2; δα = ±2%. (estimated by compiler).  <b>REFERENCES:</b>  1. Pray, H.A.; Stephan, E.L. <i>Battelle Memorial Institute Report BMI-840, 1953.</i>																															

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfuric acid, Ammonium salt; (NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub> ; [7783-20-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Bruhn, G.; Gerlach, J.; Pawlek, F. <i>Z. Anorg. Allgem. Chem.</i> <u>1965</u> , 337, 68-79.	
<b>VARIABLES:</b> T/K - 298-473 Concentration	<b>PREPARED BY:</b> C.L. Young	
<b>EXPERIMENTAL VALUES:</b>		
T/K	Conc of salt/mol l <sup>-1</sup>	$\alpha^a$ /cm <sup>3</sup> (STP) cm <sup>3</sup> atm <sup>-1</sup>
298.15	0.25 0.75 1.5 3.0	0.0248 0.0195 0.0133 0.0081
323.15	0.25 0.75 1.5 3.0	0.0186 0.0148 0.0095 0.0072
373.15	0.25 0.75 1.5 3.0	0.0149 0.0131 0.0082 0.0050
423.15	0.75 1.5 3.0	0.01429 0.00865 0.00656
473.15	1.5 3.0	0.01241 0.00812
<sup>a</sup> Bunsen coefficient.		
<b>AUXILIARY INFORMATION</b>		
<b>METHOD/APPARATUS/PROCEDURE:</b>  Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details given.	
	<b>ESTIMATED ERROR:</b>  $\delta T/K = \pm 2$ ; $\delta \alpha = \pm 2\%$ . (estimated by compiler).	
	<b>REFERENCES:</b>  1. Pray, H.A.; Stephan, E.L. <i>Battelle Memorial Institute Report BMI-840</i> , <u>1953</u> .	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Aluminum chloride; AlCl <sub>3</sub> ; [7446-70-0] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A.  <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.																																										
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 2.204	<b>PREPARED BY:</b>  H. L. Clever																																										
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="352 458 935 870" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Aluminum chloride c<sub>3</sub>/mol dm<sup>-3</sup></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.0</td> <td>0.03114<sup>1</sup></td> </tr> <tr> <td></td> <td>0.309</td> <td>0.02532</td> </tr> <tr> <td></td> <td>0.365</td> <td>0.02465</td> </tr> <tr> <td></td> <td>0.599</td> <td>0.02107</td> </tr> <tr> <td></td> <td>0.606</td> <td>0.02102</td> </tr> <tr> <td></td> <td>0.724</td> <td>0.01971</td> </tr> <tr> <td></td> <td>0.831</td> <td>0.01840</td> </tr> <tr> <td></td> <td>1.182</td> <td>0.01460</td> </tr> <tr> <td></td> <td>1.524</td> <td>0.01188</td> </tr> <tr> <td></td> <td>1.696</td> <td>0.01074</td> </tr> <tr> <td></td> <td>1.732</td> <td>0.01058</td> </tr> <tr> <td></td> <td>1.897</td> <td>0.01012</td> </tr> <tr> <td></td> <td>2.204</td> <td>0.00887</td> </tr> </tbody> </table> <p><sup>1</sup>Value from reference 1.</p> <p>Up to a concentration of 1.7 mol dm<sup>-3</sup> AlCl<sub>3</sub> the data correlates with the Setschenow equation <math>\log(L_0/L) = 0.274 c_3</math>.</p> <p>Over the entire concentration range the empirical equation <math>\log(L_0/L) = 0.303 c_3 / (1 + 0.0859 c_3)</math> correlates the data better.</p>		T/K	Aluminum chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L	298.15	0.0	0.03114 <sup>1</sup>		0.309	0.02532		0.365	0.02465		0.599	0.02107		0.606	0.02102		0.724	0.01971		0.831	0.01840		1.182	0.01460		1.524	0.01188		1.696	0.01074		1.732	0.01058		1.897	0.01012		2.204	0.00887
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<b>AUXILIARY INFORMATION</b>																																											
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used.  The aqueous salt solution is degassed by boiling under reflux and under vacuum.  The gas phase volume and the solvent volume are measured by displacement of mercury.  Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded.  The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. High purity grade stated to be 99.995 per cent.  (2) Aluminum chloride.  (3) Water. No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89.																																										



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Aluminum sulfate; Al <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub> ; [10043-01-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A.  <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.																														
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 0.812	<b>PREPARED BY:</b> H. L. Clever																														
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="400 463 971 781" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Aluminum sulfate c<sub>3</sub>/mol dm<sup>-3</sup></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">0.0</td> <td style="text-align: center;">0.03114<sup>1</sup></td> </tr> <tr> <td></td> <td style="text-align: center;">0.138</td> <td style="text-align: center;">0.02466</td> </tr> <tr> <td></td> <td style="text-align: center;">0.236</td> <td style="text-align: center;">0.02115</td> </tr> <tr> <td></td> <td style="text-align: center;">0.378</td> <td style="text-align: center;">0.01639</td> </tr> <tr> <td></td> <td style="text-align: center;">0.430</td> <td style="text-align: center;">0.01528</td> </tr> <tr> <td></td> <td style="text-align: center;">0.501</td> <td style="text-align: center;">0.01340</td> </tr> <tr> <td></td> <td style="text-align: center;">0.643</td> <td style="text-align: center;">0.01024</td> </tr> <tr> <td></td> <td style="text-align: center;">0.674</td> <td style="text-align: center;">0.00964</td> </tr> <tr> <td></td> <td style="text-align: center;">0.812</td> <td style="text-align: center;">0.00766</td> </tr> </tbody> </table> <p data-bbox="373 791 633 817"><sup>1</sup>From reference 1.</p> <p data-bbox="373 836 969 890">The author correlated the data with the Setschenow equation <math>\log(L_Q/L) = 0.745 c_3</math>.</p>		T/K	Aluminum sulfate c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L	298.15	0.0	0.03114 <sup>1</sup>		0.138	0.02466		0.236	0.02115		0.378	0.01639		0.430	0.01528		0.501	0.01340		0.643	0.01024		0.674	0.00964		0.812	0.00766
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used. The aqueous salt solution is degassed by boiling under reflux and under vacuum. The gas phase volume and the solvent volume are measured by displacement of mercury. Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded. The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. High purity grade stated to be 99.995 per cent. (2) Aluminum sulfate. (3) Water. No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89.																														

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hydrates aluminum oxide; Al <sub>2</sub> O <sub>3</sub> ·xH <sub>2</sub> O; [1333-84-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Shkol'nikova, R. I.  <i>Uch. Zap. Leningr. Gos. Univ., Ser. Khim. Nauk.</i> <u>1959</u> , Nr. 18, 64-86.  <i>Chem. Abstr.</i> <u>1961</u> , 55, 25443b.																								
<b>VARIABLES:</b> T/K= 293.15 - 313.15 P/kPa= 101.325 Al <sub>2</sub> O <sub>3</sub> /Wt % = 0.1 - 0.42	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th>T/K</th> <th>Al<sub>2</sub>O<sub>3</sub>/Wt %</th> <th>Bunsen Coefficient <math>\alpha \times 10^3</math></th> </tr> </thead> <tbody> <tr> <td rowspan="3">293.15</td> <td>0.1</td> <td>31.0</td> </tr> <tr> <td>0.35</td> <td>28.7</td> </tr> <tr> <td>0.42</td> <td>26.0</td> </tr> <tr> <td rowspan="3">303.15</td> <td>0.1</td> <td>26.5</td> </tr> <tr> <td>0.35</td> <td>26.5</td> </tr> <tr> <td>0.42</td> <td>21.0</td> </tr> <tr> <td rowspan="3">313.15</td> <td>0.1</td> <td>23.1</td> </tr> <tr> <td>0.35</td> <td>23.1</td> </tr> <tr> <td>0.42</td> <td>16.5</td> </tr> </tbody> </table> <p>The enthalpy of solution of oxygen was calculated from the temperature coefficient of the Bunsen coefficient. It is 2780, 2680, 3250, and 4150 cal mol<sup>-1</sup> in water, and 0.1, 0.35, and 0.42 wt % Al<sub>2</sub>O<sub>3</sub> respectively.</p>		T/K	Al <sub>2</sub> O <sub>3</sub> /Wt %	Bunsen Coefficient $\alpha \times 10^3$	293.15	0.1	31.0	0.35	28.7	0.42	26.0	303.15	0.1	26.5	0.35	26.5	0.42	21.0	313.15	0.1	23.1	0.35	23.1	0.42	16.5
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<b>AUXILIARY INFORMATION</b>																									
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure of Lannung were modified (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Stated to be 99.98 - 99.99 per cent.  (2) Aluminum oxide. No information.  (3) Water. No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Lannung, A. <i>J. Am. Chem. Soc.</i> <u>1930</u> , 52, 68.																								

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Bruhn, G.; Gerlach, J.; Pawlek, F.	
(2) Sulfuric acid, copper (2+) salt (1:1); CuSO <sub>4</sub> ; [7758-98-7]		Z. Anorg. Allgem. Chem. <u>1965</u> , 337, 68-79.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES:		PREPARED BY:	
T/K = 298-523 Concentration		C.L. Young	
EXPERIMENTAL VALUES:			
T/K	Conc of salt/mol l <sup>-1</sup>	$\alpha^a$ /cm <sup>3</sup> (STP) cm <sup>3</sup> atm <sup>-1</sup>	
298.15	0.5	0.02440	
	1.0	0.02193	
	1.5	0.01991	
323.15	0.5	0.01775	
	1.0	0.01585	
	1.5	0.01449	
373.15	0.5	0.01491	
	1.0	0.01299	
	1.5	0.01270	
423.15	0.5	0.01670	
	1.0	0.01511	
	1.5	0.01366	
473.15	0.5	0.02330	
	1.0	0.01988	
	1.5	0.01844	
523.15	0.5	0.03355	
	1.0	0.02970	
	1.5	0.02680	
<sup>a</sup> Bunsen coefficient.			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE		SOURCE AND PURITY OF MATERIALS:	
Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.		No details given.	
		ESTIMATED ERROR:	
		$\delta T/K = \pm 2$ ; $\delta \alpha = \pm 2\%$ . (estimated by compiler)	
		REFERENCES:	
		1. Pray, H.A.; Stephan, E.L. <i>Battelle Memorial Institute Report BMI-840</i> , <u>1953</u> .	

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Sulfuric acid, nickel(2+) salt (1:1); NiSO<sub>4</sub>; [7786-81-4]</p> <p>(3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Bruhn, G.; Gerlach, J.; Pawlek, F. <i>Z. Anorg. Allgem. Chem.</i> <u>1965</u>, 337, 68-79.</p>																																						
<p>VARIABLES:</p> <p>T/K = 298-423 Concentration</p>	<p>PREPARED BY:</p> <p>C.L. Young</p>																																						
<p>EXPERIMENTAL VALUES:</p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">T/K</th> <th style="text-align: left;">Conc of salt/mol l<sup>-1</sup></th> <th style="text-align: left;"><math>\alpha^a</math>/cm<sup>3</sup> (STP) cm<sup>3</sup> atm<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="3">298.15</td> <td>0.5</td> <td>0.02450</td> </tr> <tr> <td>1.0</td> <td>0.02175</td> </tr> <tr> <td>1.5</td> <td>0.02006</td> </tr> <tr> <td rowspan="3">323.15</td> <td>0.5</td> <td>0.01830</td> </tr> <tr> <td>1.0</td> <td>0.01571</td> </tr> <tr> <td>1.5</td> <td>0.01447</td> </tr> <tr> <td rowspan="3">373.15</td> <td>0.5</td> <td>0.01450</td> </tr> <tr> <td>1.0</td> <td>0.01336</td> </tr> <tr> <td>1.5</td> <td>0.01240</td> </tr> <tr> <td rowspan="3">398.15</td> <td>0.5</td> <td>0.01565</td> </tr> <tr> <td>1.0</td> <td>0.01329</td> </tr> <tr> <td>1.5</td> <td>0.01215</td> </tr> <tr> <td rowspan="3">423.15</td> <td>0.5</td> <td>0.01661</td> </tr> <tr> <td>1.0</td> <td>0.01492</td> </tr> <tr> <td>1.5</td> <td>0.01370</td> </tr> </tbody> </table>		T/K	Conc of salt/mol l <sup>-1</sup>	$\alpha^a$ /cm <sup>3</sup> (STP) cm <sup>3</sup> atm <sup>-1</sup>	298.15	0.5	0.02450	1.0	0.02175	1.5	0.02006	323.15	0.5	0.01830	1.0	0.01571	1.5	0.01447	373.15	0.5	0.01450	1.0	0.01336	1.5	0.01240	398.15	0.5	0.01565	1.0	0.01329	1.5	0.01215	423.15	0.5	0.01661	1.0	0.01492	1.5	0.01370
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p style="text-align: center;">No details given.</p> <hr/> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 2</math>; <math>\delta \alpha = \pm 2\%</math>. (estimated by compiler).</p> <hr/> <p>REFERENCES:</p> <p>1. Pray, H.A.; Stephan, E.L.; <i>Battelle Memorial Institute Report BMI-840, 1953</i></p>																																						

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfuric acid, cobalt salt; CoSO <sub>4</sub> ; [10124-43-3] (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Bruhn, G.; Gerlach, J; Pawlek, F. Z. Anorg. Allgem. Chem. <u>1965</u> , 337, 68-79.
<b>VARIABLES:</b> T/K - 298-423 Concentration		<b>PREPARED BY:</b> C.L. Young
<b>EXPERIMENTAL VALUES:</b>		
T/K	Conc of salt/mol l <sup>-1</sup>	$\alpha^a$ /cm <sup>3</sup> (STP) cm <sup>3</sup> atm <sup>-1</sup>
298.15	0.5	0.02448
	1.0	0.02150
	1.5	0.02020
323.15	0.5	0.01772
	1.0	0.01521
	1.5	0.01467
373.15	0.5	0.01520
	1.0	0.01320
	1.5	0.01190
398.15	0.5	0.01513
	1.0	0.01355
	1.5	0.01308
423.15	0.5	0.01712
<sup>a</sup> Bunsen coefficient		
<b>AUXILIARY INFORMATION</b>		
<b>METHOD/APPARATUS/PROCEDURE:</b> Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.		<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.
		<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 2$ ; $\delta \alpha = \pm 2\%$ . (estimated by compiler).
		<b>REFERENCES:</b> 1. Pray, H.A.; Stephan, E.L. Battelle Memorial Institute Report BMI-840, <u>1953</u> .

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hydrated iron oxide; Fe <sub>2</sub> O <sub>3</sub> ·xH <sub>2</sub> O; [12259-21-1] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Shkol'nikova, R. I. <i>Uch. Zap. Leningr. Gos. Univ., Ser. Khim. Nauk.</i> 1959, Nr. 18, 64-86. <i>Chem. Abstr.</i> 1961, 55, 25443b.																								
<b>VARIABLES:</b> T/K= 293.15 - 313.15 P/kPa= 101.325 Fe <sub>2</sub> O <sub>3</sub> /wt % = 0.1 - 0.8	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="369 466 879 825"> <thead> <tr> <th>T/K</th> <th>Fe<sub>2</sub>O<sub>3</sub>/wt %</th> <th>Bunsen Coefficient α x 10<sup>3</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="3">293.15</td> <td>0.1</td> <td>30.1</td> </tr> <tr> <td>0.5</td> <td>29.6</td> </tr> <tr> <td>0.8</td> <td>27.9</td> </tr> <tr> <td rowspan="3">303.15</td> <td>0.1</td> <td>25.3</td> </tr> <tr> <td>0.5</td> <td>21.5</td> </tr> <tr> <td>0.8</td> <td>20.1</td> </tr> <tr> <td rowspan="3">313.15</td> <td>0.1</td> <td>21.3</td> </tr> <tr> <td>0.5</td> <td>16.1</td> </tr> <tr> <td>0.8</td> <td>13.0</td> </tr> </tbody> </table> <p>The enthalpy of solution of oxygen was calculated from the temperature coefficient of the Bunsen coefficient. It is 2780, 2970, 5560, and 6970 cal mol<sup>-1</sup> in water, and 0.1, 0.5, and 0.8 wt % Fe<sub>2</sub>O<sub>3</sub> respectively.</p>		T/K	Fe <sub>2</sub> O <sub>3</sub> /wt %	Bunsen Coefficient α x 10 <sup>3</sup>	293.15	0.1	30.1	0.5	29.6	0.8	27.9	303.15	0.1	25.3	0.5	21.5	0.8	20.1	313.15	0.1	21.3	0.5	16.1	0.8	13.0
T/K	Fe <sub>2</sub> O <sub>3</sub> /wt %	Bunsen Coefficient α x 10 <sup>3</sup>																							
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<b>AUXILIARY INFORMATION</b>																									
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure of Lannung were modified (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Stated to be 99.98 - 99.99 per cent. (2) Iron oxide. No information. (3) Water. No information.																								
<b>ESTIMATED ERROR:</b>																									
<b>REFERENCES:</b> 1. Lannung, A. <i>J. Am. Chem. Soc.</i> 1930, 52, 68.																									

COMPONENTS: (1) Oxygen; O <sub>2</sub> : [7782-44-7] (2) Manganous sulphate; MnSO <sub>4</sub> ·4H <sub>2</sub> O; [7785-87-7] (3) Water; H <sub>2</sub> O; [7732-18-5]		ORIGINAL MEASUREMENTS: Murray, C.N.; Riley, J.P.; Wilson, T.R.S. <i>Deep-Sea Research</i> <u>1968</u> , 15, 237-8.		
VARIABLES: T/K = 323.7		PREPARED BY: R. Battino		
EXPERIMENTAL VALUES:				
t/°C	T/K	10 <sup>3</sup> α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>	10 <sup>3</sup> L	10 <sup>6</sup> x <sub>1</sub>
Manganous sulphate (480 g MnSO <sub>4</sub> ·4H <sub>2</sub> O/l)				
25.5	298.7	9.52	11.28	7.67
Manganous chloride (600 g MnCl <sub>2</sub> ·4H <sub>2</sub> O/l); [13446-34-9]				
25.5	298.7	8.03	9.51	6.47
(320 g NaOH + 600 g NaI)/l				
25.5	298.7	0.19	0.23	0.16
(400 g NaOH + 900 g NaI)/l				
25.5	298.7	0.24	0.28	0.19
α = Bunsen coefficient.				
L = Ostwald coefficient; calculated by compiler.				
x <sub>1</sub> = mole fraction solubility at 101.325 kPa partial pressure of gas; calculated by compiler. Calculated for undissociated salts.				
NaOH; [1310-73-2] - NaI; [7681-82-5]				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE: Used the Ben-Naim and Baer (1) apparatus. A liquid-saturated gas is dissolved in the stirred solution. The volume dissolved is determined on a gas buret. Measurement is done at constant pressure.		SOURCE AND PURITY OF MATERIALS: No details given		
		ESTIMATED ERROR: δα/α = ±0.01 for first two solutions and ±0.1 for last two solutions. Estimate by compiler.		
		REFERENCES: 1. Ben-Naim, A.; Baer, S. <i>Trans. Faraday Soc.</i> 1963, 59, 2735-8.		

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Uranium, difluorodioxo-, (Uranyl fluoride); UO <sub>2</sub> F <sub>2</sub> ; [13536-84-0] (3) Water; H <sub>2</sub> O; [7732-18-5]				Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H. <i>Battelle Memorial Institute Report BMI-1067, 1956.</i>			
VARIABLES:				PREPARED BY:			
T/K = 373-436 P/bar = 16-106 Concentration				C. L. Young			
EXPERIMENTAL VALUES:							
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility *	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility *
373.15	40	25.5	0.406	373.15	100	21.7	0.530
		25.5	0.418			65.5	0.91
		25.5	0.413			65.5	0.899
		39.6	0.62			65.5	0.91
		39.6	0.590			65.5	0.91
		39.6	0.644			96.2	1.26
		66.2	0.973			95.5	1.30
		66.2	0.975			95.5	1.31
		66.2	0.985		243	17.9	0.203
		66.2	1.02			19.0	0.222
		104.8	1.58			19.7	0.231
		104.8	1.545			31.7	0.323
		104.8	1.51			33.4	0.368
		104.8	1.54			33.4	0.372
	100	21.7	0.313			67.6	0.750
		21.7	0.318			67.6	0.715
		21.7	0.315			67.6	0.730
		21.7	0.534			67.6	0.740
		21.7	0.493			105.8	1.095
		21.7	0.515			105.8	1.090
* ml oxygen at 1 atmosphere and 273.15 K/g of solution. P <sup>†</sup> partial pressure of oxygen.							
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Gas and liquid equilibrated for 18 hours. Pressure measured with Bourdon gauge and temperature measured with thermocouple. Composition of liquid estimated by volumetric method. Details in source. Partial pressure estimated by subtracting vapor pressure from total pressure.				No details given.			
				ESTIMATED ERROR: δT/K = ±0.6; δP/bar = ±0.3; δ(Solubility) = ±3% (estimated by compiler).			
				REFERENCES:			



<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Uranium, difluorodioxo-, (Uranyl fluoride); UO<sub>2</sub>F<sub>2</sub>; [13536-84-0]</p> <p>(3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H.</p> <p><i>Battelle Memorial Institute Report BMI-1067, 1956.</i></p>
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EXPERIMENTAL VALUES:				continued			
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility *	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility *
373.15	243	105.8	1.120	435.93	40	16.2	0.34
		105.8	1.100			19.3	0.376
408.15	40	18.3	0.28			19.3	0.384
		18.3	0.32			33.1	0.61
		18.3	0.29			33.1	0.635
		30.3	0.489			33.1	0.67
		30.3	0.465			33.1	0.647
		30.3	0.480			33.8	0.665
		62.1	0.982			60.0	1.12
		62.1	1.00			60.0	1.17
		62.1	0.96			60.0	1.12
		62.1	0.97			60.9	1.21
		98.9	1.485			60.9	1.16
		98.9	1.58			61.3	1.16
		98.9	1.51			94.7	1.80
	100	20.3	0.271			97.5	1.93
		20.3	0.281			99.0	1.93
		20.3	0.31		100	15.9	0.28
		20.0	0.281			15.9	0.248
		34.1	0.540			15.9	0.285
		33.8	0.505			15.9	0.252
		33.8	0.510			33.1	0.56
		33.8	0.507			33.8	0.515
		66.2	0.969			33.8	0.56
		66.2	0.940			34.5	0.58
		66.8	0.949			60.3	1.0
		97.6	1.393			60.3	0.998
		97.6	1.380			60.3	1.02
		97.6	1.390			82.7	1.43
		97.6	1.390			84.5	1.42
	243	23.4	0.260			85.8	1.48
		24.8	0.291			87.9	1.51
		23.4	0.272		243	21.0	0.306
		33.8	0.405			22.4	0.33
		34.1	0.408			22.4	0.295
		34.1	0.416			22.4	0.31
		33.8	0.405			37.2	0.54
		65.5	0.74			37.6	0.55
		65.2	0.76			37.6	0.53
		65.2	0.765			63.8	0.91
		95.5	1.06			63.8	0.84
		95.5	1.06			63.8	0.925
		95.5	1.10			63.8	0.84
435.93	40	13.4	0.283			100.0	1.40
		14.1	0.276			100.3	1.30
		16.2	0.31			102.4	1.33
		16.2	0.32				

\* ml oxygen at 1 atmosphere and 273.15 K/g of solution.

P<sup>†</sup> partial pressure of oxygen.

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Pray, H.A.; Stephan, E.F.			
(2) Dioxosulfatouranium (Uranyl sulfate); UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3]				U. S. Atomic Energy Commission 1953, BMI-840.			
(3) Water; H <sub>2</sub> O; [7732-18-5]							
VARIABLES:				PREPARED BY:			
T/K = 373 - 436				R. Battino			
P/MPa = 0.96 - 10.5							
EXPERIMENTAL VALUES:							
P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	s <sup>b</sup>	10 <sup>4</sup> x <sub>1</sub> <sup>a,c</sup>	P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	s <sup>b</sup>	
Water.	212°F	(373K)		40gU/dm <sup>3</sup>	212°F	(373K)	
332	2.29	0.380	3.06	277	1.91	0.290	
355	2.45	0.435	3.50	287	1.98	0.290	
374	2.58	0.465	3.74	295	2.03	0.310	
453	3.12	0.550	4.42	310	2.14	0.320	
489	3.37	0.570	4.59	621	4.28	0.643	
500	3.45	0.650	5.23	643	4.43	0.672	
526	3.63	0.665	5.35	664	4.58	0.685	
671	4.63	0.870	7.00	918	6.33	0.965	
808	5.57	0.995	8.00	955	6.58	0.975	
887	6.11	1.130	9.09	988	6.81	1.020	
933	6.43	1.180	9.49	1020	7.03	1.060	
1292	8.91	1.600	12.87	1337	9.22	1.400	
1335	9.20	1.600	12.87	1386	9.56	1.370	
1410	9.72	1.820	14.64	1447	9.98	1.560	
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Solubility in units of ml O<sub>2</sub>(STP)/g of solvent or solution.</p> <p><sup>c</sup> Mole fraction solubility at partial pressure of oxygen indicated. Henry's constant is 6897(±240)MPa/mole fraction or 6.807 x 10<sup>4</sup>atm/mole fraction.</p>							
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
A sample of saturated solution is withdrawn from a stainless steel pressurized and thermostatted autoclave and analyzed for the dissolved gas content. Details and a drawing are given in the paper.				No details given.			
				ESTIMATED ERROR:			
				δS/S = ±0.03, compiler's estimate.			
				REFERENCES:			

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Pray, H.A.; Stephan, E.F.
(2) Dioxosulfatouranium (Uranyl sulfate); UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3]	U. S. Atomic Energy Commission 1953, BMI-840.
(3) Water; H <sub>2</sub> O; [7732-18-5]	

continued

P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>		P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>
100g U/dm <sup>3</sup>	212°F	(373K)		243g U/dm <sup>3</sup>	212°F	(373K)
348	2.40	0.345		505	3.48	0.338
354	2.44	0.350		516	3.56	0.340
360	2.48	0.370		538	3.71	0.360
367	2.53	0.348		663	4.57	0.435
387	2.67	0.368		685	4.72	0.480
640	4.41	0.565		743	5.12	0.490
650	4.48	0.551		760	5.24	0.468
665	4.58	0.570		1070	7.38	0.670
676	4.66	0.585		1084	7.47	0.730
985	6.79	0.935		1235	8.51	0.800
1010	6.96	0.915		1277	8.80	0.800
1044	7.20	1.010		1365	9.41	0.868
1363	9.40	1.260				
1400	9.65	1.180				
1434	9.89	1.32				

P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>	10 <sup>4</sup> x <sub>1</sub> <sup>a,c</sup>	P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>
Water	275°F	(408K)		40g U/dm <sup>3</sup>	275°F	(408K)
510	3.52	0.655	5.04	489	3.37	0.535
525	3.62	0.645	4.97	500	3.45	0.565
555	3.83	0.685	5.28	533	3.67	0.555
590	4.07	0.73	5.62	561	3.87	0.585
1090	7.51	1.42	10.94	700	4.83	0.765
1145	7.89	1.45	11.17	738	5.09	0.83
1173	8.09	1.51	11.63	764	5.27	0.83
1180	8.13	1.60	12.32	1033	7.12	1.16
1195	8.24	1.60	12.32	1056	7.28	1.185
1215	8.38	1.55	11.94	1074	7.40	1.22
				1440	9.93	1.61
				1468	10.12	1.58
				1495	10.31	1.675
				1522	10.49	1.66
100g U/dm <sup>3</sup>	275°F	(408K)		243g U/dm <sup>3</sup>	275°F	(408K)
575	3.96	0.540		538	3.71	0.398
595	4.10	0.555		563	3.88	0.398
617	4.25	0.60		585	4.03	0.400
1288	8.88	1.23		600	4.14	0.400
1310	9.03	1.21		1278	8.81	0.86
1334	9.20	1.25		1305	9.00	0.87
				1352	9.32	0.88

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Solubility in units of ml O<sub>2</sub>(STP)/g of solvent or solution.

<sup>c</sup> Mole fraction solubility at partial pressure of oxygen indicated. Henry's constant is 6995(±232)MPa/mole fraction or 6.904 x 10<sup>4</sup> atm/mole fraction.

continued on following page

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Dioxosulfatouranium (Uranyl sulfate); UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Pray, H.A.; Stephan, E.F. <i>U. S. Atomic Energy Commission</i> <u>1953</u> , BMI-840.
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continued

P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>	10 <sup>4</sup> x <sub>1</sub> <sup>a,c</sup>	P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>
Water.	325°F	(436K)		40g U/dm <sup>3</sup>	325°F	(436K)
195	1.34	0.303	2.44	146	1.01	0.171
195	1.34	0.306	2.46	304	2.10	0.339
195	1.34	0.314	2.53	279	1.92	0.327
530	3.65	0.830	6.68	392	2.70	0.471
560	3.86	0.880	7.08	448	3.09	0.576
600	4.14	0.905	7.28	474	3.27	0.638
950	6.55	1.41	11.34	593	4.09	0.755
950	6.55	1.42	11.42	609	4.20	0.814
960	6.62	1.51	12.15	709	4.89	0.951
1410	9.72	2.12	17.06	719	4.96	0.925
1440	9.93	2.28	18.34	758	5.23	1.001
				939	6.47	1.335
100g U/dm <sup>3</sup>	325°F	(436K)		984	6.78	1.301
139	0.96	0.174		993	6.85	1.390
145	1.00	0.177		1300	8.96	1.765
150	1.03	0.179		1320	9.10	1.770
333	2.30	0.396		1346	9.28	1.716
352	2.43	0.351		1468	10.12	1.920
550	3.79	0.614		1475	10.17	1.850
575	3.96	0.596		1514	10.44	1.85
605	4.17	0.669		1520	10.48	1.98
782	5.39	0.842				
866	5.97	0.865		243g U/dm <sup>3</sup>	325°F	(436K)
975	6.72	0.996		599	4.13	0.457
1020	7.03	1.081		610	4.21	0.436
1030	7.10	1.061		631	4.35	0.445
1333	9.19	1.451		666	4.59	0.515
1331	9.18	1.410		1355	9.34	0.954
1363	9.40	1.400		1378	9.50	0.955
1431	9.87	1.432		1409	9.71	0.984
				1436	9.90	1.00

a Calculated by compiler.

b Solubility in units of ml O<sub>2</sub> (STP)/g of solvent or solution.

c Mole fraction solubility at partial pressure of oxygen indicated. Henry's constant is 5537 (±158) MPa/mole fraction or 5.465 x 10<sup>4</sup> atm/mole fraction.

d Solution concentrations given as grams of uranium per liter of solution.

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Uranium, dioxo[sulfato(2-)-0-]-, (Uranyl sulfate); UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3] (3) Water; H <sub>2</sub> O; [7732-18-5]				Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H.  <i>Battelle Memorial Institute Report BMI-1067, 1956.</i>			
VARIABLES:				PREPARED BY:			
T/K - 373-561 P/bar = 10-175 Concentration				C. L. Young			
EXPERIMENTAL VALUES:							
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*
373.15	40	19.1	0.290	373.15	100	26.7	0.368
		19.8	0.290			44.1	0.565
		20.3	0.310			44.8	0.551
		21.4	0.320			45.9	0.570
		42.8	0.643			46.6	0.585
		44.3	0.672			67.9	0.935
		45.8	0.685			69.6	0.915
		63.3	0.965			72.0	1.010
		65.8	0.975			94.0	1.26
		68.1	1.020			96.5	1.18
		70.3	1.060			98.9	1.32
		92.2	1.400			148.2	1.80
		95.6	1.370			150.0	1.85
		99.8	1.560			165.8	1.95
		137.6	2.04			170.0	1.97
		141.0	2.08			175.5	2.10
	100	24.0	0.345		243	34.8	0.338
		24.4	0.350			35.6	0.340
		24.8	0.370			37.1	0.360
		25.3	0.348			44.5	0.430
* ml of oxygen at 1 atmosphere and 273.15 K/g of solution. P <sup>†</sup> partial pressure of oxygen.							
continued on following page							
AUXILIARY INFORMATION							
METHOD /APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Gas and liquid equilibrated for 18 hours. Pressure measured with Bourdon gauge and temperature measured with thermocouple. Composition of liquid estimated by volumetric method. Details in source. Partial pressure estimated by subtracting vapor pressure from total pressure.				No details given.			
				ESTIMATED ERROR: δT/K = ±0.6; δP/bar = ±0.3; δ(Solubility) = ±3% (estimated by compiler).			
				REFERENCES:			

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H.  <i>Battelle Memorial Institute Report</i> BMI-1067, 1956.			
(2) Uranium, dioxo[sulfato(2-)-0-]-, (Uranyl sulfate); UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3]							
(3) Water; H <sub>2</sub> O; [7732-18-5]							
EXPERIMENTAL VALUES:				continued			
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*
373.15	243	44.8	0.450	408.15	234	20.3	0.234
		45.7	0.435			53.7	0.585
		47.2	0.480			56.1	0.630
		51.2	0.490			74.7	0.812
		73.8	0.670			76.5	0.815
		74.7	0.730			91.3	0.980
		83.1	0.790			93.0	0.970
		85.2	0.800			99.6	1.06
		88.0	0.800			100.9	1.00
		94.1	0.868			103.0	1.07
		109.3	0.990			119.6	1.21
		112.0	1.00			120.9	1.22
		128.6	1.13			129.2	1.28
		133.4	1.23			131.3	1.31
		135.5	1.16			148.5	1.44
		136.5	1.20			150.0	1.43
		139.6	1.22			152.0	1.50
		141.0	1.23	435.93	40	10.1	0.171
		154.0	1.32			30.9	0.576
		156.2	1.36			32.7	0.638
		158.2	1.38			40.9	0.755
408.15	40	33.7	0.535			42.0	0.814
		34.5	0.565			48.9	0.951
		36.7	0.555			49.6	0.925
		38.7	0.585			52.3	1.001
		48.3	0.765			64.7	1.335
		50.9	0.830			67.8	1.301
		52.7	0.830			68.5	1.390
		71.2	1.160			89.6	1.770
		72.8	1.185			89.6	1.765
		74.0	1.220			91.0	1.770
		99.3	1.610			91.3	1.76
		101.2	1.580			94.7	1.87
		103.1	1.675			101.2	1.920
		104.9	1.660			104.8	1.980
		144.4	2.320			115.4	2.260
		147.2	2.400			117.5	2.240
	100	39.6	0.540			118.9	2.270
		41.0	0.555			120.2	2.220
		42.5	0.600			123.0	2.260
		88.8	1.23			130.9	2.320
		90.3	1.21			132.7	2.340
		92.0	1.25			146.4	2.48
		120.9	1.64			150.6	2.54
		123.6	1.69			158.9	2.61
		126.4	1.71			158.9	2.61
		148.2	1.95			161.6	2.67
		148.7	1.94			163.0	2.55
		159.5	2.03			176.8	2.74
		162.2	2.10		100	9.6	0.174
		166.4	2.12			10.0	0.177
	234	18.6	0.231			10.3	0.179

\* ml of oxygen at 1 atmosphere and 273.15 K/g of solution.

P<sup>†</sup> partial pressure of oxygen.

continued on following page

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Uranium, dioxo[sulfato(2-)-0-]- [1314-64-3]</p> <p>(3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H.</p> <p><i>Battelle Memorial Institute Report BMI-1067, 1956.</i></p>
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EXPERIMENTAL VALUES:				continued			
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*
435.93	100	23.0	0.396	435.93	243	157.5	1.65
		37.9	0.614			158.9	1.73
		39.6	0.596	477.59	40	7.8	0.29
		41.7	0.669			8.5	0.31
		53.9	0.842			9.2	0.33
		59.7	0.865			22.3	0.69
		67.2	0.996			23.0	0.72
		70.3	1.081			24.3	0.74
		71.0	1.061			37.4	1.12
		91.8	1.451			38.5	1.14
		91.8	1.410			40.9	1.14
		94.0	1.400			51.9	1.48
		98.7	1.432			54.7	1.55
		123.7	1.88			76.0	1.76
		126.8	1.91			80.9	1.80
		128.5	1.83			113.3	2.34
		149.2	2.04			115.3	2.30
		152.0	2.14			117.4	2.38
		155.4	2.16			136.0	2.60
		156.1	2.08			140.2	2.66
		159.2	2.10			147.1	2.83
		162.3	2.21			151.2	2.88
	243	15.4	0.22			154.6	2.93
		16.8	0.239		100	45.4	1.04
		38.9	0.508			46.4	1.06
		40.3	0.52			58.7	1.29
		41.6	0.534			60.9	1.30
		54.1	0.70			62.9	1.44
		55.4	0.68			86.4	1.67
		56.8	0.705			87.8	1.70
		75.8	0.90			102.2	1.84
		77.5	0.94			103.6	1.85
		80.3	0.97			120.9	1.96
		83.4	1.02			125.0	2.04
		85.1	1.03			128.4	2.08
		92.7	1.06			132.0	2.20
		94.0	1.11			148.4	2.24
		100.2	1.18			150.9	2.34
		102.3	1.18			151.9	2.31
		103.7	1.23			154.0	2.34
		105.1	1.21			159.5	2.48
		105.1	1.28		243	27.4	0.49
		105.8	1.22			28.1	0.48
		106.5	1.22			29.2	0.51
		109.1	1.34			45.0	0.78
		110.6	1.30			64.3	1.10
		114.0	1.27			65.7	1.05
		116.1	1.32			74.0	1.12
		130.6	1.46			76.7	1.17
		132.7	1.50			85.7	1.22
		153.7	1.65			88.5	1.31
		155.4	1.67				

\* ml of oxygen at 1 atmosphere and 273.15 K/g of solution.

P<sup>†</sup> partial pressure of oxygen.

continued on following page

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H.  <i>Battelle Memorial Institute Report</i> BMI-1067, 1956.			
(2) Uranium, dioxo[sulfato(2-)-O-]-, (Uranyl sulfate; UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3])							
(3) Water; H <sub>2</sub> O; [7732-18-5]							
EXPERIMENTAL VALUES:				continued			
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility*
477.59	243	120.2	1.49	533.15	100	86.8	1.77
		122.2	1.54			90.9	1.84
		138.8	1.64			94.4	1.84
		140.2	1.66			115.1	2.22
		142.2	1.64			116.5	2.14
		163.4	1.77			139.2	2.44
		164.8	1.81			142.0	2.42
		165.7	1.78			146.1	2.42
533.15	40	6.1	0.296			147.5	2.42
		6.8	0.30			150.2	2.50
		7.5	0.36		243	18.5	0.58
		8.2	0.41			19.2	0.62
		17.3	0.98			20.6	0.64
		17.9	0.97			37.9	0.84
		17.9	0.96			39.9	0.90
		18.5	1.00			42.0	0.97
		26.1	1.24			49.6	1.00
		27.2	1.30			52.0	1.05
		28.5	1.34			54.4	1.14
		29.2	1.36			57.8	1.16
		33.0	1.39			60.6	1.18
		33.4	1.39			74.4	1.25
		35.4	1.47			76.1	1.26
		51.0	1.68			77.8	1.24
		53.4	1.69			85.4	1.36
		69.9	1.98			96.5	1.48
		74.0	2.05			97.8	1.51
		74.7	2.00			110.9	1.50
		95.8	2.27			111.6	1.60
		99.9	2.38			133.7	1.66
		101.3	2.48			135.1	1.73
		104.0	2.46			136.2	1.75
		110.9	2.61	560.93	40	8.6	0.65
		118.5	2.66			10.3	0.73
		120.6	2.70			11.0	0.79
		121.3	2.78			14.1	1.03
		122.0	2.74			15.5	1.12
		122.0	2.78			16.2	1.17
	100	10.3	0.45			31.4	1.81
		12.1	0.50			32.1	1.96
		18.9	0.815			43.4	2.15
		19.6	0.854			44.8	2.21
		22.0	0.92			46.5	2.21
		30.3	1.19			74.1	2.36
		31.6	1.27			78.9	2.49
		33.7	1.32			80.3	2.52
		49.6	1.54			83.1	2.62
		53.0	1.61			93.4	2.70
		55.1	1.62			94.8	2.72
		64.7	1.66			125.1	3.12
		66.8	1.71			126.5	3.24

\* ml of oxygen at 1 atmosphere and 273.15 K/g of solution.

P<sup>†</sup> partial pressure of oxygen.

continued on following page



COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H. <i>Battelle Memorial Institute Report</i> BMI-1067, <u>1956</u> .			
(2) Uranium, dioxo[sulfato(2-)-0-]-, (Uranyl sulfate); UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3]							
(3) Water; H <sub>2</sub> O; [7732-18-5]							
EXPERIMENTAL VALUES:				continued			
T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility *	T/K	g Uranium per liter	P <sup>†</sup> /bar	Solubility *
560.93	40	127.9	3.28	560.93	100	60.3	1.95
		129.3	3.28			62.1	1.85
		133.4	3.23			76.9	1.91
	100	11.4	0.76			79.3	2.03
		12.4	0.81			82.4	2.06
		22.4	1.37			101.0	2.14
		23.8	1.47			104.5	2.22
		24.5	1.53			107.2	2.22
		41.0	1.71			122.4	2.38
		42.4	1.82			126.5	2.42
		59.0	1.88			130.7	2.51
* ml of oxygen at 1 atmosphere and 273.15 K/g of solution.							
P <sup>†</sup> partial pressure of oxygen.							

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Uranyl Sulfate; UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3] (3) Copper Sulfate; CuSO <sub>4</sub> ; [7758-98-7] (4) Sulfuric Acid; H <sub>2</sub> SO <sub>4</sub> ; [7664-93-9] (5) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Anderson, C.J.; Keeler, R.A.; Klach, S.J. <i>J. Chem. Eng. Data</i> <u>1962</u> , 7, 290-4.		
<b>VARIABLES:</b> T/K = 373-573 P/MPa = 0.4-5.2		<b>PREPARED BY:</b> R. Battino		
<b>EXPERIMENTAL VALUES:</b>				
t/°C	T <sup>a</sup> /K	10 <sup>4</sup> x <sub>1</sub> <sup>b</sup>	P <sub>O<sub>2</sub></sub> <sup>c</sup> /psia	10 <sup>-5</sup> K <sup>d</sup>
Water				
125	398	2.46	246 (1.70) <sup>h</sup>	10.0
150	423	2.55	226 (1.56)	8.86
200	473	3.65	210 (1.45)	5.75
100	373	3.77	395 (2.65)	10.2
150	423	3.69	341 (2.35)	9.24
Uranyl Sulfate Solution A <sup>e</sup>				
250	523	13.5	534 (3.68)	3.95
300	573	16.3	343 (2.36)	2.10
250	523	17.2	733 (5.05)	4.25
275	548	20.5	622 (4.29)	3.03
300	573	22.9	508 (3.50)	2.22
250	523	14.6	753 (5.19)	5.14
275	548	20.1	702 (4.84)	3.49
300	573	23.5	623 (4.30)	2.65
100	373	0.980	100 (0.689)	10.2
125	398	0.763	76.3(0.526)	10.0
150	423	0.65	56 (0.386)	8.6
100	373	3.47	350 (2.41)	10.1
125	398	3.40	316 (2.18)	9.30
150	423	2.89	246 (1.70)	8.50
continued on following page				
AUXILIARY INFORMATION				
<b>METHOD/APPARATUS/PROCEDURE:</b> Kr/ <sup>85</sup> Kr stock mixture and O <sub>2</sub> are added separately to a thermostatted stainless steel vessel containing about 275 cm <sup>3</sup> of solution. At equilibrium both liquid and vapor were sampled and the krypton in each phase was determined by counting the <sup>85</sup> Kr tag. No details were given on how the oxygen solubilities were calculated.		<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.		
		<b>ESTIMATED ERROR:</b> δK/K = ±0.03, compiler's estimate. δT/K = ±2		
		<b>REFERENCES:</b>		

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Uranyl Sulfate; UO <sub>2</sub> SO <sub>4</sub> ; [1314-64-3] (3) Copper Sulfate; CuSO <sub>4</sub> ; [7758-98-7] (4) Sulfuric Acid; H <sub>2</sub> SO <sub>4</sub> ; [7664-93-9] (5) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Anderson, C.J.; Keeler, R.A.; Klach, S.J. J. Chem. Eng. Data <u>1962</u> , 7, 290-4.
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continued

t/°C	T <sup>a</sup> /K	10 <sup>4</sup> x <sub>1</sub> <sup>b</sup>	P <sub>O<sub>2</sub></sub> <sup>c</sup> /psia	10 <sup>-5</sup> K <sup>d</sup>
Uranyl Sulfate Solution B <sup>f</sup>				
100	373	3.209	335.3 (2.31) <sup>h</sup>	10.45
150	423	3.88	341 (2.35)	8.80
250	523	8.04	283 (1.95)	3.52
300	573	9.59	233 (1.61)	2.43
100	373	3.400	340.3 (2.35)	10.01
150	423	3.92	331 (2.28)	8.45
250	523	8.27	283 (1.95)	3.42
300	573	10.9	238 (1.64)	2.19
100	373	3.529	365.3 (2.52)	10.35
150	423	4.30	376 (2.59)	8.74
250	523	10.2	328 (2.26)	3.23
300	573	14.7	258 (1.78)	1.75
250	523	7.92	248 (1.71)	3.13
300	573	10.0	193 (1.33)	1.93
Mean Values <sup>g</sup>				
100	373			10.2
125	398			9.75
150	423			8.66
200	473			5.75
250	523			3.45
300	573			2.10

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Mole fraction solubility at 1 psia partial pressure of gas.

<sup>c</sup> Oxygen partial pressure in psia.

<sup>d</sup> Henry's law constant in psia per mole fraction.

<sup>e</sup> Solution A: 0.02 mol dm<sup>-3</sup> uranyl sulfate, 0.005 mol dm<sup>-3</sup> copper sulfate, 0.005 mol dm<sup>-3</sup> sulfuric acid.

<sup>f</sup> Solution B: 0.04 mol dm<sup>-3</sup> uranyl sulfate, 0.01 mol dm<sup>-3</sup> copper sulfate, 0.01 mol dm<sup>-3</sup> sulfuric acid.

<sup>g</sup> Mean values of Henry's law constant for water and the two sulfate solutions.

<sup>h</sup> Pressure in parentheses in MPa, calculated by compiler.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Magnesium chloride; MgCl <sub>2</sub> ; [7786-30-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G.  <i>J. Phys. Chem.</i> <u>1916</u> , 20, 495-502.																																													
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 5 one atm)	<b>PREPARED BY:</b>  H. L. Clever																																													
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="236 466 1076 793"> <thead> <tr> <th>T/K</th> <th>Magnesium Chloride c<sub>3</sub>/mol dm<sup>-3</sup></th> <th>Solution density<sup>1</sup> ρ/g cm<sup>-3</sup></th> <th>Solubility<sup>2</sup> cm<sup>3</sup> (STP) O<sub>2</sub> per dm<sup>3</sup></th> <th>Setschenow Constant<sup>3</sup> k<sub>s</sub></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.0</td> <td>1.000</td> <td>5.78</td> <td>-</td> </tr> <tr> <td></td> <td>0.125</td> <td>1.011</td> <td>5.35</td> <td>0.269</td> </tr> <tr> <td></td> <td>0.25</td> <td>1.022</td> <td>5.04</td> <td>0.238</td> </tr> <tr> <td></td> <td>0.5</td> <td>1.044</td> <td>4.37</td> <td>0.243</td> </tr> <tr> <td></td> <td>1</td> <td>1.085</td> <td>3.18</td> <td>0.260</td> </tr> <tr> <td></td> <td>2</td> <td>1.160</td> <td>2.22</td> <td>0.208</td> </tr> <tr> <td></td> <td>4</td> <td>1.284</td> <td>0.78</td> <td>0.217</td> </tr> <tr> <td></td> <td>5</td> <td>1.343</td> <td>0.54</td> <td>0.206</td> </tr> </tbody> </table> <p><sup>1</sup> The author calculated the densities from data in the <i>International Critical Tables</i>. Use the density values with caution, some of them appear to be in error.</p> <p><sup>2</sup> The solubility in water is about 3 per cent smaller than the presently accepted value.</p> <p><sup>3</sup> The Setschenow constant (salt effect parameter) is calculated from <math>k_s = (1/c_3) \log (\text{Solubility in water}/\text{Solubility in solution})</math>.</p>		T/K	Magnesium Chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>	298.15	0.0	1.000	5.78	-		0.125	1.011	5.35	0.269		0.25	1.022	5.04	0.238		0.5	1.044	4.37	0.243		1	1.085	3.18	0.260		2	1.160	2.22	0.208		4	1.284	0.78	0.217		5	1.343	0.54	0.206
T/K	Magnesium Chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>																																										
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solutions were thermostated in tall cylinder open to the air. They were shaken by hand several times a day for a period of four days.  A sample of 250 cm <sup>3</sup> was analyzed for oxygen by a modified Winkler method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air at one atm. (2) Magnesium chloride. No information. (3) Water. No information.  <b>ESTIMATED ERROR:</b> The solubility values may be in 5 to 10 per cent error. The salt concentrations above one mol dm <sup>-3</sup> may be in error by 10 per cent.  <b>REFERENCES:</b>																																													

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Magnesium Chloride; MgCl <sub>2</sub> ; [7786-30-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Eucken, A.; Hertzberg, G. <i>Z. Physik. Chem.</i> <u>1950</u> , 195, 1 - 23.																														
<b>VARIABLES:</b> T/K = 273.15, 293.15 P/kPa = 101.325 $m_{\text{MgCl}_2} / \text{mol kg}^{-1} = 0 - 1.93$	<b>PREPARED BY:</b> P. L. Long H. L. Clever																														
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Magnesium Chloride mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th style="text-align: center;">Ostwald Coefficient L</th> <th style="text-align: center;">Setschenow Constant k = (1/m) log(L<sup>0</sup>/L)</th> </tr> </thead> <tbody> <tr> <td rowspan="4" style="text-align: center; vertical-align: top;">273.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">0.0490</td> <td style="text-align: center;">-</td> </tr> <tr> <td style="text-align: center;">0.49</td> <td style="text-align: center;">0.0358</td> <td style="text-align: center;">0.280</td> </tr> <tr> <td style="text-align: center;">1.13</td> <td style="text-align: center;">0.0234</td> <td style="text-align: center;">0.284</td> </tr> <tr> <td style="text-align: center;">1.70</td> <td style="text-align: center;">0.0163</td> <td style="text-align: center;">0.281</td> </tr> <tr> <td rowspan="4" style="text-align: center; vertical-align: top;">293.14</td> <td style="text-align: center;">0</td> <td style="text-align: center;">0.0332</td> <td style="text-align: center;">-</td> </tr> <tr> <td style="text-align: center;">0.65</td> <td style="text-align: center;">0.0225</td> <td style="text-align: center;">0.260</td> </tr> <tr> <td style="text-align: center;">1.24</td> <td style="text-align: center;">0.0158</td> <td style="text-align: center;">0.259</td> </tr> <tr> <td style="text-align: center;">1.93</td> <td style="text-align: center;">0.0107</td> <td style="text-align: center;">0.255</td> </tr> </tbody> </table>		T/K	Magnesium Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	Setschenow Constant k = (1/m) log(L <sup>0</sup> /L)	273.15	0	0.0490	-	0.49	0.0358	0.280	1.13	0.0234	0.284	1.70	0.0163	0.281	293.14	0	0.0332	-	0.65	0.0225	0.260	1.24	0.0158	0.259	1.93	0.0107	0.255
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<b>AUXILIARY INFORMATION</b>																															
<b>METHOD/APPARATUS/PROCEDURE:</b> Gas absorption. The apparatus consists of a gas buret and an adsorption flask connected by a capillary tube. The whole apparatus is shaken. The capillary tube is a 2m-long glass helix. An amount of gas is measured at STP and placed in the gas buret. After shaking, the difference from the original amount of gas placed in the gas buret is determined.	<b>SOURCE AND PURITY OF MATERIALS:</b> Components. Neither source nor purity given.  <b>ESTIMATED ERROR:</b> $\delta L/L = 0.01$  <b>REFERENCES:</b>																														

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Magnesium chloride; MgCl <sub>2</sub> ; [7786-30-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A.  <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.																																				
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 3.872	<b>PREPARED BY:</b> H. L. Clever																																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Magnesium chloride c<sub>3</sub>/mol dm<sup>-3</sup></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">0.0</td> <td style="text-align: center;">0.03114<sup>1</sup></td> </tr> <tr> <td></td> <td style="text-align: center;">0.336</td> <td style="text-align: center;">0.02676</td> </tr> <tr> <td></td> <td style="text-align: center;">0.546</td> <td style="text-align: center;">0.02383</td> </tr> <tr> <td></td> <td style="text-align: center;">0.599</td> <td style="text-align: center;">0.02368</td> </tr> <tr> <td></td> <td style="text-align: center;">1.178</td> <td style="text-align: center;">0.01841</td> </tr> <tr> <td></td> <td style="text-align: center;">1.778</td> <td style="text-align: center;">0.01363</td> </tr> <tr> <td></td> <td style="text-align: center;">2.126</td> <td style="text-align: center;">0.01171</td> </tr> <tr> <td></td> <td style="text-align: center;">2.485</td> <td style="text-align: center;">0.00987</td> </tr> <tr> <td></td> <td style="text-align: center;">2.871</td> <td style="text-align: center;">0.00857</td> </tr> <tr> <td></td> <td style="text-align: center;">3.304</td> <td style="text-align: center;">0.00740</td> </tr> <tr> <td></td> <td style="text-align: center;">3.872</td> <td style="text-align: center;">0.00635</td> </tr> </tbody> </table> <p style="text-align: center;"><sup>1</sup>Value from reference 1.</p> <p>The author correlated the data with the Setschenow equation <math>\log(L_0/L) = 0.200 c_3</math> at concentration up to 2.5 mol dm<sup>-3</sup> MgCl<sub>2</sub>. For the entire concentration range he correlated the data with the empirical equation <math>\log(L_0/L) = 0.222 c_3 / (1 + 0.0566 c_3)</math>.</p>		T/K	Magnesium chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L	298.15	0.0	0.03114 <sup>1</sup>		0.336	0.02676		0.546	0.02383		0.599	0.02368		1.178	0.01841		1.778	0.01363		2.126	0.01171		2.485	0.00987		2.871	0.00857		3.304	0.00740		3.872	0.00635
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used. The aqueous salt solution is degassed by boiling under reflux and under vacuum. The gas phase volume and the solvent volume are measured by displacement of mercury. Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded. The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. High purity grade stated to be 99.995 per cent. (2) Magnesium chloride. (3) Water. No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89.																																				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Magnesium sulfate; MgSO <sub>4</sub> ; [7487-88-9] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A.  <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.												
<b>VARIABLES:</b> T/K = 288.15 - 308.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 2.608	<b>PREPARED BY:</b> H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> For the entire concentration range the data correlated better with the empirical equation $\log(L_0/L) = AC_3/(1 + BC_3)$ with the values: <table border="1" data-bbox="386 568 901 715" style="margin: 20px auto;"> <thead> <tr> <th>T/K</th> <th>A/dm<sup>3</sup> mol<sup>-1</sup></th> <th>B/dm<sup>3</sup> mol<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>0.288</td> <td>-0.0012</td> </tr> <tr> <td>298.15</td> <td>0.250</td> <td>-0.0583</td> </tr> <tr> <td>308.15</td> <td>0.293</td> <td>-0.0359</td> </tr> </tbody> </table> <p style="text-align: right;">continued on following page</p>		T/K	A/dm <sup>3</sup> mol <sup>-1</sup>	B/dm <sup>3</sup> mol <sup>-1</sup>	288.15	0.288	-0.0012	298.15	0.250	-0.0583	308.15	0.293	-0.0359
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## EXPERIMENTAL VALUES:

continued

T/K	Magnesium sulfate c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L
288.15	0.0	0.03643 <sup>1</sup>
	0.280	0.03065
	0.364	0.02867
	0.581	0.02481
	0.617	0.02384
	1.082	0.01777
	1.213	0.01605
	1.228	0.01611
	1.239	0.01584
	1.314	0.01504
	1.500	0.01386
	1.746	0.01131
	2.102	0.00881
	2.130	0.00860
	2.431	0.00701
	2.450	0.00712
2.456	0.00699	
298.15	0.0	0.03114 <sup>1</sup>
	0.172	0.02786
	0.284	0.02609
	0.583	0.02150
	0.994	0.01671
	1.302	0.01368
	1.422	0.01284
	1.742	0.01058
	1.784	0.01000
	2.007	0.00847
	2.120	0.00773
	2.156	0.00752
	2.291	0.00667
	2.339	0.00640
308.15	0.0	0.02764 <sup>1</sup>
	0.306	0.02235
	0.577	0.01896
	0.580	0.01875
	0.672	0.01753
	0.711	0.01746
	1.218	0.01270
	1.422	0.01113
	1.728	0.00918
	2.096	0.00672
	2.351	0.00570
	2.608	0.00463

<sup>1</sup> Values from reference 1.

The author correlated the data with the Setschenow equation  $\log(L_0/L) = KC_3$  at concentrations below 1.3, 1.7, and 1.7 mol dm<sup>-3</sup> and temperatures of 288.15, 298.15 and 308.15 K respectively. The values of K are:

T/K	K/dm <sup>3</sup> mol <sup>-1</sup>
288.15	0.290
298.15	0.273
308.15	0.280



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Calcium nitrate; Ca(NO <sub>3</sub> ) <sub>2</sub> ; [10124-37-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A.  <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.																				
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol cm <sup>-3</sup> = 0 - 2.416	<b>PREPARED BY:</b> H. L. Clever																				
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<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 1.536	<b>PREPARED BY:</b> H. L. Clever																											
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="431 453 984 741"> <thead> <tr> <th>T/K</th> <th>Barium chloride c<sub>3</sub>/mol dm<sup>-3</sup></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.0</td> <td>0.03114<sup>1</sup></td> </tr> <tr> <td></td> <td>0.270</td> <td>0.02726</td> </tr> <tr> <td></td> <td>0.530</td> <td>0.02363</td> </tr> <tr> <td></td> <td>0.738</td> <td>0.02202</td> </tr> <tr> <td></td> <td>0.913</td> <td>0.02008</td> </tr> <tr> <td></td> <td>1.168</td> <td>0.01744</td> </tr> <tr> <td></td> <td>1.324</td> <td>0.01654</td> </tr> <tr> <td></td> <td>1.536</td> <td>0.01458</td> </tr> </tbody> </table> <p><sup>1</sup>Value from reference 1.</p> <p>The author correlated the data by the Setschenow equation <math>\log(L_0/L) = 0.212 c_3</math>.</p>		T/K	Barium chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L	298.15	0.0	0.03114 <sup>1</sup>		0.270	0.02726		0.530	0.02363		0.738	0.02202		0.913	0.02008		1.168	0.01744		1.324	0.01654		1.536	0.01458
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used. The aqueous salt solution is degassed by boiling under reflux and under vacuum. The gas phase volume and the solvent volume are measured by displacement of mercury. Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded. The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. High purity grade stated to be 99.995 per cent. (2) Barium chloride. (3) Water. No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89.																											

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Lithium chloride; LiCl; [7447-41-8] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G. <i>J. Phys. Chem.</i> <u>1916</u> , <i>20</i> , 495-502.																																													
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 4 one atm)	<b>PREPARED BY:</b> H. L. Clever																																													
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solutions were thermostated in tall cylinder open to the air. They were shaken by hand several times a day for a period of four days. A sample of 250 cm <sup>3</sup> was analyzed for oxygen by a modified Winkler method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air at one atm. (2) Lithium chloride. No information. (3) Water. No information. <b>ESTIMATED ERROR:</b> The solubility values may be in 5 to 10 per cent error. The salt concentrations above one mol dm <sup>-3</sup> may be in error by 10 per cent. <b>REFERENCES:</b>																																													

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Lithium Chloride; LiCl; [7447-41-8] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Eucken, A.; Hertzberg, G.  <i>Z. Physik. Chem.</i> <u>1950</u> , <i>195</i> , 1 - 23.																														
<b>VARIABLES:</b> T/K =273.15, 293.15 P/kPa =101.325 m <sub>LiCl</sub> /mol kg <sup>-1</sup> = 0 - 2.32	<b>PREPARED BY:</b> P. L. Long H. L. Clever																														
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<b>METHOD/APPARATUS/PROCEDURE:</b> Gas absorption. The apparatus consists of a gas buret and an adsorption flask connected by a capillary tube. The whole apparatus is shaken. The capillary tube is a 2m-long glass helix. An amount of gas is measured at STP and placed in the gas buret. After shaking, the difference from the original amount of gas placed in the gas buret is determined.	<b>SOURCE AND PURITY OF MATERIALS:</b> Components. Neither source nor purity given.  <b>ESTIMATED ERROR:</b> $\delta L/L = 0.01$  <b>REFERENCES:</b>																														

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Alkali metal hydroxides; LiOH, NaOH, KOH, RbOH, and CsOH (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Khomutov, N. E.; Konnik, E. I. <i>Zh. Fiz. Khim.</i> <u>1974</u> , <i>48</i> , 620-5. <i>Russ. J. Phys. Chem.</i> <u>1974</u> , <i>48</i> , 359-62.																																												
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<b>METHOD/APPARATUS/PROCEDURE:</b> Air, saturated with water vapor from the salt solution, is bubbled for several hours through 500 cm <sup>3</sup> of solution.  Three samples are taken and analyzed by the Winkler chemical method.  The solubility unit is mg dm <sup>-3</sup> at the normal oxygen partial pressure in air of 0.21 atm. The solubility in water is 8.15 mg dm <sup>-3</sup> .  The results are presented graphically as log S vs. dm <sup>-3</sup> . The slope is given as the salt effect parameter (Sechenow constant) k.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air treated to free from dust and any foreign gases. (2) Salts. No information. (3) Water. No information.  <b>ESTIMATED ERROR:</b> δT/K = 0.1 δS/mg dm <sup>-3</sup> = 0.05 Max error in S is 1.8 per cent.  <b>REFERENCES:</b>																																												



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<p>Air (dust free and foreign gas free), saturated with water vapor from the salt solution, is bubbled for several hours through 500 cm<sup>3</sup> of solution.</p> <p>Three samples are taken and analyzed by the Winkler chemical method. For fluoride solutions a stoichiometric amount of boric acid was added before analysis to bind the fluoride as tetrafluoroborate ion.</p> <p>The solubility unit is mg dm<sup>-3</sup> at the normal oxygen partial pressure in air of 0.21 atm. The solubility in water is 8.15 mg dm<sup>-3</sup>.</p> <p>The results are presented graphically as log S vs. c<sub>3</sub>. The slope is given as the salt effect parameter (Sechenow constant) k.</p>	<p>(1) Oxygen. Air treated to free from dust and any foreign gases.</p> <p>(2) Salts. No information.</p> <p>(3) Water. No information.</p> <hr/> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"> <math>\delta T/K = 0.1</math>  <math>\delta S/\text{mg dm}^{-3} = 0.05</math>            Max error in S 1.8 per cent.         </p> <hr/> <p>REFERENCES:</p>																																												

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T/K	Maximum Salt Concentration c <sub>3</sub> /mol dm <sup>-3</sup>	Number of Experimental Points	Salt Effect Parameter k = (1/c <sub>3</sub> ) log(S <sup>0</sup> /S)
Lithium chloride; LiCl; [7447-41-8]			
298.15	1.2	9	(0.112 to 0.070) <sup>1</sup>
Sodium chloride; NaCl; [7647-14-5]			
298.15	1.2	7	0.136
Potassium chloride; KCl; [7447-40-7]			
298.15	1.2	6	0.129
Rubidium chloride; RbCl; [7791-11-9]			
298.15	0.5	7	0.120
Cesium chloride; CsCl; [7647-17-8]			
298.15	0.5	7	0.098
<sup>1</sup> Lithium chloride salts out linearly from 0 to about 0.1 mol dm <sup>-3</sup> (k = 0.112) and above 0.2 mol dm <sup>-3</sup> (k = 0.070).			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:	SOURCE AND PURITY OF MATERIALS:		
Air, saturated with water vapor from the salt solution, is bubbled for several hours through 500 cm <sup>3</sup> of solution.  Three samples are taken and analyzed by the Winkler chemical method.	(1) Oxygen. Air treated to free from dust and any foreign gases.  (2) Salts. No information.  (3) Water. No information.		
The solubility unit is mg dm <sup>-3</sup> at the normal oxygen partial pressure in air of 0.21 atm. The solubility in water is 8.15 mg dm <sup>-3</sup> .	ESTIMATED ERROR: δT/K = 0.1 δS/mg dm <sup>-3</sup> = 0.05 Max error in S is 1.8 per cent		
The results are presented graphically as log S vs. c <sub>3</sub> . The slope is given as the salt effect parameter (Sechenow constant) k.	REFERENCES:		

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Alkali metal bromides, LiBr, NaBr, KBr, RbBr, and CsBr (3) Water, H <sub>2</sub> O; [7732-18-5]		Khomutov, N. E.; Konnik, E. I. <i>Zh. Fiz. Khim.</i> <u>1974</u> , <i>48</i> , 620-5. <i>Russ. J. Phys. Chem.</i> <u>1974</u> , <i>48</i> , 359-62.	
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EXPERIMENTAL VALUES:			
T/K	Maximum Salt Concentration c <sub>3</sub> /mol dm <sup>-3</sup>	Number of Experimental Points	Salt Effect Parameter k = (1/c <sub>3</sub> ) log(S <sup>0</sup> /S)
Lithium bromide; LiBr; [7550-35-8]			
298.15	1.2	10	(0.252 to 0.084) <sup>1</sup>
Sodium bromide; NaBr; [7647-15-6]			
298.15	1.2	7	0.131
Potassium bromide; KBr; [7758-02-3]			
298.15	1.2	6	0.117
Rubidium bromide; RbBr; [7789-39-1]			
298.15	0.5	7	0.104
Cesium bromide; CsBr; [7787-69-1]			
298.15	0.5	7	0.078
<sup>1</sup> Lithium bromide salts out linearly between 0 and about 0.07 mol dm <sup>-3</sup> (k = 0.252) and above about 0.15 mol dm <sup>-3</sup> (k = 0.084).			
AUXILIARY INFORMATION			
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Air, saturated with water vapor from the salt solution, is bubbled for several hours through 500 cm <sup>3</sup> of solution.  Three samples are taken and analyzed by the Winkler chemical method.  The solubility unit is mg dm <sup>-3</sup> at the normal oxygen partial pressure in air of 0.21 atm. The solubility in water is 8.15 mg dm <sup>-3</sup> .  The results are presented graphically as log S vs. c <sub>3</sub> . The slope is given as the salt effect parameter (Sechenow constant) k.		(1) Oxygen. Air treated to free from dust and any foreign gases. (2) Salts. No information. (3) Water. No information.	
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(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Alkali metal iodides; LiI, NaI, KI, RbI, and CaI (3) Water; H <sub>2</sub> O; [7732-18-5]	Khomutov, N. E.; Konnik, E. I. <i>Zh. Fiz. Khim.</i> <u>1974</u> , <i>48</i> , 620-5. <i>Russ. J. Phys. Chem.</i> <u>1974</u> , <i>48</i> , 359-62.																																												
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Dialkali metal carbonates; Li <sub>2</sub> CO <sub>3</sub> , Na <sub>2</sub> CO <sub>3</sub> , and K <sub>2</sub> CO <sub>3</sub> (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Khomutov, N. E.; Konnik, E. I. <i>Zh. Fiz. Khim.</i> <u>1974</u> , <i>48</i> , 620-5. <i>Russ. J. Phys. Chem.</i> <u>1974</u> , <i>48</i> , 359-62.																												
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<b>VARIABLES:</b> T/K = 288-298 Concentration	<b>PREPARED BY:</b> C.L. Young; R. Battino																																
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<b>METHOD /APPARATUS/PROCEDURE:</b>  Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried.  (3) Degassed.																																
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium chloride; NaCl; [7647-14-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G.  <i>J. Phys. Chem.</i> <u>1916</u> , 20, 495-502.																																													
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 4	<b>PREPARED BY:</b> H. L. Clever																																													
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T/K	Sodium Chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>																																										
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solutions were thermostated in tall cylinder open to the air. They were shaken by hand several times a day for a period of four days.  A sample of 250 cm <sup>3</sup> was analyzed for oxygen by a modified Winkler method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air at one atm. (2) Sodium chloride. No information. (3) Water. No information.  <b>ESTIMATED ERROR:</b> The solubility values may be in 5 to 10 per cent error. The salt concentrations above one mol dm <sup>-3</sup> may be in error by 10 per cent.  <b>REFERENCES:</b>																																													

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Eucken, A.; Hertzberg, G.	
(2) Sodium Chloride; NaCl; [7647-14-5]		Z. Physik. Chem. <u>1950</u> , 195, 1 - 23.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES: T/K = 273.15 - 298.15 P/kPa = 101.325 m <sub>NaCl</sub> /mol kg <sup>-1</sup> = 0 - 2.49		PREPARED BY: P. L. Long H. L. Clever	
EXPERIMENTAL VALUES:			
T/K	Sodium Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	Setschenow Constant k = (1/m) log(L <sup>0</sup> /L)
273.15	0	0.0490	-
	0.48	0.0409	0.165
	1.23	0.0306	0.166
	2.49	0.0193	0.162
288.15	0	0.0365	-
	0.69	0.0289	0.148
	1.74	0.0203	0.146
293.15	0	0.0332	-
	0.81	0.0254	0.139
	1.77	0.0187	0.141
298.15	0	0.0307	-
	0.64	0.0250	0.139
	1.53	0.0187	0.141
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Gas absorption. The apparatus consists of a gas buret and an adsorption flask connected by a capillary tube. The whole apparatus is shaken. The capillary tube is a 2m-long glass helix. An amount of gas is measured at STP and placed in the gas buret. After shaking, the difference from the original amount of gas placed in the gas buret is determined.		Components. Neither source nor purity given.	
		ESTIMATED ERROR:	
		δL/L = 0.01	
		REFERENCES:	

NaCl/g eq dm <sup>-3</sup>		Bunsen Coefficient, $\alpha \times 10^3$											Salt Effect Parameter $k_s$	
T/K		0.0	0.5	1.0	1.5	2.0	2.5	3.0	3.5	4.0	4.5	5.0		5.4
273.15		48.9	39.8	32.1 31.2 <sup>1</sup>	26.3	21.4 22.5 <sup>1</sup>	17.4	14.1 15.1 <sup>1</sup>	11.5	9.2	7.6	6.2	5.2 6.1 <sup>1</sup>	0.180
278.15		42.9	35.4	29.1 27.9 <sup>1</sup>	24.0	19.8 20.4 <sup>1</sup>	16.3	13.4 13.6 <sup>1</sup>	11.1	9.1	7.5	6.2	5.3 5.9 <sup>1</sup>	0.168
283.15		38.5	32.0	26.6 25.3 <sup>1</sup>	22.2	18.4 18.6 <sup>1</sup>	15.3	12.8 12.5 <sup>1</sup>	10.6	8.8	7.3	6.1	5.3 5.6 <sup>1</sup>	0.160
288.15		34.2	28.6	23.9 23.1 <sup>1</sup>	20.0	16.7 17.0 <sup>1</sup>	13.9	11.6 11.7 <sup>1</sup>	9.7	8.1	6.8	5.7	4.9 5.4 <sup>1</sup>	0.156
293.15		30.8	25.9	21.9 21.4 <sup>1</sup>	18.4	15.5 15.7 <sup>1</sup>	13.1	11.0 11.0 <sup>1</sup>	9.3	7.8	6.6	5.5	4.8 5.2 <sup>1</sup>	0.149
298.15		28.2	23.9	20.2 20.0 <sup>1</sup>	17.1	14.5 14.7 <sup>1</sup>	12.2	10.4 10.4 <sup>1</sup>	8.8	7.4	6.3	5.3	4.7 5.0 <sup>1</sup>	0.145
303.15		26.3	22.5	19.1 18.7 <sup>1</sup>	16.3	13.9 14.0 <sup>1</sup>	11.8	10.0 10.0 <sup>1</sup>	8.6	7.3	6.2	5.3	4.7 4.8 <sup>1</sup>	0.139

<sup>1</sup> Appears to be experimental data of the authors.

The table of smoothed Bunsen coefficients of oxygen dissolved in aqueous sodium chloride solutions was prepared by the authors. The complete source of data for the table is not clear. The data of L. Winkler (*Z. angew. Chem.* 1911, 24, 341) are mentioned. A 1958 report of A. A. Cherepinnikov, mentioned in the paper, was not available to the compiler.

## COMPONENTS:

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Sodium chloride; NaCl;  
 [7647-14-5]  
 (3) Water; H<sub>2</sub>O; [7732-18-5]

## ORIGINAL MEASUREMENTS:

Mishina, T. A.; Avdeeva, O. I.  
 Bozhovskaya, T. K.  
*Materialy Vses. Nauchn. Issled.  
 Geol. Inst.* 1961, 46, 93-110.

## VARIABLES:

T/K = 273.15 - 303.15  
 P/kPa = 101.325  
 c<sub>3</sub>/mol dm<sup>-3</sup> = 0 - 5.4

## PREPARED BY:

A. L. Cramer  
 H. I. Clever.

## EXPERIMENTAL VALUES:

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium chloride; NaCl; [7647-14-5] or geothermal brines (3) Water; H <sub>2</sub> O; [7732-18-5]		Cramer, S. D. <i>Ind. Eng. Chem., Process Design Develop.</i> , 1980, 19. 300-5.			
VARIABLES:		PREPARED BY:			
T/K = 274.65 - 583.15 O <sub>2</sub> P/MPa = 4.3 - 5.2 m <sub>3</sub> /m <sup>3</sup> kg <sup>-1</sup> = 0 - 5.69		H. L. Clever			
Brine Characteristics					
Brine	Molality m/mol kg <sup>-1</sup>	Molarity c/mol dm <sup>-3</sup>	Ionic Strength I <sup>1</sup>	Constituents	
Water	0	0	0	Demineralized	
NaCl-1	0.87	0.85	0.87	NaCl	
NaCl-2	2.97	2.78	2.97	NaCl	
NaCl-3	5.69	5.09	5.69	NaCl	
EMGB	0.57	0.56	0.60	Mixed chlorides <sup>2</sup>	
SSGB	4.87	4.19	7.34	Mixed chlorides <sup>2</sup>	
<sup>1</sup> Based on molal concentrations. <sup>2</sup> Composition in the table below. Also see footnotes on page before.					
Composition (in ppm by weight) of the Geothermal Brines.					
Constituent	EMGB	SSGB	Constituent	EMGB	SSGB
Na	11 000	53 000	Rb	1.7	70
Ca	1 370	28 800	Cs	4	20
K	1 430	16 500	Mg	22	10
Fe	0.2	2 000	Cu	0.05	3 <sup>1</sup>
Mn	0.9	1 370	Ag	0.04	<1 <sup>1</sup>
Zn	0.02	500	Cl	18 000	155 000
Sr	226	440	NH <sub>4</sub>	3.9	Not det'n.
SiO <sub>2</sub>	101	400	Br	35	"
B	27	390	F	1.5	"
Ba	58	250	SO <sub>4</sub>	16	"
Li	55	210	S	Not det'n.	30
Pb	0.3	80			
<sup>1</sup> Not included in the synthetic brine.					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
The oxygen solubilities were determined from PVT measurements using the technique of gas extraction. The apparatus consists of (1) a high pressure, high temperature stainless steel stirred reactor fitted with a Pyrex liner for dissolving the gas in the brine, (2) a heat exchanger for cooling samples of gas saturated brine to room temperature, and (3) a low-pressure, constant-temperature unit for PVT measurements on collected gas and liquid samples.			(1) Oxygen. Source not given, stated to be 99.5 per cent. (2) Sodium chloride and SSGB. Prepared from reagent grade chemicals dissolved in demineralized water. (3) Water. Demineralized water. EMGB. Natural sample.		
Henry's constant is defined as $K^0 = \bar{f}_g/a_g$ . The fugacity, $\bar{f}_g = \phi_g P_g$ , where $\phi_g$ is the fugacity coefficient, and $P_g$ is the oxygen partial pressure. The activity, $a_g = \gamma x_g$ , where $\gamma$ is the activity coefficient of the dissolved gas, and $x_g$ is the mole fraction. The mole fraction is calculated with respect to the gas, the ionic species and the water.			ESTIMATED ERROR:		
$x_i = m_g / (m_g + \sum m_j \nu_{ij} + 1000/M_{H_2O})$			Author's analysis of experimental error.		
Variable		Uncertainty		Exp Error	
				%	
Reactor pressure		0.068 MPa		1.4	
Reactor temperature		2°C		4.2	
Sample volume:					
liquid fraction		0.4 cm <sup>3</sup>		2.6	
gas fraction		0.4 cm <sup>3</sup>		2.6	
Gas buret temp		2°C		0.6	
Atmospheric press		1 mmHg		0.3	
Brine conc		0.2 m		0.5	

COMPONENTS:  
 (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Sodium chloride; NaCl;  
 [7647-14-5]  
 or geothermal brines  
 (3) Water; H<sub>2</sub>O; [7732-18-5]

ORIGINAL MEASUREMENTS:  
 Cramer, S. D.  
*Ind. Eng. Chem., Process Design  
 Develop.* 1980, 19, 300-5.

EXPERIMENTAL VALUES:

continued

Water			Sodium Chloride $m_3/\text{mol kg}^{-1} = 0.87^1$			Sodium Chloride $m_3/\text{mol kg}^{-1} = 2.97^2$			Sodium Chloride $m_3/\text{mol kg}^{-1} = 5.69^3$		
Temperature T/K	t/°C	Henry's Constant $K \times 10^{-3}/$ MPa	Temperature T/K	t/°C	Henry's Constant $K \times 10^{-3}/$ MPa	Temperature T/K	t/°C	Henry's Constant $K \times 10^{-3}/$ MPa	Temperature T/K	t/°C	Henry's Constant $K \times 10^{-3}/$ MPa
276.15	3.0	2.53	274.65	1.5	4.02	274.65	1.5	10.02	276.15	3.0	20.29
279.65	6.5	2.92	279.85	6.7	4.98	280.65	7.5	10.28	280.55	7.4	22.77
280.65	7.5	3.33	286.65	13.5	5.09	284.95	11.8	11.24	286.85	13.7	22.98
286.85	13.7	3.67	293.35	20.2	5.68	292.15	19.0	11.78	299.45	26.3	23.69
292.15	19.0	4.06	303.35	30.2	7.02	296.65	23.5	12.14	321.05	47.9	26.16
295.55	22.4	4.63				300.55	27.4	12.77	332.25	59.1	26.29
297.45	24.3	4.31	315.15	42.0	7.51	322.75	49.6	14.55	346.65	73.5	26.95
301.65	28.5	4.98	315.65	42.5	7.52	332.25	59.1	15.95	357.25	84.1	26.52
305.15	32.0	5.11	322.75	49.6	8.06	348.35	75.2	14.73	368.35	95.2	28.39
315.15	42.0	5.25	323.15	50.0	8.01	368.85	95.7	14.29	385.85	110.7	24.80
315.65	42.5	5.27	324.15	51.0	7.76	390.55	117.4	12.21	390.55	117.4	23.90
322.75	49.6	6.48	334.65	61.5	8.10	410.55	137.4	12.79	401.65	128.5	23.94
323.15	50.0	5.65	336.05	62.9	8.92	430.65	157.5	13.18	438.85	165.7	16.49
324.15	51.0	5.83	343.35	70.2	8.63	458.35	185.2	9.45	461.05	187.9	14.72
333.85	60.7	7.34	357.15	84.0	9.44	513.65	240.5	6.72	481.05	207.9	14.69
344.95	71.8	7.06	372.15	99.0	9.58	513.85	240.7	6.89	514.95	241.8	19.90
348.35	75.2	7.06	398.15	125.0	8.57	542.75	269.6	4.96	532.95	259.8	9.89
363.35	90.2	7.27	423.85	150.7	7.79	569.35	296.2	4.04	543.15	270.0	10.25
363.35	90.2	7.27	439.95	166.8	6.79				562.15	289.0	8.16
373.35	100.2	7.52	476.05	202.9	6.14						
387.75	114.6	7.50	514.35	241.2	3.72						
396.05	122.9	6.91	530.45	257.3	3.50						
413.35	140.2	6.89	559.05	285.9	2.27						
438.35	165.2	5.88									
461.05	187.9	4.38									
513.85	240.7	2.94									
561.15	288.0	1.35									

<sup>1</sup> Author designated NaCl-1<sup>2</sup> Author designated NaCl-2<sup>3</sup> Author designated NaCl-3

COMPONENTS:  
 (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Sodium chloride; NaCl;  
 [7647-14-5]  
 or geothermal brines  
 (3) water; H<sub>2</sub>O; [7732-18-5]

ORIGINAL MEASUREMENTS:  
 Cramer, S. D.  
*Ind. Eng. Chem., Process Design  
 Develop.* 1990, 19, 300-5.

EXPERIMENTAL VALUES:

continued

Water			Water			EMGB <sup>1</sup> m/mol kg <sup>-1</sup> = 0.57			SSGB <sup>2</sup> m/mol kg <sup>-1</sup> = 4.87		
Temperature T/K	Henry's Constant t/°C K x 10 <sup>-3</sup> / MPa	Henry's Constant K x 10 <sup>-3</sup> / MPa	Temperature T/K	Henry's Constant t/°C K x 10 <sup>-3</sup> / MPa	Henry's Constant K x 10 <sup>-3</sup> / MPa	Temperature T/K	Henry's Constant t/°C K x 10 <sup>-3</sup> / MPa	Henry's Constant K x 10 <sup>-3</sup> / MPa	Temperature T/K	Henry's Constant t/°C K x 10 <sup>-3</sup> / MPa	Henry's Constant K x 10 <sup>-3</sup> / MPa
276.15	3.0	2.53	348.35	75.2	7.06	275.45	2.3	3.65	274.95	1.8	12.41
279.65	6.5	2.92	363.35	90.2	7.27	279.95	6.8	3.87	280.65	7.5	14.64
280.65	7.5	3.33	373.35	100.2	7.52	286.65	13.5	4.34	285.15	12.0	15.99
286.85	13.7	3.67	387.75	114.6	7.50	319.65	46.5	7.26	292.15	19.0	15.90
292.15	19.0	4.06	396.05	122.9	6.91	333.85	60.7	7.48	294.45	21.3	18.02
295.55	22.4	4.63	413.35	140.2	6.89	352.35	79.2	7.88	301.65	28.5	18.64
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305.15	32.0	5.11	513.85	240.7	2.94	391.15	118.0	7.57	349.95	76.8	19.77
315.15	42.0	5.25	561.15	288.0	1.35	428.15	155.0	6.14	367.15	94.0	19.77
315.65	42.5	5.27				473.75	200.6	4.34	396.65	123.5	17.76
322.75	49.6	6.48				475.15	202.0	4.66	411.05	137.9	15.67
323.15	50.0	5.65				495.15	222.0	3.79	423.35	150.2	14.49
324.15	51.0	5.83							425.55	152.4	13.87
333.85	60.7	7.34							461.05	187.9	11.10
344.95	71.8	7.06							503.25	230.1	9.36
									545.55	272.4	6.10
									559.65	286.5	7.20
									583.15	310.0	5.63

<sup>1</sup> East Mesa geothermal brine, an unflashed sample from geothermal well Mesa G-1. (1)  
 The composition of the low-salinity brine is given on the next page.

<sup>2</sup> Salton Sea geothermal brine, a synthetic brine based on an analysis of unflashed hypersaline brine from geothermal well IID-2 on the Salton sea geothermal field (2). The composition of the brine is given on the next page.

## REFERENCES:

- Berthold, C. E.; Hadzeriga, P.; Christopher, D. H.; Applegate, T. A.; Gillespie, D. M.  
 "Process Technology for Recovering Geothermal Brine Minerals", PB-241867, Hazen Research, Inc.,  
 Golden, Co., 1975, Feb. 4.
- Helgeson, H. C. *Am. J. Sci.* 1968, 266, 129.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium bromide; NaBr; [7647-15-6] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G.  <i>J. Phys. Chem.</i> <u>1916</u> , <i>20</i> , 495-502.																																																		
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 6	<b>PREPARED BY:</b> H. L. Clever																																																		
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<b>VARIABLES:</b>  T/K = 298.15 O <sub>2</sub> P/kPa = 101.325	<b>PREPARED BY:</b>  P. L. Long H. L. Clever															
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="197 516 1065 715"> <thead> <tr> <th>Temperature <i>t</i> / °C</th> <th>Solvent Volume cm<sup>3</sup></th> <th>Oxygen Volume Absorbed cm<sup>3</sup></th> <th>Bunsen Coefficient <math>\alpha \times 10^2</math></th> <th>Ostwald Coefficient L x 10<sup>2</sup></th> </tr> </thead> <tbody> <tr> <td>25</td> <td>298.15</td> <td>49.54 49.54</td> <td>0.44 0.44</td> <td>0.81 av.</td> <td>0.89 av.</td> </tr> </tbody> </table> <p data-bbox="197 735 1065 815">The solvent was a mixture of 800 g H<sub>2</sub>O 200 g Na<sub>2</sub>SO<sub>4</sub> (anhydrous) 40 cm<sup>3</sup> H<sub>2</sub>SO<sub>4</sub> (conc., 36 N)</p> <p data-bbox="197 834 1065 954">Thus the solution molality was</p> <table data-bbox="447 854 802 954"> <tbody> <tr> <td><math>m_{\text{Na}_2\text{SO}_4} / \text{mol kg}^{-1}</math></td> <td>1.76</td> </tr> <tr> <td><math>m_{\text{H}_2\text{SO}_4} / \text{mol kg}^{-1}</math></td> <td>0.90</td> </tr> </tbody> </table>		Temperature <i>t</i> / °C	Solvent Volume cm <sup>3</sup>	Oxygen Volume Absorbed cm <sup>3</sup>	Bunsen Coefficient $\alpha \times 10^2$	Ostwald Coefficient L x 10 <sup>2</sup>	25	298.15	49.54 49.54	0.44 0.44	0.81 av.	0.89 av.	$m_{\text{Na}_2\text{SO}_4} / \text{mol kg}^{-1}$	1.76	$m_{\text{H}_2\text{SO}_4} / \text{mol kg}^{-1}$	0.90
Temperature <i>t</i> / °C	Solvent Volume cm <sup>3</sup>	Oxygen Volume Absorbed cm <sup>3</sup>	Bunsen Coefficient $\alpha \times 10^2$	Ostwald Coefficient L x 10 <sup>2</sup>												
25	298.15	49.54 49.54	0.44 0.44	0.81 av.	0.89 av.											
$m_{\text{Na}_2\text{SO}_4} / \text{mol kg}^{-1}$	1.76															
$m_{\text{H}_2\text{SO}_4} / \text{mol kg}^{-1}$	0.90															
<b>AUXILIARY INFORMATION</b>																
<b>METHOD/APPARATUS/PROCEDURE:</b>  The apparatus was described in detail in an earlier paper (1). The apparatus consists of a gas buret, a pressure compensator, a 200 cm <sup>3</sup> absorption bulb, and a mercury leveling bulb. The absorption bulb is attached to a shaking mechanism.  The solvent and the gas are placed in the absorption bulb. The bulb was shaken until equilibrium was reached. The remaining gas was returned to the buret. The difference in the final and initial volumes was taken as the gas absorbed.	<b>SOURCE AND PURITY OF MATERIALS:</b>  (1) Oxygen. Source not given. Purity stated to be 99 <sup>+</sup> per cent. (2,3) Sodium sulfate and sulfuric acid. Sources not given. Analytical grades. (4) Water. Distilled.  <b>ESTIMATED ERROR:</b>  $\delta\alpha / \text{cm}^3 = 0.001$ (authors)  <b>REFERENCES:</b>  1. Kobe, K. A.; Williams, J. S. <i>Ind. Eng. Chem., Anal. Ed.</i> <u>1935</u> , <i>7</i> , 37.															

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium sulfate; Na <sub>2</sub> SO <sub>4</sub> ; [7757-82-6] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b>  Linek, V.; Mayrhoferova, J.  <i>Chem. Eng. Sci.</i> <u>1970</u> , <i>25</i> , 787 - 800.																																		
<b>VARIABLES:</b> $T/K = 288 - 308$ $p/kPa = 101.325 \text{ (1 atm)}$ $c_2/\text{kmol m}^{-3} = 0 - 1.0$	<b>PREPARED BY:</b> H. L. Clever																																		
<b>EXPERIMENTAL VALUES:</b>  <table border="1" data-bbox="319 519 937 970"> <thead> <tr> <th colspan="2">Temperature</th> <th rowspan="2">Sodium Sulfate<sup>1</sup> <math>c_2/\text{kmol m}^{-3}</math><sup>2</sup></th> <th rowspan="2">Oxygen Solubility <math>c_1/\text{kmol m}^{-3}</math><sup>2</sup></th> </tr> <tr> <th><math>t/^\circ\text{C}</math></th> <th><math>T/K</math></th> </tr> </thead> <tbody> <tr> <td>15</td> <td>288</td> <td>0.50</td> <td>9.88</td> </tr> <tr> <td rowspan="5">20</td> <td rowspan="5">293</td> <td>0</td> <td>13.60</td> </tr> <tr> <td>0.25</td> <td>10.92</td> </tr> <tr> <td>0.50</td> <td>8.93</td> </tr> <tr> <td>0.75</td> <td>7.42</td> </tr> <tr> <td>1.00</td> <td>6.06</td> </tr> <tr> <td>25</td> <td>298</td> <td>0.50</td> <td>8.15</td> </tr> <tr> <td>30</td> <td>303</td> <td>0.50</td> <td>7.49</td> </tr> <tr> <td>35</td> <td>308</td> <td>0.50</td> <td>7.03</td> </tr> </tbody> </table> <p data-bbox="293 989 1027 1087"><sup>1</sup> The table of data in the original paper is labeled sodium sulfite, however, the measurements were made in sodium sulfate solution and it was assumed they were the same in sodium sulfite.</p> <p data-bbox="293 1107 895 1136"><sup>2</sup> <math>\text{kmol m}^{-3}</math> is the same number as <math>\text{mol dm}^{-3}</math>.</p>		Temperature		Sodium Sulfate <sup>1</sup> $c_2/\text{kmol m}^{-3}$ <sup>2</sup>	Oxygen Solubility $c_1/\text{kmol m}^{-3}$ <sup>2</sup>	$t/^\circ\text{C}$	$T/K$	15	288	0.50	9.88	20	293	0	13.60	0.25	10.92	0.50	8.93	0.75	7.42	1.00	6.06	25	298	0.50	8.15	30	303	0.50	7.49	35	308	0.50	7.03
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<b>METHOD/APPARATUS/PROCEDURE:</b>  The details of the method were not given.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. No information. (2) Sodium sulfate. No information. (3) Water. Distilled in all glass apparatus.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>																																		

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium sulfate; Na <sub>2</sub> SO <sub>4</sub> ; [7757-82-6] (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89-94.
VARIABLES: T/K= 288.15-308.15 O <sub>2</sub> P/kPa= 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 1.656	PREPARED BY: H. L. Clever; C. L. Young

## EXPERIMENTAL VALUES:

T/K	Sodium sulfate c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L	T/K	Sodium sulfate c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L
288.15	0.0	0.03643	298.15	0.762	0.01704
	0.105	0.03370		0.988	0.01455
	0.216	0.03058		1.228	0.01244
	0.315	0.02734		1.240	0.01225
	0.479	0.02386		1.498	0.01067
	0.594	0.02183		1.517	0.01040
	0.701	0.02030			
	0.891	0.01823			
298.15	0.0	0.03114	308.15	0.0	0.02764
	0.155	0.02732		0.317	0.02043
	0.239	0.02489		0.609	0.01650
	0.510	0.02018		0.967	0.01286
	0.513	0.02032		1.301	0.01055
	0.618	0.01855		1.656	0.00860

The author correlated the data by the empirical equation  $\log(L_0/L) = Ac_3/(1 + Bc_3)$ . The constants for the equation are:

T/K	A/dm <sup>3</sup> mol <sup>-1</sup>	B/dm <sup>3</sup> mol <sup>-1</sup>
288.15	0.420	0.251
298.15	0.398	0.183
308.15	0.421	0.231

## AUXILIARY INFORMATION

## METHOD/APPARATUS/PROCEDURE:

The apparatus is similar to that described by Horiuti (1).

The aqueous salt solution is degassed by boiling under reflux and under vacuum.

The gas phase volume and the solvent volume are measured by displacement of mercury.

Dry gas is intermittently added until equilibrium is attained. At that time total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded.

The salt concentration and density are determined after the measurement. Salt solution vapor pressure is taken from the literature. A correction for the increase of the liquid volume by the dissolved gas is made.

## SOURCE AND PURITY OF MATERIALS:

- (1) Oxygen. Extra pure grade. Stated to be 99.995 per cent.
- (2) Sodium sulfate. "Gauranteed reagent".
- (3) Water. No information.

## ESTIMATED ERROR:

Average deviation 0.3 to 0.5 per cent

## REFERENCES:

1. Horiuti, J.  
*J. Sci. Pap. Inst. Phys. Chem. Res. Tokyo* 1931, 17, 125.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium sulfite; Na <sub>2</sub> SO <sub>3</sub> ; [7757-83-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Gestrich, W.; Pontow, B. <i>Chem.-Ing.-Tech.</i> <u>1977</u> , 49, 564-5.																																																																				
<b>VARIABLES:</b> T/K = 273.15-303.15 P/kPa = 60.0 - 200 (0.6 - 2 bar) c <sub>3</sub> /mol dm <sup>-3</sup> = 0.05 - 1.2	<b>PREPARED BY:</b> H. L. Clever																																																																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Sodium sulfite c<sub>3</sub>/mol dm<sup>-3</sup></th> <th style="text-align: center;">Henry's constant<sup>1</sup> K x 10<sup>3</sup></th> <th style="text-align: center;">Measured pH at 293.15 K</th> </tr> </thead> <tbody> <tr> <td rowspan="5" style="text-align: center;">273.15</td> <td style="text-align: center;">0.05</td> <td style="text-align: center;">2.08</td> <td style="text-align: center;">8.30</td> </tr> <tr> <td style="text-align: center;">0.2</td> <td style="text-align: center;">1.61</td> <td style="text-align: center;">8.15</td> </tr> <tr> <td style="text-align: center;">0.6</td> <td style="text-align: center;">1.33</td> <td style="text-align: center;">8.03</td> </tr> <tr> <td style="text-align: center;">0.8</td> <td style="text-align: center;">1.03</td> <td style="text-align: center;">7.97</td> </tr> <tr> <td style="text-align: center;">1.2</td> <td style="text-align: center;">0.747</td> <td style="text-align: center;">7.78</td> </tr> <tr> <td rowspan="5" style="text-align: center;">288.15</td> <td style="text-align: center;">0.05</td> <td style="text-align: center;">1.50</td> <td style="text-align: center;">8.30</td> </tr> <tr> <td style="text-align: center;">0.2</td> <td style="text-align: center;">1.32</td> <td style="text-align: center;">8.15</td> </tr> <tr> <td style="text-align: center;">0.6</td> <td style="text-align: center;">0.995</td> <td style="text-align: center;">8.03</td> </tr> <tr> <td style="text-align: center;">0.8</td> <td style="text-align: center;">0.831</td> <td style="text-align: center;">7.97</td> </tr> <tr> <td style="text-align: center;">1.2</td> <td style="text-align: center;">0.518</td> <td style="text-align: center;">7.78</td> </tr> <tr> <td rowspan="5" style="text-align: center;">298.15</td> <td style="text-align: center;">0.05</td> <td style="text-align: center;">1.25</td> <td style="text-align: center;">8.30</td> </tr> <tr> <td style="text-align: center;">0.2</td> <td style="text-align: center;">1.12</td> <td style="text-align: center;">8.15</td> </tr> <tr> <td style="text-align: center;">0.6</td> <td style="text-align: center;">0.872</td> <td style="text-align: center;">8.03</td> </tr> <tr> <td style="text-align: center;">0.8</td> <td style="text-align: center;">0.600</td> <td style="text-align: center;">7.97</td> </tr> <tr> <td style="text-align: center;">1.2</td> <td style="text-align: center;">0.463</td> <td style="text-align: center;">7.78</td> </tr> <tr> <td rowspan="5" style="text-align: center;">303.15</td> <td style="text-align: center;">0.05</td> <td style="text-align: center;">1.08</td> <td style="text-align: center;">8.30</td> </tr> <tr> <td style="text-align: center;">0.2</td> <td style="text-align: center;">1.03</td> <td style="text-align: center;">8.15</td> </tr> <tr> <td style="text-align: center;">0.6</td> <td style="text-align: center;">0.775</td> <td style="text-align: center;">8.03</td> </tr> <tr> <td style="text-align: center;">0.8</td> <td style="text-align: center;">0.647</td> <td style="text-align: center;">7.97</td> </tr> <tr> <td style="text-align: center;">1.2</td> <td style="text-align: center;">0.476</td> <td style="text-align: center;">7.78</td> </tr> </tbody> </table> <p style="text-align: center;"><sup>1</sup>Henry's constant, 10<sup>3</sup> K/mol dm<sup>-3</sup> atm<sup>-1</sup>.</p>		T/K	Sodium sulfite c <sub>3</sub> /mol dm <sup>-3</sup>	Henry's constant <sup>1</sup> K x 10 <sup>3</sup>	Measured pH at 293.15 K	273.15	0.05	2.08	8.30	0.2	1.61	8.15	0.6	1.33	8.03	0.8	1.03	7.97	1.2	0.747	7.78	288.15	0.05	1.50	8.30	0.2	1.32	8.15	0.6	0.995	8.03	0.8	0.831	7.97	1.2	0.518	7.78	298.15	0.05	1.25	8.30	0.2	1.12	8.15	0.6	0.872	8.03	0.8	0.600	7.97	1.2	0.463	7.78	303.15	0.05	1.08	8.30	0.2	1.03	8.15	0.6	0.775	8.03	0.8	0.647	7.97	1.2	0.476	7.78
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus consists of an absorption flask (ca. 40 cm<sup>3</sup>) with a magnetic stirrer, a mercury manometer, and a motor controlled buret for the oxygen.</p> <p>Five to six measurements were made at each temperature and salt concentration at pressures between 0.6 and 2 bar. Only the measurements at 298.15 K were shown in a graph. The Henry's constants were tabulated, and are given above. No value for water was given.</p> <p>The salt solution was prepared in a 38:1 ratio of Na<sub>2</sub>SO<sub>3</sub> and Na<sub>2</sub>S<sub>2</sub>O<sub>5</sub>.</p> <p>The temperature coefficient of Henry's constant gives an enthalpy of solution of (-3.07 ± 0.05) kcal mol<sup>-1</sup>.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.																																																																				
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium nitrate; NaNO <sub>3</sub> ; [7631-99-4] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A. <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-89.																														
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 5.121	<b>PREPARED BY:</b> H. L. Clever																														
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium hydroxide; NaOH; [1310-73-2] (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Geffcken, G. <i>Z. Phys. Chem.</i> <u>1904</u> , 49, 257-302.
<b>VARIABLES:</b> T/K = 288-298 Composition		<b>PREPARED BY:</b> C.L. Young; R. Battino
<b>EXPERIMENTAL VALUES:</b>		
T/K	Conc of hydroxide/mol dm <sup>-3</sup> (soln)	Ostwald coefficient, <i>L</i>
288.15	0.559	0.02777
	0.601	0.02784
	1.033	0.02291
	1.059	0.02262
	2.077	0.01479
	2.089	0.01456
298.15	0.559	0.02434
	0.601	0.02424
	1.033	0.02020
	1.059	0.01991
	2.077	0.01295
	2.089	0.01272
<b>AUXILIARY INFORMATION</b>		
<b>METHOD /APPARATUS/PROCEDURE:</b>  Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried. (3) Degassed.	
	<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1; \delta L = \pm 1\%$ . (estimated by compiler).	
	<b>REFERENCES:</b>	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium hydroxide; NaOH; [1310-73-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Levina, M.I.; Stisibarovskaya, N. P. <i>Russ. J. Phys. Chem.</i> <u>1939</u> , <i>12</i> , 653-9.
<b>VARIABLES:</b> T/K = 273-533 P/MPa = 9.81 Concentration	<b>PREPARED BY:</b> V. Katovic

EXPERIMENTAL VALUES:			Oxygen Solubility <sup>b</sup> NaOH Solution/N			
t/°C	T <sup>a</sup> /K	H <sub>2</sub> O	0.5	2	4	
Total pressure of 100 kg/cm <sup>2</sup> (9.81 MPa)						
0	273	0.66	0.54	0.28	0.09	
25	298	0.51	0.40	0.19	0.08	
35	308	0.44	0.34	0.16	0.07	
50	323	0.34	0.30	0.12	0.07	
75	348	0.31	0.27	0.11	0.07	
100	373	0.33	0.28	0.13	0.08	
125	398	0.34	0.27	0.14	--	
150	423	0.41	0.32	0.17	0.08	
200	473	0.51	0.37	0.20	0.11	
240	513	0.57	0.48	0.25	0.14	

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Solubility in cm<sup>3</sup> (STP) per 1 gram of solvent at total pressure of 100 kg/cm<sup>2</sup> (9.81 MPa).

continued on following page

#### AUXILIARY INFORMATION

<b>METHOD/APPARATUS/PROCEDURE:</b> Solubility determined by an apparatus described in the paper by measuring the volume of liquid and air. Oxygen was determined with pyrogallol.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From air. (2,3) No details given.
	<b>ESTIMATED ERROR:</b>
	<b>REFERENCES:</b>



COMPONENTS:	EVALUATOR:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Levina, M.I.; Stisibarovskaya, N. P.
(2) Sodium hydroxide; NaOH; [1310-73-2]	<i>Russ. J. Phys. Chem.</i> <u>1939</u> ,12, 653-9.
(3) Water; H <sub>2</sub> O; [7732-18-5]	

## CRITICAL EVALUATION:

continued

t/°C	T <sup>a</sup> K	H <sub>2</sub> O	Solubility Coefficient <sup>b</sup>		
			NaOH Solution/N	0.5	2
Partial pressure of O <sub>2</sub> of 100 kg/cm <sup>2</sup> (0.81 MPa)					
0	273	3.14	2.55	1.32	0.43
25	298	2.45	1.91	0.89	0.33
35	308	2.09	1.62	0.78	0.33
50	323	1.78	1.41	0.59	0.33
75	348	1.46	1.30	0.51	0.33
100	373	1.55	1.34	0.61	0.38
125	398	1.62	1.32	0.66	--
150	423	2.05	0.82	0.40	1.06
200	473	2.88	2.12	1.09	1.06 <sup>c</sup>
240	513	4.09	3.50	1.76	0.95

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Solubility coefficient of cm<sup>3</sup> (STP) per 1 gram of solution at a partial oxygen pressure of 100 kg/cm<sup>2</sup> (9.81 MPa).

<sup>c</sup> Value reported in paper was 10.61 which must be a typographical error.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium hydroxide; NaOH; [1310-73-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Bruhn, G.; Gerlach, J.; Pawlek, F. <i>Z. Anorg. Allgem. Chem.</i> <u>1965</u> , 337, 68-79.																																						
<b>VARIABLES:</b>  T/K = 323-523 Concentration	<b>PREPARED BY:</b>  C.L. Young																																						
<b>EXPERIMENTAL VALUES:</b>																																							
<table border="1"> <thead> <tr> <th data-bbox="163 518 211 542">T/K</th> <th data-bbox="339 514 698 542">Conc of hydroxide/mol l<sup>-1</sup></th> <th data-bbox="786 514 1060 568">Bunsen coefficient, α/cm<sup>3</sup>(STP)cm<sup>-3</sup> atm<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td data-bbox="136 592 221 616" rowspan="3">323.15</td> <td data-bbox="484 592 523 616">0.5</td> <td data-bbox="873 592 975 616">0.01692</td> </tr> <tr> <td data-bbox="484 618 523 642">1.0</td> <td data-bbox="873 618 975 642">0.01356</td> </tr> <tr> <td data-bbox="484 644 523 667">1.5</td> <td data-bbox="873 644 975 667">0.01104</td> </tr> <tr> <td data-bbox="136 677 221 701" rowspan="3">373.15</td> <td data-bbox="484 677 523 701">0.5</td> <td data-bbox="873 677 975 701">0.01369</td> </tr> <tr> <td data-bbox="484 703 523 727">1.0</td> <td data-bbox="873 703 975 727">0.01199</td> </tr> <tr> <td data-bbox="484 729 523 753">1.5</td> <td data-bbox="873 729 975 753">0.00954</td> </tr> <tr> <td data-bbox="136 763 221 787" rowspan="3">423.15</td> <td data-bbox="484 763 523 787">0.5</td> <td data-bbox="873 763 961 787">0.0160</td> </tr> <tr> <td data-bbox="484 789 523 813">1.0</td> <td data-bbox="873 789 975 813">0.01225</td> </tr> <tr> <td data-bbox="484 815 523 838">1.5</td> <td data-bbox="873 815 975 838">0.01052</td> </tr> <tr> <td data-bbox="136 848 221 872" rowspan="3">473.15</td> <td data-bbox="484 848 523 872">0.5</td> <td data-bbox="873 848 975 872">0.02133</td> </tr> <tr> <td data-bbox="484 874 523 898">1.0</td> <td data-bbox="873 874 975 898">0.01698</td> </tr> <tr> <td data-bbox="484 900 523 924">1.5</td> <td data-bbox="873 900 975 924">0.01568</td> </tr> <tr> <td data-bbox="136 934 221 958" rowspan="3">523.15</td> <td data-bbox="484 934 523 958">0.5</td> <td data-bbox="873 934 975 958">0.03160</td> </tr> <tr> <td data-bbox="484 960 523 984">1.0</td> <td data-bbox="873 960 975 984">0.02563</td> </tr> <tr> <td data-bbox="484 986 523 1009">1.5</td> <td data-bbox="873 986 975 1009">0.02078</td> </tr> </tbody> </table>		T/K	Conc of hydroxide/mol l <sup>-1</sup>	Bunsen coefficient, α/cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	323.15	0.5	0.01692	1.0	0.01356	1.5	0.01104	373.15	0.5	0.01369	1.0	0.01199	1.5	0.00954	423.15	0.5	0.0160	1.0	0.01225	1.5	0.01052	473.15	0.5	0.02133	1.0	0.01698	1.5	0.01568	523.15	0.5	0.03160	1.0	0.02563	1.5	0.02078
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<b>AUXILIARY INFORMATION</b>																																							
<b>METHOD/APPARATUS/PROCEDURE:</b>  Static equilibrium cell. Similar to that described by Pray and Stephan (1). Composition of liquid determined by stripping solution of gas and estimating volumetrically.	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details given.  <b>ESTIMATED ERROR:</b> δT/K = ±2; δα = ±2%. (estimated by compiler).  <b>REFERENCES:</b> 1. Pray, H.A.; Stephan, E.L. <i>Battelle Memorial Institute Report, BMI-840, 1953.</i>																																						

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Sodium hydroxide; NaOH; [1310-73-2]</p> <p>(3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Yasunishi, A.</p> <p><i>Kagaku Kogaku Rombunshu</i> <u>1978</u>, 4, 185-9.</p>
<p>VARIABLES:</p> <p>T/K = 288.15 - 308.15</p> <p>O<sub>2</sub> P/kPa = 101.325</p> <p>c<sub>3</sub>/mol dm<sup>-3</sup> = 0 - 6.423</p>	<p>PREPARED BY:</p> <p>H. L. Clever</p>
<p>EXPERIMENTAL VALUES:</p> <p style="text-align: right;">continued on following page</p>	
<p>AUXILIARY INFORMATION</p>	
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used.</p> <p>The aqueous salt solution is degassed by boiling under reflux and under vacuum.</p> <p>The gas phase volume and the solvent volume are measured by displacement of mercury.</p> <p>Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded.</p> <p>The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. High purity grade stated to be 99.995 per cent.</p> <p>(2) Sodium hydroxide.</p> <p>(3) No information.</p> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p> <p>1. Yasunishi, A., <i>J. Chem. Eng. Jpn.</i> <u>1977</u>, 10, 89.</p>

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium hydroxide; NaOH; [1310-73-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Yasunishi, A. <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.
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 EXPERIMENTAL VALUES: continued

T/K	Sodium hydroxide c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L
288.15	0.0	0.03643 <sup>1</sup>
	0.589	0.02869
	1.064	0.02375
	1.997	0.01686
	2.676	0.01353
	3.547	0.01039
	4.095	0.00815
	4.447	0.00723
	5.188	0.00551
	5.419	0.00524
298.15	0.0	0.03114 <sup>1</sup>
	0.624	0.02437
	1.025	0.02099
	1.959	0.01490
	3.613	0.00800
	4.115	0.00688
	4.779	0.00530
	6.423	0.00297
308.15	0.0	0.02764 <sup>1</sup>
	0.674	0.02084
	0.773	0.02033
	0.986	0.01817
	1.630	0.01445
	2.153	0.01201
	2.476	0.01079
	3.424	0.00756

<sup>1</sup> Values from reference 1.

The author correlated the data by the Setschenow equation  $\log(L_0/L) = KC_3$ . Values of K are 0.158, 0.160, and 0.167 for temperatures of 288.15, 298.15, and 308.15 K, respectively. The data were also correlated by the empirical equation  $\log(L_0/L) = AC_3/(1 + BC_3)$ . Values of A and B are

T/K	A/dm <sup>3</sup> mol <sup>-1</sup>	B/dm <sup>3</sup> mol <sup>-1</sup>
288.15	0.171	0.0181
298.15	0.164	0.0049
308.15	0.181	0.0310

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium hydroxide; NaOH; [1310-73-2] Sodium nitrate; NaNO <sub>3</sub> ; [7631-99-4] Sodium bicarbonate; NaHCO <sub>3</sub> ; [144-55-8] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Broden, A.; Simonson, R.  <i>Sven. Papperstidn.</i> 1978, 81, 541 - 544; 1979, 82, 487 - 491.																																																																																											
<b>VARIABLES:</b> $T/K = 323 - 423$ $p/\text{MPa} = 1 - 5$ $c_2/\text{mol dm}^{-3} = \text{up to } 1.0$	<b>PREPARED BY:</b>  H. L. Clever																																																																																											
<b>EXPERIMENTAL VALUES:</b> The experimental data are presented by graphs and by the constants of an equation. The equation is $c_1/\text{mmol dm}^{-3} = \alpha_1 + \alpha_2(T/K) + \alpha_3(p/\text{MPa}) + \alpha_4(p/\text{MPa})(T/K)^2 + \alpha_5(p/\text{MPa})/(T/K) + \alpha_6(p/\text{MPa})^2 + \alpha_7(p/\text{MPa})^2/(T/K).$ <p><math>p/\text{MPa}</math> is the oxygen partial pressure. The solubility of oxygen in water was fitted to both a five and a seven constant equation. Only the first five constants were used for the electrolyte solutions. The constants for the equation are given below.</p>																																																																																												
<table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;"><math>\alpha_1</math></th> <th style="text-align: center;"><math>10^2\alpha_2</math></th> <th style="text-align: center;"><math>10^{-1}\alpha_3</math></th> <th style="text-align: center;"><math>10^4\alpha_4</math></th> <th style="text-align: center;"><math>10^{-4}\alpha_5</math></th> <th style="text-align: center;"><math>\alpha_6</math></th> <th style="text-align: center;"><math>10^{-2}\alpha_7</math></th> </tr> </thead> <tbody> <tr> <td colspan="7">Water, standard deviation 0.45 mmol dm<sup>-3</sup>.</td> </tr> <tr> <td style="text-align: center;">5.351</td> <td style="text-align: center;">-1.252</td> <td style="text-align: center;">-7.954</td> <td style="text-align: center;">2.135</td> <td style="text-align: center;">2.125</td> <td></td> <td></td> </tr> <tr> <td colspan="7">Water, standard deviation 0.42 mmol dm<sup>-3</sup>, improved representation of the pressure dependence of the data at low temperatures.</td> </tr> <tr> <td style="text-align: center;">-2.545</td> <td style="text-align: center;">0.807</td> <td style="text-align: center;">-8.414</td> <td style="text-align: center;">2.096</td> <td style="text-align: center;">2.322</td> <td style="text-align: center;">1.027</td> <td style="text-align: center;">-3.911</td> </tr> <tr> <td colspan="7">Sodium hydroxide, 0.01 mol dm<sup>-3</sup></td> </tr> <tr> <td style="text-align: center;">3.236</td> <td style="text-align: center;">-0.7466</td> <td style="text-align: center;">-5.602</td> <td style="text-align: center;">1.558</td> <td style="text-align: center;">1.542</td> <td></td> <td></td> </tr> <tr> <td colspan="7">Sodium hydroxide, 0.10 mol dm<sup>-3</sup></td> </tr> <tr> <td style="text-align: center;">9.582</td> <td style="text-align: center;">-2.436</td> <td style="text-align: center;">-9.477</td> <td style="text-align: center;">2.517</td> <td style="text-align: center;">2.460</td> <td></td> <td></td> </tr> <tr> <td colspan="7">Sodium bicarbonate, 0.10 mol dm<sup>-3</sup></td> </tr> <tr> <td style="text-align: center;">6.817</td> <td style="text-align: center;">-1.750</td> <td style="text-align: center;">-6.743</td> <td style="text-align: center;">1.885</td> <td style="text-align: center;">1.800</td> <td></td> <td></td> </tr> <tr> <td colspan="7">Sodium bicarbonate, 0.50 mol dm<sup>-3</sup></td> </tr> <tr> <td style="text-align: center;">0</td> <td style="text-align: center;">0</td> <td style="text-align: center;">-6.479</td> <td style="text-align: center;">1.757</td> <td style="text-align: center;">1.740</td> <td></td> <td></td> </tr> </tbody> </table>		$\alpha_1$	$10^2\alpha_2$	$10^{-1}\alpha_3$	$10^4\alpha_4$	$10^{-4}\alpha_5$	$\alpha_6$	$10^{-2}\alpha_7$	Water, standard deviation 0.45 mmol dm <sup>-3</sup> .							5.351	-1.252	-7.954	2.135	2.125			Water, standard deviation 0.42 mmol dm <sup>-3</sup> , improved representation of the pressure dependence of the data at low temperatures.							-2.545	0.807	-8.414	2.096	2.322	1.027	-3.911	Sodium hydroxide, 0.01 mol dm <sup>-3</sup>							3.236	-0.7466	-5.602	1.558	1.542			Sodium hydroxide, 0.10 mol dm <sup>-3</sup>							9.582	-2.436	-9.477	2.517	2.460			Sodium bicarbonate, 0.10 mol dm <sup>-3</sup>							6.817	-1.750	-6.743	1.885	1.800			Sodium bicarbonate, 0.50 mol dm <sup>-3</sup>							0	0	-6.479	1.757	1.740		
$\alpha_1$	$10^2\alpha_2$	$10^{-1}\alpha_3$	$10^4\alpha_4$	$10^{-4}\alpha_5$	$\alpha_6$	$10^{-2}\alpha_7$																																																																																						
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus consisted of a stainless steel autoclave of 3 dm <sup>3</sup> volume, connected to a centrifugal pump which circulated the solvent at a rate of 2 dm <sup>3</sup> min <sup>-1</sup> and sprayed the solvent back into the top of the autoclave. The system was attached to controls to measure and control the temperature and pressure.  Equilibration was reached within 30 min. Samples of 0.426 cm <sup>3</sup> were taken under conditions of no change in temperature or pressure. The gas was stripped from the solvent and analysed by GC on a 200 x 0.46 cm column filled with 80 - 100 mesh 5 A Molecular sieve. The column temperature was 40 °C, the detector temperature was 75 °C, the carrier gas was helium.  All salt concentrations are referred to 298 K and atmospheric pressure.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. (2) Electrolytes. (3) Water.  No information on the source and purity of the materials.  <b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ $\delta p/\text{MPa} = \pm 0.005$  Sodium nitrate. No equation was given for the solubility of oxygen in aqueous sodium nitrate. There is a graph of $\log c_2^0/c_1$ vs. $c_2$ showing measurements were made in 0.1, 0.5, and 1.0 mol dm <sup>-3</sup> solutions at temperatures of 323, 373, and 423 K and pressures of 1, 3, and 5 MPa.																																																																																											

COMPONENTS:			ORIGINAL MEASUREMENTS:	
(1) Oxygen; $O_2$ ; [7782-44-7]			Jhaveri, A.S.; Sharma, M.M.	
(2) Disodium sulfate; $Na_2SO_4$ ; [7757-82-6]			Chem. Eng. Sci. <u>1968</u> , 23, 1-8.	
(3) Sodium hydroxide; NaOH; [1310-73-2]				
(4) Sodium dithionite; $Na_2S_2O_4$ ; [7775-14-6]				
(5) Water; $H_2O$ ; [7732-18-5]				
VARIABLES:		PREPARED BY:		
T/K = 306		R. Battino		
Composition				
EXPERIMENTAL VALUES:				
$Na_2SO_4$ /mol $\ell^{-1}$	NaOH /mol $\ell^{-1}$	$Na_2SO_4$ /mol $\ell^{-1}$	$10^5 x_1$	$10^7 C^*$ /mol $cm^{-3}$
0	0.0875	0.0254	1.83	10.4
0	0.0875	0.0342	1.87	10.35
0	0.0875	0.0720	1.81	10.0
0	0.0875	0.084	1.80	9.92
0	0.0875	0.131	1.70	9.38
0	0.0875	0.169	1.66	9.17
0	0.0375	0.276	1.52	8.40
1.0	0.20	0.0955	0.699	3.86
1.0	0.20	0.218	0.627	3.46
1.0	0.20	0.286	0.594	3.28
0	0.532	0.0167	0.147	0.81
0	0.532	0.0261	0.191	1.055
0	0.532	0.09	0.380	2.10
0	0.532	0.182	0.695	3.84
<p>a All measurements at 33°C (306K)</p> <p>b <math>x_1</math>, the mole fraction solubility at 101.325 kPa (1 atm) partial gas pressure calculated by compiler.</p> <p>c <math>C^*</math> is the reported unit of solubility.</p>				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:	
Most measurements were carried out in a continuous-flow glass stirred cell. Some measurements were carried out in a packed column. The unreacted sodium dithionite was estimated iodometrically using the procedures found in reference 1.			"Chemicals were reagent grade."	
			ESTIMATED ERROR:	
			$\delta C^*/C^* = \pm 0.02$ (compiler's estimate)	
			REFERENCES:	
			1. Committee on Analytical Methods, Am. Dyestuff Rept. <u>1957</u> , 46, 443.	

COMPONENTS:			ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]			Guseva, M.S.; Konnik, E.I.; Saifi, R.N.; Kuz'min, A.A.; Mordukhovich, I.L.  Fiz. Khim. Rastvorov, 1972, 105-8. Ed. by Samoilov, O.Ya. "Nauka" Moscow, USSR, Chem. Abstr. 1972, 77, 157007v.			
(2) Sodium acetate; C <sub>2</sub> H <sub>3</sub> O <sub>2</sub> Na; [127-09-3]						
(3) Potassium hydroxide and sulfuric acid to control pH						
(4) Water; H <sub>2</sub> O; [7732-18-5]						
VARIABLES:			PREPARED BY:			
T/K = 293-313 pH = 0-14			V. Katovic			
EXPERIMENTAL VALUES:						
	20°C (293K)		30°C (303K)		40°C (313K)	
pH	c <sup>a</sup> /mg ℓ <sup>-1</sup>	10 <sup>3</sup> C/ g-equiv ℓ <sup>-1</sup>	c <sup>a</sup> /mg ℓ <sup>-1</sup>	10 <sup>3</sup> C/ g-equiv ℓ <sup>-1</sup>	c <sup>a</sup> /mg ℓ <sup>-1</sup>	10 <sup>3</sup> C/ g-equiv ℓ <sup>-1</sup>
Aqueous solutions <sup>b</sup>						
0	7.6	0.95	6.4	0.79	5.7	0.71
1	8.6	1.07	6.9	0.87	6.3	0.78
2-12	8.9	1.12	7.5	0.93	6.4	0.80
13	8.9	1.11	7.4	0.92	6.2	0.78
14	6.6	0.83	5.5	0.63	4.3	0.54
0.1 N Sodium acetate solution <sup>b</sup>						
0	7.2	0.90	5.9	0.74	5.5	0.69
1	8.4	1.04	6.8	0.85	6.3	0.78
2-12	8.8	1.10	7.4	0.93	6.3	0.79
13	8.4	1.04	7.1	0.89	6.2	0.78
14	6.4	0.80	5.5	0.68	4.3	0.54
<p><sup>a</sup> Solubilities at 101.325kPa partial pressure of air.</p> <p><sup>b</sup> The pH was adjusted by the addition of KOH or H<sub>2</sub>SO<sub>4</sub>.</p>						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:			
The solubility of oxygen was measured after bubbling air through the solution for 30 minutes. The dissolved oxygen was determined by the Winkler method. The pH of the solutions was adjusted by the addition of KOH or H <sub>2</sub> SO <sub>4</sub> .			(1) From air.			
			(2,3) No details given.			
			(4) Double distilled, specific conductance of 2 x 10 <sup>-6</sup> ohm <sup>-1</sup> cm <sup>-1</sup> .			
			ESTIMATED ERROR:			
			δT/K = ±0.1, authors' estimate.			
			δc/c = ±0.05, authors' estimate.			
			REFERENCES:			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sodium carbonate; Na <sub>2</sub> CO <sub>3</sub> ; [497-19-8] (3) Water: H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A.  <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4, 185-9.																																																																																																												
<b>VARIABLES:</b> T/K = 288.15 - 308.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 2.958	<b>PREPARED BY:</b>  H. L. Clever																																																																																																												
<table border="1"> <thead> <tr> <th data-bbox="84 446 329 472">EXPERIMENTAL VALUES:</th> <th data-bbox="329 446 480 472">T/K</th> <th data-bbox="480 446 743 519">Sodium carbonate c<sub>3</sub>/mol dm<sup>-3</sup></th> <th data-bbox="743 446 934 519">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td></td> <td>288.15</td> <td>0.0</td> <td>0.03643<sup>1</sup></td> </tr> <tr> <td></td> <td></td> <td>0.205</td> <td>0.02990</td> </tr> <tr> <td></td> <td></td> <td>0.421</td> <td>0.02524</td> </tr> <tr> <td></td> <td></td> <td>0.647</td> <td>0.02139</td> </tr> <tr> <td></td> <td></td> <td>0.868</td> <td>0.01794</td> </tr> <tr> <td></td> <td></td> <td>1.043</td> <td>0.01552</td> </tr> <tr> <td></td> <td></td> <td>1.313</td> <td>0.01255</td> </tr> <tr> <td></td> <td>298.15</td> <td>0.0</td> <td>0.03114<sup>1</sup></td> </tr> <tr> <td></td> <td></td> <td>0.202</td> <td>0.02621</td> </tr> <tr> <td></td> <td></td> <td>0.379</td> <td>0.02288</td> </tr> <tr> <td></td> <td></td> <td>0.798</td> <td>0.01623</td> </tr> <tr> <td></td> <td></td> <td>1.235</td> <td>0.01155</td> </tr> <tr> <td></td> <td></td> <td>1.258</td> <td>0.01137</td> </tr> <tr> <td></td> <td></td> <td>1.593</td> <td>0.00917</td> </tr> <tr> <td></td> <td></td> <td>1.636</td> <td>0.00840</td> </tr> <tr> <td></td> <td></td> <td>1.906</td> <td>0.00703</td> </tr> <tr> <td></td> <td></td> <td>2.128</td> <td>0.00613</td> </tr> <tr> <td></td> <td>308.15</td> <td>0.0</td> <td>0.02764<sup>1</sup></td> </tr> <tr> <td></td> <td></td> <td>0.407</td> <td>0.01973</td> </tr> <tr> <td></td> <td></td> <td>0.858</td> <td>0.01350</td> </tr> <tr> <td></td> <td></td> <td>1.245</td> <td>0.00979</td> </tr> <tr> <td></td> <td></td> <td>1.631</td> <td>0.00722</td> </tr> <tr> <td></td> <td></td> <td>2.086</td> <td>0.00512</td> </tr> <tr> <td></td> <td></td> <td>2.337</td> <td>0.00406</td> </tr> <tr> <td></td> <td></td> <td>2.532</td> <td>0.00354</td> </tr> <tr> <td></td> <td></td> <td>2.958</td> <td>0.00255</td> </tr> </tbody> </table> <p style="text-align: right; margin-right: 50px;"><sup>1</sup>Values from reference 1.</p>		EXPERIMENTAL VALUES:	T/K	Sodium carbonate c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L		288.15	0.0	0.03643 <sup>1</sup>			0.205	0.02990			0.421	0.02524			0.647	0.02139			0.868	0.01794			1.043	0.01552			1.313	0.01255		298.15	0.0	0.03114 <sup>1</sup>			0.202	0.02621			0.379	0.02288			0.798	0.01623			1.235	0.01155			1.258	0.01137			1.593	0.00917			1.636	0.00840			1.906	0.00703			2.128	0.00613		308.15	0.0	0.02764 <sup>1</sup>			0.407	0.01973			0.858	0.01350			1.245	0.00979			1.631	0.00722			2.086	0.00512			2.337	0.00406			2.532	0.00354			2.958	0.00255
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used. The aqueous salt solution is degassed by boiling under reflux and under vacuum. The gas phase volume and the solvent volume are measured by displacement of mercury. Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded. The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. High purity grade stated to be 99.995 per cent. (2) Sodium carbonate. (3) Water. No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89.  The author correlated the data with the Setschnow equation $\log(L_0/L) = KC_3$ . Values of K are 0.356, 0.338, and 0.353 at 288.15, 298.15 and 308.15 K, respectively.																																																																																																												



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Trialkali metal phosphates; Na <sub>3</sub> PO <sub>4</sub> and K <sub>3</sub> PO <sub>4</sub> (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Khomutov, N. E.; Konnik, E. I. <i>Zh. Fiz. Khim.</i> <u>1974</u> , <i>48</i> , 620-5. <i>Russ. J. Phys. Chem.</i> <u>1974</u> , <i>48</i> , 359-62.																				
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~21 (air at 1 atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 0.6	<b>PREPARED BY:</b> H. L. Clever																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Maximum Salt Concentration c<sub>3</sub>/mol dm<sup>-3</sup></th> <th style="text-align: center;">Number of Experimental Points</th> <th style="text-align: center;">Salt Effect Parameter k = (1/c<sub>3</sub>) log(S<sup>0</sup>/S)</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Trisodium phosphate; Na<sub>3</sub>PO<sub>4</sub>; [7601-54-9]</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">0.6</td> <td style="text-align: center;">7</td> <td style="text-align: center;">0.652</td> </tr> <tr> <td colspan="4" style="text-align: center;">Tripotassium phosphate; K<sub>3</sub>PO<sub>4</sub>; [7778-53-2]</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">0.6</td> <td style="text-align: center;">6</td> <td style="text-align: center;">0.507</td> </tr> </tbody> </table>		T/K	Maximum Salt Concentration c <sub>3</sub> /mol dm <sup>-3</sup>	Number of Experimental Points	Salt Effect Parameter k = (1/c <sub>3</sub> ) log(S <sup>0</sup> /S)	Trisodium phosphate; Na <sub>3</sub> PO <sub>4</sub> ; [7601-54-9]				298.15	0.6	7	0.652	Tripotassium phosphate; K <sub>3</sub> PO <sub>4</sub> ; [7778-53-2]				298.15	0.6	6	0.507
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<b>AUXILIARY INFORMATION</b>																					
<b>METHOD/APPARATUS/PROCEDURE:</b> Air, saturated with water vapor from the salt solution, is bubbled for several hours through 500 cm <sup>3</sup> of solution. Three samples are taken and analyzed by the Winkler chemical method. The solubility unit is mg dm <sup>-3</sup> at the normal oxygen partial pressure in air of 0.21 atm. The solubility in water is 8.15 mg dm <sup>-3</sup> . The results are presented graphically as log S vs. dm <sup>-3</sup> . The slope is given as the salt effect parameter (Sechenow constant) k.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air treated to free from dust and any foreign gases. (2) Salts. No information. (3) Water. No information. <b>ESTIMATED ERROR:</b> δT/K = 0.1 δS/mg dm <sup>-3</sup> = 0.05 Max error in S is 1.8 per cent. <b>REFERENCES:</b>																				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium hydroxide; KOH; [1310-58-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Geffcken, G. <i>Z. Phys. Chem.</i> <u>1904</u> , 49, 257-302.																					
<b>VARIABLES:</b> T/K = 288-298 Concentration	<b>PREPARED BY:</b> C.L. Young; R. Battino																					
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<table border="1"> <thead> <tr> <th data-bbox="178 531 225 550">T/K</th> <th data-bbox="339 531 786 550">Conc of hydroxide/mol dm<sup>3</sup> (soln)</th> <th data-bbox="863 531 1172 550">Ostwald coefficient, <i>L</i></th> </tr> </thead> <tbody> <tr> <td data-bbox="165 599 251 619" rowspan="4">288.15</td> <td data-bbox="530 599 602 619">0.577</td> <td data-bbox="935 599 1034 619">0.02791</td> </tr> <tr> <td data-bbox="530 623 602 642">0.579</td> <td data-bbox="935 623 1034 642">0.02791</td> </tr> <tr> <td data-bbox="530 646 602 666">1.157</td> <td data-bbox="935 646 1034 666">0.02191</td> </tr> <tr> <td data-bbox="530 670 602 689">1.170</td> <td data-bbox="935 670 1034 689">0.02181</td> </tr> <tr> <td data-bbox="165 693 251 713" rowspan="4">298.15</td> <td data-bbox="530 693 602 713">0.577</td> <td data-bbox="935 693 1034 713">0.02447</td> </tr> <tr> <td data-bbox="530 717 602 736">0.579</td> <td data-bbox="935 717 1034 736">0.02435</td> </tr> <tr> <td data-bbox="530 740 602 760">1.157</td> <td data-bbox="935 740 1034 760">0.01920</td> </tr> <tr> <td data-bbox="530 764 602 784">1.170</td> <td data-bbox="935 764 1034 784">0.01914</td> </tr> </tbody> </table>		T/K	Conc of hydroxide/mol dm <sup>3</sup> (soln)	Ostwald coefficient, <i>L</i>	288.15	0.577	0.02791	0.579	0.02791	1.157	0.02191	1.170	0.02181	298.15	0.577	0.02447	0.579	0.02435	1.157	0.01920	1.170	0.01914
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<b>METHOD /APPARATUS/PROCEDURE:</b>  Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried. (3) Degassed.  <b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1$ ; $\delta L = \pm 1\%$ . (estimated by compiler).  <b>REFERENCES:</b>																					

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5] (3) Potassium hydroxide; KOH; [1310-58-3]		<b>ORIGINAL MEASUREMENTS:</b> Knaster, M. B.; Apel'baum, L. A. <i>Zh. Fiz. Khim.</i> <u>1964</u> , <i>38</i> , 223 - 225. <i>Russ. J. Phys. Chem.</i> <u>1964</u> , <i>38</i> , 120 - 122.																																																														
<b>VARIABLES:</b> T/K: 294.15, 318.15, 348.15 P/kPa: 101.325 (1 atm) c <sub>3</sub> /mol dm <sup>-3</sup> : 0 - 10		<b>PREPARED BY:</b> H. L. Clever																																																														
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<b>METHOD/APPARATUS/PROCEDURE:</b> The KOH solution was introduced into the saturating vessel. The solution was saturated with gas, which was bubbled through the solution at a rate of 15 dm <sup>3</sup> h <sup>-1</sup> for 5 h. The gas stream was turned off and the solution was allowed to stand for one h to allow suspended gas bubbles to escape. A known amount of the gas-saturated solution was transferred to an evacuated flask. The gas evolved from the solution was withdrawn, together with water vapor, into an evacuated and calibrated portion of the apparatus. The water vapor was frozen out in a liquid oxygen trap. The pressure (ca. 1 mmHg) of the residual gas at a known temperature and volume was measured on a McLeod gage.		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. The gas was produced by electrolysis and subjected to a standard purification process. (2) Water. No information. (3) Potassium hydroxide. No information.																																																														
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium hydroxide; KOH; [1310-58-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Davis, R.E.; Horvath, G.L.; Tobias, C.W.  <i>Electrochim. Acta</i> <u>1967</u> , <i>12</i> , 287-97.								
<b>VARIABLES:</b> T/K = 298 P/kPa = 101.325 C/N = 0-12	<b>PREPARED BY:</b>  R. Battino								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="111 466 1181 593"> <thead> <tr> <th>T/K<sup>a</sup></th> <th>Mole fraction<sup>b</sup> 10<sup>5</sup>x<sub>1</sub></th> <th>Ostwald Coefficient<sup>c</sup> 10<sup>2</sup>L</th> <th>Molarity<sup>d</sup> 10<sup>3</sup>C</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>2.276</td> <td>2.823</td> <td>1.26</td> </tr> </tbody> </table> <p data-bbox="98 629 563 662"><sup>a</sup> Temperature reported to 0.2°C.</p> <p data-bbox="98 682 1151 736"><sup>b</sup> Mole fraction solubility at 101.325 kPa (1atm) partial pressure of gas calculated by compiler.</p> <p data-bbox="98 756 461 789"><sup>c</sup> Calculated by compiler.</p> <p data-bbox="98 805 606 838"><sup>d</sup> At 1 atm partial pressure of gas.</p> <p data-bbox="98 854 1063 909"><sup>e</sup> In the range 0-12N KOH and a partial pressure of oxygen of 1 atm the oxygen solubility is given by</p> $\log_{10} S = \log_{10} (1.26 \times 10^{-3}) - 0.1746 C$ <p data-bbox="125 942 1165 1040">where S is the oxygen solubility in g-mol dm<sup>-3</sup>, and C the concentration of KOH in g-mol dm<sup>-3</sup>. This is for 25°C. Data are given graphically for 0°C and 60°C. Both the solubility and the coefficient of C in the above equation decrease as the temperature increases.</p>		T/K <sup>a</sup>	Mole fraction <sup>b</sup> 10 <sup>5</sup> x <sub>1</sub>	Ostwald Coefficient <sup>c</sup> 10 <sup>2</sup> L	Molarity <sup>d</sup> 10 <sup>3</sup> C	298.15	2.276	2.823	1.26
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> Solubility measurements were made by the Van Slyke manometric method (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) 99.6% pure (2) Reagent grade (3) Distilled								
<b>ESTIMATED ERROR:</b>  $\delta C/C = \pm 0.01$ , estimate by authors									
<b>REFERENCES:</b>  1. Van Slyke, D.D; Neill, J.M. <i>J. Biol. Chem.</i> <u>1924</u> , <i>61</i> , 523.									



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium Hydroxide; KOH; [1310-58-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>EVALUATOR:</b> Shoor, S. K.; Walker, R. D. Jr.; Gubbins, K. E.  <i>J. Phys. Chem.</i> 1969, 73, 312-7.
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**EXPERIMENTAL VALUES:** continued

T/K	Potassium Hydroxide		Mol Fraction O <sub>2</sub> /X <sub>1</sub> × 10 <sup>3</sup>	Solubility	Salt Effect
	Wt %	mol dm <sup>-3</sup>		Ratio γ = X <sup>0</sup> /X	Parameter k <sub>s</sub> = (1/C) log(X <sup>0</sup> /X)
298.15	0.0	0.0	0.0225	1.00	-
	5.00	0.92		1.53	0.201
	13.50	2.67		3.06	0.182
	23.00	5.00		8.15	0.182
	31.61	7.35		20.1	0.177
	40.70	10.12		70.1	0.182
	50.65	13.75		230.	0.172
				0.180 (authors)	
313.15	0.0	0.0	0.0190	1.00	-
	5.0	0.92		1.54	0.204
	13.50	2.67		2.87	0.171
	23.00	5.00		7.24	0.172
	31.61	7.35		17.8	0.170
	40.70	10.12		53.3	0.171
				0.168 (authors)	
333.15	0.0	0.0	0.0160	1.00	-
	5.00	0.92		1.45	0.175
	13.50	2.67		2.58	0.154
	23.00	5.00		6.30	0.160
	31.61	7.35		15.6	0.162
	40.70	10.12		45.3	0.164
	50.65	13.75		162.	0.161
				0.159 (authors)	
353.15	0.0	0.0	0.0144	1.00	-
	5.00	0.92		1.35	0.142
	13.50	2.67		2.50	0.149
	23.00	5.00		5.73	0.152
	31.61	7.35		14.4	0.158
	40.70	10.12		40.1	0.158
	50.65	13.75		143.	0.157
				0.155 (authors)	
373.15	0.0	0.0	0.0142	1.00	-
	40.70	10.12		38.4	0.157
	50.65	13.75		141.	0.156
	56.50	16.20		338.	0.156
				0.155 (authors)	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium chloride; KCl; [7447-40-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G. <i>J. Phys. Chem.</i> <u>1916</u> , <i>20</i> , 495-502.																																						
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 20.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 4	<b>PREPARED BY:</b> H. L. Clever																																						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="264 499 1114 823"> <thead> <tr> <th>T/K</th> <th>Potassium Chloride c<sub>3</sub>/mol dm<sup>-3</sup></th> <th>Solution density<sup>1</sup> ρ/g cm<sup>-3</sup></th> <th>Solubility<sup>2</sup> cm<sup>3</sup> (STP) O<sub>2</sub> per dm<sup>3</sup></th> <th>Setschenow Constant<sup>3</sup> k<sub>s</sub></th> </tr> </thead> <tbody> <tr> <td rowspan="8">298.15</td> <td>0.0</td> <td>1.000</td> <td>5.78</td> <td>-</td> </tr> <tr> <td>0.125</td> <td>1.003</td> <td>5.52</td> <td>0.160</td> </tr> <tr> <td>0.25</td> <td>1.0086</td> <td>5.30</td> <td>0.151</td> </tr> <tr> <td>0.5</td> <td>1.020</td> <td>4.98</td> <td>0.129</td> </tr> <tr> <td>1</td> <td>1.042</td> <td>4.26</td> <td>0.133</td> </tr> <tr> <td>2</td> <td>1.086</td> <td>3.21</td> <td>0.128</td> </tr> <tr> <td>3</td> <td>1.134</td> <td>2.36</td> <td>0.130</td> </tr> <tr> <td>4</td> <td>1.170</td> <td>1.86</td> <td>0.123</td> </tr> </tbody> </table> <p data-bbox="135 842 1133 921"><sup>1</sup> The author calculated the densities from data in the <i>International Critical Tables</i>. Use the density values with caution, some of them appear to be in error.</p> <p data-bbox="135 931 1172 989"><sup>2</sup> The solubility in water is about 3 per cent smaller than the presently accepted value.</p> <p data-bbox="135 999 1120 1068"><sup>3</sup> The Setschenow constant (salt effect parameter) is calculated from <math>k_s = (1/c_3) \log (\text{Solubility in water}/\text{Solubility in solution})</math>.</p>		T/K	Potassium Chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>	298.15	0.0	1.000	5.78	-	0.125	1.003	5.52	0.160	0.25	1.0086	5.30	0.151	0.5	1.020	4.98	0.129	1	1.042	4.26	0.133	2	1.086	3.21	0.128	3	1.134	2.36	0.130	4	1.170	1.86	0.123
T/K	Potassium Chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>																																			
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<b>AUXILIARY INFORMATION</b>																																							
<b>METHOD/APPARATUS/PROCEDURE:</b> The solutions were thermostated in tall cylinder open to the air. They were shaken by hand several times a day for a period of four days. A sample of 250 cm <sup>3</sup> was analyzed for oxygen by a modified Winkler method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air at one atm. (2) Potassium chloride. No information. (3) Water. No information.  <b>ESTIMATED ERROR:</b> The solubility values may be in 5 to 10 per cent error. The salt concentrations above one mol dm <sup>-3</sup> may be in error by 10 per cent.  <b>REFERENCES:</b>																																						

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium Chloride; KCl; [7447-40-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Bikov, M. M. <i>Tr. Voronezhsk. Gos. Univ.</i> <u>1937</u> , 9, 29-57.
<b>VARIABLES:</b> T/K = 273-510 P/MPa = 9.81 Concentration	<b>PREPARED BY:</b> V. Katovic

EXPERIMENTAL VALUES:		Oxygen Solubility <sup>b</sup>			
t/°C	T <sup>a</sup> /K	H <sub>2</sub> O	KCl Solution/N		
			0.5	1.0	2.0
Total pressure of 100 kg/cm <sup>2</sup> (9.81MPa)					
0	273	0.66	0.635	0.510	0.331
25	298	0.51	0.396	0.336	0.232
50	323	0.34	0.290	0.265	0.206
75	348	0.31	0.261	0.230	0.172
100	373	0.33	0.265	0.233	0.174
150	423	0.41	0.321	0.253	0.211
200	473	0.51	0.372	0.309	0.245
240	513	0.57	0.465	0.386	0.272

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Solubility in cm<sup>3</sup>(STP) per 1 gram of solvent.

continued on following page

#### AUXILIARY INFORMATION

<b>METHOD/APPARATUS/PROCEDURE:</b> Details of the method and a drawing of the apparatus are given in the paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From air. (2) No details given. (3) Distilled.
	<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.2$ $\delta S/S = \pm 0.01$ compiler's estimate for solubility.
	<b>REFERENCES:</b>



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium Chloride; KCl; [7447-40-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>EVALUATOR:</b> Bikov, M. M. <i>Tr. Voronezhsk. Gos. Univ.</i> <u>1937</u> , 9, 29-57.
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## CRITICAL EVALUATION:

continued

t/°C	T <sup>a</sup> /K	H <sub>2</sub> O	Solubility Coefficient <sup>b</sup> KCl Solution/N		
			0.5	1.0	2.0
0	273	3.24	3.023	2.430	1.575
25	298	2.45	1.885	1.601	1.106
50	323	1.78	1.380	1.265	0.981
75	348	1.46	1.249	1.100	0.820
100	373	1.55	1.273	1.121	0.836
150	423	2.05	1.605	1.276	1.046
200	473	2.88	2.094	1.735	1.370
240	513	4.09	3.338	2.748	1.905

<sup>a</sup> Calculated by compiler.

<sup>b</sup> The solubility coefficient is cm<sup>3</sup> (STP) of oxygen dissolved per 1 gram of solution at an oxygen partial pressure of 100 kg/cm<sup>2</sup> (9.81MPa).

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium Chloride: KCl; [7447-40-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Eucken, A.; Hertzberg, G. <i>Z. Physik. Chem.</i> <u>1950</u> , 195, 1 - 23.																														
<b>VARIABLES:</b> T/K= 273.15, 293.15 P/kPa= 101.325 $m_{\text{KCl}}/\text{mol kg}^{-1} = 0 - 2.76$	<b>PREPARED BY:</b> P. L. Long H. L. Clever																														
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Potassium Chloride mol kg<sup>-1</sup> H<sub>2</sub>O</th> <th style="text-align: center;">Ostwald Coefficient L</th> <th style="text-align: center;">Setschenow Constant k = (1/m) log(L<sup>0</sup>/L)</th> </tr> </thead> <tbody> <tr> <td rowspan="4" style="text-align: center; vertical-align: top;">273.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">0.0490</td> <td style="text-align: center;">-</td> </tr> <tr> <td style="text-align: center;">0.62</td> <td style="text-align: center;">0.0387</td> <td style="text-align: center;">0.167</td> </tr> <tr> <td style="text-align: center;">1.18</td> <td style="text-align: center;">0.0309</td> <td style="text-align: center;">0.170</td> </tr> <tr> <td style="text-align: center;">2.76</td> <td style="text-align: center;">0.0172</td> <td style="text-align: center;">0.165</td> </tr> <tr> <td rowspan="4" style="text-align: center; vertical-align: top;">293.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">0.0332</td> <td style="text-align: center;">-</td> </tr> <tr> <td style="text-align: center;">0.47</td> <td style="text-align: center;">0.0285</td> <td style="text-align: center;">0.142</td> </tr> <tr> <td style="text-align: center;">0.97</td> <td style="text-align: center;">0.0243</td> <td style="text-align: center;">0.140</td> </tr> <tr> <td style="text-align: center;">1.59</td> <td style="text-align: center;">0.0196</td> <td style="text-align: center;">0.144</td> </tr> </tbody> </table>		T/K	Potassium Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	Setschenow Constant k = (1/m) log(L <sup>0</sup> /L)	273.15	0	0.0490	-	0.62	0.0387	0.167	1.18	0.0309	0.170	2.76	0.0172	0.165	293.15	0	0.0332	-	0.47	0.0285	0.142	0.97	0.0243	0.140	1.59	0.0196	0.144
T/K	Potassium Chloride mol kg <sup>-1</sup> H <sub>2</sub> O	Ostwald Coefficient L	Setschenow Constant k = (1/m) log(L <sup>0</sup> /L)																												
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<b>AUXILIARY INFORMATION</b>																															
<b>METHOD/APPARATUS/PROCEDURE:</b> Gas absorption. The apparatus consists of a gas buret and an adsorption flask connected by a capillary tube. The whole apparatus is shaken. The capillary tube is a 2m-long glass helix. An amount of gas is measured at STP and placed in the gas buret. After shaking, the difference from the original amount of gas placed in the gas buret is determined.	<b>SOURCE AND PURITY OF MATERIALS:</b> Components. Neither source nor purity given.																														
	<b>ESTIMATED ERROR:</b> $\delta L/L = 0.01$																														
	<b>REFERENCES:</b>																														

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium chloride; KCl; [7447-40-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Yasunishi, A. <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4(2), 185-9.
<b>VARIABLES:</b> T/K = 288.15 - 308.15 O <sub>2</sub> P/kPa = 101.325 c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 4.124	<b>PREPARED BY:</b> H. L. Clever
<b>EXPERIMENTAL VALUES:</b> <p style="text-align: center;">See following page.</p>	
<b>AUXILIARY INFORMATION</b>	
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus and procedure are described in reference (1). A Horiuti type apparatus is used.</p> <p>The aqueous salt solution is degassed by boiling under reflux and under vacuum.</p> <p>The gas phase volume and the solvent volume are measured by displacement of mercury.</p> <p>Dry gas is intermittently added until equilibrium is attained. At that time the total pressure in the dissolution vessel and the gas volume remaining in the buret are recorded.</p> <p>The salt solution concentration and density are determined after the solubility measurement. The salt solution vapor pressure is either taken from the literature or estimated. A correction for the increase of the liquid volume by the dissolved gas is made.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. High purity grade stated to be 99.995 per cent. (2) Potassium chloride. (3) Water. No information.
<b>ESTIMATED ERROR:</b>	
<b>REFERENCES:</b> 1. Yasunishi, A. <i>J. Chem. Eng. Jpn.</i> <u>1977</u> , 10, 89.	

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium chloride; KCl; [7447-40-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Yasunishi, A. <i>Kagaku Kogaku Rombunshu</i> <u>1978</u> , 4(2), 185-9.
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## EXPERIMENTAL VALUES:

T/K	Potassium chloride c <sub>3</sub> /mol dm <sup>-3</sup>	Ostwald Coefficient L
288.15	0.0	0.03643 <sup>1</sup>
	0.421	0.03270
	0.821	0.02996
	1.295	0.02670
	1.725	0.02368
	2.258	0.02127
	3.162	0.01685
	3.192	0.01675
	3.797	0.01417
	298.15	0.0
0.413		0.02844
0.595		0.02720
1.050		0.02452
1.172		0.02425
1.256		0.02360
1.295		0.02348
1.501		0.02249
1.972		0.01973
2.099		0.01951
2.558		0.01745
3.092		0.01641
3.604		0.01427
4.035	0.01405	
308.15	0.0	0.02764 <sup>1</sup>
	0.454	0.02497
	1.018	0.02253
	1.400	0.02120
	1.725	0.01962
	2.054	0.01827
	3.039	0.01507
	3.254	0.01419
	3.865	0.01307
	4.124	0.01330

<sup>1</sup> Values from reference 1.

The author correlated the data by the Setschenow equation,  $\log(L_0/L) = KC_3$ , up to concentrations of 3.2 mol dm<sup>-3</sup> KCl. Values of K are 0.106, 0.095, and 0.087 at temperatures of 288.15, 298.15 and 308.15 K, respectively. For the entire concentration range the data are correlated better by the empirical equation  $\log(L_0/L) = AC_3/(1 + BC_3)$ . The values of A and B are

T/K	A/dm <sup>3</sup> mol <sup>-1</sup>	B/dm <sup>3</sup> mol <sup>-1</sup>
288.15	0.105	-0.0022
298.15	0.103	0.0378
308.15	0.0919	0.0291

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium bromide; KBr; [7758-02-3] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G. <i>J. Phys. Chem.</i> <u>1916</u> , <i>20</i> , 495-502.																						
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 4	<b>PREPARED BY:</b> H. L. Clever																						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="297 493 1155 731"> <thead> <tr> <th>T/K</th> <th>Potassium bromide c<sub>3</sub>/mol dm<sup>-3</sup></th> <th>Solution density<sup>1</sup> ρ/g cm<sup>-3</sup></th> <th>Solubility<sup>2</sup> cm<sup>3</sup> (STP) O<sub>2</sub> per dm<sup>3</sup></th> <th>Setschenow Constant<sup>3</sup> k<sub>s</sub></th> </tr> </thead> <tbody> <tr> <td rowspan="4">298.15</td> <td>0.0</td> <td>1.000</td> <td>5.78</td> <td>-</td> </tr> <tr> <td>0.25</td> <td>1.019</td> <td>5.29</td> <td>0.154</td> </tr> <tr> <td>2</td> <td>1.079</td> <td>3.27</td> <td>0.124</td> </tr> <tr> <td>4</td> <td>1.162</td> <td>1.84</td> <td>0.124</td> </tr> </tbody> </table> <p data-bbox="164 751 1173 827"><sup>1</sup> The author calculated the densities from data in the <i>International Critical Tables</i>. Use the density values with caution, some of them appear to be in error.</p> <p data-bbox="164 846 1215 898"><sup>2</sup> The solubility in water is about 3 per cent smaller than the presently accepted value.</p> <p data-bbox="164 918 1158 978"><sup>3</sup> The Setschenow constant (salt effect parameter) is calculated from <math>k_s = (1/c_3) \log (\text{Solubility in water}/\text{Solubility in solution})</math>.</p>		T/K	Potassium bromide c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>	298.15	0.0	1.000	5.78	-	0.25	1.019	5.29	0.154	2	1.079	3.27	0.124	4	1.162	1.84	0.124
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium iodide; KI; [7681-11-0] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G.  <i>J. Phys. Chem.</i> <u>1916</u> , <i>20</i> , 495-502.
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 5	<b>PREPARED BY:</b> H. L. Clever

**EXPERIMENTAL VALUES:**

T/K	Potassium iodide c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>
298.15	0.0	1.000	5.78	-
	0.125	1.013	5.65	0.079
	0.25	1.027	5.49	0.089
	0.5	1.056	5.20	0.092
	1	1.116	4.75	0.085
	2	1.23	3.77	0.093
	5	1.46	1.81	0.101

<sup>1</sup> The author calculated the densities from data in the *International Critical Tables*. Use the density values with caution, some of them appear to be in error.

<sup>2</sup> The solubility in water is about 3 per cent smaller than the presently accepted value.

<sup>3</sup> The Setschenow constant (salt effect parameter) is calculated from  $k_s = (1/c_3) \log (\text{Solubility in water/Solubility in solution})$ .

**AUXILIARY INFORMATION****METHOD/APPARATUS/PROCEDURE:**

The solutions were thermostated in tall cylinder open to the air. They were shaken by hand several times a day for a period of four days.

A sample of 250 cm<sup>3</sup> was analyzed for oxygen by a modified Winkler method.

**SOURCE AND PURITY OF MATERIALS:**

- (1) Oxygen. Air at one atm.
- (2) Potassium iodide. No information.
- (3) Water. No information.

**ESTIMATED ERROR:**

The solubility values may be in 5 to 10 per cent error. The salt concentrations above one mol dm<sup>-3</sup> may be in error by 10 per cent.

**REFERENCES:**

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Geffcken, G.	
(2) Sulfuric acid, dipotassium salt; (Potassium sulfate); K <sub>2</sub> SO <sub>4</sub> ; [7778-80-5]		Z. Phys. Chem. <u>1904</u> , 49, 257-302.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES:		PREPARED BY:	
T/K = 288-298 Concentration		C.L. Young, R. Battino	
EXPERIMENTAL VALUES:			
T/K	Conc of salt/mol dm <sup>-3</sup> (soln)	Ostwald coefficient, L	
288.15	0.2495	0.02944	
	0.2530	0.02922	
	0.4840	0.02395	
	0.4850	0.02377	
298.15	0.2495	0.02528	
	0.2530	0.02530	
	0.4850	0.02096	
AUXILIARY INFORMATION			
METHOD / APPARATUS / PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Volumetric method using simple adsorption pipet and buret. Diagram and detailed description given in original paper.		(1) Prepared by heating potassium chlorate and manganese dioxide. Washed with potassium hydroxide solution. Dried.	
		(3) Degassed.	
		ESTIMATED ERROR:	
		δT/K = ±0.1; δL = ±1%. (estimated by compiler).	
		REFERENCES:	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium sulfate; K <sub>2</sub> SO <sub>4</sub> ; [7778-80-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G.  <i>J. Phys. Chem.</i> <u>1916</u> , 20, 495-502.																						
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 20.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 0.5	<b>PREPARED BY:</b>  H. L. Clever																						
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T/K	Potassium sulfate c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	Setschenow Constant <sup>3</sup> k <sub>s</sub>																			
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium nitrate; KNO <sub>3</sub> ; [7757-79-1] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G. <i>J. Phys. Chem.</i> <u>1916</u> , 20, 495-502.																										
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Rubidium chloride; RbCl; [7791-11-9] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G. <i>J. Phys. Chem.</i> <u>1916</u> , <i>20</i> , 495-502.										
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<b>REFERENCES:</b>															

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I. A.	
(2) 4-Methyl-1,3-dioxolan-2-one or propylene carbonate; C <sub>4</sub> H <sub>6</sub> O <sub>3</sub> ; [108-32-7]		Zh. Fiz. Khim. 1979, 53, 1189-92. Russ. J. Phys. Chem. 1979, 53, 1133-4.	
(3) Lithium chloride; LiCl; [7447-41-8]			
VARIABLES:		PREPARED BY:	
T/K = 298.15 (?) P/kPa = ~ 21.3 - 101.325 m <sub>3</sub> /mol kg <sup>-1</sup> : = 0, 0.2		H. L. Clever	
EXPERIMENTAL VALUES:			
T/K	Oxygen Pressure <sup>2</sup> p/atm	Lithium Chloride <sup>3</sup> m <sub>3</sub> /mol kg <sup>-1</sup>	Absorption Coefficient cm <sup>3</sup> cm <sup>-3</sup>
298.15 <sup>1</sup>	air-satu- rated	0	0.144 ± 0.016 <sup>4</sup>
	0.3	0	0.128 ± 0.005
	0.5	0	0.169 ± 0.005
	0.7	0	0.239 ± 0.017
	1.0	0	0.319 ± 0.003
	air-satu- rated	0.2	0.115 ± 0.001
	0.3	0.2	0.107 ± 0.004
	0.5	0.2	0.147 ± 0.008
	0.7	0.2	0.181 ± 0.006
	1.0	0.2	0.214 ± 0.006
<sup>1</sup> The temperature is not given in the paper. However, the authors quote values from other of their papers which were measured at 298.15 K. <sup>2</sup> Dry air has an oxygen partial pressure of ~0.21 atm. The other runs were made with a mixture of helium and oxygen. In all cases the total pressure was apparently one atm. <sup>3</sup> The authors did not define m. The compiler asumed m/mol kg <sup>-1</sup> . <sup>4</sup> The airsaturated absorption coefficient is a mole fraction 5.45 x 10 <sup>-4</sup> .			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
<p>The oxygen concentration was determined by an electrochemical sensor. The sensor was calibrated against an oxygen saturated ethanol solution. The Bunsen coefficient was taken as 0.213 cm<sup>3</sup> cm<sup>-3</sup> atm<sup>-1</sup>.</p> <p>Solutions were saturated in three hours without stirring.</p> <p>The solvent water content was determined by the Fisher method. Water content of 0.0053 - 0.017 % had no effect on the oxygen solubility.</p> <p>The sensitivity of the method with respect to oxygen is 3 µg dm<sup>-3</sup>.</p>		<p>(1) Oxygen. Either air or a He/O<sub>2</sub> mixture.</p> <p>(2) Propylene carbonate. Freshly distilled after special purification.</p> <p>(3) Lithium chloride. No information.</p>	
		ESTIMATED ERROR:	
		The authors state the relative error in O <sub>2</sub> concentration to be 4 - 5 %.	
		REFERENCES:	

COMPONENTS:	ORIGINAL MEASUREMENTS:																														
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 4-Methyl-1,3-dioxolan-2-one or propylene carbonate; C <sub>4</sub> H <sub>6</sub> O <sub>3</sub> ; [108-32-7] (3) Lithium aluminum chloride; LiAlCl <sub>4</sub> ; [17611-22-2]	Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I. A. <i>Zh. Fiz. Khim.</i> <u>1979</u> , <i>53</i> , 1189-92. <i>Russ. J. Phys. Chem.</i> <u>1979</u> , <i>53</i> , 1133-4.																														
VARIABLES:	PREPARED BY:																														
T/K = 298.15 (?) P/kPa = ~21.3 - 101.325 m <sub>3</sub> /mol kg <sup>-1</sup> = 0, 0.2	H. L. Clever																														
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<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever

**EXPERIMENTAL VALUES:**

T/K	C <sub>LiClO<sub>4</sub></sub> /mol dm <sup>-3</sup>	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha \times 10^2$	Ostwald Coefficient Li $\times 10^2$
298.15	0.00	0.170	4.99 ± 0.25 <sup>1</sup>	5.45
	0.20		5.13	
	0.45		5.31	
	0.60		4.95	
	0.80		5.13	

<sup>1</sup>Average of four measurements ± average deviation.

The mole fraction and Ostwald coefficient values were calculated by the compiler.

**AUXILIARY INFORMATION****METHOD/APPARATUS/PROCEDURE:**

The apparatus and procedure used were based on those described by Morrison and Billett (1). Gas saturation is achieved by allowing a thin film of solvent to flow down a glass helix containing the gas and solvent vapor at a total pressure of one atm. About 100 cm<sup>3</sup> of solvent is saturated at a flow rate of 2 - 3 cm<sup>3</sup> m<sup>-1</sup>.

The authors solubility values for oxygen dissolved in water and in dimethylsulfoxide were 3.5 and 21 per cent lower, respectively, than values reported by other workers.

The authors reported a Bunsen coefficient which they had calculated from their measured Ostwald coefficients.

**SOURCE AND PURITY OF MATERIALS:**

- (1) Oxygen. No information.
- (2) Butrolactone. Matheson, Coleman and Bell. Fractionally distilled under reduced pressure through spinning band column. Use 40 percent from the center of an initial one liter sample.
- (3) Lithium perchlorate. No information.

**ESTIMATED ERROR:**

$$\delta T/K = 0.5$$

$$\delta \alpha/\alpha = 0.023 - 0.050$$

(authors)

**REFERENCES:**

1. Morrison, T. J.; Billett, F. *J. Chem. Soc.* 1948, 2033.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 4-Methyl-1,3-dioxolan-2-one or propylene carbonate; C <sub>4</sub> H <sub>6</sub> O <sub>3</sub> ; [108-32-7] (3) Lithium perchlorate; LiClO <sub>4</sub> ; [7791-03-9]	<b>ORIGINAL MEASUREMENTS:</b>  Baird, W. R.; Foley, R. T.  <i>J. Chem. Eng. Data</i> <u>1972</u> , <i>17</i> , 355-7.																		
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T/K	C <sub>LiClO<sub>4</sub></sub> /mol dm <sup>-3</sup>	Mol Fraction x <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α x 10 <sup>2</sup>	Ostwald Coefficient L x 10 <sup>2</sup>															
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COMPONENTS:			ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Potassium hydroxide; KOH; [1310-58-3] (3) Methanol; CH <sub>4</sub> O; [67-56-1] (4) Water; H <sub>2</sub> O; [7732-18-5]			Pospisil, J.; Luzny, Z. <i>Czech. Chem. Comm.</i> <u>1960</u> , <i>25</i> , 589-92.	
VARIABLES: T/K = 293.15 P/kPa = 101.325 Concentration			PREPARED BY: R. W. CARGILL	
EXPERIMENTAL VALUES:				
<u>SOLVENT COMPOSITION</u>				
CH <sub>3</sub> OH wt %	H <sub>2</sub> O wt %	KOH added mol dm <sup>-3</sup>	Bunsen Coefficient α/cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	Ostwald Coefficient L
0	100	0.0	0.0300	0.0322
		0.179	0.0272	0.0292
		0.893	0.0223	0.0239
		1.786	0.0173	0.0186
		3.571	0.0127	0.0136
		5.357	0.0112	0.0120
20	80	0.0	0.0814	0.0874
		0.179	0.0751	0.0806
		0.893	0.0583	0.0626
		1.786	0.0470	0.0504
		3.571	0.0357	0.0383
		5.357	0.0313	0.0336
44	56	0.0	0.1610	0.1728
		0.179	0.1540	0.1653
		0.893	0.1335	0.1433
		1.786	0.1201	0.1289
		3.571	0.1052	0.1129
		5.357	0.1003	0.1076
continued on following page				
AUXILIARY INFORMATION				
METHOD / APPARATUS / PROCEDURE:			SOURCE AND PURITY OF MATERIALS:	
The solvent was stirred magnetically in a wide, flat-bottomed flask, in contact with the gas. Equilibrium was established in 60-90 minutes. A gas burette was used to measure the absorption of gas in up to 100 cm <sup>3</sup> of solution. The absorption flask and burette were thermostatted.			(1) Oxygen. Electrochemical oxygen from a cylinder.	
The solution was degassed by boiling for 30 minutes under reflux. Each measurement was made 3 - 5 times, and the average value is given.			(2) KOH. Analytical purity.	
			(3) Methanol. Twice redistilled, density at 293.15K = 0.7932.	
			(4) Water. Distilled.	
			ESTIMATED ERROR:	
			δL/L = ±0.01 (authors)	
			REFERENCES:	

COMPONENTS	ORIGINAL MEASUREMENTS
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Pospisil, J.; Luzny, Z. <i>Czech. Chem. Comm.</i> <u>1960</u> , 25, 589-92.
(2) Potassium hydroxide; KOH; [1310-58-3]	
(3) Methanol; CH <sub>4</sub> O; [67-56-1]	
(4) Water; H <sub>2</sub> O; [7732-18-5]	

EXPERIMENTAL VALUES:

continued

SOLVENT COMPOSITION

CH <sub>3</sub> OH wt %	H <sub>2</sub> O wt %	KOH added mol dm <sup>-3</sup>	Bunsen Coefficient $\alpha/\text{cm}^3(\text{STP})\text{cm}^{-3}\text{atm}^{-1}$	Ostwald Coefficient L
67.5	32.5	0.0	0.2158	0.2316
		0.179	0.2050	0.2200
		0.893	0.1820	0.1953
		1.786	0.1704	0.1829
		3.571	0.1599	0.1716
		5.357	0.1551	0.1664
100	0	0.0	0.2359	0.2532
		0.179	0.2258	0.2423

The Ostwald coefficients were calculated by the compiler as were the solvent compositions, using density data given in the paper, by reference to *International Critical Tables*, 1928 Vol. III, p 115-116.

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5] (3) Polar organic compounds	EVALUATOR: R.W. Cargill Department of Molecular & Life Sciences Dundee College of Technology Bell Street, Dundee  December 1980
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## CRITICAL EVALUATION:

The solubility of oxygen in mixtures of water with polar organic compounds has been measured in several laboratories. As is usual different solubility units are employed by different workers, which sometimes makes it difficult to compare their results. However, a comparative study has been made where possible and some reliable conclusions have been drawn.

Most of the papers report only the solubility data and tabulate the variables carefully. Some authors (1, 8, 9), however, also attempt to explain the variation in solubility caused by different parameters and relate their studies to current models of the structure of water. In one case (1) thermodynamic functions of the solubility process were also calculated and are presented graphically in the original paper.

Each of the mixed solvent systems is described below, along with relevant comments and an evaluation. Much more work is necessary on most of these systems, however, before complete confidence may be placed in the results.

First of all it is worth mentioning the work which was done by Mejane *et al.* (5) and by Enders *et al.* (2) on the solubility of oxygen in various aqueous alcohol mixtures (including drinks), and also the work by Joslyn and Supplee (3) on its solubility in aqueous sugar solutions. These measurements, however, were not sufficiently accurate nor were the variables properly controlled to make the results useful for scientific purposes. Of more quantitative use are the data on the following systems.

## 1. Oxygen + water + methanol

Pospisil and Luzny (6) in 1960 determined the solubility of oxygen at 293.15 K in water + methanol mixtures of five different compositions. Tokunaga (9) also studied this system in 1975 and gave data for several different solvent compositions between 0.0 and 1.0 mole fraction of methanol, at 273.15 K, 293.15 K, and 313.15 K. The data from both laboratories agree well for the pure water and pure methanol solvents at the common temperature of 293.15 K, but the three values given by Pospisil and Luzny for intermediate compositions are very high compared with Tokunaga's which are more numerous and conform to the pattern expected for this system. A data sheet has been prepared for Tokunaga's work and the results may be accepted tentatively. Pospisil and Luzny's results are given in the system oxygen + water + methanol + potassium hydroxide referred to later, even though they are in some doubt.

## 2. Oxygen + water + ethanol

This system has been studied more than any other of this type. The experimental work which was reported in 1968 by Shchukarev and Tolmacheva (8) was done in 1939-1941. The whole range of solvent composition was covered at four temperatures between 273.15 K and 323.15 K. Kretschmer *et al.* (4) in 1946 reported the solubility of oxygen in a 95% ethanol-water mixture at four temperatures between 248.15 K and 323.15 K. Tokunaga's work (9) reported in 1975 again covers the whole range of solvent composition at temperatures of 273.15 K, 293.15 K, and 313.15K, as does Cargill's (1) in 1976 for several temperatures in the wider range of 276-335 K.

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5] (3) Polar organic compounds	EVALUATOR: R.W. Cargill Department of Molecular & Life Sciences Dundee College of Technology Bell Street, Dundee  December 1980
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CRITICAL EVALUATION: continued

In order to compare the results of these investigations it was necessary to convert the units in Cargill's work from S<sub>0</sub> (cm<sup>3</sup> kg<sup>-1</sup>) to L (the Ostwald coefficient) used by the other workers. The conversion formula is

$$L = S_0 \times \rho_t \times \frac{T}{273.15} \times 10^{-3}$$

The table below gives selected values of L from Cargill's work.

Mol fraction of ethanol x <sub>3</sub>	Ostwald coefficient x 10 <sup>3</sup> at	
	293.15 K	313.15 K
0	33.1	26.4
0.008	33.3	26.7
0.032	34.4	28.0
0.063	33.9	29.1
0.097	33.3	30.6
0.120	33.3	32.3
0.162	35.9	37.8
0.229	45.6	49.0
0.493	104	112
0.780	174	183
0.992	232	242

There is good agreement between the sets of data except in the following cases:

- (a) Shchukarev and Tolmacheva's results are 20-40% lower than those of the other workers, at the higher temperature of 323.15 K and where x<sub>3</sub> > 0.4, and should therefore be regarded as in error for that temperature only. This is confirmed by the unusual temperature effect which the authors themselves reported.
- (b) Tokunaga's results are generally 2-3% higher than those of Cargill and of Shchukarev and Tolmacheva over their common temperature range, but where x<sub>3</sub> < 0.15, his results are up to 20% higher and some data points show a scatter. It is felt that the work of these other authors is more reliable in that concentration range.

Thus data sheets have been prepared for each set of results, and these may be accepted tentatively, bearing in mind the criticisms in paragraphs (a) and (b) above. The units which the authors themselves used are employed in these data sheets, and this may be a help to different readers who have different uses for the data.

3. Oxygen + water + 1-propanol, and

4. Oxygen + water + 2-propanol

Tokunaga (9) has reported the solubility of oxygen in mixtures of water + 1-propanol, and water + 2-propanol, for mol fraction x<sub>3</sub> 0.00 to 1.00 and at temperatures of 273.15K, 293.15K, and 313.15K. A data sheet has been prepared for each system.

continued on following page

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5] (3) Polar organic compounds.	EVALUATOR: R.W. Cargill Department of Molecular & Life Sciences Dundee College of Technology Bell Street, Dundee  December 1980
CRITICAL EVALUATION: <span style="float: right;">continued</span>  5. Oxygen + water + 2-methyl-2-propanol  Cargill's work (1) on this system covers it in detail over the whole concentration range and between 276 K and 335 K. See the data sheets.  6. Oxygen + water + methanol + potassium hydroxide  Pospisil and Luzny (6) measured the solubility of oxygen in a wide range of mixtures of water, methanol, and potassium hydroxide at 293.15 K. Since some uncertainty exists about the accuracy of some of the data (see system 1 above) they are given as doubtful on a data sheet.  The only other reported measurements of the solubility of oxygen in aqueous alcohol mixtures are those by Schlöpfer <i>et al.</i> (7). At the temperature of 303.15 K the solubility of oxygen was measured in mixtures of water with methanol, ethanol, 1-propanol, 2-propanol, 1-butanol, ethylene glycol, and glycerol over the whole range of solvent composition. These solubilities were given with an accuracy of 2.5% and were presented graphically. Therefore no data sheets were prepared for them.  <u>REFERENCES</u>  1. Cargill, R.W. <i>J. Chem. Soc. Faraday Trans. I</i> <u>1976</u> , <i>72</i> , 2296. 2. Enders, C.; Kleber, W.; Paukner, E. <i>Brauwissenschaft</i> <u>1956</u> , <i>2</i> , 50. 3. Joslyn, M.A.; Supplee, H. <i>Food Res.</i> <u>1949</u> , <i>14</i> , 209. 4. Kretschner, C.B.; Nowakowska, J.; Wiebe, R. <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506. 5. Mejane, J.V.; Debailleul, M.; Lecerf, J. <i>Ind. Aliment Agr.</i> <u>1974</u> , <i>90</i> , 719. 6. Pospisil, J.; Luzny, Z. <i>Czech. Chem. Comm.</i> <u>1960</u> , <i>25</i> , 589. 7. Schlöpfer, P.; Audykowski, T.; Bukowiecki, A. <i>Schweiz Arch. Angew. Wiss. Tech.</i> <u>1949</u> , <i>15</i> , 299. 8. Shchukarev, S.A.; Tolmacheva, T.A. <i>Zh. Strukt. Khim.</i> <u>1968</u> , <i>9</i> , 21 (or <i>J. Struct. Chem.</i> <u>1968</u> , <i>9</i> , 16) 9. Tokunaga, J. <i>J. Chem. Eng. Data.</i> <u>1975</u> , <i>20</i> , 41.	

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Methanol; CH <sub>4</sub> O; [67-56-1] (3) Water; H <sub>2</sub> O; [7732-18-5]		Tokunaga, J. <i>J. Chem. Eng. Data</i> , <u>1975</u> , 20,41-6.			
VARIABLES: T/K = 273-313 Composition		PREPARED BY:  C.L.Young, R.W. Cargill			
EXPERIMENTAL VALUES:					
T/K	Mole fraction of alcohol, $x_{CH_4O}$	Ostwald coefficient*,L	Henry's Constant /atm	Mole fraction of oxygen in liquid**, $x_{O_2}$	
273.15	0.0000	0.0490	25400	0.0000394	
	0.0150	0.0511	24000	0.0000417	
	0.0612	0.0535	21800	0.0000459	
	0.1051	0.0526	21300	0.0000469	
	0.1423	0.0503	21600	0.0000463	
	0.1978	0.0488	21200	0.0000472	
	0.3068	0.0533	17700	0.0000565	
	0.3813	0.0606	14700	0.0000680	
	0.5057	0.0777	10300	0.0000971	
	0.6328	0.104	7030	0.000142	
	0.8097	0.154	4200	0.000238	
	1.0000	0.237	2390	0.000418	
	293.15	0.0000	0.0347	38400	0.0000260
		0.0188	0.0384	34000	0.0000294
0.0492		0.0435	29100	0.0000344	
0.0907		0.0472	25700	0.0000389	
0.1103		0.0449	26600	0.0000376	
0.1564		0.0411	27800	0.0000360	
0.2066		0.0418	26100	0.0000383	
0.3054		0.0540	18500	0.0000541	
0.3976		0.0689	13400	0.0000746	
0.4895		0.0859	9990	0.000100	
0.5927		0.112	7050	0.000143	
0.7046		0.144	5050	0.000198	
AUXILIARY INFORMATION					
METHOD /APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:			
Volumetric apparatus with multibulb buret and magnetic stirrer. Amount of solution and gas absorbed determined volumetrically. Partial pressure determined from total pressure and vapor pressure of solvent solution. Details in source.		(1) High purity grade sample, purity 99.9 mole per cent.			
		(2,3) Guaranteed reagent, further purified by distillation. Solution degassed by boiling.			
		ESTIMATED ERROR:  $\delta T/K = \pm 0.5$ ; $\delta x_{O_2} = \pm 1-2\%$ .			
		REFERENCES:			

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Tokunaga, J.		
(2) Methanol; CH <sub>4</sub> O; [67-56-1]		J. Chem. Eng. Data. <u>1975</u> , 20, 41-6.		
(3) Water; H <sub>2</sub> O; [7732-18-5]				
EXPERIMENTAL VALUES:				
T/K	Mole fraction of alcohol, $x_{CH_4O}$	Ostwald coefficient*, L	Henry's Constant /atm	Mole fraction of oxygen in liquid**, $x_{O_2}$
293.15	0.8041	0.173	3930	0.000254
	0.8923	0.205	3120	0.000321
	0.9426	0.221	2790	0.000358
	1.0000	0.246	2400	0.000417
313.15	0.0000	0.0272	50700	0.0000197
	0.0569	0.0358	37200	0.0000269
	0.0972	0.0328	39000	0.0000256
	0.2106	0.0428	26800	0.0000373
	0.2974	0.0577	18400	0.0000543
	0.4357	0.0820	11500	0.0000870
	0.5052	0.0962	9240	0.000108
	0.5848	0.116	7170	0.000139
	0.7009	0.148	5180	0.000193
	0.8010	0.182	3900	0.000256
	0.8905	0.213	3140	0.000318
	1.0000	0.255	2440	0.000410
* at $1.01325 \times 10^5$ Pa partial pressure				
** at $1.01325 \times 10^5$ Pa partial pressure (calculated from the reciprocal of Henry's Constant)				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Shchukarev, S.A.; Tolmacheva, T.A. <i>Zh. Strukt. Khim.</i> 1968, 9, 21-8; <i>J. Struct. Chem.</i> 1968, 9, 16-21.																																																																																																																																																																
<b>VARIABLES:</b> T/K = 277 - 323 P/kPa = 101.325 Composition = 0 - 100%	<b>PREPARED BY:</b> R. Battino; P. L. Long; R.W. Cargill																																																																																																																																																																
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th colspan="2">T/K<sup>a</sup> = 277.15</th> <th colspan="2">T/K = 285.15</th> <th colspan="2">T/K = 298.15</th> <th colspan="2">T/K = 323.15</th> </tr> <tr> <th>Mole Fraction Water<sup>b</sup></th> <th>Ostwald Coeff. L</th> <th>Mole Fraction Water</th> <th>Ostwald Coeff. L</th> <th>Mole Fraction Water</th> <th>Ostwald Coeff. L</th> <th>Mole Fraction Water</th> <th>Ostwald Coeff. L</th> </tr> </thead> <tbody> <tr><td>1</td><td>0.0451</td><td>1</td><td>0.0381</td><td>1</td><td>0.0310</td><td>1</td><td>0.0238</td></tr> <tr><td>0.978</td><td>0.0476</td><td>0.973</td><td>0.0392</td><td>0.980</td><td>0.0326</td><td>0.969</td><td>0.0240</td></tr> <tr><td>0.956</td><td>0.0462</td><td>0.952</td><td>0.0417</td><td>0.973</td><td>0.0326</td><td>0.890</td><td>0.0245</td></tr> <tr><td>0.936</td><td>0.0441</td><td>0.923</td><td>0.0394</td><td>0.947</td><td>0.0325</td><td>0.864</td><td>0.0270</td></tr> <tr><td>0.928</td><td>0.0432</td><td>0.900</td><td>0.0358</td><td>0.909</td><td>0.0323</td><td>0.860</td><td>0.0272</td></tr> <tr><td>0.891</td><td>0.0385</td><td>0.870</td><td>0.0356</td><td>0.904</td><td>0.0322</td><td>0.785</td><td>0.0391</td></tr> <tr><td>0.854</td><td>0.0384</td><td>0.843</td><td>0.0362</td><td>0.894</td><td>0.0321</td><td>0.750</td><td>0.044</td></tr> <tr><td>0.830</td><td>0.0379</td><td>0.700</td><td>0.0570</td><td>0.875</td><td>0.0338</td><td>0.616</td><td>0.069</td></tr> <tr><td>0.818</td><td>0.0386</td><td>0.539</td><td>0.0949</td><td>0.811</td><td>0.0403</td><td>0.476</td><td>0.0935</td></tr> <tr><td>0.492</td><td>0.105</td><td>0.275</td><td>0.156</td><td>0.683</td><td>0.0629</td><td>0.262</td><td>0.131</td></tr> <tr><td>0.158</td><td>0.136</td><td>0.158</td><td>0.185</td><td>0.525</td><td>0.0980</td><td>0.140</td><td>0.154</td></tr> <tr><td>0.008</td><td>0.233</td><td>0.149</td><td>0.184</td><td>0.289</td><td>0.152</td><td>0.141</td><td>0.154</td></tr> <tr><td></td><td></td><td>0.004</td><td>0.231</td><td>0.134</td><td>0.189</td><td>0.139</td><td>0.153</td></tr> <tr><td></td><td></td><td>0.002</td><td>0.232</td><td>0.120</td><td>0.193</td><td>0.002</td><td>0.180</td></tr> <tr><td></td><td></td><td></td><td></td><td>0.049</td><td>0.208</td><td>0.002</td><td>0.180</td></tr> <tr><td></td><td></td><td></td><td></td><td>0.049</td><td>0.208</td><td>0.001</td><td>0.182</td></tr> <tr><td></td><td></td><td></td><td></td><td>0.029</td><td>0.221</td><td></td><td></td></tr> <tr><td></td><td></td><td></td><td></td><td>0.002</td><td>0.283</td><td></td><td></td></tr> </tbody> </table>		T/K <sup>a</sup> = 277.15		T/K = 285.15		T/K = 298.15		T/K = 323.15		Mole Fraction Water <sup>b</sup>	Ostwald Coeff. L	Mole Fraction Water	Ostwald Coeff. L	Mole Fraction Water	Ostwald Coeff. L	Mole Fraction Water	Ostwald Coeff. L	1	0.0451	1	0.0381	1	0.0310	1	0.0238	0.978	0.0476	0.973	0.0392	0.980	0.0326	0.969	0.0240	0.956	0.0462	0.952	0.0417	0.973	0.0326	0.890	0.0245	0.936	0.0441	0.923	0.0394	0.947	0.0325	0.864	0.0270	0.928	0.0432	0.900	0.0358	0.909	0.0323	0.860	0.0272	0.891	0.0385	0.870	0.0356	0.904	0.0322	0.785	0.0391	0.854	0.0384	0.843	0.0362	0.894	0.0321	0.750	0.044	0.830	0.0379	0.700	0.0570	0.875	0.0338	0.616	0.069	0.818	0.0386	0.539	0.0949	0.811	0.0403	0.476	0.0935	0.492	0.105	0.275	0.156	0.683	0.0629	0.262	0.131	0.158	0.136	0.158	0.185	0.525	0.0980	0.140	0.154	0.008	0.233	0.149	0.184	0.289	0.152	0.141	0.154			0.004	0.231	0.134	0.189	0.139	0.153			0.002	0.232	0.120	0.193	0.002	0.180					0.049	0.208	0.002	0.180					0.049	0.208	0.001	0.182					0.029	0.221							0.002	0.283		
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<p><sup>a</sup> Temperature reported to 1°C, but as integer values, i.e., 4, 12, 25, 50°C.</p> <p><sup>b</sup> Mole fraction ethanol = 1 - mole fraction water.</p>																																																																																																																																																																	
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<b>METHOD/APPARATUS/PROCEDURE:</b> Degassed water is transferred to an absorption vessel. The water is sealed over mercury. Gas is added and stirring accomplished with a magnetic bob. Uptake of gas is read on buret system which is thermostatted along with the absorption vessel. Details of operation and a drawing are in the original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> <ol style="list-style-type: none"> <li>Prepared by electrolysis of NaOH solution, followed by removal of hydrogen traces, and thoroughly dried before use. No purity given.</li> <li>Dried to at least 99.7% for solubility in pure ethanol; for all others, alcohol was redistilled twice and diluted with distilled water.</li> <li>Distilled</li> </ol> <b>ESTIMATED ERROR:</b> $\delta L/L = \pm 0.01$ , estimate by compiler. $\delta x/x = \pm 0.002$ , estimate by compiler.																																																																																																																																																																
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Mejane, J. V.; Debailleul, M.; Lecerf, J. <i>Ind. Aliment. Agr.</i> 1974, 90, 719-27. <i>Chem. Abstr.</i> 1974, 80, 119192f.
<b>VARIABLES:</b> T/K = 273-383 Composition	<b>PREPARED BY:</b> R. Battino

<b>EXPERIMENTAL VALUES:</b>			
Degré alcoolique °G.L.	[O <sub>2</sub> ] <sup>a</sup> / mg dm <sup>-3</sup>	Degré alcoolique °G.L.	[O <sub>2</sub> ]/ mg dm <sup>-3</sup>
0	9.17	60	13.3
5	9.5	65	15.5
10	8.8	70	18.3
15	7.9	75	22.6
20	7.8	80	27.6
25	7.9	85	33.8
30	7.8	90	41.0
35	7.9	95	48.7
40	8.4	96	52.0
45	8.8	98	56.3
50	10.0	100	61.9
55	11.9		

<sup>a</sup> Oxygen solubility at a partial gas pressure of 158 mm Hg (21.1 kPa).  
continued on following page

#### AUXILIARY INFORMATION

<b>METHOD/APPARATUS/PROCEDURE:</b> The various alcohol solutions were saturated with air and the oxygen solubility determined polarographically for P <sub>O<sub>2</sub></sub> = 158 mm Hg.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given (2) "surfin" (3)
	<b>ESTIMATED ERROR:</b> δ°G.L. = ± 0.1 δT/K = ± 0.1 δ[O <sub>2</sub> ] = ± 3%, Compiler's estimate
	<b>REFERENCES:</b>

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Mejane, J. V.; Debailleul, M.; Lecerf, J. <i>Ind. Aliment. Agr.</i> <u>1974</u> , <u>90</u> , 719-27. <i>Chem. Abstr.</i> <u>1974</u> , <u>80</u> , 119192f.
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continued

$\begin{matrix} \text{°G.L.} \\ \text{t/°C} \end{matrix}$	10	20	30	40	50	60	70	80	90	100
0	12.6	11.7	11.1	11.9	14.2	17.6	21.4	30.1	44.8	65.0
5	11.3	10.6	10.1	10.8	12.6	16.0	20.8	29.7	44.2	64.6
10	10.1	9.6	9.2	9.7	11.2	14.6	20.1	29.3	43.5	64.1
15	9.2	8.9	8.6	9.0	10.5	13.9	19.3	28.8	42.8	63.0
20	8.3	8.1	8.0	8.4	10.0	13.3	18.5	27.9	40.9	61.2
25	7.7	7.5	7.4	7.8	9.4	12.4	17.4	25.9	38.1	56.1
30	7.2	7.1	7.0	7.3	8.9	11.5	16.4	23.9	35.0	51.8
35	6.9	6.8	6.7	7.0	8.3	10.3	14.6	21.2	30.5	44.2
40	6.6	6.6	6.4	6.8	7.7	9.3	12.8	19.6	26.5	39.0
45	6.1	6.1	6.1	6.5	7.5	9.3	12.8	18.1	25.5	37.6
50	5.5	5.6	5.8	6.2	7.3	9.3	13.0	17.9	25.0	36.6
55	5.1	5.2	5.2	5.5	6.8	9.0	12.4	16.7	23.1	34.4
60	4.7	4.7	4.7	4.9	6.4	8.7	11.6	15.1	20.6	29.8
65	4.3	4.3	4.2	4.3	5.8	7.9	10.6	13.7	18.4	26.1
70	3.8	3.7	3.5	3.6	5.1	7.1	9.2	11.8	15.4	22.2
75	3.0	2.8	2.4	2.5	3.3	4.2	5.0	6.1	7.6	9.9
80	2.2	1.7	1.2	1.2	1.2	0.9	0.6	0	0	0
85	1.3	0.7	0.1	0	0	0	0	0	0	0
90	0.4	0	0	0	0	0	0	0	0	0

<sup>a</sup> Smoothed values of oxygen solubility in mg dm<sup>-3</sup> at a partial pressure of 158mm Hg (21.1 kPa).

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Tokunaga, J. <i>J. Chem. Eng. Data</i> <u>1975</u> , 20, 41-6.		
<b>VARIABLES:</b> T/K = 273-313 Composition		<b>PREPARED BY:</b> C.L. Young; R.W. Cargill		
<b>EXPERIMENTAL VALUES:</b>				
T/K	Mole fraction of alcohol, $x_{C_2H_6O}$	Ostwald coefficient*,L	Henry's Constant /atm	Mole fraction of oxygen in liquid,** $x_{O_2}$
273.15	0.0000	0.0490	25400	0.0000394
	0.0056	0.0485	25400	0.0000394
	0.0089	0.0512	23900	0.0000418
	0.0176	0.0487	24700	0.0000405
	0.0353	0.0489	23800	0.0000420
	0.0552	0.0467	24100	0.0000415
	0.0715	0.0444	24700	0.0000405
	0.1065	0.0403	25800	0.0000388
	0.1376	0.0372	26600	0.0000376
	0.1762	0.0364	25700	0.0000389
	0.2384	0.0437	19500	0.0000513
	0.3646	0.0689	10500	0.0000952
	0.4350	0.0912	7260	0.000138
	0.5464	0.111	5290	0.000189
	0.6676	0.142	3650	0.000274
	0.8981	0.206	2060	0.000485
1.0000	0.238	1660	0.000602	
293.15	0.0000	0.0347	38400	0.0000260
	0.0810	0.0420	27400	0.0000365
	0.1058	0.0409	27000	0.0000370
	0.2057	0.0456	20800	0.0000481
	0.3085	0.0663	12400	0.0000806
	0.4052	0.0890	8100	0.000123
<b>AUXILIARY INFORMATION</b>				
<b>METHOD /APPARATUS/PROCEDURE:</b>  Volumetric apparatus with multibulb buret and magnetic stirrer. Amount of solution and gas absorbed determined volumetrically. Partial pressure determined from total pressure and vapor pressure of solvent solution. Details in source.		<b>SOURCE AND PURITY OF MATERIALS:</b>  (1) High purity grade sample, purity 99.9 mole per cent.  (2,3) Guaranteed reagent, further purified by distillation. Solution degassed by boiling.		
		<b>ESTIMATED ERROR:</b>  $\delta T/K = \pm 0.5$ ; $\delta x_{O_2} = \pm 1-2\%$ .		
		<b>REFERENCES:</b>		

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Tokunaga, J. <i>J. Chem. Eng. Data</i> <u>1975</u> , 20, 46-6.
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EXPERIMENTAL VALUES:				
T/K	Mole fraction of alcohol, $x_{\text{C}_2\text{H}_6\text{O}}$	continued Ostwald coefficient*,L	Henry's Constant /atm	Mole fraction of oxygen in liquid,** $x_{\text{O}_2}$
293.15	0.5280	0.118	5320	0.000188
	0.5978	0.137	4260	0.000235
	0.7171	0.165	3170	0.000315
	0.8065	0.189	2550	0.000392
	0.9382	0.225	1930	0.000518
	1.0000	0.244	1690	0.000592
313.15	0.0000	0.0272	50700	0.0000197
	0.0158	0.0430	31900	0.0000313
	0.0465	0.0383	33800	0.0000296
	0.1022	0.0366	32100	0.0000312
	0.2014	0.0483	20700	0.0000483
	0.3063	0.0675	12900	0.0000775
	0.3924	0.0885	8700	0.000115
	0.4940	0.114	5980	0.000167
	0.5817	0.137	4540	0.000220
	0.6915	0.163	3420	0.000292
	0.7984	0.193	2630	0.000380
	0.8723	0.213	2240	0.000446
	0.9317	0.230	1980	0.000505
	1.0000	0.247	1760	0.000568

\* at  $1.01325 \times 10^5$  Pa partial pressure

\*\* at  $1.01325 \times 10^5$  Pa partial pressure (calculated from the reciprocal of Henry's Constant).

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b>  Cargill, R.W. <i>J. Chem. Soc., Faraday Trans. I</i> <u>1976</u> , 72, 2296-2300.	
<b>VARIABLES:</b> T/K = 277.3 - 334.4 P/kPa = 101.325 Concentration		<b>PREPARED BY:</b>  R.W.Cargill	
<b>EXPERIMENTAL VALUES:</b>			
Mol Fraction Ethanol	T/K	S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup>	log(S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup> )
0.78	277.7	194	2.287
0.78	294.3	198	2.296
0.78	314.2	200	2.301
0.78	331.9	202	2.306
0.99	278.9	269	2.430
0.99	294.8	274	2.437
0.99	313.3	274	2.438
0.99	330.8	275	2.439
continued on following page			
<b>AUXILIARY INFORMATION</b>			
<b>METHOD/APPARATUS/PROCEDURE:</b>  <b>METHOD:</b> Absorption of gas by a thin film of liquid. The Morrison and Billett (1) method was modified by replacing valve A with a constant flow pump, and by measuring the mass of the solvent leaving the absorption tube (instead of the volume) on a top-pan balance.  <b>APPARATUS/PROCEDURE:</b> The solvent is degassed using the vapor pump principle (1). Each determination absorbs about 20 cm <sup>3</sup> of gas in up to 500 cm <sup>3</sup> of solvent, which was recycled. The density of the solvent was checked after each run, so that the exact composition of the solution could be determined (2).		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. British Oxygen Co. Gas 99.5 per cent pure, stored over saturated brine. (2) Ethanol. Absolute Alcohol. (3) Water. Distilled then deionized.	
		<b>ESTIMATED ERROR:</b> $\delta T/K = 0.1$ $\delta P/mmHg = 0.5$ Solubility values reproducible within 0.5 per cent (author).	
		<b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J.Chem.Soc.</i> <u>1948</u> , 2033; <u>1952</u> , 3819 2. International Critical Tables, Volume III, pp 112-118. 3. Morrison, T. J.; Billett, F. <i>J.Chem.Soc.</i> <u>1952</u> , 3819	

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Ethanol; C<sub>2</sub>H<sub>6</sub>O; [64-17-5]  
 (3) Water; H<sub>2</sub>O; [7732-18-5]

Cargill, R.W.  
*J.Chem.Soc., Faraday Trans. I*  
 1976, 72, 2296-2300.

## EXPERIMENTAL VALUES:

continued

Mol Fraction Ethanol	T/K	S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup>	log(S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup> )
0.00	277.0	43.7	1.640
0.00	279.4	41.0	1.613
0.00	283.1	37.4	1.573
0.00	285.7	36.4 <sup>a</sup>	1.561
0.00	286.2	35.2	1.547
0.00	286.5	35.6 <sup>a</sup>	1.551
0.00	290.4	32.6 <sup>a</sup>	1.513
0.00	293.2	30.8	1.489
0.00	294.7	30.1 <sup>a</sup>	1.479
0.00	303.1	26.5 <sup>a</sup>	1.423
0.00	312.5	23.3 <sup>a</sup>	1.368
0.00	322.4	21.1 <sup>a</sup>	1.324
0.00	331.6	19.8 <sup>a</sup>	1.296
0.00	338.4	19.1 <sup>a</sup>	1.279
0.00	345.6	18.3 <sup>a</sup>	1.263
0.00	348.0	18.2 <sup>a</sup>	1.260
0.008	277.8	43.5	1.638
0.008	285.5	36.1	1.558
0.008	294.9	30.2	1.480
0.008	304.1	26.2	1.419
0.008	313.3	23.1	1.364
0.008	324.2	21.2	1.326
0.008	333.5	20.0	1.301
0.021	277.7	44.5	1.648
0.021	285.1	38.0	1.580
0.021	294.9	31.4	1.497
0.021	305.2	26.9	1.430
0.021	314.3	23.9	1.379
0.021	332.4	21.1	1.325
0.032	279.3	43.2	1.635
0.032	286.0	37.3	1.572
0.032	295.9	31.2	1.494
0.032	304.9	27.5	1.439
0.032	313.8	24.8	1.395
0.032	324.3	22.5	1.353
0.032	334.4	21.3	1.329
0.063	277.3	43.0	1.633
0.063	285.4	37.1	1.569
0.063	295.3	31.5	1.498
0.063	306.2	27.2	1.435
0.063	313.3	26.2	1.418
0.063	330.3	24.5	1.389

continued on following page

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Ethanol; C<sub>2</sub>H<sub>6</sub>O; [64-17-5]  
 (3) Water· H<sub>2</sub>O; [7732-18-5]

Cargill, R.W

*J.Chem.Soc., Faraday Trans. I* 1976  
 72, 2296-2300.

## EXPERIMENTAL VALUES:

continued

Mol Fraction Ethanol	T/K	S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup>	log(S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup> )
0.097	278.7	38.6	1.586
0.097	280.8	37.0	1.568
0.097	286.2	34.8	1.542
0.097	293.3	31.8	1.502
0.097	304.2	29.4	1.468
0.097	313.4	27.8	1.444
0.097	324.7	26.7	1.427
0.097	333.9	26.4	1.422
0.12	277.7	37.0	1.568
0.12	285.5	34.3	1.535
0.12	297.3	31.3	1.496
0.12	319.5	29.4	1.469
0.12	332.9	29.5	1.470
0.16	277.6	36.6	1.564
0.16	288.6	35.5	1.550
0.16	308.8	34.7	1.540
0.16	331.9	37.0	1.568
0.23	277.7	45.7	1.660
0.23	294.3	45.8	1.661
0.23	314.3	46.2	1.665
0.23	322.5	48.0	1.681
0.23	333.4	49.2	1.692
0.31	277.8	67.5	1.829
0.31	283.5	67.3	1.828
0.31	298.1	69.0	1.839
0.31	318.3	71.3	1.853
0.49	277.7	110	2.041
0.49	295.3	111	2.044
0.49	314.8	116	2.063
0.49	333.1	121	2.081

<sup>a</sup> Values from reference 3. The solubility, S<sub>O</sub>, calculated as cm<sup>3</sup> gas at 273.15 K and O<sub>2</sub> partial pressure of 101.325 kPa (1 atm) per kg of solvent. In the critical evaluation of this system some of these data have been converted to Ostwald coefficients.

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Propanol; C <sub>3</sub> H <sub>8</sub> O; [71-23-8] (3) Water; H <sub>2</sub> O; [7732-18-5]		ORIGINAL MEASUREMENTS: Tokunaga, J. <i>J. Chem. Eng. Data.</i> <u>1975</u> , 20, 41-6.			
VARIABLES: T/K = 273-313 Composition		PREPARED BY: C.L. Young; R.W. Cargill			
EXPERIMENTAL VALUES:					
T/K	Mole fraction of alcohol, $x_{\text{C}_3\text{H}_8\text{O}}$	Ostwald coefficient,* L	Henry's Constant /atm	Mole fraction of oxygen in liquid,** $x_{\text{O}_2}$	
273.15	0.0000	0.0490	25400	0.0000394	
	0.0240	0.0507	23000	0.0000435	
	0.0477	0.0446	24700	0.0000405	
	0.0719	0.0411	25400	0.0000394	
	0.1007	0.0417	23400	0.0000427	
	0.1248	0.0454	20300	0.0000493	
	0.1982	0.0647	12300	0.0000813	
	0.2852	0.0840	8090	0.000124	
	0.4223	0.106	5190	0.000193	
	0.6208	0.154	2830	0.000353	
	0.7842	0.173	2130	0.000469	
	0.8784	0.187	1810	0.000552	
	1.0000	0.209	1480	0.000676	
	293.15 <sup>†</sup>	0.0000	0.0347	38400	0.0000260
		0.0230	0.0370	33800	0.0000296
		0.0432	0.0353	33700	0.0000297
0.0847		0.0401	26800	0.0000373	
0.1057		0.0446	22900	0.0000437	
0.2050		0.0703	11800	0.0000847	
0.3133		0.0970	7060	0.000142	
0.4175		0.119	4910	0.000204	
0.5103		0.138	3760	0.000266	
0.6020		0.152	3080	0.000325	
0.6953		0.169	2500	0.000400	
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:  Volumetric apparatus with multibulb buret and magnetic stirrer. Amount of solution and gas absorbed determined volumetrically. Partial pressure determined from total pressure and vapor pressure of solvent solution. Details in source.		SOURCE AND PURITY OF MATERIALS: (1) High purity grade sample, purity 99.9 mole per cent. (2,3) Guaranteed reagent, further purified by distillation. Solution degassed by boiling.			
		ESTIMATED ERROR: $\delta T/K = \pm 0.5$ ; $\delta x_{\text{O}_2} = \pm 1-2\%$ .			
		REFERENCES:			



COMPONENTS : (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Propanol; C <sub>3</sub> H <sub>8</sub> O; [71-23-8] (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS : Tokunaga, J. <i>J. Chem. Eng. Data.</i> <u>1975</u> ,20,41-6.
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## EXPERIMENTAL VALUES :

T/K	Mole fraction of alcohol, x <sub>C<sub>3</sub>H<sub>8</sub>O</sub>	Ostwald coefficient,* L	Henry's Constant /atm	Mole fraction of oxygen in liquid,**x <sub>O<sub>2</sub></sub>
293.15	0.7987	0.184	2080	0.000481
	0.9085	0.202	1710	0.000585
	1.0000	0.221	1450	0.000690
313.15	0.0000	0.0272	50700	0.0000197
	0.0225	0.0305	42300	0.0000236
	0.0428	0.0265	46100	0.0000217
	0.0657	0.0294	39200	0.0000255
	0.0834	0.0347	32700	0.0000306
	0.1043	0.0393	27500	0.0000364
	0.2044	0.0707	12000	0.0000833
	0.3034	0.0983	7180	0.000139
	0.4033	0.122	4990	0.000200
	0.5056	0.142	3740	0.000267
	0.6063	0.159	2950	0.000339
	0.6972	0.173	2470	0.000405
	0.8010	0.188	2060	0.000485
	0.8955	0.205	1730	0.000578
	1.0000	0.226	1440	0.000694

\* at  $1.01325 \times 10^5$  Pa partial pressure

\*\* at  $1.01325 \times 10^5$  Pa partial pressure (calculated from the reciprocal of Henry's Constant).

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Propanol; C <sub>3</sub> H <sub>8</sub> O; [67-63-0] (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b> Tokunaga, J. <i>J. Chem. Eng. Data</i> , <u>1975</u> , 20,41-6.		
<b>VARIABLES:</b> T/K = 273-313 Composition		<b>PREPARED BY:</b> C.L. Young; R.W. Cargill		
<b>EXPERIMENTAL VALUES:</b>				
T/K	Mole fraction of alcohol, $x_{\text{C}_3\text{H}_8\text{O}}$	Ostwald coefficient* $L$	Henry's Constant /atm	Mole fraction of oxygen in liquid,** $x_{\text{O}_2}$
273.15	0.0000	0.0490	25400	0.0000394
	0.0096	0.0495	24500	0.0000408
	0.0168	0.0491	24200	0.0000413
	0.0467	0.0430	25600	0.0000391
	0.0851	0.0352	28700	0.0000348
	0.1116	0.0329	29000	0.0000345
	0.1602	0.0431	19900	0.0000503
	0.2779	0.0751	9130	0.000110
	0.3591	0.102	5900	0.000169
	0.4838	0.126	4000	0.000250
	0.5417	0.142	3310	0.000302
	0.6902	0.173	2300	0.000435
	0.7936	0.197	1820	0.000549
	1.0000	0.231	1300	0.000769
293.15	0.0000	0.0347	38400	0.0000260
	0.0220	0.0392	32000	0.0000313
	0.0408	0.0346	34600	0.0000289
	0.0733	0.0334	33100	0.0000302
	0.0943	0.0346	30400	0.0000329
	0.1994	0.0605	13800	0.0000725
	0.2985	0.0917	7600	0.000132
	0.3920	0.115	5220	0.000192
	0.5950	0.162	2860	0.000350
	<b>AUXILIARY INFORMATION</b>			
<b>METHOD /APPARATUS/PROCEDURE:</b> Volumetric apparatus with multibulb buret and magnetic stirrer. Amount of solution and gas absorbed determined volumetrically. Partial pressure determined from total pressure and vapor pressure of solvent solution. Details in source.		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) High purity grade sample, purity 99.9 mole per cent. (2,3) Guaranteed reagent, further purified by distillation. Solution degassed by boiling.		
		<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.5$ ; $\delta x_{\text{O}_2} = \pm 1-2\%$ .		
		<b>REFERENCES:</b>		

COMPONENTS :		ORIGINAL MEASUREMENTS :		
(1)	Oxygen; O <sub>2</sub> ; [7782-44-7]	Tokunaga, J.		
(2)	2-Propanol; C <sub>3</sub> H <sub>8</sub> O; [67-63-0]	J. Chem. Eng. Data. <u>1975</u> , 20, 41-6.		
(3)	Water; H <sub>2</sub> O; [7732-18-5]			
EXPERIMENTAL VALUES:				
T/K	Mole fraction of alcohol, x <sub>C<sub>3</sub>H<sub>8</sub>O</sub>	Ostwald coefficient,* L	Henry's Constant /atm	Mole fraction of oxygen in liquid,**x <sub>O<sub>2</sub></sub>
293.15	0.7836	0.204	1860	0.000538
	1.0000	0.246	1270	0.000787
313.15	0.0000	0.0272	50700	0.0000197
	0.0791	0.0368	31200	0.0000321
	0.0993	0.0390	28000	0.0000357
	0.1496	0.0524	18500	0.0000541
	0.1984	0.0690	12700	0.0000787
	0.3003	0.105	6960	0.000144
	0.3952	0.131	4790	0.000209
	0.5000	0.156	3500	0.000286
	0.5978	0.179	2700	0.000370
	0.6995	0.199	2170	0.000461
	0.7930	0.220	1790	0.000559
	0.8950	0.238	1510	0.000662
	1.0000	0.255	1280	0.000781
* at 1.01325 x 10 <sup>5</sup> Pa partial pressure				
** at 1.01325 x 10 <sup>5</sup> Pa partial pressure (calculated from the reciprocal of Henry's Constant).				

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Müller, C.	
(2) 1,2,3-Propanetriol (Glycerol); C <sub>3</sub> H <sub>8</sub> O <sub>3</sub> ; [56-81-5]		Z. Physik. Chem. <u>1912</u> , 81, 483-503.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES:		PREPARED BY:	
T/K = 285 - 288		R. Battino	
P/kPa = 101.325			
EXPERIMENTAL VALUES:			
T/K <sup>a</sup>	Weight Percentage <sup>b</sup> Glycerol	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> $\alpha$
285.35	20.5	3.034	2.904
285.65	25.	2.775	2.654
287.75	37.3	2.147	2.038
286.65	45.	1.889	1.800
285.55	52.	1.697	1.623
285.25	71.5	1.055	1.010
286.45	88.5	0.950	0.906
<p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> 1,2,3-propanetriol.</p> <p><sup>c</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>d</sup> Bunsen coefficient.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Water is degassed by pumping under vacuum. The absorption vessel is about 600 cm <sup>3</sup> and is separately thermostatted from the buret gas measuring system. Both are connected by a copper capillary tube. Gas uptake is measured on the gas burets. The absorption flask volume and all liquid volumes were calibrated with mercury. The original paper contains details and a drawing of the apparatus. Solubilities were also reported in aqueous solutions of sucrose, d-glucose, and chloral hydrate.		(1) From the heading of KMnO <sub>4</sub> and washed in concentrated KOH solution.	
		(2) 1,2,3-Propanetriol from Merck.	
		(3) No comment by author.	
		ESTIMATED ERROR:	
		$\delta\alpha/\alpha = \pm 0.01$ , estimated by compiler.	
		REFERENCES:	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Methyl-2-propanol ( <u>t</u> -Butanol); C <sub>4</sub> H <sub>10</sub> O [75-65-0] (3) Water; H <sub>2</sub> O; [7732-18-5]		<b>ORIGINAL MEASUREMENTS:</b>  Cargill, R.W. <i>J.Chem.Soc., Faraday Trans. I</i> <u>1976</u> , <i>72</i> , 2296-2300.	
<b>VARIABLES:</b> T/K = 277.5 - 333.9 p/kPa = 101.325 Concentration		<b>PREPARED BY:</b>  R.W. Cargill	
<b>EXPERIMENTAL VALUES:</b>			
Mol Fraction Alcohol	T/K	S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup>	log(S <sub>O</sub> cm <sup>3</sup> kg <sup>-1</sup> )
0.60	278.4	214	2.331
0.60	294.9	211	2.325
0.60	312.5	218	2.338
0.60	331.4	226	2.354
0.76	280.1	246	2.390
0.76	303.1	243	2.386
0.76	313.6	243	2.386
0.76	328.0	245	2.389
0.93	280.5	266	2.425
0.93	297.8	261	2.417
0.93	313.0	256	2.409
continued on following page			
AUXILIARY INFORMATION			
<b>METHOD/APPARATUS/PROCEDURE:</b> <b>METHOD:</b> Absorption of gas by a thin film of liquid. The Morrison and Billett (1) method was modified by replacing valve A with a constant flow pump, and by measuring the mass of the solvent leaving the absorption tube (instead of the volume) on a top-pan balance.  <b>APPARATUS/PROCEDURE:</b> The solvent is degassed using the vapor pump principle (1). Each determination absorbs about 20 cm <sup>3</sup> of gas in up to 500 cm <sup>3</sup> of solvent, which was recycled. The density of the solvent was checked after each run, so that the exact composition of the solution could be determined (2).		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. British Oxygen Co. Gas 99.5 per cent pure, stored over saturated brine. (2) 2-Methyl-2-propanol. Reagent-grade (98 per cent boils 82-83°C). (3) Water. Distilled then deionized.	
		<b>ESTIMATED ERROR:</b> δT/K = 0.1 δP/mmHg = 0.5 Solubility values reproducible within 0.5 per cent (author).	
		<b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J.Chem.Soc.</i> <u>1948</u> , 2033; <u>1952</u> , 3819 2. International Critical Tables, Volume III, pp 112-118 3. Morrison, T. J; Billet, F. <i>J.Chem.Soc.</i> <u>1952</u> , 3819	

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) 2-Methyl-2-propanol (*t*-Butanol); C<sub>4</sub>H<sub>10</sub>O;  
 [75-65-0]  
 (3) Water; H<sub>2</sub>O; [7732-18-5]

Cargill, R. W.

*J. Chem. Soc., Faraday Trans. I* 1976, 72,  
2296-2300.

## EXPERIMENTAL VALUES:

continued

Mol Fraction Alcohol	T/K	S <sub>o</sub> /cm <sup>3</sup> kg <sup>-1</sup>	log(S <sub>o</sub> cm <sup>3</sup> kg <sup>-1</sup> )
0.00	277.0	43.7	1.640
0.00	279.4	41.0	1.613
0.00	283.1	37.4	1.573
0.00	285.7	36.4 <sup>a</sup>	1.561
0.00	286.2	35.2	1.547
0.00	286.5	35.6 <sup>a</sup>	1.551
0.00	290.4	32.6 <sup>a</sup>	1.513
0.00	293.2	30.8	1.489
0.00	294.7	30.1 <sup>a</sup>	1.479
0.00	303.1	26.5 <sup>a</sup>	1.423
0.00	312.5	23.3 <sup>a</sup>	1.368
0.00	322.4	21.1 <sup>a</sup>	1.324
0.00	331.6	19.8 <sup>a</sup>	1.296
0.00	338.4	19.1 <sup>a</sup>	1.279
0.00	345.6	18.3 <sup>a</sup>	1.263
0.00	348.0	18.2 <sup>a</sup>	1.260
0.006	277.7	42.8	1.631
0.006	285.5	35.8	1.554
0.006	292.8	31.3	1.495
0.006	296.5	28.8	1.459
0.006	304.2	26.2	1.419
0.006	318.5	22.1	1.344
0.006	332.9	19.8	1.296
0.014	278.0	43.5	1.638
0.014	278.7	42.6	1.629
0.014	285.5	36.6	1.563
0.014	297.0	29.4	1.469
0.014	304.2	26.1	1.417
0.014	308.3	24.7	1.392
0.014	314.4	23.2	1.366
0.014	325.2	21.7	1.336
0.014	333.0	20.5	1.312
0.014	333.4	20.5	1.312
0.022	277.6	42.7	1.630
0.022	285.5	35.3	1.548
0.022	295.9	29.2	1.466
0.022	304.7	26.2	1.418
0.022	314.4	23.4	1.370
0.022	324.7	21.8	1.338
0.022	334.4	20.6	1.313
0.032	278.4	38.9	1.590
0.032	285.5	32.9	1.517
0.032	294.3	29.4	1.469
0.032	305.1	26.1	1.416
0.032	314.3	24.3	1.386
0.032	324.2	23.6	1.373
0.032	333.9	22.4	1.351

continued on following page

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) 2-Methyl-2-propanol (t-Butanol);  
 C<sub>4</sub>H<sub>10</sub>O; [75-65-0]  
 (3) Water; H<sub>2</sub>O; [7732-18-5]

Cargill, R.W.

*J.Chem.Soc., Faraday Trans. I* 1976, *72*,  
2296-2300.

## EXPERIMENTAL VALUES:

Mol Fraction Alcohol	T/K	S <sub>O</sub> /cm <sup>3</sup> kg <sup>-1</sup>	Log(S <sub>O</sub> cm <sup>3</sup> kg <sup>-1</sup> )
0.044	277.8	35.1	1.545
0.044	285.5	31.9	1.504
0.044	294.8	27.9	1.446
0.044	304.7	26.6	1.424
0.044	314.9	24.7	1.393
0.044	324.7	25.0	1.398
0.044	335.1	25.1	1.399
0.062	283.5	29.5	1.470
0.062	296.9	28.8	1.460
0.062	310.8	29.3	1.467
0.062	327.5	30.4	1.483
0.093	277.8	37.6	1.575
0.093	287.9	38.7	1.588
0.093	310.4	41.1	1.614
0.093	321.7	42.7	1.630
0.093	333.5	43.5	1.638
0.15	285.8	62.4	1.795
0.15	298.0	63.8	1.805
0.15	313.0	65.8	1.818
0.15	332.7	70.3	1.847
0.18	277.7	70.8	1.850
0.18	288.1	72.4	1.860
0.18	299.6	73.1	1.864
0.18	310.6	76.2	1.882
0.18	321.4	76.2	1.882
0.18	333.6	80.2	1.904
0.25	284.4	96.8	1.986
0.25	303.6	101	2.006
0.25	323.7	107	2.029
0.31	277.8	122	2.087
0.31	295.3	129	2.111
0.31	313.8	130	2.113
0.31	333.4	133	2.124
0.44	279.2	167	2.222
0.44	287.6	169	2.229
0.44	297.6	169	2.227
0.44	308.0	172	2.236
0.44	319.5	173	2.237
0.44	331.1	177	2.247

<sup>a</sup> Values from reference 3. The solubility, S<sub>O</sub>, calculated as cm<sup>3</sup> gas at 273.15 K and O<sub>2</sub> partial pressure of 101.325 kPa (1 atm) per kg of solvent.

<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) 2,2,2-Trichloro-1,1-ethane-diol (Chloral hydrate); [302-17-0]  (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b>  Müller, C.  <i>Z. Physik. Chem.</i> <u>1912</u> , <i>81</i> , 483-503.																																								
<b>VARIABLES:</b> T/K = 286 - 291 P/kPa = 101.325	<b>PREPARED BY:</b>  R. Battino																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K<sup>a</sup></th> <th style="text-align: center;">Weight Percentage Chloral hydrate<sup>b</sup></th> <th style="text-align: center;">Ostwald Coeff.<sup>c</sup> 10<sup>2</sup>L</th> <th style="text-align: center;">Bunsen Coeff.<sup>d</sup> 10<sup>2</sup>α</th> </tr> </thead> <tbody> <tr><td style="text-align: center;">291.45</td><td style="text-align: center;">22.9</td><td style="text-align: center;">2.944</td><td style="text-align: center;">2.759</td></tr> <tr><td style="text-align: center;">290.05</td><td style="text-align: center;">28.</td><td style="text-align: center;">2.856</td><td style="text-align: center;">2.690</td></tr> <tr><td style="text-align: center;">288.55</td><td style="text-align: center;">36.6</td><td style="text-align: center;">2.736</td><td style="text-align: center;">2.590</td></tr> <tr><td style="text-align: center;">289.75</td><td style="text-align: center;">38.6</td><td style="text-align: center;">2.548</td><td style="text-align: center;">2.402</td></tr> <tr><td style="text-align: center;">285.95</td><td style="text-align: center;">51.3</td><td style="text-align: center;">2.553</td><td style="text-align: center;">2.439</td></tr> <tr><td style="text-align: center;">289.35</td><td style="text-align: center;">58.44</td><td style="text-align: center;">2.489</td><td style="text-align: center;">2.350</td></tr> <tr><td style="text-align: center;">289.05</td><td style="text-align: center;">70.</td><td style="text-align: center;">2.814</td><td style="text-align: center;">2.659</td></tr> <tr><td style="text-align: center;">290.35</td><td style="text-align: center;">80.85</td><td style="text-align: center;">3.402</td><td style="text-align: center;">3.200</td></tr> <tr><td style="text-align: center;">290.05</td><td style="text-align: center;">80.9</td><td style="text-align: center;">3.334</td><td style="text-align: center;">3.140</td></tr> </tbody> </table>		T/K <sup>a</sup>	Weight Percentage Chloral hydrate <sup>b</sup>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α	291.45	22.9	2.944	2.759	290.05	28.	2.856	2.690	288.55	36.6	2.736	2.590	289.75	38.6	2.548	2.402	285.95	51.3	2.553	2.439	289.35	58.44	2.489	2.350	289.05	70.	2.814	2.659	290.35	80.85	3.402	3.200	290.05	80.9	3.334	3.140
T/K <sup>a</sup>	Weight Percentage Chloral hydrate <sup>b</sup>	Ostwald Coeff. <sup>c</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>d</sup> 10 <sup>2</sup> α																																						
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<p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> 2,2,2-Trichloro-1,1-ethanediol.</p> <p><sup>c</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>d</sup> Bunsen coefficient.</p>																																									
<b>AUXILIARY INFORMATION</b>																																									
<b>METHOD/APPARATUS/PROCEDURE:</b>  Water is degassed by pumping under vacuum. The absorption vessel is about 600 cm <sup>3</sup> and is separately thermostatted from the buret gas measuring system. Both are connected by a copper capillary tube. Gas uptake is measured on the gas burets. The absorption flask volume and all liquid volumes were calibrated with mercury. The original paper contains details and a drawing of the apparatus. Solubilities were also reported in aqueous solutions of sucrose, d-glucose, and glycerol.	<b>SOURCE AND PURITY OF MATERIALS:</b>  (1) From the heating of KMnO <sub>4</sub> and washed in concentrated KOH solution.  (2) 2,2,2-Trichloro-1,1-ethanediol- from Merck or from Münster.  (3) No comment by author.  <b>ESTIMATED ERROR:</b>  $\delta\alpha/\alpha = \pm 0.01$ , estimated by compiler.  <b>REFERENCES:</b>																																								



COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfuric acid monododecyl ester sodium salt (Sodium dodecyl sulfate or SDS); C <sub>12</sub> H <sub>26</sub> O <sub>4</sub> S.Na; [151-21-3] (3) Water; H <sub>2</sub> O; [7732-18-5]		ORIGINAL MEASUREMENTS: Matheson, I. B. C.; King, A. D. <i>J. Coll. Interface Sci.</i> 1978, 66, 464-9.				
VARIABLES: T/K = 298.15 P/kPa = 340 - 841 SDS/mol kg <sup>-1</sup> H <sub>2</sub> O = 0 - 0.300		PREPARED BY:  H. L. Clever				
EXPERIMENTAL VALUES:						
T/K	Sulfuric acid monodecyl ester sodium salt mol kg <sup>-1</sup> H <sub>2</sub> O	Pressure pounds per square inch, gauge	Volume gas evolved ml	Ambient Pressure mmHg	Ambient Temperature °C	Henry's constant K x 10 <sup>3</sup> mol Ar kg <sup>-1</sup> H <sub>2</sub> O atm <sup>-1</sup>
298.15	0	49.3	12.5	746.3	25.1	
		71.5	18.0	743.5	25.2	
		74.7	18.6	745.5	24.8	
		108.5	26.2	747.0	24.8	
		122.0	29.7	745.5	25.9	
	0.100	65.5	16.9	755.3	23.0	1.47±0.03
		90.3	22.2	751.1	23.3	
		121.0	30.5	756.7	22.0	
	0.200	52.2	14.9	741.7	22.6	1.61±0.02
		69.0	19.4	741.0	23.1	
		91.0	25.0	743.2	22.9	
	0.300	56.6	16.5	754.0	22.4	1.70±0.01
66.9		19.4	743.8	22.0		
86.5		25.2	752.4	21.9		
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE: The apparatus consists of a jacketed thermostated thick-walled cylindrical brass bomb which rests on a variable speed magnetic stirrer. An inlet line to the bomb is connected to a gas manifold, and an exit line is connected to a Warburg manometer. Bourden gauges are used to record the pressure. The solution, consisting of 100 g of water and the colloidal electrolyte, is contained in a glass liner inside of the bomb. The solution is degassed by evacuation to just above water vapor pressure and then stirring for several hours. The gas is introduced over the solution at the desired pressure and the solution is stirred for a minimum of five hours. The gas is vented to atmospheric pressure. The gas from the supersaturated solution is collected in the Warburg manometer and its volume measured at atmospheric pressure and ambient temperature. Corrections for gas lost during venting and thermal equilibration and for water vapor pressure are made. The solubility is reported as Henry's constant, K/mol gas kg <sup>-1</sup> water atm <sup>-1</sup> = gas molality/pressure, m/p.			SOURCE AND PURITY OF MATERIALS: (1) Oxygen. Source not given. Chemically pure or equivalent of 99.5 mol per cent purity or better. (2) Sulfuric acid monodecyl ester sodium salt. Aldrich Chemical Co. Inc. Recrystallized from ethanol and dried <u>in vacuo</u> . (3) Water. Laboratory distilled.			
			ESTIMATED ERROR:  δK/K = 0.02			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2,2,4-Trimethylpentane or iso-octane; C <sub>8</sub> H <sub>18</sub> ; [540-84-1] (3) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	<b>ORIGINAL MEASUREMENTS:</b> Kretschmer, C. B.; Nowakowaska, J.; Wiebe, R.  <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506-9.												
<b>VARIABLES:</b> T/K = 273.15 - 323.15 P/kPa = 101.325 Ethanol/vol % = 50	<b>PREPARED BY:</b> P. L. Long; H.L. Clever; R.W. Cargill												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="379 485 900 677" style="margin: 10px auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>273.15</td> <td>0.3119</td> <td>0.3119</td> </tr> <tr> <td>298.15</td> <td>0.2898</td> <td>0.3163</td> </tr> <tr> <td>323.15</td> <td>0.2726</td> <td>0.3225</td> </tr> </tbody> </table> <p>The Ostwald coefficients were measured at a total pressure of 101.325 kPa (1 atm). The compiler calculated the Bunsen coefficient value for an oxygen partial pressure of 101.325 kPa (1 atm) assuming the Ostwald coefficient was independent of pressure.</p> <p>The solvent is 2,2,4-trimethylpentane in ethanol, 50 per cent by volume.</p>		T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	273.15	0.3119	0.3119	298.15	0.2898	0.3163	323.15	0.2726	0.3225
T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L											
273.15	0.3119	0.3119											
298.15	0.2898	0.3163											
323.15	0.2726	0.3225											
<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was similar to that of Horiuti (1), it consisted of a gas buret, manometer, and absorption pipet equipped with a magnetic stirrer. All volumes were calibrated by mercury displacement.  The solvent was partly degassed by boiling under reflux. About 40 cm <sup>3</sup> of solvent was admitted into the absorption pipet, and pumped on to complete the degassing. Dry gas, measured in the buret, was admitted, final equilibrium was established after 1 to 3 hours stirring. During the solution process the total pressure was kept at one atm by additions of dry gas.  The solubility value was corrected for the increase of solvent volume with gas absorption, and for the nitrogen impurity in the oxygen.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Contained 0.4 per cent N <sub>2</sub> . Passed through Drierite to dry. (2) 2,2,4-Trimethylpentane. "Certified material," source not given. Dried over CaSO <sub>4</sub> , distilled, b.p. (760 mmHg)/°C 4' 99.24, density, $\rho_4^{25}$ /g cm <sup>-3</sup> 0.68774. (3) Ethanol. Source not given. Dried with Mg. Density, $\rho$ /g cm <sup>-3</sup> 0.78508.  <b>ESTIMATED ERROR:</b> Gas buret $\delta V/\text{cm}^3 = 0.005$ Average deviation from the mean 0.3%, maximum deviation 0.9% (authors).  <b>REFERENCES:</b> 1. Horiuti, J. <i>J. Sci Papers Inst. Phys. Chem. Res. (Tokyo)</i> <u>1931</u> , <i>17</i> , 125.												

## COMPONENTS:

- (1) Oxygen;  $O_2$ ; [7782-44-7]  
 (2) n-Alkanes

## EVALUATOR:

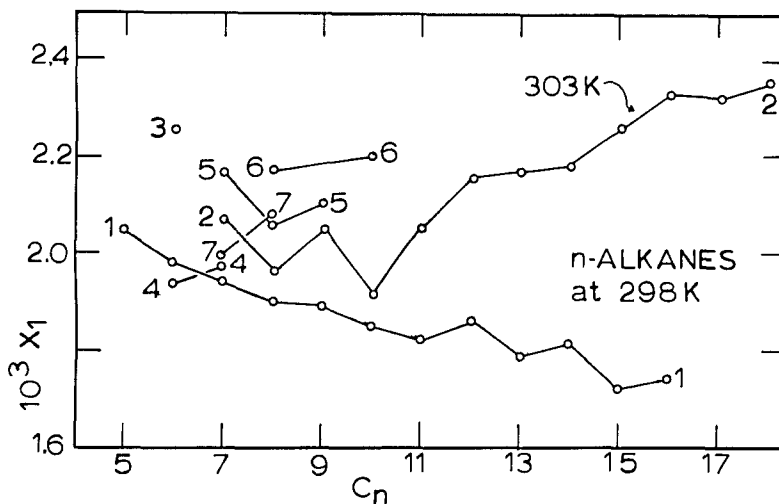
Rubin Battino  
 Department of Chemistry  
 Wright State University  
 Dayton, OH 45435 U.S.A.

## CRITICAL EVALUATION:

The solubility of oxygen in the n-alkanes has been studied by some seven workers (1-7) with surprisingly poor agreement. This is most striking when examining the figure below. The work of Makranczy, et al. (1) shows a decreasing solubility with increasing carbon number while that of Blance and Batiste (2) shows an increasing solubility. The work of these two groups appears to be of comparable precision. However, a judgment on accuracy must depend on a definitive study of these systems. There does appear to be a general trend for solubilities in even-numbered n-alkanes to be higher than for those in the odd-numbered members.

The solubility of oxygen in 2,2,4-trimethylpentane (isooctane) was measured by four groups (7-10) and the four values at 298.15, respectively, by reference number are: 2.43, 2.814, 2.59 (at 293.15), and  $2.529 \times 10^{-3}$  mole fraction solubility at 101.325 kPa partial pressure of gas. The average value is  $2.58 \times 10^{-3} \pm 0.17$  ( $\sigma$ ).

The n-alkanes need to be re-studied.



continued on following page

COMPONENTS:  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) n-Alkanes	EVALUATOR:  Rubin Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.
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## CRITICAL EVALUATION:

continued

References

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10. Kretschmer, C.G.; Nowakowska, J.; Wiebe, R. *Ind. Eng. Chem.* 1946, *38*, 506-9.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Pentane; C <sub>5</sub> H <sub>12</sub> ; [109-66-0]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Ruzs, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> <u>1976</u> , <i>4</i> , 269-80.												
<b>VARIABLES:</b> T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> S. A. Johnson H. L. Clever												
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> Volumetric method. The apparatus of Bodor, Bor, Mohai and Sipos (1) was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> Both the gas and liquid were analytical grade reagents of Hungarian or of foreign origin. No further information.												
<b>ESTIMATED ERROR:</b> $\delta X_1/X_1 = 0.03$													
<b>REFERENCES:</b> 1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , <i>1</i> , 55. <i>Chem. Abstr.</i> <u>1961</u> , <i>55</i> , 3175h.													

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hexane; C <sub>6</sub> H <sub>14</sub> ; [110-54-3]	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K. Candidates thesis, <u>1970</u> , Leningrad.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="263 477 987 636" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^3</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient <math>L</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">2.258</td> <td style="text-align: center;">0.385</td> <td style="text-align: center;">0.421</td> </tr> </tbody> </table> <p>The mole fraction solubility value is quoted in (1).</p> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient $L$	298.15	2.258	0.385	0.421
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> Probably used volumetric method described by Naumenko <i>et al.</i> (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> No information.								
<b>ESTIMATED ERROR:</b>									
<b>REFERENCES:</b> <ol style="list-style-type: none"> <li>1. Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I.A. <i>Zh. Fiz. Khim.</i> <u>1979</u>, <i>53</i>, 1989.</li> <li>2. Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim.</i> <u>1969</u>, <i>42</i>, 2090.</li> </ol>									

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<b>VARIABLES:</b> T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> S. A. Johnson H. L. Clever												
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Alkanes; C <sub>6</sub> H <sub>14</sub> and C <sub>7</sub> H <sub>16</sub>	<b>ORIGINAL MEASUREMENTS:</b> Guerry, D. Jr.  Ph.D. thesis, 1944, Vanderbilt University, Nashville, TN.																												
<b>VARIABLES:</b> T/K = 293.15, 298.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																												
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<b>AUXILIARY INFORMATION</b>																													
<b>METHOD/APPARATUS/PROCEDURE:</b> A Van Slyke-Neill Manometric Apparatus manufactured by the Eimer and Amend Co. was used.  The procedure of Van Slyke (1) for pure liquids was modified (2) so that small solvent samples (2 cm <sup>3</sup> ) could be used with almost complete recovery of the sample.  An improved temperature control system was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> Hexane. Eastman Kodak Co. B.p. (760.3 mmHg) t/°C 68.85 - 68.90.  Heptane. B.p. (753.9 mmHg) t/°C 98.27 - 98.28 (corr.).																												
<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air reduction Co. Purity 99.5 per cent.  (2) Alkanes. Distilled from sodium in air. In addition to the solubility data the thesis contains data of the refractive index, density, vapor pressure, and b.p.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$  <b>REFERENCES:</b> 1. Van Slyke, D. D. <i>J. Biol. Chem.</i> <u>1939</u> , <i>130</i> , 545.  2. Ijams, C. C. Ph.D. thesis, <u>1941</u> Vanderbilt University																												



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Heptane; C <sub>7</sub> H <sub>16</sub> ; [142-82-5]	<b>ORIGINAL MEASUREMENTS:</b> Thomsen, E. S.; Gjaldbaek, J. C. <i>Acta Chem. Scand.</i> <u>1963</u> , <i>17</i> , 127-33.																												
<b>VARIABLES:</b> T/K = 298.15 - 307.95 Total P/kPa = 101.325	<b>PREPARED BY:</b> E. S. Thomsen																												
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<b>VARIABLES:</b>  T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b>  S. A. Johnson H. L. Clever

**EXPERIMENTAL VALUES:**

T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L
298.15	1.94	0.295	0.322
313.15	1.54	0.230	0.264

The mole fraction solubilities and the Bunsen coefficients were calculated by the compiler.

Smoothed Data:  $\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -11,950 + 92.003 T$

See the evaluation of the oxygen + heptane system for the recommended equation.

**AUXILIARY INFORMATION**

<b>METHOD/APPARATUS/PROCEDURE:</b>  Volumetric method. The apparatus of Bodor, Bor, Mohai and Sipos (1) was used.	<b>SOURCE AND PURITY OF MATERIALS:</b>  Both the gas and liquid were analytical grade reagents of Hungarian or of foreign origin. No further information.
	<b>ESTIMATED ERROR:</b>  $\delta X_1/X_1 = 0.03$
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<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) Octane; C <sub>8</sub> H <sub>18</sub> ; [111-65-9]	<b>ORIGINAL MEASUREMENTS:</b>  Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.  <i>Hung. J. Ind. Chem.</i> <u>1976</u> , <i>4</i> , 269-80.												
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313.15	1.48	0.200	0.229										
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<b>METHOD/APPARATUS/PROCEDURE:</b>  Volumetric method. The apparatus of Bodor, Bor, Mohai and Sipos (1) was used.	<b>SOURCE AND PURITY OF MATERIALS:</b>  Both the gas and liquid were analytical grade reagents of Hungarian or of foreign origin. No further information.  <b>ESTIMATED ERROR:</b>  $\delta X_1/X_1 = 0.03$  <b>REFERENCES:</b>  1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , <i>1</i> , 55. <i>Chem. Abstr.</i> <u>1961</u> , <i>55</i> , 3157h.												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Octane; C <sub>8</sub> H <sub>18</sub> ; [111-65-9]	<b>ORIGINAL MEASUREMENTS:</b> Wilcock, R. J.; Battino, R.; Danforth, W. F.; Wilhelm, E.  <i>J. Chem. Thermodyn.</i> <u>1978</u> , <i>10</i> , 817-22.																															
<b>VARIABLES:</b> T/K = 283.31 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> A. L. Cramer																															
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="379 466 1055 633"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>283.31</td> <td>2.159</td> <td>0.3015</td> <td>0.3127</td> </tr> <tr> <td>298.21</td> <td>2.177</td> <td>0.2990</td> <td>0.3264</td> </tr> <tr> <td>313.15</td> <td>2.170</td> <td>0.2927</td> <td>0.3356</td> </tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler.            The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = 120.84 + 50.591 T</math>            Std. Dev. <math>\Delta G^\circ = 8.1</math>, Coef. Corr. = 0.9999  <math>\Delta H^\circ/\text{J mol}^{-1} = 120.84</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -50.591</math></p> <table border="1" data-bbox="480 878 967 1078"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>283.15</td> <td>2.16</td> <td>14,445</td> </tr> <tr> <td>293.15</td> <td>2.17</td> <td>14,951</td> </tr> <tr> <td>303.15</td> <td>2.17</td> <td>15,457</td> </tr> <tr> <td>313.15</td> <td>2.17</td> <td>15,963</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	283.31	2.159	0.3015	0.3127	298.21	2.177	0.2990	0.3264	313.15	2.170	0.2927	0.3356	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	283.15	2.16	14,445	293.15	2.17	14,951	303.15	2.17	15,457	313.15	2.17	15,963
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3).  Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns.  Solubility Determination. The degassed solvent is passed in a thin film down a glass helical tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Products and Chemicals Co. 99.6 per cent. (2) Octane. Phillips Petroleum Co. 99 mol %, distilled, density $\rho_{298.15} = 0.6988$ .  <b>ESTIMATED ERROR:</b> $\delta T/\text{K} = 0.02$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.01$  <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u> , 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u> , <i>45</i> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , <i>43</i> , 806.																															

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2,2,4-Trimethylpentane or isooctane; C <sub>8</sub> H <sub>18</sub> ; [540-84-1]	<b>ORIGINAL MEASUREMENTS:</b> Kretschmer, C. B.; Nowakowska, J.; Wiebe, R. <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506-9.																																								
<b>VARIABLES:</b> T/K = 248.15 - 323.15 P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever																																								
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was similar to that of Horiuti (1), it consisted of a gas buret, manometer, and absorption pipet equipped with a magnetic stirrer. All volumes were calibrated by mercury displacement. The solvent was partly degassed by boiling under reflux. About 40 cm <sup>3</sup> of solvent was admitted into the absorption pipet, and pumped on to complete the degassing. Dry gas, measured in the buret, was admitted, final equilibrium was established after 1 to 3 hours stirring. During the solution process the total pressure was kept at one atm by additions of dry gas. The solubility value was corrected for the increase of solvent volume with gas absorption, and for the nitrogen impurity in the oxygen.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Contained 0.4 per cent N <sub>2</sub> . Gas dried by passing through Drierite. (2) 2,2,4-Trimethylpentane. "Certified material", source not given. Dried over CaSO <sub>4</sub> , distilled, b.p. (760 mmHg) 99.24, density $\rho_4^{25}/\text{g cm}^{-3}$ 0.68774. <b>ESTIMATED ERROR:</b> Gas buret $\delta V/\text{cm}^3 = 0.005$ Average deviation from the mean 0.3 %, maximum deviation 0.9 % (authors). <b>REFERENCES:</b> 1. Horiuti, J. <i>J. Sci Papers Inst. Phys. Chem. Res. (Tokyo)</i> <u>1931</u> , <i>17</i> , 125.																																								

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 2,2,4-Trimethylpentane (Isooctane); C<sub>8</sub>H<sub>18</sub>; [540-84-1]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Baldwin, R. R.; Daniel, S. G.; <i>J. Appl. Chem.</i>, <u>1952</u>, 2(Apr.), 161-5.</p> <p><i>J. Inst. Petrol.</i>, London, <u>1953</u>, 39, 105-24.</p>								
<p>VARIABLES:</p> <p>T/K = 293.15</p> <p>O<sub>2</sub> P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>P. L. Long H. L. Clever</p>								
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<p>AUXILIARY INFORMATION</p>									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The method consists of two operations: Saturation of the liquid with the gas under consideration; and determination of the amount of dissolved gas in the liquid saturated with the gas. All gases were passed through a liquid air trap to remove water and CO<sub>2</sub> vapors before passage through the liquid. All gases were passed through a long coil, thermostated, before the saturation process.</p> <p>Oil or similar liquid is deaerated by passing it through a continuously evacuated vessel. Gas is then passed through the liquid to saturation. Liquid is then degassed, and transferred to a storage burette, disconnected from the degassing apparatus, thermostated, and saturated with the desired gas. Burette is now connected to another degassing apparatus, portions of the oil degassed and gas collected.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. From commercial cylinders, and gas analysis on a Bone and Wheeler apparatus shows it to be at least 99.5% pure; no source given.</p> <p>(2) 2,2,3-Trimethylpentane. No information.</p> <p>ESTIMATED ERROR:</p> <p>δP/P = 0.01 δα/α = 0.01</p> <p>REFERENCES:</p>								

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<p>VARIABLES:</p> <p>T/K = 282.87 - 303.36 P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>M. E. Derrick H. L. Clever</p>																																						
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus consists of a gas-measuring buret, an absorption pipet, and reservoir for solvent. The buret is thermostated at 25°C, the pipet at any temperature from 5 to 30°C.</p> <p>The solvent is degassed by freezing with liquid nitrogen, evacuating, then boiling with a heat lamp. The solvent never comes into contact with stopcock grease.</p> <p>The amount of gas is determined by P-V measurements in the gas buret before and after admission of the gas into the pipet. No solvent vapor is allowed into the buret system. The solvent is magnetically stirred for up to 24 hours until equilibrium is reached.</p> <p>Ideal gas behavior and Henry's law are assumed to calculate the mole fraction solubility at a gas partial pressure of one atm.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Linde Oxygen Co. Standard grade, 99.7% oxygen.</p> <p>(2) C<sub>8</sub>H<sub>18</sub>: Phillips "pure" product. dried, fractionated b.p. 99.1°C.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta X_1/X_1 = 0.003</math></p> <p>REFERENCES:</p>																																						



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<b>VARIABLES:</b> T/K = 298.05 - 298.15 Total P/kPa = 101.325	<b>PREPARED BY:</b> E. S. Thomsen												
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> A calibrated all-glass combined manometer and bulb was enclosed in an air thermostat and shaken until equilibrium. Mercury was used for calibration and as the confining liquid. The solvents were degassed in the apparatus. Details are in references 1 and 2.  The absorbed volume of gas was calculated from the initial and final amounts, both saturated with solvent vapor. The amount of solvent was determined by the weight of displaced mercury.  The saturation of the liquid with the gas was carried out close to atmospheric pressure. The solubility values were reported for one atmosphere gas pressure assuming Henry's law is obeyed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Contained 0.2 percent N <sub>2</sub> . (2) Nonane, Fluka "purum." Fractionated, distillation range 0.08 K.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta X_1/X_1 = 0.015$  <b>REFERENCES:</b> 1. Lannung, A. <i>J. Am. Chem. Soc.</i> <u>1930</u> , 52, 68. 2. Gjaldbaek, J. C. <i>Acta Chem. Scand.</i> <u>1952</u> , 6, 623.												

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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Volumetric method. The apparatus of Bodor, Bor, Mohai and Sipos (1) was used.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>Both the gas and liquid were analytical grade reagents of Hungarian or of foreign origin. No further information.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta X_1/X_1 = 0.03</math></p> <p>REFERENCES:</p> <p>1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u>, 1, 55. <i>Chem. Abstr.</i> <u>1961</u>, 55, 3157h.</p>												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Decane; C <sub>10</sub> H <sub>22</sub> ; [124-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.  <i>Inst. J. Ind. Chem.</i> <u>1976</u> , 4, 269-80.												
<b>VARIABLES:</b> T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> S. A. Johnson H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="321 478 1010 638" style="margin: 10px auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>1.85</td> <td>0.212</td> <td>0.231</td> </tr> <tr> <td>313.15</td> <td>1.42</td> <td>0.159</td> <td>0.183</td> </tr> </tbody> </table> <p>The mole fraction solubilities and the Bunsen coefficients were calculated by the compiler.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -13,690 + 98,234 T</math></p> <p>See the evaluation of the oxygen + decane system for the recommended equation.</p>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	298.15	1.85	0.212	0.231	313.15	1.42	0.159	0.183
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<b>REFERENCES:</b>  1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , 1, 55. <i>Chem. Abstr.</i> <u>1961</u> , 55, 3157h.													

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Decane; C<sub>10</sub>H<sub>22</sub>; [124-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wilcock, R. J.; Battino, R.; Danforth, W. F.; Wilhelm, E.</p> <p><i>J. Chem. Thermodyn.</i> <u>1978</u>, <i>10</i>, 817-22.</p>																																		
<p>VARIABLES:</p> <p>T/K = 283.15 - 313.48 P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>H. L. Clever</p>																																		
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="339 453 997 632"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>283.15</td> <td>2.204</td> <td>0.2564</td> <td>0.2658</td> </tr> <tr> <td>298.11</td> <td>2.200</td> <td>0.2522</td> <td>0.2752</td> </tr> <tr> <td>313.48</td> <td>2.181</td> <td>0.2460</td> <td>0.2823</td> </tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler. The solubility values were adjusted to 101.325 kPa (1 atm) assuming Henry's law.</p> <p>Smoothed Data: <math>\Delta G^\circ/J \text{ mol}^{-1} = -RT \ln X_1 = -281.9 + 51.846 T</math> Std. Dev. <math>\Delta G^\circ = 5.9</math>, Coef. Corr. = 0.9999 <math>\Delta H^\circ/J \text{ mol}^{-1} = -281.9</math>, <math>\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1} = -51.846</math></p> <table border="1" data-bbox="422 880 896 1105"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>278.15</td> <td>2.21</td> <td>14,139</td> </tr> <tr> <td>288.15</td> <td>2.20</td> <td>14,658</td> </tr> <tr> <td>298.15</td> <td>2.19</td> <td>15,176</td> </tr> <tr> <td>308.15</td> <td>2.19</td> <td>15,695</td> </tr> <tr> <td>318.15</td> <td>2.18</td> <td>16,213</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	283.15	2.204	0.2564	0.2658	298.11	2.200	0.2522	0.2752	313.48	2.181	0.2460	0.2823	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/J \text{ mol}^{-1}$	278.15	2.21	14,139	288.15	2.20	14,658	298.15	2.19	15,176	308.15	2.19	15,695	318.15	2.18	16,213
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<p>AUXILIARY INFORMATION</p>																																			
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3).</p> <p>Degassing. Up to 500 cm<sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N<sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns.</p> <p>Solubility Determination. The degassed solvent is passed in a thin film down a glass helical tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Air Products and Chemicals Co. 99.6 per cent. (2) Decane. Phillips Petroleum Co. 99 mol % distilled, density, <math>\rho_{298.15} = 0.7264</math>.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.02</math> <math>\delta P/\text{mmHg} = 0.5</math> <math>\delta X_1/X_1 = 0.01</math></p> <p>REFERENCES:</p> <ol style="list-style-type: none"> <li>Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u>, 2033.</li> <li>Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u>, <i>45</i>, 830.</li> <li>Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u>, <i>43</i>, 806.</li> </ol>																																		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Undecane; C <sub>11</sub> H <sub>24</sub> ; [1120-21-4]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> <u>1976</u> , <i>4</i> , 269-80.
<b>VARIABLES:</b> T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever S. A. Johnson

**EXPERIMENTAL VALUES:**

T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L
298.15	1.82	0.193	0.211
313.15	1.38	0.144	0.165

The mole fraction solubilities and the Bunsen coefficients were calculated by the compiler.

Smoothed Data:  $\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -14,322 + 100.49 T$

The data and the equation are classed as tentative.

**AUXILIARY INFORMATION****METHOD/APPARATUS/PROCEDURE:**

Volumetric method. The apparatus of Bodor, Bor, Mohai and Sipos (1) was used.

**SOURCE AND PURITY OF MATERIALS:**

Both the gas and liquid were analytical grade reagents of Hungarian or of foreign origin. No further information.

**ESTIMATED ERROR:**

$$\delta X_1/X_1 = 0.03$$

**REFERENCES:**

1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G.

*Veszpremi Vegyip. Egy. Kozl.*  
 1957, *1*, 55.  
*Chem. Abstr.* 1961, *55*, 3157h.

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Dodecane; C<sub>12</sub>H<sub>26</sub>; [112-40-3]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L.</p> <p><i>Hung. J. Ind. Chem.</i> <u>1976</u>, 4, 269-80.</p>												
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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="296 506 980 675"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> x 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>1.86</td> <td>0.182</td> <td>0.199</td> </tr> <tr> <td>313.15</td> <td>1.38</td> <td>0.133</td> <td>0.153</td> </tr> </tbody> </table> <p>The mole fraction solubilities and the Bunsen coefficients were calculated by the compiler.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -15,447 + 104.08 T</math></p> <p>The data and the equation are classes as tentative.</p>		T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	298.15	1.86	0.182	0.199	313.15	1.38	0.133	0.153
T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L										
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Tridecane; C <sub>13</sub> H <sub>28</sub> ; [629-50-5]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> <u>1976</u> , 4, 269-80.												
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T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L										
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Tetradecane; C<sub>14</sub>H<sub>30</sub>; [629-59-4]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Makranczy, J.; Megyery-Balog, K.; Rusz, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> <u>1976</u>, <i>4</i>, 269-80.</p>												
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Pentadecane; C <sub>15</sub> H <sub>32</sub> ; [629-62-9]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Ruzs, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> <u>1976</u> , <i>4</i> , 269-80.												
<b>VARIABLES:</b> T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> S. A. Johnson H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="273 505 977 672" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Mol Fraction <math>X_1 \times 10^3</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="border-bottom: 1px solid black;">298.15</td> <td style="border-bottom: 1px solid black;">1.72</td> <td style="border-bottom: 1px solid black;">0.139</td> <td style="border-bottom: 1px solid black;">0.152</td> </tr> <tr> <td style="border-bottom: 1px solid black;">313.15</td> <td style="border-bottom: 1px solid black;">1.38</td> <td style="border-bottom: 1px solid black;">0.110</td> <td style="border-bottom: 1px solid black;">0.126</td> </tr> </tbody> </table> <p>The mole fraction solubilities and the Bunsen coefficients were calculated by the compiler.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -11,398 + 91.15 T</math>.</p> <p>The data and the equation are classed as tentative.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	1.72	0.139	0.152	313.15	1.38	0.110	0.126
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hexadecane; C <sub>16</sub> H <sub>34</sub> ; [544-76-3]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Megyery-Balog, K.; Ruzs, L.; Patyi, L. <i>Hung. J. Ind. Chem.</i> <u>1976</u> , 4, 269-80.												
<b>VARIABLES:</b> T/K = 298.15 - 313.15 P/kPa = 101.325	<b>PREPARED BY:</b> S. A. Johnson H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="284 501 985 662" style="margin: 10px auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>1.74</td> <td>0.133</td> <td>0.145</td> </tr> <tr> <td>313.15</td> <td>1.38</td> <td>0.104</td> <td>0.119</td> </tr> </tbody> </table> <p>The mole fraction solubilities and the Bunsen coefficients were calculated by the compiler.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -11,996 + 93.06 T</math></p> <p>The data and the equation are classes as tentative.</p>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	298.15	1.74	0.133	0.145	313.15	1.38	0.104	0.119
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L										
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<b>REFERENCES:</b> 1. Bodor, E.; Bor, Gy., Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , 1, 55. <i>Chem. Abstr.</i> <u>1961</u> , 55, 3157h.													

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Alkanes; C<sub>7</sub>H<sub>16</sub>, C<sub>8</sub>H<sub>18</sub>, C<sub>10</sub>H<sub>22</sub></p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Ijams, C. C.</p> <p>Ph. D. thesis, 1941, Vanderbilt University, Nashville, TN</p>																																				
<p>VARIABLES:</p> <p>T/K= 298.15</p> <p>P/kPa= 101.325</p>	<p>PREPARED BY:</p> <p>H.L. Clever</p>																																				
<p>EXPERIMENTAL VALUES:</p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^3</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Heptane; C<sub>7</sub>H<sub>16</sub>; [142-82-5]</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">1.99</td> <td style="text-align: center;">0.303</td> <td style="text-align: center;">0.331</td> </tr> <tr> <td colspan="4" style="text-align: center;">Octane; C<sub>8</sub>H<sub>18</sub>; [111-65-9]</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">2.08</td> <td style="text-align: center;">0.286</td> <td style="text-align: center;">0.312</td> </tr> <tr> <td colspan="4" style="text-align: center;">2,2,4-Trimethylpentane or isooctane; C<sub>8</sub>H<sub>18</sub>; [540-84-1]</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">2.43</td> <td style="text-align: center;">0.329</td> <td style="text-align: center;">0.359</td> </tr> <tr> <td colspan="4" style="text-align: center;">Decane; C<sub>10</sub>H<sub>22</sub>; [124-18-5]</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">2.13</td> <td style="text-align: center;">0.244</td> <td style="text-align: center;">0.266</td> </tr> </tbody> </table> <p>The mole fraction and Ostwald coefficient values were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	Heptane; C <sub>7</sub> H <sub>16</sub> ; [142-82-5]				298.15	1.99	0.303	0.331	Octane; C <sub>8</sub> H <sub>18</sub> ; [111-65-9]				298.15	2.08	0.286	0.312	2,2,4-Trimethylpentane or isooctane; C <sub>8</sub> H <sub>18</sub> ; [540-84-1]				298.15	2.43	0.329	0.359	Decane; C <sub>10</sub> H <sub>22</sub> ; [124-18-5]				298.15	2.13	0.244	0.266
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>A Van Slyke-Neill Manometric Apparatus manufactured by the Eimer and Amend Co. was used.</p> <p>The procedure of Van Slyke (1) for pure liquids was modified so that small solvent sample (2 cm<sup>3</sup>) could be used with almost 100 per cent recovery of the solvent.</p> <p>An improved temperature control system was used.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Air Reduction Co. Purity 99.5 per cent.</p> <p>(2) Alkanes. Purified. Vapor pressure and boiling point also reported in the thesis.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = 0.05</math></p> <p>REFERENCES:</p> <p>1. Van Slyke, D. D. <i>J. Biol. Chem.</i> 1939, 130, 545.</p>																																				

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Blanc, C; Batiste, M.	
(2) n-Alkanes (C <sub>7</sub> -C <sub>18</sub> )		Bull. Centr. Rech. Pan. 1970,4, 235-41. Chem. Abstr. 1973, 79, 108564g.	
VARIABLES:		PREPARED BY:	
T/K = 303 P/kPa = 101		R. Battino	
EXPERIMENTAL VALUES:			
Solvent	10 <sup>5</sup> C <sub>p</sub> <sup>a</sup> /g cm <sup>-3</sup>	10 <sup>2</sup> L <sup>b</sup>	10 <sup>2</sup> β <sup>c</sup> /cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>
t/°C = 30			
n-C <sub>7</sub> H <sub>16</sub>	44.64	34.67	31.24
n-C <sub>8</sub> H <sub>18</sub>	38.15	29.63	26.70
n-C <sub>9</sub> H <sub>20</sub>	36.45	28.31	25.51
n-C <sub>10</sub> H <sub>22</sub>	31.15	24.19	21.80
n-C <sub>11</sub> H <sub>24</sub>	30.87	23.97	21.60
n-C <sub>12</sub> H <sub>26</sub>	30.10	23.38	21.07
n-C <sub>13</sub> H <sub>28</sub>	28.27	21.95	19.78
n-C <sub>14</sub> H <sub>30</sub>	26.66	20.71	19.66
<sup>a</sup> Solubility in g O <sub>2</sub> /cm <sup>3</sup> solvent at 101.325 kPa partial pressure of gas. <sup>b</sup> Ostwald coefficient. <sup>c</sup> Bunsen coefficient.			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
The apparatus is described in the paper and uses a manometric-volumetric technique.		No details given.	
		ESTIMATED ERROR:	
		δL/L = ±0.01, authors' estimate.	
		REFERENCES:	

COMPONENTS:		ORIGINAL MEASUREMENTS:	
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(2) n-Alkanes (C <sub>7</sub> -C <sub>18</sub> )		<i>Bull. Centr. Rech. Pan.</i> 1970, 4, 235-41	
		<i>Chem. Abstr.</i> 1973, 79, 108564g	
EXPERIMENTAL VALUES:			
continued			
Solvent	10 <sup>5</sup> C <sub>p</sub> <sup>a</sup> /g cm <sup>-3</sup>	10 <sup>2</sup> L <sup>b</sup>	10 <sup>2</sup> β <sup>c</sup> /cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>
t/°C = 30			
n-C <sub>15</sub> H <sub>32</sub>	26.00	20.20	18.20
n-C <sub>16</sub> H <sub>34</sub>	25.28	19.63	17.69
n-C <sub>17</sub> H <sub>36</sub>	23.88	18.54	16.71
n-C <sub>18</sub> H <sub>38</sub>	23.00	17.87	16.10

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Cyclic hydrocarbons; C <sub>6</sub> H <sub>10</sub> and C <sub>6</sub> H <sub>12</sub>	<b>ORIGINAL MEASUREMENTS:</b> Guerry, D. Jr.  Ph.D. thesis, 1944, Vanderbilt University, Nashville, TN.																												
<b>VARIABLES:</b> T/K = 293.15, 298.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse; margin-top: 10px;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^4</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Cyclohexene; C<sub>6</sub>H<sub>10</sub>; [110-83-8]</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">10.4</td> <td style="text-align: center;">0.231</td> <td style="text-align: center;">0.248</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">10.4</td> <td style="text-align: center;">0.229</td> <td style="text-align: center;">0.250</td> </tr> <tr> <td colspan="4" style="text-align: center;">Cyclohexane; C<sub>6</sub>H<sub>12</sub>; [110-82-7]</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">12.1</td> <td style="text-align: center;">0.252</td> <td style="text-align: center;">0.270</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">12.3</td> <td style="text-align: center;">0.255</td> <td style="text-align: center;">0.278</td> </tr> </tbody> </table> <p style="margin-top: 10px;">The Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	Cyclohexene; C <sub>6</sub> H <sub>10</sub> ; [110-83-8]				293.15	10.4	0.231	0.248	298.15	10.4	0.229	0.250	Cyclohexane; C <sub>6</sub> H <sub>12</sub> ; [110-82-7]				293.15	12.1	0.252	0.270	298.15	12.3	0.255	0.278
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<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air reduction Co. Purity 99.5 per cent.  (2) Hydrocarbons. Both were Eastman Kodak Co. products. They were purified by standard methods, and distilled from Na in a nitrogen atm.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$  <b>REFERENCES:</b> 1. Van Slyke, D. D. <i>J. Biol. Chem.</i> <u>1939</u> , <i>130</i> , 545.  2. Ijams, C. C. Ph.D. thesis, <u>1941</u> Vanderbilt University																												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Cyclohexane; C <sub>6</sub> H <sub>12</sub> ; [110-82-7]	<b>ORIGINAL MEASUREMENTS:</b> Wilhelm, E.; Battino, R. <i>J. Chem. Thermodyn.</i> <u>1973</u> , <i>5</i> , 117-20.																																																			
<b>VARIABLES:</b> T/K = 283.47 - 313.06 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																																																			
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="306 487 974 776"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>283.47</td><td>1.248</td><td>0.262</td><td>0.272</td></tr> <tr><td>283.49</td><td>1.239</td><td>0.260</td><td>0.270</td></tr> <tr><td>283.64</td><td>1.243</td><td>0.261</td><td>0.271</td></tr> <tr><td>297.51</td><td>1.245</td><td>0.257</td><td>0.280</td></tr> <tr><td>297.57</td><td>1.245</td><td>0.255</td><td>0.280</td></tr> <tr><td>310.14</td><td>1.252</td><td>0.255</td><td>0.289</td></tr> <tr><td>310.38</td><td>1.234</td><td>0.251</td><td>0.285</td></tr> <tr><td>313.06</td><td>1.274</td><td>0.258</td><td>0.296</td></tr> </tbody> </table> <p>The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = 236.7 + 54.798 T</math>            Std. Dev. <math>\Delta G^\circ = 22.3</math>, Coef. Corr. = 0.9992  <math>\Delta H^\circ/\text{J mol}^{-1} = 236.7</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -54.798</math></p> <table border="1" data-bbox="446 991 924 1193"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>283.15</td><td>1.242</td><td>15,753</td></tr> <tr><td>293.15</td><td>1.246</td><td>16,301</td></tr> <tr><td>303.15</td><td>1.250</td><td>16,849</td></tr> <tr><td>313.15</td><td>1.254</td><td>17,397</td></tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	283.47	1.248	0.262	0.272	283.49	1.239	0.260	0.270	283.64	1.243	0.261	0.271	297.51	1.245	0.257	0.280	297.57	1.245	0.255	0.280	310.14	1.252	0.255	0.289	310.38	1.234	0.251	0.285	313.06	1.274	0.258	0.296	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	283.15	1.242	15,753	293.15	1.246	16,301	303.15	1.250	16,849	313.15	1.254	17,397
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<b>METHOD APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Products & Chemicals Co. Minimum purity 99.6 mole per cent. (2) Cyclohexane. Phillips Petroleum Co. Pure Grade. Distilled.																																																			
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.005$																																																				
<b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> 1948, 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> 1968, <i>45</i> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> 1971, <i>43</i> , 806.																																																				

<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> [7782-44-7] (2) Cyclohexane; C <sub>6</sub> H <sub>12</sub> ; [110-82-7]	<b>ORIGINAL MEASUREMENTS:</b>  Wild, J. D.; Sridhar, T.; Potter, O.E. <i>Chem. Eng. J.</i> <u>1978</u> , <i>15</i> , 209-14.																																																												
<b>VARIABLES:</b>  T/K = 293-371 P/kPa = 0-1206	<b>PREPARED BY:</b>  R. Battino																																																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="168 466 1072 809"> <thead> <tr> <th>T/°C</th> <th>T<sup>a</sup>/K</th> <th>P<sup>b</sup>/lb in<sup>-2</sup></th> <th>10<sup>3</sup>x<sub>1</sub><sup>c</sup></th> <th>H<sup>a,d</sup></th> </tr> </thead> <tbody> <tr><td>39</td><td>312.2</td><td>175</td><td>1.217</td><td>822</td></tr> <tr><td>39</td><td>312.2</td><td>156</td><td>1.205</td><td>930</td></tr> <tr><td>59</td><td>332.2</td><td>150</td><td>1.231</td><td>912</td></tr> <tr><td>71</td><td>344.2</td><td>135</td><td>1.25</td><td>900</td></tr> <tr><td>79</td><td>352.2</td><td>112</td><td>1.263</td><td>792</td></tr> <tr><td>80</td><td>353.2</td><td>165</td><td>1.263</td><td>792</td></tr> <tr><td>98</td><td>371.2</td><td>150</td><td>1.277</td><td>793</td></tr> <tr><td>20</td><td>293.2</td><td>0<sup>e</sup></td><td>1.16</td><td>862</td></tr> <tr><td>36</td><td>309.2</td><td>0<sup>e</sup></td><td>1.21</td><td>826</td></tr> <tr><td>47</td><td>320.2</td><td>0<sup>e</sup></td><td>1.2</td><td>833</td></tr> <tr><td>58</td><td>331.2</td><td>0<sup>e</sup></td><td>1.26</td><td>794</td></tr> </tbody> </table> <p data-bbox="151 829 1142 1103"> <sup>a</sup> Calculated by compiler.  <sup>b</sup> Gage pressure. Original table titled "pressure range".  <sup>c</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.  <sup>d</sup> Henry's law coefficient; x<sub>1</sub> = H(P/atm).  <sup>e</sup> Determined by a gas chromatographic method.  <sup>f</sup> log<sub>10</sub> x<sub>1</sub> = 0.366 log<sub>10</sub> (T/K) - 3.8385; authors' smoothing equation.  <sup>g</sup> In original paper table and equation mistakenly have H for x<sub>1</sub>.         </p>		T/°C	T <sup>a</sup> /K	P <sup>b</sup> /lb in <sup>-2</sup>	10 <sup>3</sup> x <sub>1</sub> <sup>c</sup>	H <sup>a,d</sup>	39	312.2	175	1.217	822	39	312.2	156	1.205	930	59	332.2	150	1.231	912	71	344.2	135	1.25	900	79	352.2	112	1.263	792	80	353.2	165	1.263	792	98	371.2	150	1.277	793	20	293.2	0 <sup>e</sup>	1.16	862	36	309.2	0 <sup>e</sup>	1.21	826	47	320.2	0 <sup>e</sup>	1.2	833	58	331.2	0 <sup>e</sup>	1.26	794
T/°C	T <sup>a</sup> /K	P <sup>b</sup> /lb in <sup>-2</sup>	10 <sup>3</sup> x <sub>1</sub> <sup>c</sup>	H <sup>a,d</sup>																																																									
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<b>METHOD/APPARATUS/PROCEDURE:</b>  Details of the method are given in reference (1). Air was introduced into a reactor containing one gallon of cyclohexane and brought to the desired pressure. Equilibrium was approached from above and below the pressure. The oxygen in the solution was analyzed using the pyrogallol absorption method. A gas chromatographic method was also used.	<b>SOURCE AND PURITY OF MATERIALS:</b>  (1) "High purity medical grade." (2) Distilled to a final boiling point of 80.7°C and refractive index of 1.4261.																																																												
<b>ESTIMATED ERROR:</b>  $\delta x_1 / x_1 = \pm 0.02$ , compiler's estimate $\delta T/K = \pm 0.5$																																																													
<b>REFERENCES:</b>  1. Wild, J.D. "Gas Absorption With Chemical Reaction," Ph.D. Thesis, Monash University, Clayton, Victoria, Australia <u>1968</u> .																																																													



<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Methylcyclohexane; C<sub>7</sub>H<sub>14</sub>; [108-87-2]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Field, L. R.; Wilhelm, E.; Battino, R.</p> <p><i>J. Chem. Thermodyn.</i> <u>1974</u>, <i>6</i>, 237-43.</p>																															
<p>VARIABLES:</p> <p>T/K = 284.15 - 313.26</p> <p>P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>H. L. Clever</p>																															
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) <i>cis</i> -1,3-Dimethylcyclohexane, 59 mol %; C <sub>8</sub> H <sub>16</sub> ; [638-04-0] (3) <i>trans</i> -1,3-Dimethylcyclohexane, 41 mol %; C <sub>8</sub> H <sub>16</sub> ; [2207-03-6]	<b>ORIGINAL MEASUREMENTS:</b> Geller, E. B.; Battino, R.; Wilhelm, E. <i>J. Chem. Thermodyn.</i> <u>1976</u> , <i>8</i> , 197-202.												
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COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) <i>trans</i> -1,2-Dimethylcyclohexane; C <sub>8</sub> H <sub>16</sub> ; [6876-23-9]	ORIGINAL MEASUREMENTS: Geller, E. B.; Battino, R.; Wilhelm, E.  <i>J. Chem. Thermodyn.</i> <u>1976</u> , <i>8</i> , 197-202.
VARIABLES: T/K = 298.11 - 313.05 P/kPa = 101.325	PREPARED BY: H. L. Clever A. L. Cramer

## EXPERIMENTAL VALUES:

T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L
298.11	1.734	0.2678	0.2923
313.05	1.705	0.2594	0.2973

The Bunsen coefficients were calculated by the compiler.

The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.

Smoothed Data: The Gibbs energy equation is based on only two pair of points and should be used with caution.

$$\Delta G^{\circ}/\text{J mol}^{-1} = -RT \ln X_1 = -878.35 + 55.803 T$$

$$\Delta H^{\circ}/\text{J mol}^{-1} = -878.35, \Delta S^{\circ}/\text{J K}^{-1} \text{ mol}^{-1} = -55.803$$

## AUXILIARY INFORMATION

## METHOD/APPARATUS/PROCEDURE:

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## SOURCE AND PURITY OF MATERIALS:

- (1) Oxygen. Either Air Products & Chemicals Inc., or Matheson Co., Inc. 99 mol per cent or better.
- (2) *trans*-1,2-Dimethylcyclohexane. Chemical samples Co. Fractionally distilled and stored in dark. Refractive index (NaD, 298.15 K) 1.4248.

## ESTIMATED ERROR:

$$\begin{aligned} \delta T/K &= 0.03 \\ \delta P/\text{mmHg} &= 0.5 \\ \delta X_1/X_1 &= 0.005 \end{aligned}$$

## REFERENCES:

1. Morrison, T. J.; Billett, F. *J. Chem. Soc.* 1948, 2033.
2. Battino, R.; Evans, F. D.; Danforth, W. F. *J. Am. Oil Chem. Soc.* 1968, *45*, 830.
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) <i>cis</i> -1,4-Dimethylcyclohexane, 70 mol %; C <sub>8</sub> H <sub>16</sub> ; [624-29-3] (3) <i>trans</i> -1,4-Dimethylcyclohexane, 30 mol %; C <sub>8</sub> H <sub>16</sub> ; [2207-04-7]	<b>ORIGINAL MEASUREMENTS:</b> Geller, E. B.; Battino, R.; Wilhelm, E. <i>J. Chem. Thermodyn.</i> <u>1976</u> , <i>8</i> , 197-202.												
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Cyclooctane; C <sub>8</sub> H <sub>16</sub> ; [292-64-8]	<b>ORIGINAL MEASUREMENTS:</b> Wilcock, R. J.; Battino, R.; Wilhelm, E. <i>J. Chem. Thermodyn.</i> <u>1977</u> , <i>9</i> , 111-5.																																					
<b>VARIABLES:</b> T/K = 289.18 - 313.53 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever A. L. Cramer																																					
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="317 473 988 642"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>289.18</td> <td>1.105</td> <td>0.1852</td> <td>0.1961</td> </tr> <tr> <td>298.26</td> <td>1.072</td> <td>0.1782</td> <td>0.1946</td> </tr> <tr> <td>313.53</td> <td>1.088</td> <td>0.1782</td> <td>0.2046</td> </tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler.            The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.            Smoothed Data: <math>\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -15.78 + 56.783 T</math>            Std. Dev. <math>\Delta G^{\circ} = 36.45</math>, Coef. Corr. = 0.9993  <math>\Delta H^{\circ}/J \text{ mol}^{-1} = -15.78</math>, <math>\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -56.783</math></p> <table border="1" data-bbox="415 860 896 1109"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^{\circ}/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>288.15</td> <td>1.089</td> <td>16,346</td> </tr> <tr> <td>293.15</td> <td>1.088</td> <td>16,630</td> </tr> <tr> <td>298.15</td> <td>1.088</td> <td>16,914</td> </tr> <tr> <td>303.15</td> <td>1.088</td> <td>17,198</td> </tr> <tr> <td>308.15</td> <td>1.088</td> <td>17,482</td> </tr> <tr> <td>313.15</td> <td>1.088</td> <td>17,766</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	289.18	1.105	0.1852	0.1961	298.26	1.072	0.1782	0.1946	313.53	1.088	0.1782	0.2046	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$	288.15	1.089	16,346	293.15	1.088	16,630	298.15	1.088	16,914	303.15	1.088	17,198	308.15	1.088	17,482	313.15	1.088	17,766
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Products and Chemicals Co. Minimum purity 99.6 mol per cent. (2) Cyclooctane. Chemical Samples Co. 99 mol percent, distilled, refractive index (NaD, 298.15 K) 1.4562. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.3$ $\delta X_1/X_1 = 0.005$ <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u> , 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u> , <i>45</i> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , <i>43</i> , 806.																																					

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	EVALUATOR: Rubin Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.
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## CRITICAL EVALUATION:

The solubility of oxygen in benzene was determined by five workers (1-5). Only three of these were of sufficient consistency to smooth. We used 16 data points for the smoothing and they were obtained as follows (reference-number of data points used from that reference): 1-3, 2-6, 5-7. The fitting equation used was:

$$\ln x_1 = A + B/(T/100K) + C \ln (T/100K) \quad (1)$$

The least squares fit for the 16 points gave

$$\ln x_1 = -13.90754 + 8.741567/(T/100K) + 3.530241 \ln (T/100K) \quad (2)$$

where  $x_1$  is the mole fraction solubility at 101.325 kPa partial pressure of gas. The fit in the mole fraction was to  $\pm 0.60 \times 10^{-5}$  or  $\pm 0.71$  per cent at the middle of the temperature range. Table 1 gives smoothed values of the mole fraction at 101.325 kPa partial pressure of the gas and the Ostwald coefficients at 5K intervals.

Table 1 also gives the thermodynamic functions  $\Delta\bar{G}_1^\circ$ ,  $\Delta\bar{H}_1^\circ$ , and  $\Delta\bar{S}_1^\circ$  for the transfer of gas from the vapor phase at 101.325 kPa partial pressure to the (hypothetical) solution phase of unit mole fraction. These thermodynamic properties were calculated from the smoothing equation according to the following equations:

$$\Delta\bar{G}_1^\circ = -RAT - 100RB - RCT \ln(T/100) \quad (3)$$

$$\Delta\bar{S}_1^\circ = RA + RC \ln(T/100) + RC \quad (4)$$

$$\Delta\bar{H}_1^\circ = -100RB + RCT \quad (5)$$

$$\Delta\bar{Cp}_1^\circ = RC \quad (6)$$

The  $\Delta\bar{Cp}_1^\circ$  value was constant at  $29.4 \text{ J mol}^{-1} \text{ K}^{-1}$ .

Morgan and Pyne's (3) single value and Naumenko, et al.'s (4), single value were not used since they deviated by about three standard deviations from the smoothed line. There is no apparent reason for this.

TABLE 1. Smoothed values of the solubility of oxygen in benzene, and thermodynamic functions at 5K intervals using equation 2 at 101.325 kPa partial pressure of gas.

T/K	$10^4 x_1^a$	$L^b$	$\Delta\bar{G}_1^\circ / \text{kJ mol}^{-1}$	$\Delta\bar{H}_1^\circ / \text{kJ mol}^{-1}$	$\Delta\bar{S}_1^\circ / \text{J mol}^{-1}$
283.15	7.88	0.209	16.82	1.04	-55.7
288.15	7.95	0.213	17.10	1.19	-55.2
293.15	8.02	0.217	17.38	1.34	-54.7
298.15	8.10	0.222	17.65	1.48	-54.2
303.15	8.18	0.226	17.92	1.63	-53.7
308.15	8.27	0.231	18.18	1.78	-53.2
313.15	8.37	0.236	18.45	1.92	-52.8
318.15	8.47	0.241	18.71	2.07	-52.3
323.15	8.57	0.247	18.97	2.22	-51.9
328.15	8.69	0.252	19.23	2.36	-51.4
333.15	8.80	0.258	19.49	2.51	-51.0
338.15	8.93	0.264	19.74	2.66	-50.5
343.15	9.05	0.269	19.99	2.80	-50.1

<sup>a</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.

<sup>b</sup> Ostwald coefficient.

continued on following page

COMPONENTS:  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	EVALUATOR:  Rubin Battino Department of Chemistry Wright State University Dayton, OH 45435 U.S.A.
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CRITICAL EVALUATION:

continued

References

1. Byrne, J.E.; Battino, R.; Danforth, W.F. *J. Chem. Thermodyn.* 1974, *6*, 245-50.
2. Horiuchi, J. *Sci. Papers Inst. Phys. Chem. Research (Tokyo)* 1931, *17*, 125-256.
3. Morgan, J.L.R.; Pyne, H.R. *J. Phys. Chem.* 1930, *34*, 2045-8.
4. Naumenko, N.K.; Mukhin, N.N.; Aleskovskii, V.B. *Zh. Prikl. Khim. (Leningrad)* 1969, *42*, 2522-8.
5. Schläpfer, P.; Audykowski, T.; Bukowiecki, A. *Schweiz. Arch. Angew. Wiss. Tech.* 1949, *15*, 299-307.



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	<b>ORIGINAL MEASUREMENTS:</b> Morgan, J.L.R.; Pyne, H.R. <i>J. Phys. Chem.</i> <u>1930</u> , 34, 2045-8.		
<b>VARIABLES:</b> T/K = 298	<b>PREPARED BY:</b> R. Battino		
<b>EXPERIMENTAL VALUES:</b>			
t/°C 25	T/K <sup>a</sup> 298.15	L <sup>b</sup> 0.2076 0.2079 0.2146 0.2077 0.2051 0.2037 0.2030 0.2100 0.2062	10 <sup>4</sup> x <sub>1</sub> <sup>a,c</sup> 7.581
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Ostwald coefficient.</p> <p><sup>c</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas. Calculated from average value of L of 0.2079 with a standard deviation of <u>+0.0031</u>.</p>			
<b>AUXILIARY INFORMATION</b>			
<b>METHOD/APPARATUS/PROCEDURE:</b> Used the apparatus of Morgan and Pyne (1). A method is used whereby a rocking beam connected to mercury reservoirs and pumping bulbs pumps gas through previously degassed liquid. After equilibration the gas uptake is read on attached burets. The apparatus is all glass.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From an electrolytically prepared supply and passed over a heated spiral of copper oxide before use. (2) Merck. Distilled to a boiling point of 80.4°C.		
<b>ESTIMATED ERROR:</b> δL/L = ±0.02, compiler's estimate			
<b>REFERENCES:</b> 1. Morgan, J.L.R.; Pyne, H.R. <i>J. Phys. Chem.</i> , <u>1930</u> , 34, 1573-82.			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	<b>ORIGINAL MEASUREMENTS:</b> Horiuti, J. <i>Sci. Papers Inst. Phys. Chem. Res.</i> (Tokyo) (Jpn) <u>1931/32</u> , 17, 125-256.																																																											
<b>VARIABLES:</b> T/K = 283.15 - 333.15 Total P/kPa = 101.325	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever																																																											
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="326 466 997 682"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> x 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>283.15</td><td>0.7897</td><td>0.2017</td><td>0.2091</td></tr> <tr><td>293.15</td><td>0.8070</td><td>0.2037</td><td>0.2186</td></tr> <tr><td>303.15</td><td>0.8241</td><td>0.2055</td><td>0.2281</td></tr> <tr><td>313.15</td><td>0.8394</td><td>0.2068</td><td>0.2371</td></tr> <tr><td>323.15</td><td>0.8626</td><td>0.2099</td><td>0.2483</td></tr> <tr><td>333.15</td><td>0.8788</td><td>0.2112</td><td>0.2576</td></tr> </tbody> </table> <p>Smoothed Data: <math>\ln X_1 = -9.95246 + 3.0634/(T/100) + 1.6593 \ln (T/100)</math></p> <p>Standard error about the regression line = <math>1.96 \times 10^{-6}</math></p> <table border="1" data-bbox="238 795 1080 936"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> x 10<sup>3</sup></th> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> x 10<sup>3</sup></th> </tr> </thead> <tbody> <tr><td>283.15</td><td>0.7899</td><td>313.15</td><td>0.8417</td></tr> <tr><td>293.15</td><td>0.8065</td><td>323.15</td><td>0.8603</td></tr> <tr><td>303.15</td><td>0.8237</td><td>333.15</td><td>0.8796</td></tr> </tbody> </table> <p>If the gas and solution are assumed to be ideal the fitted equation gives the following thermodynamic values.</p> <table border="1" data-bbox="176 1007 1150 1103"> <thead> <tr> <th>T/K</th> <th><math>\Delta G^\circ/\text{kJ mol}^{-1}</math></th> <th><math>\Delta H^\circ/\text{J mol}^{-1}</math></th> <th><math>\Delta S^\circ/\text{J K}^{-1} \text{mol}^{-1}</math></th> <th><math>\Delta C_p^\circ/\text{J K}^{-1} \text{mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>273.15</td><td>16.817</td><td>1359</td><td>-54.59</td><td>13.80</td></tr> <tr><td>298.15</td><td>17.631</td><td>1566</td><td>-53.88</td><td>13.80</td></tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	283.15	0.7897	0.2017	0.2091	293.15	0.8070	0.2037	0.2186	303.15	0.8241	0.2055	0.2281	313.15	0.8394	0.2068	0.2371	323.15	0.8626	0.2099	0.2483	333.15	0.8788	0.2112	0.2576	T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	283.15	0.7899	313.15	0.8417	293.15	0.8065	323.15	0.8603	303.15	0.8237	333.15	0.8796	T/K	$\Delta G^\circ/\text{kJ mol}^{-1}$	$\Delta H^\circ/\text{J mol}^{-1}$	$\Delta S^\circ/\text{J K}^{-1} \text{mol}^{-1}$	$\Delta C_p^\circ/\text{J K}^{-1} \text{mol}^{-1}$	273.15	16.817	1359	-54.59	13.80	298.15	17.631	1566	-53.88	13.80
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus consists of a gas buret, a solvent reservoir, and an absorption pipet. The volume of the pipet was determined at various meniscus heights by weighing a quantity of water. The meniscus height was read with a cathetometer.</p> <p>The dry gas introduced into the degassed solvent. The gas and solvent are mixed with a magnetic stirrer until saturation. Care taken to prevent solvent vapor from mixing with the solute gas in the gas buret. The volume of gas was determined from a gas buret reading, the volume of the solvent was determined from the meniscus height in the absorption pipet.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Prepared in the laboratory by heating potassium permanganate (Kahlbaum). Gas fractionated in liquid air. (2) Benzene. Merck. Extra pure, free from sulfur sample refluxed with sodium amalgam. Normal boiling point 80.18°C.																																																											
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ <p>The Ostwald coefficient was measured at a total pressure of one atm. The Bunsen coefficient and the mole fraction solubility values were calculated by the compiler for a gas pressure of one atm assuming the gas to behave ideally and the Ostwald coefficient to be independent of pressure.</p>																																																												

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Benzene; C<sub>6</sub>H<sub>6</sub>; [71-43-2]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Schl�pfer, P.; Audykowski, T.; Bukowiecki, A.</p> <p>Schweiz. Arch. Angew. Wiss. Tech. 1949, 15, 299-307.</p>																								
<p>VARIABLES:</p> <p>T/K = 283 - 343</p>	<p>PREPARED BY:</p> <p>R. Battino</p>																								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="484 493 822 761"> <thead> <tr> <th>t/°C</th> <th>T<sup>a</sup>/K</th> <th>L<sup>b</sup></th> </tr> </thead> <tbody> <tr><td>10</td><td>283</td><td>0.206</td></tr> <tr><td>20</td><td>293</td><td>0.219</td></tr> <tr><td>30</td><td>303</td><td>0.226</td></tr> <tr><td>40</td><td>313</td><td>0.234</td></tr> <tr><td>50</td><td>323</td><td>0.245</td></tr> <tr><td>60</td><td>333</td><td>0.256</td></tr> <tr><td>70</td><td>343</td><td>0.271</td></tr> </tbody> </table> <p>a Calculated by compiler.</p> <p>b Ostwald coefficient.</p>		t/°C	T <sup>a</sup> /K	L <sup>b</sup>	10	283	0.206	20	293	0.219	30	303	0.226	40	313	0.234	50	323	0.245	60	333	0.256	70	343	0.271
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<p>AUXILIARY INFORMATION</p>																									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The solvent was saturated with air and the dissolved oxygen determined iodimetrically.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) From air.</p> <p>(2) Specific gravity of 0.879 g cm<sup>-3</sup> at 20°C.</p> <p>ESTIMATED ERROR:</p> <p>δL/L = ±0.025, authors' estimate.</p> <p>REFERENCES:</p>																								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	<b>ORIGINAL MEASUREMENTS:</b> Byrne, J. E.; Battino, R.; Danforth, W. F. <i>J. Chem. Thermodyn.</i> <u>1974</u> , <i>6</i> , 245-50.
<b>VARIABLES:</b> T/K = 310.59 - 310.66 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever

**EXPERIMENTAL VALUES:**

T/K	Mol Fraction X <sub>1</sub> x 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L
310.59	0.847	0.2092	0.2379
310.61	0.836	0.2066	0.2349
310.64	0.828	0.2045	0.2326
310.66	0.825	0.2038	0.2318

The Bunsen coefficients and mol fraction solubilities were calculated by the compiler.

**AUXILIARY INFORMATION****METHOD/APPARATUS/PROCEDURE:**

The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3).

Degassing. Up to 500 cm<sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N<sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns.

Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.

**SOURCE AND PURITY OF MATERIALS:**

- (1) Oxygen. Air Products & Chemicals Co. Minimum purity 99.6 mole per cent.
- (2) Benzene. Baker Analyzed Reagent Grade. Thiophene free, 99.9 mol per cent.

**ESTIMATED ERROR:**

$$\begin{aligned}\delta T/K &= 0.03 \\ \delta P/\text{mmHg} &= 0.5 \\ \delta X_1/X_1 &= 0.005\end{aligned}$$

**REFERENCES:**

1. Morrison, T. J.; Billett, F. *J. Chem. Soc.* 1948, 2033.
2. Battino, R.; Evans, F. D.; Danforth, W. F. *J. Am. Oil Chem. Soc.* 1968, *45*, 830.
3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. *Anal. Chem.* 1971, *43*, 806.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2] Methylbenzene or toluene; C <sub>7</sub> H <sub>8</sub> ; [108-88-3]	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim. (Leningrad)</i> <u>1969</u> , 42, 2522-8. <i>J. Appl. Chem. USSR</i> <u>1969</u> , 42, 2376-81.																				
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																				
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<b>VARIABLES:</b> T/K = 293.71 - 313.20 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever

<b>EXPERIMENTAL VALUES:</b>					
T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L		
293.71	0.922	0.1898	0.2041		
309.69	0.909	0.1841	0.2087		
313.20	0.960	0.1991	0.2283		
The gas solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.					
The Bunsen coefficients were calculated by the compiler.					
Smoothed Data: $\Delta G^\circ / J \text{ mol}^{-1} = -RT \ln X_1 = 894.6 + 55.105 T$					
Std. Dev. $\Delta G^\circ = 66.5$ , Coef. Corr. = 0.9938					
$\Delta H^\circ / J \text{ mol}^{-1} = 894.6$ , $\Delta S^\circ / J \text{ K}^{-1} \text{ mol}^{-1} = -55.105$					
T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ / J \text{ mol}^{-1}$			
293.15	0.917	17,049			
303.15	0.928	17,600			
313.15	0.938	18,151			

## AUXILIARY INFORMATION

<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is applied intermittently through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Products & Chemicals Co. Minimum purity 99.6 mole per cent. (2) Methylbenzene. Phillips Petroleum. Pure Grade. Distilled.
Solubility Determination. The degassed solvent is passed in a thin film down a glass spiral tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.005$ <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> 1948, 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> 1968, <i>45</i> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> 1971, <i>43</i> , 806.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Aromatic hydrocarbons; C <sub>8</sub> H <sub>10</sub>	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim. (Leningrad) 1969, 42, 2522-8.</i> <i>J. Appl. Chem. 1969, 42, 2376-81.</i>																																				
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<b>VARIABLES:</b> T/K = 303.2 - 353.2	<b>PREPARED BY:</b> R. Battino																																			
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<b>METHOD/APPARATUS/PROCEDURE:</b> The p-xylene is degassed by boiling and passed while hot into a 250 ml Erlenmeyer flask which contains o-xylene saturated oxygen. After equilibrium volume changes are recorded on a buret and the amount of o-xylene in a graduated cylinder. Measurements were carried out at $750 \pm 2$ mm Hg. Henry's Law Constants were calculated from the measurements.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) Enjay 99% pure with impurities being the o- and m-isomers.  <b>ESTIMATED ERROR:</b> $\delta T/T = \pm 0.1$ $\delta$ (Henry's Constant) = $\pm 3\%$ (compiler)  <b>REFERENCES:</b>																																			



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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Alcohols</p>	<p>EVALUATOR:</p> <p>H. L. Clever  Department of Chemistry  Emory University  Atlanta, GA 30322 USA</p> <p>1981, March</p>
<p>CRITICAL EVALUATION:</p> <p style="text-align: center;">An Evaluation of the Mole Fraction Solubility of Oxygen  in Alcohols at an Oxygen Partial Pressure  of 101.325 kPa (1 atm).</p> <p>The solubility measurements evaluated in this section were carried out at an oxygen partial pressure of 200 kPa or less. Most of the measurements were made at a total pressure near 101.325 kPa (1 atm). The mole fraction solubility values are calculated for an oxygen partial pressure of 101.325 kPa assuming the gas is ideal, Henry's constant is obeyed, and the Ostwald coefficient is independent of pressure. The assumptions probably introduce a total error that is smaller than the experimental error of the solubility measurement.</p> <p>Most of the oxygen solubility measurements were made with pure oxygen, but some were made with air at a pressure near 101.325 kPa, which has an oxygen partial pressure of about 21.3 kPa (0.21 atm). Both volumetric methods and chemical methods were used to determine the oxygen dissolved in the saturated solution.</p> <p>Oxygen solubility values from twelve papers are evaluated. Only the results of Carius (1) are rejected. All other solubility values are classed as tentative. The results of Kretschmer, Nowakowska, and Wiebe (6) and Battino <i>et al.</i> (10, 11) are preferred wherever there is a choice.</p> <p>The experimental methods used by the authors of the twelve papers are varied. Carius (1) used the original Bunsen technique. His results are high and should be rejected. Timofeev (2) used the original Ostwald technique. His results compare well with modern values. Metschl (3) saturated the solvent at oxygen pressures up to 456 kPa (4.5 atm). The solubility value he reports is essentially the volume of oxygen "shaken out" of the supersaturated solution as the pressure drops from 202 to 101 kPa (2 to 1 atm). His results appear to have a higher uncertainty than the others. Cauquil (4) used an Ostwald-like technique. Some of her results are doubtful. Ijams (5) used a modified van Slyke method. He carefully applied all corrections but he used a small sample volume which in some cases appears to result in a greater than average uncertainty.</p> <p>Kretschmer, Nowakowska, and Wiebe (6) used the method of Horiuti. Their solvents were well characterized, and the experimental details of the measurement appear to have been carried out carefully. Schlöpfer, Audykowski, and Bukowiecki (7) saturated the solvent with air and determined the dissolved oxygen iodimetrically. When their Ostwald coefficients are recalculated as mole fractions at 101.325 kPa oxygen pressure they compare well with other data at temperatures below 313 K. At higher temperatures their results appear to scatter. Shchukarev and Tolmacheva (8) use a volumetric method. Their results at a temperature of 288 K and below appear more reliable than their results at 298 K and above. Naumenko (9) uses a volumetric method. Battino <i>et al.</i> (10, 11) use a modified Morrison and Billett method. Their solvents are well characterized and the solubility measurement is carried out with care. Makranczy, Rusz, and Balog-Megyery (12) use a volumetric method to measure directly an Ostwald coefficient. In general their results at 298.15 K have appeared to be reliable while results at higher temperatures are not as reliable. (See evaluations in noble gas volumes of the <i>Solubility Series</i>). However, their results for many of the oxygen + alcohol systems they studied tend to be below average values when compared with other workers' results.</p>	

## Oxygen + Methanol [67-56-1]

Kretschmer *et al.* (6) report solubility values at temperatures of 248.15, 273.15, 298.15, and 323.15 K. Makranczy *et al.* (12) report one value at 298.15 K which is 7.5 per cent lower than the Kretschmer *et al.* value. Although both sets of data are classed as tentative, the thermodynamic change and solubility values below are based on a linear regression of the Kretschmer *et al.* data.

The equation for use between 248.15 and 323.15 K is

$$\ln x_1 = -8.2471 + 1.3742/(T/100 \text{ K})$$

with a standard error about the regression line of  $3.67 \times 10^{-6}$ .

The temperature independent thermodynamic changes for the transfer of one mole of oxygen from the gas at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^\circ / \text{kJ mol}^{-1} -1.142 \text{ and } \Delta \bar{S}_1^\circ / \text{J K}^{-1} \text{ mol}^{-1} -68.6$$

The smoothed solubility values and the Gibbs energy of solution are given in Table 1.

Table 1. Solubility of oxygen in methanol at an oxygen partial pressure of 101.325 kPa. Tentative values of mole fraction solubility and partial molar Gibbs energy of solution as a function of temperature.

$T/\text{K}$	Mol Fraction $10^4 x_1$	$\Delta \bar{G}_1^\circ / \text{kJ mol}^{-1}$
253.15	4.51	16.215
263.15	4.42	16.900
273.15	4.33	17.589
283.15	4.26	18.271
293.15	4.19	18.958
298.15	4.15	19.301
303.15	4.12	19.644
313.15	4.06	20.330
323.15	4.01	21.014

## Oxygen + Ethanol [64-17-5]

The solubility of oxygen in ethanol is reported in at least eight papers. The results of Carius (1), a student of R. W. Bunsen, range from 18 per cent at 274 K to 28 per cent at 296 K greater than presently accepted values. The data are rejected.

The mole fraction solubility values at 298.15 K and an oxygen partial pressure of 101.325 kPa from the other papers are given below.

$10^4 x_1$	Reference
4.39	McKranczy <i>et al.</i> (12)
5.10	Metschl (3)
(5.53) <sup>1</sup>	Shchukarev and Tolmacheva (8)
(5.68) <sup>2</sup>	Timofeev (2)
5.74	Naumenko (9)
5.798	Kretschmer <i>et al.</i> (6)
(5.88) <sup>3</sup>	Schläpfer <i>et al.</i> (7)

<sup>1</sup> Extrapolated from the two measurements made at 277.15 and 285.15 K. The experimental value at 298.15 K is  $6.78 \times 10^{-4}$ .

<sup>2</sup> Extrapolated from the seven measurements made between 273.15 and 296.55 K.

<sup>3</sup> Interpolated from the eight measurements made between 273.15 and 343.15 K.

The mole fraction solubility values from the seven papers were compared. In general the higher values were favored if there were no other good reasons for a decision. A linear regression was carried out using the Kretschmer *et al.* data weighted two times; and at a weight of one, the Timofeev data, except the 296.55 K value; the Schläpfer *et al.* data; the Shchukarev and Tolmacheva value at 277.15 K and the Naumenko value. The linear regression of the 24 temperature/solubility pairs gives the equation for use between 248.15 and 343.15 K

$$\ln x_1 = -7.8738 + 1.2693/(T/100 \text{ K})$$

with a standard deviation about the regression line of  $1.13 \times 10^{-5}$ .

The temperature independent thermodynamic changes in enthalpy and entropy for the transfer of one mole of oxygen from the gas at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^\circ / \text{kJ mol}^{-1} -1.055 \text{ and } \Delta \bar{S}_1^\circ / \text{J K}^{-1} \text{ mol}^{-1} -65.5$$

The smoothed solubility values and the Gibbs energy of solution are given in Table 2.

Table 2. Solubility of oxygen in ethanol at an oxygen partial pressure of 101.325 kPa. Tentative values of the mole fraction solubility and partial Gibbs energy of solution as a function of temperature.

$T/\text{K}$	Mol Fraction <sup>1</sup> $10^4 x_1$	$\Delta \bar{G}_1^\circ / \text{kJ mol}^{-1}$
253.15	6.285	15.517
263.15	6.165	16.172
273.15	6.055	16.827
283.15	5.960	17.481
293.15	5.870	18.136
298.15	5.825	18.463
303.15	5.785	18.790
313.15	5.700	19.445
323.15	5.635	20.100
333.15	5.570	20.754
343.15	5.510	21.409

<sup>1</sup> Mole fraction values rounded to the nearest  $0.005 \times 10^{-4}$ .

A definitive study of the oxygen + ethanol system is yet to be carried out. Thus, the data of Table 2 are classed as tentative.

The equation and smoothed data based on the data of Kretschmer *et al.* (see their data sheet) may be an equally satisfactory representation of the system. From the equation based on their data  $\Delta \bar{H}_1^\circ / \text{kJ mol}^{-1}$  is -1.32 and  $\Delta \bar{S}_1^\circ / \text{J K}^{-1} \text{ mol}^{-1}$  is -66.3.

#### Oxygen + 1-Propanol [71-23-8]

Makranczy *et al.* (12) report one solubility value at 298.15 K which is a mole fraction of  $5.03 \times 10^{-4}$ . It is classed as tentative.

#### Oxygen + 2-Propanol [67-63-0]

Only Kretschmer *et al.* (6) have reported solubility measurements on the oxygen + 2-propanol system. A linear regression of their three measurements over the temperature interval of 273.15 to 323.15 K gives the equation

$$\ln x_1 = -7.5774 + 1.2638/(T/100 \text{ K})$$

with a standard error about the regression line of  $9.35 \times 10^{-6}$ .

The temperature independent thermodynamic changes in enthalpy and entropy for the transfer of one mole of oxygen from the gas at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^{\circ}/\text{kJ mol}^{-1} -1.051 \text{ and } \Delta \bar{S}_1^{\circ}/\text{J K}^{-1} \text{ mol}^{-1} -63.0.$$

The smoothed values of the mole fraction solubility and the Gibbs energy are in Table 3.

Table 3. The solubility of oxygen in 2-propanol at an oxygen partial pressure of 101.325 kPa. Tentative values of the mole fraction solubility and partial molar Gibbs energy of solution as a function of temperature.

T/K	Mol Fraction $10^4 x_1$	$\Delta \bar{G}_1^{\circ}/\text{kJ mol}^{-1}$
273.15	8.13	16.158
283.15	8.00	16.788
293.15	7.88	17.418
298.15	7.82	17.733
303.15	7.77	18.048
313.15	7.66	18.678
323.15	7.57	19.308

#### Oxygen + 1-Butanol [71-36-3]

Kretschmer *et al.* (6) report three solubility values at the temperatures 273.15, 298.15 and 323.15 K. Makranczy *et al.* (12) report one value at 298.15 K which is 27 per cent smaller than the Kretschmer *et al.* (6) value. Although both sets of data are classed as tentative, the values of the thermodynamic changes and the solubility values below are based on a linear regression of the Kretschmer *et al.* data.

The equation for use between 273.15 and 323.15 K is

$$\ln x_1 = -7.6234 + 1.4553/(T/100 \text{ K})$$

with a standard error about the regression line of  $8.71 \times 10^{-6}$ .

The temperature independent thermodynamic changes in enthalpy and entropy for the transfer of one mole of oxygen from the gas at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^{\circ}/\text{kJ mol}^{-1} -1.210 \text{ and } \Delta \bar{S}_1^{\circ}/\text{J K}^{-1} \text{ mol}^{-1} -63.4$$

The smoothed values of mole fraction solubility and Gibbs energy of solution are in Table 4.

Table 4. The solubility of oxygen in 1-butanol at an oxygen partial pressure of 101.325 kPa. Tentative values of the mole fraction solubility and partial molar Gibbs energy of solution as a function of temperature.

T/K	Mol Fraction $10^4 x_1$	$\Delta \bar{G}_1^{\circ}/\text{kJ mol}^{-1}$
273.15	8.33	16.103
283.15	8.17	16.737
293.15	8.03	17.371
298.15	7.96	17.688
303.15	7.90	18.005
313.15	7.78	18.322
323.15	7.67	19.292

## Oxygen + 2-methyl-1-propanol [78-83-1]

Only Battino *et al.* (10) have reported data on this system. A linear regression of their eight measurements between 274.09 and 327.96 K gives the equation

$$\ln x_1 = -7.9459 + 2.5735/(T/100 \text{ K})$$

with a standard error about the regression line of  $9.40 \times 10^{-6}$ .

The temperature independent thermodynamic changes in enthalpy and entropy for the transfer of one mole of oxygen from the gas at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^\circ / \text{kJ mol}^{-1} -2.140 \text{ and } \Delta \bar{S}_1^\circ / \text{J K}^{-1} \text{ mol}^{-1} -66.1$$

The smoothed values of the mole fraction solubility and the Gibbs energy are in Table 5.

Table 5. The solubility of oxygen in 2-methyl-1-propanol at an oxygen partial pressure of 101.325 kPa. Tentative values of the mole fraction solubility and partial molar Gibbs energy of solution as a function of temperature.

$T/\text{K}$	Mol Fraction $10^4 x_1$	$\Delta \bar{G}_1^\circ / \text{kJ mol}^{-1}$
273.15	9.08	15.906
283.15	8.79	16.567
293.15	8.52	17.227
298.15	8.395	17.558
303.15	8.28	17.888
313.15	8.05	18.548
323.15	7.85	19.209

## Oxygen + 1-Pentanol [71-41-0]

## Oxygen + 1-Hexanol [111-27-3]

Makranczy *et al.* (12) report one solubility value on each of these systems at 298.15 K. The values are classed as tentative. However, when the values are compared with the solubility values for the other normal alcohols there is reason to suspect these values may be low.

$T/\text{K}$	Alcohol	Mol Fraction $10^4 x_1$
298.15	1-Pentanol	6.30
298.15	1-Hexanol	7.06

## Oxygen + 1-Heptanol [111-70-6]

Both Makranczy *et al.* (12) and Ijams (5) report a single solubility value at 298.15 K. The mole fraction solubility values at 101.325 kPa oxygen partial pressure are

$$\begin{array}{ll} \text{Ijams} & 10.8 \times 10^{-4} \\ \text{Makranczy } et al. & 7.59 \times 10^{-4} \end{array}$$

Although the two values differ by 30 per cent both are classed as tentative. However, in view of the trends in solubility with alcohol carbon number, the Ijams value is preferred.

## Oxygen + 1-Octanol [111-87-5]

The following mole fraction solubility values are reported at 298.15 K and 101.325 kPa oxygen partial pressure

Ijams (5)	$11.5 \times 10^{-4}$
Wilcock <i>et al.</i> (11)	$11.3 \times 10^{-4}$
Makranczy <i>et al.</i> (12)	$11.8 \times 10^{-4}$

The agreement is satisfactory.

Wilcock *et al.* report a second value at 283.35 K.

The tentative values for the system are based on the two determinations by Wilcock *et al.* The equation, based on only two experiments, should be used with caution.

$$\ln x_1 = -7.2357 + 1.3472/(T/100 \text{ K})$$

The temperature independent changes in enthalpy and entropy for the transfer of one mole of oxygen from the gas phase at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^\circ / \text{kJ mol}^{-1} -1.120 \text{ and } \Delta \bar{S}_1^\circ / \text{J K}^{-1} \text{ mol}^{-1} -60.2$$

The smoothed values of the mole fraction solubility and the Gibbs energy are in Table 6.

Table 6. The solubility of oxygen in 1-octanol at an oxygen partial pressure of 101.325 kPa. Tentative values of the mole fraction solubility and partial molar Gibbs energy of solution as a function of temperature.

$T/\text{K}$	Mol Fraction $10^4 x_1$	$\Delta \bar{G}_1^\circ / \text{kJ mol}^{-1}$
283.15	11.6	15.914
288.15	11.5	16.215
293.15	11.4	16.516
298.15	11.3	16.817

## Oxygen + 1-Nonanol [143-08-8]

Makranczy *et al.* (12) report one measurement at 298.15 K which is classed as tentative. It is equivalent to a mole fraction solubility at 101.325 kPa oxygen of  $8.86 \times 10^{-4}$ .

## Oxygen + 1-Decanol [112-30-1]

Wilcock *et al.* (11) report solubility values at 282.74, 298.10 and 313.56. Makranczy *et al.* (12) report one value at 298.15. Both sets of solubility values are classed as tentative, but the values given below are based on a linear regression of the Wilcock *et al.* data only.

$$\ln x_1 = -6.9009 + 0.6185/(T/100 \text{ K})$$

with a standard error about the regression line of  $2.48 \times 10^{-5}$ .

The temperature independent changes in enthalpy and entropy for the transfer of one mole of oxygen from the gas phase at a partial pressure of 101.325 kPa to the infinitely dilute solution are

$$\Delta \bar{H}_1^\circ / \text{kJ mol}^{-1} -0.514 \text{ and } \Delta \bar{S}_1^\circ / \text{J K}^{-1} \text{ mol}^{-1} -57.4$$

The smoothed values of the mole fraction solubility and the Gibbs energy are in Table 7.

Table 7. The solubility of oxygen in 1-decanol at an oxygen partial pressure of 101.325 kPa. Tentative values of the mole fraction solubility and partial molar Gibbs energy of solution as a function of temperature.

$T/K$	Mol Fraction $10^4 x_1$	$\Delta\bar{G}_1^\circ/kJ\ mol^{-1}$
283.15	12.53	15.732
293.15	12.43	16.306
298.15	12.39	16.592
303.15	12.35	16.879
313.15	12.27	17.453

Oxygen + 1-Undecanol [112-42-5]

Oxygen + 1-Dodecanol [112-53-8]

Makranczy *et al.* (12) report one solubility value on each system at 298.15 K. The values are classed as tentative.

$T/K$	Alcohol	Mol Fraction $10^4 x_1$
298.15	1-Undecanol	10.3
298.15	1-Dodecanol	10.8

Oxygen + Cyclohexanol [108-93-0]

Cauquil (4) reports one value at 299.15 K. The mole fraction of  $8.55 \times 10^{-4}$  is classed as tentative.

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2. Timofeev, W. *Z. Physik. Chem.* 1890, *6*, 141.
3. Metschl, J. *J. Phys. Chem.* 1924, *28*, 53.
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Methanol; CH <sub>4</sub> O; [67-56-1]	<b>ORIGINAL MEASUREMENTS:</b> Kretschmer, C. B.; Nowakowska, J.; Wiebe, R.  <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506-9.																																								
<b>VARIABLES:</b> T/K = 248.15 - 323.15 P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="276 470 1006 637" style="margin: 10px auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>248.15</td> <td>0.4580</td> <td>0.2672</td> <td>0.2427</td> </tr> <tr> <td>273.15</td> <td>0.4315</td> <td>0.2446</td> <td>0.2446</td> </tr> <tr> <td>298.15</td> <td>0.4122</td> <td>0.2268</td> <td>0.2476</td> </tr> <tr> <td>323.15</td> <td>0.4038</td> <td>0.2155</td> <td>0.2550</td> </tr> </tbody> </table> <p>The Ostwald coefficients were measured at a total pressure of 101.325 kPa (1 atm). The compiler calculated the Bunsen coefficient and mole fraction values for an oxygen partial pressure of 101.325 kPa (1 atm) assuming the Ostwald coefficient was independent of pressure.</p> <p>Smoothed Data: <math>\ln x_1 = -8.2471 + 1.3742/(T/100K)</math>            Standard error about the regression line = <math>3.67 \times 10^{-6}</math></p> <table border="1" data-bbox="493 823 848 1136" style="margin: 10px auto;"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> </tr> </thead> <tbody> <tr><td>253.15</td><td>0.4509</td></tr> <tr><td>263.15</td><td>0.4417</td></tr> <tr><td>273.15</td><td>0.4333</td></tr> <tr><td>283.15</td><td>0.4257</td></tr> <tr><td>293.15</td><td>0.4187</td></tr> <tr><td>298.15</td><td>0.4154</td></tr> <tr><td>303.15</td><td>0.4123</td></tr> <tr><td>313.15</td><td>0.4064</td></tr> <tr><td>323.15</td><td>0.4009</td></tr> </tbody> </table>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	248.15	0.4580	0.2672	0.2427	273.15	0.4315	0.2446	0.2446	298.15	0.4122	0.2268	0.2476	323.15	0.4038	0.2155	0.2550	T/K	Mol Fraction $x_1 \times 10^3$	253.15	0.4509	263.15	0.4417	273.15	0.4333	283.15	0.4257	293.15	0.4187	298.15	0.4154	303.15	0.4123	313.15	0.4064	323.15	0.4009
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<b>AUXILIARY INFORMATION</b>																																									
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus was similar to that of Horiuti (1), it consisted of a gas buret, manometer, and absorption pipet equipped with a magnetic stirrer. All volumes were calibrated by mercury displacement.</p> <p>The solvent was partly degassed by boiling under reflux. About 40 cm<sup>3</sup> of solvent was admitted into the absorption pipet, and pumped on to complete the degassing. Dry gas, measured in the buret, was admitted, final equilibrium was established after 1 to 3 hours stirring. During the solution process the total pressure was kept at one atm by additions of dry gas.</p> <p>The solubility value was corrected for the increase of solvent volume with gas absorption, and for the nitrogen impurity in the oxygen.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Contained 0.4 per cent N <sub>2</sub> . Passed through Drierite to dry. (2) Methanol. Source not given. Distilled, dried with metallic Al, b.p. (760 mmHg)/°C 64.50, density, $\rho_4^{25}/g\text{ cm}^{-3}$ 0.78650.  <b>ESTIMATED ERROR:</b> Gas buret $\delta V/cm^3 = 0.005$ Average deviation from the mean 0.3%, maximum deviation 0.9% (authors).  <b>REFERENCES:</b> 1. Horiuti, J. <i>J. Sci Papers Inst. Phys. Chem. Res. (Tokyo)</i> <u>1931</u> , <i>17</i> , 125.																																								

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Methanol; CH <sub>4</sub> O; [67-56-1]		ORIGINAL MEASUREMENTS: Makranczy, J.; Ruzs, L.; Balog-Megyery, K.  <i>Hung. J. Ind. Chem.</i> <u>1979</u> 7, 41-6.	
VARIABLES:  T/K = 298		PREPARED BY:  C.L. Young	
EXPERIMENTAL VALUES:			
T/K	P <sup>+</sup> /kPa	Ostwald coefficient,	Mole fraction of oxygen*, x <sub>O<sub>2</sub></sub>
298.15	101.3	0.229	0.000381
* calculated by compiler + partial pressure of oxygen			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:  Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.		SOURCE AND PURITY OF MATERIALS:  No details given	
		ESTIMATED ERROR:  $\delta x_{O_2} = \pm 3\%$	
		REFERENCES: 1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , 1, 55. <i>Chem. Abstr.</i> <u>1961</u> , 55, 3175h.	

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]		Timofeev, W. Z. Physik. Chem. <u>1890</u> , 6, 141-52.		
VARIABLES:		PREPARED BY:		
T/K = 273-297 P/kPa = 101.325		R. Battino, H. L. Clever		
EXPERIMENTAL VALUES:				
t/°C	T <sup>a</sup> /K	10 <sup>4</sup> x <sub>1</sub> <sup>a,b</sup>	L <sup>a,c</sup>	α <sup>d</sup> /cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>
First series				
0	273.15	5.946	0.23344	0.23344 (3)
6.35	279.65	5.885	0.23493	0.22947 (4)
11.3	284.45	5.810	0.23467	0.22535 (3)
17.1	290.25	5.750	0.23552	0.22164 (4)
23.4	296.55	5.704	0.23707	0.21836 (2)
Second series				
3.5	276.65	5.911	0.23419	0.23123 (2)
15.1	288.25	5.774	0.23539	0.22306 (1)
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.</p> <p><sup>c</sup> Ostwald coefficient.</p> <p><sup>d</sup> Bunsen coefficient. Number in parentheses is the number of observations.</p> <p><sup>e</sup> All measurements in 99.7 wt % ethanol.</p>				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
Used a Bunsen absorption apparatus as modified by Ostwald. Basically, a manometric/volumetric apparatus. Details and a drawing are given in the paper.		No details given.		
		ESTIMATED ERROR:		
		δ <sub>α</sub> /α = ±0.01, compiler's estimate.		
		REFERENCES:		

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Ethanol; C<sub>2</sub>H<sub>6</sub>O; [64-17-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Metschl, J.</p> <p><i>J. Phys. Chem.</i> <u>1924</u>, 28, 417-37.</p>								
<p>VARIABLES:</p> <p>T/K = 298.15</p> <p>P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>M. E. Derrick</p> <p>H. L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="326 491 1023 668"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^4</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>5.10</td> <td>0.195</td> <td>0.213</td> </tr> </tbody> </table> <p>The compiler calculated the mole fraction and Ostwald coefficient values.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	5.10	0.195	0.213
T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L						
298.15	5.10	0.195	0.213						
<p>AUXILIARY INFORMATION</p>									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The degassed solvent is saturated with oxygen at 6 to 10 different pressures between 1.5 and 4.5 atm.</p> <p>The pressure is reduced to one atm, and the "supersaturated gas" is shaken out of the solvent and measured.</p> <p>The slope of a plot of the volume of gas reduced to standard conditions shaken out of 100 cm<sup>3</sup> of solvent <i>vs.</i> the pressure of saturation is nearly identical to the solubility-pressure graph (Henry's law). The slope of the curve is used to obtain the Bunsen coefficient. From the method of calculation the value represents the volume of gas shaken out of the solvent when the pressure is reduced from 2 to 1 atm.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Commercial cylinder. Prepared by Linde process, 97 per cent pure.</p> <p>(2) Ethanol. Treated with metallic sodium and distilled. Specific gravity 0.7992 at 15 °C. About 98 per cent pure.</p> <p>ESTIMATED ERROR:</p> <p>REFERENCES:</p>								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	<b>ORIGINAL MEASUREMENTS:</b> Kretschmer, C. B.; Nowakowska, J.; Wiebe, R.  <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506-9.																																								
<b>VARIABLES:</b> T/K = 248.15 - 323.15 P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever																																								
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Ethanol; C<sub>2</sub>H<sub>6</sub>O; [64-17-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Schläpfer, P.; Audykowski, T.; Bukowiecki, A.</p> <p><i>Schweiz. Arch. Angew. Wiss. Tech.</i> <u>1949</u>, 15, 299-307.</p>																											
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	<b>ORIGINAL MEASUREMENTS:</b> Shchukarev, S.A.; Tolmacheva, T.A. <i>Zh. Strukt. Khim.</i> 1968,9,21-8; <i>J.Struct. Chem.</i> 1968,9,16-21.																				
<b>VARIABLES:</b> T/K = 277-323 P/kPa = 101.325	<b>PREPARED BY:</b> R. Battino																				
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T/K <sup>a</sup>	Mole Fraction <sup>b</sup> 10 <sup>4</sup> x <sub>1</sub>	Ostwald Coeff. <sup>c</sup> L	Mole Percent <sup>d</sup>																		
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<b>AUXILIARY INFORMATION</b>																					
<b>METHOD APPARATUS/PROCEDURE:</b> Degassed solvent is transferred to an absorption vessel. The solvent is sealed over mercury. Gas is added and stirring accomplished with a magnetic bob. Uptake of gas is read on a gas buret system which is thermostatted along with the absorption vessel. Details of operation and a drawing are in the original paper. The paper also reports the solubility of oxygen in water/ethanol mixtures, 0-100%.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Prepared by electrolysis of NaOH solution, followed by removal of hydrogen traces, and thoroughly dried before use. No purity given. (2) Dried to at least 99.7%.																				
<b>ESTIMATED ERROR:</b> δL/L = ±0.01, estimate by compiler.																					
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K. Candidates thesis, <u>1970</u> , Leningrad.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="289 486 1019 642" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Mol Fraction <math>x_1 \times 10^4</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="border-bottom: 1px solid black;">298.15</td> <td style="border-bottom: 1px solid black;">5.74</td> <td style="border-bottom: 1px solid black;">0.219</td> <td style="border-bottom: 1px solid black;">0.239</td> </tr> </tbody> </table> <p>The mole fraction solubility value is quoted in (1)</p> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	5.74	0.219	0.239
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> Probably used volumetric method described by Naumenko <i>et al.</i> (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> No information. <b>ESTIMATED ERROR:</b> <b>REFERENCES:</b> 1. Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I. A. <i>Zh. Fiz. Khim.</i> <u>1979</u> , <i>53</i> , 1989. 2. Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim.</i> <u>1969</u> , <i>42</i> , 2090.								



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<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C.L. Young</p>								
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Propanol or isopropyl alcohol; C <sub>3</sub> H <sub>8</sub> O; [67-63-0]	<b>ORIGINAL MEASUREMENTS:</b> Kretschmer, C. B.; Nowakowska, J.; Wiebe, R. <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506-9.																																
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<b>VARIABLES:</b> T/K = 273.15 - 323.15 P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever																																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="277 466 1008 613"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>273.15</td> <td>0.8363</td> <td>0.2085</td> <td>0.2085</td> </tr> <tr> <td>298.15</td> <td>0.7894</td> <td>0.1924</td> <td>0.2100</td> </tr> <tr> <td>323.15</td> <td>0.7707</td> <td>0.1835</td> <td>0.2171</td> </tr> </tbody> </table> <p>The Ostwald coefficients were measured at a total pressure of 101.325 kPa (1 atm). The compiler calculated the Bunsen coefficient and mole fraction values for an oxygen partial pressure of 101.325 kPa (1 atm) assuming the Ostwald coefficient was independent of pressure.</p> <p>Smoothed Data: <math>\ln x_1 = -7.6234 + 1.4553/(T/100K)</math>            Standard error about the regression line = <math>8.71 \times 10^{-6}</math></p> <table border="1" data-bbox="494 799 843 1060"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> </tr> </thead> <tbody> <tr> <td>273.15</td> <td>0.833</td> </tr> <tr> <td>283.15</td> <td>0.817</td> </tr> <tr> <td>293.15</td> <td>0.803</td> </tr> <tr> <td>298.15</td> <td>0.796</td> </tr> <tr> <td>303.15</td> <td>0.790</td> </tr> <tr> <td>313.15</td> <td>0.778</td> </tr> <tr> <td>323.15</td> <td>0.767</td> </tr> </tbody> </table>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	273.15	0.8363	0.2085	0.2085	298.15	0.7894	0.1924	0.2100	323.15	0.7707	0.1835	0.2171	T/K	Mol Fraction $x_1 \times 10^3$	273.15	0.833	283.15	0.817	293.15	0.803	298.15	0.796	303.15	0.790	313.15	0.778	323.15	0.767
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was similar to that of Horiuti (1), it consisted of a gas buret, manometer, and absorption pipet equipped with a magnetic stirrer. All volumes were calibrated by mercury displacement. The solvent was partly degassed by boiling under reflux. About 40 cm <sup>3</sup> of solvent was admitted into the absorption pipet, and pumped on to complete the degassing. Dry gas, measured in the buret, was admitted, final equilibrium was established after 1 to 3 hours stirring. During the solution process the total pressure was kept at one atm by additions of dry gas. The solubility value was corrected for the increase of solvent volume with gas absorption, and for the nitrogen impurity in the oxygen.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Contained 0.4 per cent N <sub>2</sub> . Passed through Drierite to dry. (2) 1-Butanol. Source not given. Distilled, dried with metallic Al, b.p. (760 mmHg)/°C 117.67, density, $\rho_4^{25}/g\text{ cm}^{-3}$ 0.80573. <b>ESTIMATED ERROR:</b> Gas buret $\delta V/\text{cm}^3 = 0.005$ Average deviation from the mean 0.3%, maximum deviation 0.9% (authors). <b>REFERENCES:</b> 1. Horiuti, J. <i>J. Sci Papers Inst. Phys. Chem. Res. (Tokyo)</i> <u>1931</u> , <i>17</i> , 125.																																

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VARIABLES:  T/K = 298		PREPARED BY:  C.L. Young	
EXPERIMENTAL VALUES:			
T/K	P <sup>+</sup> /kPa	Ostwald coefficient,	Mole fraction of oxygen*, x <sub>O<sub>2</sub></sub>
298.15	101.3	0.153	0.000575
<p>* calculated by compiler + partial pressure of oxygen</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:  Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.		SOURCE AND PURITY OF MATERIALS:  No details given	
		ESTIMATED ERROR:  $\delta x_{O_2} = \pm 3\%$	
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Methyl-1-propanol or Isobutanol; C <sub>4</sub> H <sub>9</sub> OH; [78-83-1]	<b>ORIGINAL MEASUREMENTS:</b> Battino. R.; Evans, F. D.; Danforth. W. F.; Wilhelm, E. <i>J. Chem. Thermodyn.</i> <u>1971</u> , 3, 743-51.																																																									
<b>VARIABLES:</b> T/K = 274.09 - 327.96 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																																																									
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="348 453 1019 725"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>274.09</td><td>0.897</td><td>0.221</td><td>0.222</td></tr> <tr><td>282.85</td><td>0.874</td><td>0.214</td><td>0.222</td></tr> <tr><td>297.63</td><td>0.847</td><td>0.205</td><td>0.223</td></tr> <tr><td>298.25</td><td>0.854</td><td>0.206</td><td>0.225</td></tr> <tr><td>308.37</td><td>0.822</td><td>0.196</td><td>0.222</td></tr> <tr><td>312.78</td><td>0.807</td><td>0.192</td><td>0.220</td></tr> <tr><td>314.14</td><td>0.801</td><td>0.190</td><td>0.219</td></tr> <tr><td>327.96</td><td>0.765</td><td>0.179</td><td>0.215</td></tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler.            The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -2196.4 + 66.256 T</math>            Std. Dev. <math>\Delta G^\circ = 26.3</math>, Coef. Corr. = 0.9998  <math>\Delta H^\circ/\text{J mol}^{-1} = -2196.4</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -66.256</math></p> <table border="1" data-bbox="414 924 901 1153"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>278.15</td><td>0.895</td><td>16,233</td></tr> <tr><td>288.15</td><td>0.866</td><td>16,895</td></tr> <tr><td>298.15</td><td>0.839</td><td>17,558</td></tr> <tr><td>308.15</td><td>0.816</td><td>18,220</td></tr> <tr><td>318.15</td><td>0.794</td><td>18,883</td></tr> <tr><td>328.15</td><td>0.774</td><td>19,546</td></tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	274.09	0.897	0.221	0.222	282.85	0.874	0.214	0.222	297.63	0.847	0.205	0.223	298.25	0.854	0.206	0.225	308.37	0.822	0.196	0.222	312.78	0.807	0.192	0.220	314.14	0.801	0.190	0.219	327.96	0.765	0.179	0.215	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	278.15	0.895	16,233	288.15	0.866	16,895	298.15	0.839	17,558	308.15	0.816	18,220	318.15	0.794	18,883	328.15	0.774	19,546
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent is passed in a thin film down a glass helical tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Products and Chemicals Co. 99.6 per cent. (2) 2-methyl-1-propanol. Fisher Co. Certified grade (99 mole per cent). <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.01$ <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u> , 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u> , 45, 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , 43, 806.																																																									

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Pentanol; C <sub>5</sub> H <sub>12</sub> O; [71-41-0] or 1-Hexanol; C <sub>6</sub> H <sub>14</sub> O; [111-27-3]		ORIGINAL MEASUREMENTS: Makranczy, J.; Ruzs, L.; Balog-Megyery, K.  <i>Hung. J. Ind. Chem.</i> <u>1979</u> , <i>7</i> , 41-6.	
VARIABLES:  T/K = 298		PREPARED BY:  C.L. Young	
EXPERIMENTAL VALUES:			
T/K	P <sup>+</sup> /kPa	Ostwald coefficient	Mole fraction of oxygen*, x <sub>O<sub>2</sub></sub>
		1-Pentanol	
298.15	101.3	0.142	0.000630
		1-Hexanol	
298.15	101.3	0.138	0.000706
* calculated by compiler + partial pressure of oxygen			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:  Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.		SOURCE AND PURITY OF MATERIALS:  No details given.	
		ESTIMATED ERROR:  $\delta x_{O_2} = \pm 3\%$	
		REFERENCES: 1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , <i>1</i> , 55. <i>Chem. Abstr.</i> <u>1961</u> , <i>55</i> , 3175h.	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Aliphatic alcohols; C <sub>7</sub> H <sub>16</sub> O and C <sub>8</sub> H <sub>18</sub> O	<b>ORIGINAL MEASUREMENTS:</b> Ijams, C. C. Ph.D. thesis, 1941, Vanderbilt University, Nashville, TN.																				
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b>																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="282 487 1010 765"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">1-Heptanol; C<sub>7</sub>H<sub>16</sub>O; [111-70-6]</td> </tr> <tr> <td>298.15</td> <td>1.08</td> <td>0.171</td> <td>0.187</td> </tr> <tr> <td colspan="4" style="text-align: center;">1-Octanol; C<sub>8</sub>H<sub>18</sub>O; [111-87-5]</td> </tr> <tr> <td>298.15</td> <td>1.15</td> <td>0.163</td> <td>0.178</td> </tr> </tbody> </table> <p>The mole fraction and Ostwald coefficient values were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	1-Heptanol; C <sub>7</sub> H <sub>16</sub> O; [111-70-6]				298.15	1.08	0.171	0.187	1-Octanol; C <sub>8</sub> H <sub>18</sub> O; [111-87-5]				298.15	1.15	0.163	0.178
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<b>AUXILIARY INFORMATION</b>																					
<b>METHOD/APPARATUS/PROCEDURE:</b> A Van Slyke-Neill Manometric Apparatus manufactured by the Eimer and Amend Co. was used. The procedure of Van Slyke (1) for pure liquids was modified so that small solvent sample (2 cm <sup>3</sup> ) could be used with almost 100 per cent recovery of the solvent. An improved temperature control system was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Reduction Co. Purity 99.5 per cent. (2) Aliphatic alcohols. Purified. Vapor pressure and boiling point also reported in the thesis. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ <b>REFERENCES:</b> 1. Van Slyke, D. D. <i>J. Biol. Chem.</i> 1939, 130, 545.																				



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Heptanol; C <sub>7</sub> H <sub>16</sub> O; [111-70-6] or 1-Octanol; C <sub>8</sub> H <sub>18</sub> O; [111-87-5]	<b>ORIGINAL MEASUREMENTS:</b> Makranczy, J.; Ruzs, L.; Balog - Megyery, K. <i>Hung. J. Ind. Chem.</i> <u>1979</u> , 7, 41-6.
<b>VARIABLES:</b> T/K = 298	<b>PREPARED BY:</b> C.L. Young
<b>EXPERIMENTAL VALUES:</b>	
T/K            P <sup>+</sup> /kPa	Ostwald coefficient            Mole fraction of oxygen*, x <sub>O<sub>2</sub></sub>
298.15        101.3	1-Heptanol 0.131                            0.000759
298.15        101.3	1-Octanol 0.183**                          0.00118
* calculated by compiler + partial pressure of oxygen ** appears to be an error in table 1 of the source reference.	
<b>AUXILIARY INFORMATION</b>	
<b>METHOD/APPARATUS/PROCEDURE:</b> Volumetric method. The apparatus of Bodor, Bor, Mohai, and Sipos (1) was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given  <b>ESTIMATED ERROR:</b> $\delta x_{O_2} = \pm 3\%$  <b>REFERENCES:</b> 1. Bodor, E.; Bor, Gy.; Mohai, B.; Sipos, G. <i>Veszpremi Vegyip. Egy. Kozl.</i> <u>1957</u> , 1, 55. <i>Chem. Abstr.</i> <u>1961</u> , 55, 3175h.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Octanol; C <sub>8</sub> H <sub>17</sub> OH; [111-87-5]	<b>ORIGINAL MEASUREMENTS:</b> Wilcock, R. J.; Battino, R.; Danforth, W. F.; Wilhelm, E.  <i>J. Chem. Thermodyn.</i> <u>1978</u> , <i>10</i> , 817-22.																											
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<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="326 487 993 632"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>283.35</td> <td>1.159</td> <td>0.1662</td> <td>0.1724</td> </tr> <tr> <td>298.13</td> <td>1.132</td> <td>0.1602</td> <td>0.1749</td> </tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler.            The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.            Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -1120.1 + 60.160 T</math>  <math>\Delta H^\circ/\text{J mol}^{-1} = -1120.1</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -60.160</math></p> <table border="1" data-bbox="427 819 905 1023"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>283.15</td> <td>1.16</td> <td>15,914</td> </tr> <tr> <td>288.15</td> <td>1.15</td> <td>16,215</td> </tr> <tr> <td>293.15</td> <td>1.14</td> <td>16,516</td> </tr> <tr> <td>298.15</td> <td>1.13</td> <td>16,816</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	283.35	1.159	0.1662	0.1724	298.13	1.132	0.1602	0.1749	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	283.15	1.16	15,914	288.15	1.15	16,215	293.15	1.14	16,516	298.15	1.13	16,816
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<p>VARIABLES:</p> <p>T/K = 282.74 - 313.56 P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>A. L. Cramer</p>																																		
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="379 498 1050 667"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>282.74</td> <td>1.263</td> <td>0.1496</td> <td>0.1549</td> </tr> <tr> <td>298.10</td> <td>1.219</td> <td>0.1428</td> <td>0.1558</td> </tr> <tr> <td>313.56</td> <td>1.237</td> <td>0.1429</td> <td>0.1641</td> </tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler. The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law. Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln x_1 = -475.93 + 57.247 T</math> Std. Dev. <math>\Delta G^\circ = 35.1</math>, Coef. Corr. = 0.9992 <math>\Delta H^\circ/\text{J mol}^{-1} = -475.9</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -57.247</math></p> <table border="1" data-bbox="477 906 961 1129"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>278.15</td> <td>1.26</td> <td>15,447</td> </tr> <tr> <td>288.15</td> <td>1.25</td> <td>16,020</td> </tr> <tr> <td>298.15</td> <td>1.24</td> <td>16,592</td> </tr> <tr> <td>308.15</td> <td>1.23</td> <td>17,165</td> </tr> <tr> <td>318.15</td> <td>1.22</td> <td>17,737</td> </tr> </tbody> </table>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	282.74	1.263	0.1496	0.1549	298.10	1.219	0.1428	0.1558	313.56	1.237	0.1429	0.1641	T/K	Mol Fraction $x_1 \times 10^3$	$\Delta G^\circ/\text{J mol}^{-1}$	278.15	1.26	15,447	288.15	1.25	16,020	298.15	1.24	16,592	308.15	1.23	17,165	318.15	1.22	17,737
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(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Makranczy, J.; Ruzs, L.;	
(2) 1-Undecanol; C <sub>11</sub> H <sub>24</sub> O; [112-42-5]		Balog-Megyery, K.	
or		<i>Hung. J. Ind. Chem.</i> <u>1979</u> , 7, 41-6.	
1-Dodecanol; C <sub>12</sub> H <sub>26</sub> O; [112-53-8]			
VARIABLES:		PREPARED BY:	
T/K = 298		C.L. Young	
EXPERIMENTAL VALUES:			
T/K	P <sup>+</sup> /kPa	Ostwald coefficient	Mole fraction of oxygen*, x <sub>O<sub>2</sub></sub>
		1-Undecanol	
298.15	101.3	0.121	0.00103
		1-Dodecanol	
298.15	101.3	0.118	0.00108
* calculated by compiler			
+ partial pressure of oxygen			
AUXILIARY INFORMATION			
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Cyclohexanol; C <sub>6</sub> H <sub>14</sub> O; [108-93-0]	<b>ORIGINAL MEASUREMENTS:</b> Cauquil, G. <i>J. Chim. Phys.</i> <u>1927</u> , <i>24</i> , 53-5.								
<b>VARIABLES:</b> T/K = 299.15 P/kPa = 102.125	<b>PREPARED BY:</b> P. L. Long H. L. Clever								
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus consists of a flask and a mercury leveling bulb to control the pressure.</p> <p>The solvent volume was measured, the gas introduced over the solvent. The gas absorbed was found by difference between the initial and final gas volumes.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Purity not stated. (2) Cyclohexanol. Source not given. Distilled. B.p. (766 mmHg) T/K 334.0. Degassed and tested to be air free.								
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Propanone or acetone; C <sub>3</sub> H <sub>6</sub> O; [67-64-1]	<b>ORIGINAL MEASUREMENTS:</b> Metschl, J. <i>J. Phys. Chem.</i> <u>1924</u> , <i>28</i> , 417-37.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever								
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The degassed solvent is saturated with oxygen at 6 to 10 different pressures between 1.5 and 4.5 atm.</p> <p>The pressure is reduced to one atm, and the "supersaturated gas" is shaken out of the solvent and measured.</p> <p>The slope of a plot of the volume of gas reduced to standard conditions shaken out of 100 cm<sup>3</sup> of solvent <i>vs.</i> the pressure of saturation is nearly identical to the solubility-pressure graph (Henry's law). The slope of the curve is used to obtain the Bunsen coefficient. From the method of calculation the value represents the volume of gas shaken out of the solvent when the pressure is reduced from 2 to 1 atm.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Commercial cylinder. Prepared by Linde process, 97 per cent pure. (2) Acetone. Chemically pure. Dried over anhydrous copper sulfate and distilled.								
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Propanone or Acetone; C <sub>3</sub> H <sub>6</sub> O; [67-64-1]	<b>ORIGINAL MEASUREMENTS:</b> Horiuti, J. <i>Sci. Papers Inst. Phys. Chem. Res.</i> (Tokyo)(Jpn) <u>1931/32</u> , 17, 125-256.																																								
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If the gas and solution are assumed to be ideal the fitted equation gives the following thermodynamic values.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$																																								
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<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="289 480 1019 623"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>248.15</td> <td>0.8115</td> <td>0.2631</td> <td>0.2390</td> </tr> <tr> <td>273.15</td> <td>0.8192</td> <td>0.2570</td> <td>0.2570</td> </tr> <tr> <td>298.15</td> <td>0.8440</td> <td>0.2560</td> <td>0.2794</td> </tr> </tbody> </table> <p>The Ostwald coefficients were measured at a total pressure of 101.325 kPa (1 atm). The compiler calculated the Bunsen coefficient and mole fraction values for an oxygen partial pressure of 101.325 kPa (1 atm) assuming the Ostwald coefficient was independent of pressure.</p> <p>Smoothed Data: <math>\ln x_1 = -6.8904 - 0.5703/(T/100K)</math></p> <p>Standard error about the regression line = <math>8.06 \times 10^{-6}</math></p> <table border="1" data-bbox="506 833 861 1068"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> </tr> </thead> <tbody> <tr> <td>253.15</td> <td>0.812</td> </tr> <tr> <td>263.15</td> <td>0.819</td> </tr> <tr> <td>273.15</td> <td>0.826</td> </tr> <tr> <td>283.15</td> <td>0.832</td> </tr> <tr> <td>293.15</td> <td>0.838</td> </tr> <tr> <td>298.15</td> <td>0.840</td> </tr> </tbody> </table>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	248.15	0.8115	0.2631	0.2390	273.15	0.8192	0.2570	0.2570	298.15	0.8440	0.2560	0.2794	T/K	Mol Fraction $x_1 \times 10^3$	253.15	0.812	263.15	0.819	273.15	0.826	283.15	0.832	293.15	0.838	298.15	0.840
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was similar to that of Horiuti (1), it consisted of a gas buret, manometer, and absorption pipet equipped with a magnetic stirrer. All volumes were calibrated by mercury displacement. The solvent was partly degassed by boiling under reflux. About 40 cm <sup>3</sup> of solvent was admitted into the absorption pipet, and pumped on to complete the degassing. Dry gas, measured in the buret, was admitted, final equilibrium was established after 1 to 3 hours stirring. During the solution process the total pressure was kept at one atm by additions of dry gas. The solubility value was corrected for the increase of solvent volume with gas absorption, and for the nitrogen impurity in the oxygen.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Contained 0.4 per cent N <sub>2</sub> . Passed through Drierite to dry. (2) 2-Propanone. Source not given. Treated with Ag <sub>2</sub> O, dried over CaSO <sub>4</sub> , distilled, b.p. (760 mmHg)/°C 56.10 - 56.14, density, $\rho_4^{25}/g \text{ cm}^{-3}$ 0.78490. <b>ESTIMATED ERROR:</b> Gas buret $\delta V/\text{cm}^3 = 0.005$ Average deviation from the mean 0.3%, maximum deviation 0.9% (authors). <b>REFERENCES:</b> 1. Horiuti, J. <i>J. Sci Papers Inst. Phys. Chem. Res. (Tokyo)</i> <u>1931</u> , <i>17</i> , 125.																														

<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) 2-Propanone (Acetone); C <sub>2</sub> H <sub>6</sub> O; [67-64-1]	<b>ORIGINAL MEASUREMENTS:</b>  Bub, G.K.; Hillebrand, W. A.  <i>J. Chem. Eng. Data</i> <u>1979</u> , 24, 315-9.																																																																		
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Hexanone; C <sub>6</sub> H <sub>12</sub> O; [591-78-6]	<b>ORIGINAL MEASUREMENTS:</b> Bub, G. K.; Hillebrand, W. A. <i>J. Chem. Eng. Data</i> <u>1979</u> , 24, 315-9.																																																																					
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Cyclohexanone; C <sub>6</sub> H <sub>10</sub> O; [108-94-1]	<b>ORIGINAL MEASUREMENTS:</b> Guerry, D. Jr. Ph. D. thesis, 1944, Vanderbilt University Nashville, TN												
<b>VARIABLES:</b> T/K= 293-298 P/kPa= 101.325	<b>PREPARED BY:</b> H. L. Clever												
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<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> A modified Van Slyke-Neill manometric apparatus (1, 2) was used. The modifications were improved temperature control, and procedures that allowed small samples (2 cm <sup>3</sup> ) with almost 100 per cent recovery of the solvent.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Reduction Co. Purity 99.5 per cent. (2) Cyclohexanone. Eastman Kodak Co. Purified and distilled, b. p. (754.5 mmHg) t/ <sup>o</sup> C 155.19 (corr.). Refractive index, density, and vapor pressure data are in the thesis. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ <b>REFERENCES:</b> 1. Ijams, C. C. Ph. D. thesis, 1941 Vanderbilt University 2. Van Slyke, D. D. <i>J. Biol. Chem.</i> 1939, 130, 545.												

<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) 1,1'-Oxybisethane or diethyl ether; C <sub>4</sub> H <sub>10</sub> O; [60-29-7]	<b>ORIGINAL MEASUREMENTS:</b>  Christoff, A.  <i>Z. Phys. Chem.</i> <u>1912</u> , 79, 456-60.								
<b>VARIABLES:</b>  T/K = 273.15 P/kPa = Atmospheric	<b>PREPARED BY:</b>  M. E. Derrick H. L. Clever								
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<b>METHOD/APPARATUS/PROCEDURE:</b>  <p>The apparatus is a modified Ostwald apparatus described by Just (1), and modified by Skirrow (2). The apparatus consists of a thermostated gas buret and an absorption flask.</p> <p>The modification involves the use of vapor free gas in the gas buret. A correction is made for the vapor pressure of the liquid. A steel capillary tube with a stopcock, which prevents the gas and the liquid vapor from mixing in the buret, is used to connect the absorption flask and the buret.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b>  (1) Oxygen. Prepared from KClO <sub>3</sub> .  (2) Diethylether. Merck and Co. Stated to be pure and anhydrous.  <b>ESTIMATED ERROR:</b>  $\delta L/L = 0.03$  <b>REFERENCES:</b>  1. Just, G. <i>Z. Phys. Chem.</i> <u>1901</u> , 37, 342.  2. Skirrow, F. W. <i>Z. Phys. Chem.</i> <u>1902</u> , 41, 139.								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1,1-Oxybisethane or Diethylether; C <sub>4</sub> H <sub>10</sub> O; [60-29-7]	<b>ORIGINAL MEASUREMENTS:</b> Horiuti, J. <i>Sci. Papers Inst. Phys. Chem. Res.</i> (Tokyo) (Jpn) <u>1931/32</u> , 17, 125-256.																																																								
<b>VARIABLES:</b> T/K = 195.05 - 293.15 Total P/kPa = 101.325	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever																																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="322 472 997 687"> <thead> <tr> <th>T/K</th> <th>Mol Fraction x<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>195.05</td><td>2.537</td><td>0.6309</td><td>0.4505</td></tr> <tr><td>213.05</td><td>2.287</td><td>0.5550</td><td>0.4329</td></tr> <tr><td>232.65</td><td>2.067</td><td>0.4983</td><td>0.4244</td></tr> <tr><td>253.25</td><td>1.996</td><td>0.4581</td><td>0.4247</td></tr> <tr><td>273.15</td><td>1.939</td><td>0.4325</td><td>0.4325</td></tr> <tr><td>293.15</td><td>1.432</td><td>0.4203</td><td>0.4511</td></tr> </tbody> </table> <p>Smoothed Data: <math>\ln x_1 = 2.34441 - 9.53953/(T/100) - 5.17850 \ln (T/100)</math></p> <p>Standard error about the regression line = <math>1.56 \times 10^{-4}</math></p> <table border="1" data-bbox="247 799 1096 1015"> <thead> <tr> <th>T/K</th> <th>Mol Fraction x<sub>1</sub> × 10<sup>3</sup></th> <th>T/K</th> <th>Mol Fraction x<sub>1</sub> × 10<sup>3</sup></th> </tr> </thead> <tbody> <tr><td>193.15</td><td>2.47</td><td>253.15</td><td>1.96</td></tr> <tr><td>203.15</td><td>2.43</td><td>263.15</td><td>1.85</td></tr> <tr><td>213.15</td><td>2.36</td><td>273.15</td><td>1.74</td></tr> <tr><td>223.15</td><td>2.27</td><td>283.15</td><td>1.64</td></tr> <tr><td>233.15</td><td>2.17</td><td>293.15</td><td>1.53</td></tr> <tr><td>243.15</td><td>2.07</td><td></td><td></td></tr> </tbody> </table> <p>The Ostwald coefficient was measured at a total pressure of one atm. The Bunsen coefficient and the mole fraction solubility values were calculated by the compiler for a gas pressure of one atm assuming the gas to behave ideally and the Ostwald coefficient to be independent of pressure.</p>		T/K	Mol Fraction x <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	195.05	2.537	0.6309	0.4505	213.05	2.287	0.5550	0.4329	232.65	2.067	0.4983	0.4244	253.25	1.996	0.4581	0.4247	273.15	1.939	0.4325	0.4325	293.15	1.432	0.4203	0.4511	T/K	Mol Fraction x <sub>1</sub> × 10 <sup>3</sup>	T/K	Mol Fraction x <sub>1</sub> × 10 <sup>3</sup>	193.15	2.47	253.15	1.96	203.15	2.43	263.15	1.85	213.15	2.36	273.15	1.74	223.15	2.27	283.15	1.64	233.15	2.17	293.15	1.53	243.15	2.07		
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<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Reduction Co. Purity 99.5 per cent.  (2) Dipropyl ether. Eastman Kodak Co. Refluxed four hours over Na, then distilled from Na in a N <sub>2</sub> atm. B.p. (746.2 mmHg) t/°C 89.03 - 89.28 (corr.). Refractive index, density, and vapor pressure data are in the thesis.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$  <b>REFERENCES:</b> 1. Van Slyke, D. D. <i>J. Biol. Chem.</i> <u>1939</u> , <i>130</i> , 545.  2. Ijams, C. C. Ph.D. thesis, <u>1941</u> Vanderbilt University												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; 7782-44-7 (2) Cyclic ethers; C <sub>4</sub> H <sub>8</sub> O, C <sub>4</sub> H <sub>8</sub> O <sub>2</sub> , and C <sub>5</sub> H <sub>10</sub> O	<b>ORIGINAL MEASUREMENTS:</b> Guerry, D. Jr. Ph. D. thesis, 1944, Vanderbilt University, Nashville, TN																																								
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<b>VARIABLES:</b> T/K = 194.75 - 313.15 Total P/kPa = 101.325		<b>PREPARED BY:</b> M. E. Derrick H. L. Clever		
<b>EXPERIMENTAL VALUES:</b>				
	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L
	194.75	0.8327	0.2666	0.1901
	212.35	0.8153	0.2556	0.1987
	232.25	0.8172	0.2500	0.2126
	252.35	0.8304	0.2477	0.2288
	273.15	0.8567	0.2488	0.2488
	283.15	0.8695	0.2492	0.2583
	295.00	0.8872	0.2503	0.2703
	303.15	0.9007	0.2513	0.2789
	313.15	0.9120	0.2510	0.2877
Smoothed Data: $\ln X_1 = -10.8973 + 4.6638/(T/100) + 2.1142 \ln (T/100)$ Standard error about the regression line = $2.96 \times 10^{-6}$				
	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>
	193.15	0.8326	263.15	0.8423
	203.15	0.8226	273.15	0.8541
	213.15	0.8176	283.15	0.8677
	223.15	0.8166	293.15	0.8827
	233.15	0.8191	303.15	0.8991
	243.15	0.8245	313.15	0.9168
	253.15	0.8323		
The Ostwald coefficient was measured at a total pressure of one atm. The Bunsen coefficient and the mole fraction solubility values were calculated by the compiler for a gas pressure of one atm assuming the gas to behave ideally and the Ostwald coefficient to be independent of pressure.				
<b>AUXILIARY INFORMATION</b>				
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus consists of a gas buret, a solvent reservoir, and an absorption pipet. The volume of the pipet was determined at various meniscus heights by weighing a quantity of water. The meniscus height was read with a cathetometer. The dry gas introduced into the degassed solvent. The gas and solvent are mixed with a magnetic stirrer until saturation. Care taken to prevent solvent vapor from mixing with the solute gas in the gas buret. The volume of gas was determined from a gas buret reading, the volume of the solvent was determined from the meniscus height in the absorption pipet.			<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Prepared in the laboratory by heating potassium permanganate (Kahlbaum). Gas fractionated in liquid air. (2) Acetic acid, methyl ester. Merck. Extra pure grade treated with phosphorous pentoxide several times and distilled several times. Normal boiling point, 57.12°C.	
			<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$	
If the gas and solution are assumed to be ideal the fitted equation gives the following thermodynamic values.				
T/K	$\Delta G^\circ/kJ \text{ mol}^{-1}$	$\Delta H^\circ/J \text{ mol}^{-1}$	$\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1}$	$\Delta C_p^\circ/J \text{ K}^{-1} \text{ mol}^{-1}$
273.15	16.045	924	-55.36	17.58
298.15	17.410	1363	-53.82	17.58

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Propanone or acetone; C <sub>3</sub> H <sub>6</sub> O; [67-64-1] (3) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	<b>ORIGINAL MEASUREMENTS:</b> Kretschmer, C. B.; Nowakowska, J.; Wiebe, R. <i>Ind. Eng. Chem.</i> <u>1946</u> , <i>38</i> , 506-9.												
<b>VARIABLES:</b> T/K = 273.15 - 323.15 P/kPa = 101.325 Ethanol/vol % = 50	<b>PREPARED BY:</b> P. L. Long H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="363 493 879 687" style="margin: 10px auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>273.15</td> <td>0.2409</td> <td>0.2409</td> </tr> <tr> <td>298.15</td> <td>0.2338</td> <td>0.2552</td> </tr> <tr> <td style="border-bottom: 1px solid black;">323.15</td> <td style="border-bottom: 1px solid black;">0.2310</td> <td style="border-bottom: 1px solid black;">0.2733</td> </tr> </tbody> </table> <p>The Ostwald coefficients were measured at a total pressure of 101.325 kPa (1 atm). The compiler calculated the Bunsen coefficient value for an oxygen partial pressure of 101.325 kPa (1 atm) assuming the Ostwald coefficient was independent of pressure.</p> <p>The solvent is acetone in ethanol, 50 per cent by volume.</p>		T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	273.15	0.2409	0.2409	298.15	0.2338	0.2552	323.15	0.2310	0.2733
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was similar to that of Horiuti (1), it consisted of a gas buret, manometer, and absorption pipet equipped with a magnetic stirrer. All volumes were calibrated by mercury displacement. The solvent was partly degassed by boiling under reflux. About 40 cm <sup>3</sup> of solvent was admitted into the absorption pipet, and pumped on to complete the degassing. Dry gas, measured in the buret, was admitted, final equilibrium was established after 1 to 3 hours stirring. During the solution process the total pressure was kept at one atm by additions of dry gas. The solubility value was corrected for the increase of solvent volume with gas absorption, and for the nitrogen impurity in the oxygen.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Contained 0.4 per cent N <sub>2</sub> . Passed through Drierite to dry. (2) 2-Propanone. Source not given. Treated with Ag <sub>2</sub> O, dried over CaSO <sub>4</sub> , distilled, b.p. (760 mmHg)/°C 56.10-56.14, density, $\rho_4^{25}$ /g cm <sup>-3</sup> 0.78490. (3) Ethanol. Source not given. Dried with Mg. Density, $\rho/g$ cm <sup>-3</sup> 0.78508. <b>ESTIMATED ERROR:</b> Gas buret $\delta V/cm^3 = 0.005$ Average deviation from the mean 0.3%, maximum deviation 0.9% (authors). <b>REFERENCES:</b> 1. Horiuti, J. <i>J. Sci Papers Inst. Phys. Chem. Res. (Tokyo)</i> <u>1931</u> , <i>17</i> , 125.												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Various solvents (see table below)	<b>ORIGINAL MEASUREMENTS:</b> Schläpfer, P.; Andykowski, T.; Bukowieck, A. <i>Schweiz. Arch. Angew. Wiss. Tech.</i> <u>1949</u> , 15, 299-307.																																		
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<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">Solvent</th> <th style="text-align: right;">L<sup>a</sup></th> </tr> </thead> <tbody> <tr> <td colspan="2" style="text-align: center;">20°C (293K)</td> </tr> <tr> <td>methanol; CH<sub>4</sub>O; [67-56-1]</td> <td style="text-align: right;">0.247</td> </tr> <tr> <td>ethanol; C<sub>2</sub>H<sub>6</sub>O; [64-17-5]</td> <td style="text-align: right;">0.243</td> </tr> <tr> <td>1-propanol; C<sub>3</sub>H<sub>8</sub>O; [540-67-0]</td> <td style="text-align: right;">0.214</td> </tr> <tr> <td>2-propanol; C<sub>3</sub>H<sub>8</sub>O; [67-63-0]</td> <td style="text-align: right;">0.247</td> </tr> <tr> <td>1-butanol; C<sub>4</sub>H<sub>10</sub>O; [71-36-3]</td> <td style="text-align: right;">0.212</td> </tr> <tr> <td>2-propanone (acetone); C<sub>3</sub>H<sub>6</sub>O; [67-64-1]</td> <td style="text-align: right;">0.274</td> </tr> <tr> <td>methyl acetate; C<sub>3</sub>H<sub>6</sub>O<sub>2</sub>; [79-20-9]</td> <td style="text-align: right;">0.269</td> </tr> <tr> <td>ethyl acetate; C<sub>4</sub>H<sub>8</sub>O<sub>2</sub>; [141-78-6]</td> <td style="text-align: right;">0.214</td> </tr> <tr> <td>diethyl ether; C<sub>4</sub>H<sub>10</sub>O; [60-29-7]</td> <td style="text-align: right;">0.450</td> </tr> <tr> <td>tetra chloroethane (carbon tetrachloride); CCl<sub>4</sub>; [56-23-5]</td> <td style="text-align: right;">0.300</td> </tr> <tr> <td>tetrachloroethylene; C<sub>2</sub>Cl<sub>4</sub>; [127-18-4]</td> <td style="text-align: right;">0.199</td> </tr> <tr> <td>petroleum ether</td> <td style="text-align: right;">0.438</td> </tr> <tr> <td>olefin poor gasoline</td> <td style="text-align: right;">0.334</td> </tr> <tr> <td>cracked gasoline</td> <td style="text-align: right;">0.326</td> </tr> <tr> <td>2,2,4-trimethylpentane (isooctane); C<sub>8</sub>H<sub>18</sub>; [540-84-1]</td> <td style="text-align: right;">0.335</td> </tr> </tbody> </table> <p style="text-align: right;">continued on following page</p>		Solvent	L <sup>a</sup>	20°C (293K)		methanol; CH <sub>4</sub> O; [67-56-1]	0.247	ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	0.243	1-propanol; C <sub>3</sub> H <sub>8</sub> O; [540-67-0]	0.214	2-propanol; C <sub>3</sub> H <sub>8</sub> O; [67-63-0]	0.247	1-butanol; C <sub>4</sub> H <sub>10</sub> O; [71-36-3]	0.212	2-propanone (acetone); C <sub>3</sub> H <sub>6</sub> O; [67-64-1]	0.274	methyl acetate; C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> ; [79-20-9]	0.269	ethyl acetate; C <sub>4</sub> H <sub>8</sub> O <sub>2</sub> ; [141-78-6]	0.214	diethyl ether; C <sub>4</sub> H <sub>10</sub> O; [60-29-7]	0.450	tetra chloroethane (carbon tetrachloride); CCl <sub>4</sub> ; [56-23-5]	0.300	tetrachloroethylene; C <sub>2</sub> Cl <sub>4</sub> ; [127-18-4]	0.199	petroleum ether	0.438	olefin poor gasoline	0.334	cracked gasoline	0.326	2,2,4-trimethylpentane (isooctane); C <sub>8</sub> H <sub>18</sub> ; [540-84-1]	0.335
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The solvents were saturated with air at 20°C. Then the dissolved oxygen was determined iodimetrically with a thiosulfate titration. For five of the solvents the solubility was determined via a physical method (manometric/volumetric, described in the paper) since there were interferences to the iodimetric method.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From air. (2) The specific gravity is given in the original paper for all of the solvents used. <b>ESTIMATED ERROR:</b> ΔL/L = ±0.025, authors' estimate. <b>REFERENCES:</b>																																		

COMPONENTS:	EVALUATOR:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Various solvents (see table below)	Schläpfer, P.; Audykowski, T.; Bukowieck, A.  <i>Schweiz. Arch. Angew. Wiss. Tech.</i> <u>1949</u> , 15, 299-307.
CRITICAL EVALUATION: continued	
Solvent	L <sup>a</sup>
paraffin oil	0.159
benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	0.219
p-xylene; C <sub>8</sub> H <sub>10</sub> ; [106-42-3]	0.220
dimethoxymethane (methylal); C <sub>3</sub> H <sub>8</sub> O <sub>2</sub> ; [109-87-5]	0.325
castor oil	0.151
water H <sub>2</sub> O; [7732-18-5]	0.033
aniline; C <sub>6</sub> H <sub>7</sub> N; [62-53-3]	0.107 <sup>b</sup>
1,4-dioxane; C <sub>4</sub> H <sub>8</sub> O <sub>2</sub> ; [123-91-1]	0.174 <sup>b</sup>
2,4,6-trimethy-1,3,5-trioxane (paraldehyde); C <sub>6</sub> H <sub>12</sub> O <sub>3</sub> ; [123-63-7]	0.281 <sup>b</sup>
ethylene glycol; C <sub>2</sub> H <sub>6</sub> O <sub>2</sub> ; [107-21-1]	0.014 <sup>b</sup>
1,2,3-propanetriol (glycerin); C <sub>3</sub> H <sub>8</sub> O <sub>3</sub> ; [56-81-5]	0.008 <sup>b</sup>
<sup>a</sup> Ostwald coefficient.	
<sup>b</sup> Determined by physical method described in paper.	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Tetrachloromethane; CCl <sub>4</sub> ; [56-23-5]	<b>ORIGINAL MEASUREMENTS:</b> Metschl, J. <i>J. Phys. Chem.</i> <u>1924</u> , 28, 417-37.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="273 493 1006 640"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^4</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>9.74</td> <td>0.225</td> <td>0.246</td> </tr> </tbody> </table> <p>The compiler calculated the mole fraction and Ostwald coefficient values.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	9.74	0.225	0.246
T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L						
298.15	9.74	0.225	0.246						
<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> The degassed solvent is saturated with oxygen at 6 to 10 different pressures between 1.5 and 4.5 atm.  The pressure is reduced to one atm, and the "supersaturated gas" is shaken out of the solvent and measured.  The slope of a plot of the volume of gas reduced to standard conditions shaken out of 100 cm <sup>3</sup> of solvent <i>vs.</i> the pressure of saturation is nearly identical to the solubility-pressure graph (Henry's law). The slope of the curve is used to obtain the Bunsen coefficient. From the method of calculation the value represents the volume of gas shaken out of the solvent when the pressure is reduced from 2 to 1 atm.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Commercial cylinder. Prepared by Linde process, 97 per cent pure. (2) Tetrachloromethane. Chemically pure. Dried over KOH and distilled.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b>								

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Tetrachloromethane; CCl<sub>4</sub>; [56-23-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Horiuti, J.</p> <p><i>Sci. Papers Inst. Phys. Chem. Res. (Tokyo) (Jpn)</i> <u>1931/32</u>, 17, 125-256.</p>																																																																			
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus consists of a gas buret, a solvent reservoir, and an absorption pipet. The volume of the pipet was determined at various meniscus heights by weighing a quantity of water. The meniscus height was read with a cathetometer.</p> <p>The dry gas introduced into the degassed solvent. The gas and solvent are mixed with a magnetic stirrer until saturation. Care taken to prevent solvent vapor from mixing with the solute gas in the gas buret. The volume of gas was determined from a gas buret reading, the volume of the solvent was determined from the meniscus height in the absorption pipet.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Prepared in the laboratory by heating potassium permanganate (Kahlbaum). Gas fractionated in liquid air.</p> <p>(2) Tetrachloromethane. Kahlbaum. Dried, and distilled. Normal boiling point 76.74°C.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.05</math></p>																																																																			
<p>The Ostwald coefficient was measured at a total pressure of one atm. The Bunsen coefficient and the mole fraction solubility values were calculated by the compiler for a gas pressure of one atm assuming the gas to behave ideally and the Ostwald coefficient to be independent of pressure.</p>																																																																				



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Tetrachloromethane; CCl <sub>4</sub> ; [56-23-5]	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K. Candidates thesis, <u>1970</u> , Leningrad.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever								
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> Probably used volumetric method described by Naumenko <i>et al.</i> (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> No information.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I. A. <i>Zh. Fiz. Khim.</i> <u>1979</u> , <i>53</i> , 1989. 2. Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prkl. Khim.</i> <u>1969</u> , <i>42</i> , 2090.								

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1,2-Dibromo-1,1,2,3,3,3-hexafluoropropane; C<sub>3</sub>F<sub>6</sub>Br<sub>2</sub>; [661-95-0]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, <i>9</i>, 137-46.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
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<p>* appears to be the Ostwald coefficient x 10<sup>2</sup>, units were stated as ml/100 ml (total pressure was the barometric pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using the density given in source</p>							
<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) A 3M sample, boiling pt. 72.8°C.</p> <p>ESTIMATED ERROR: <math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p>						
<p>REFERENCES:</p>							

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1,1,1,3,3,4,4,5,5,5-decafluoro-2-(trifluoromethyl)-2-pentanol; C<sub>8</sub>HF<sub>13</sub>O; [67728-22-7]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lawson, D.D.; Moacanin, J.; Scherer, K.V.; Terranova, T.J.; Ingham, J.D.</p> <p><i>J. Fluorine Chem.</i> <u>1978</u>, <i>12</i>, 221-36.</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved sample of liquid analysed by gas chromatography using a molecular sieve to retain the fluorocarbon. Details not given in source but method in ref. (1) was equivalent.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Prepared by Jet Propulsion Laboratory, Caltech.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 3\%</math></p> <p style="text-align: center;">(estimated by compiler)</p> <p>REFERENCES:</p> <p>1. Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, <i>9</i>, 137-146.</p>						

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<b>METHOD/APPARATUS/PROCEDURE:</b> The oxygen solubility was determined by a volumetric gas method.  The liquids were deaerated for 20 to 30 minutes under reduced pressure with the aid of an oil pump. The deaeration was monitored from the readings of a thermocouple vacuum gage.  The liquids were saturated with oxygen under an oxygen partial pressure of about 760 mmHg at 25°C for 2 hours. The amount of gas absorbed was then determined.  Details of the method are given in an earlier paper (1).	<b>SOURCE AND PURITY OF MATERIALS:</b>  The source and purity of the materials were not given.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.1$ $\delta \alpha/\alpha = 0.023$ (relative)  <b>REFERENCES:</b> 1. Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim. 1969, 42, 2090.</i>																																				

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VARIABLES:		PREPARED BY:		
T/K = 273.15 - 353.15 Total P/kPa = 101.325		M. E. Derrick H. L. Clever		
EXPERIMENTAL VALUES:				
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	
273.15	0.7776	0.1748	0.1748	
283.15	0.7815	0.1740	0.1804	
293.15	0.7874	0.1736	0.1863	
303.15	0.7902	0.1725	0.1915	
313.15	0.7966	0.1722	0.1974	
323.15	0.8023	0.1717	0.2031	
333.15	0.8105	0.1717	0.2094	
343.15	0.8213	0.1722	0.2163	
353.15	0.8250	0.1712	0.2214	
Smoothed Data: $\ln X_1 = -9.51003 + 3.0621/(T/100) + 1.2243 \ln (T/100)$				
Standard error about the regression line = $1.63 \times 10^{-6}$				
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	
273.15	0.7780	323.15	0.8036	
283.15	0.7815	333.15	0.8108	
293.15	0.7859	343.15	0.8184	
303.15	0.7911	353.15	0.8266	
313.15	0.7970			
The Ostwald coefficient was measured at a total pressure of one atm. The Bunsen coefficient and the mole fraction solubility values were calculated by the compiler for a gas pressure of one atm assuming the gas to behave ideally and the Ostwald coefficient to be independent of pressure.				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
The apparatus consists of a gas buret, a solvent reservoir, and an absorption pipet. The volume of the pipet was determined at various meniscus heights by weighing a quantity of water. The meniscus height was read with a cathetometer.		(1) Oxygen. Prepared in the laboratory by heating potassium permanganate (Kahlbaum). Gas fractionated in liquid air.		
The dry gas introduced into the degassed solvent. The gas and solvent are mixed with a magnetic stirrer until saturation. Care taken to prevent solvent vapor from mixing with the solute gas in the gas buret. The volume of gas was determined from a gas buret reading, the volume of the solvent was determined from the meniscus height in the absorption pipet.		(2) Chlorobenzene. Kahlbaum. Dried, and distilled. Normal boiling point 131.96°C.		
		ESTIMATED ERROR:		
		$\delta T/K = 0.05$		
If the gas and solution are assumed to be ideal the fitted equation gives the following thermodynamic values.				
T/K	$\Delta G^\circ/kJ \text{ mol}^{-1}$	$\Delta H^\circ/J \text{ mol}^{-1}$	$\Delta S^\circ/J \text{ K}^{-1} \text{ mol}^{-1}$	$\Delta C_p^\circ/J \text{ K}^{-1} \text{ mol}^{-1}$
273.15	16.258	235.5	-58.66	10.18
298.15	17.713	489.0	-57.77	10.18

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Chlorohexane; C <sub>6</sub> H <sub>11</sub> Cl; [544-10-5]	<b>ORIGINAL MEASUREMENTS:</b> Guerry, D. Jr. Ph.D. thesis, 1944, Vanderbilt University, Nashville, TN.												
<b>VARIABLES:</b> T/K = 293-298 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="280 479 1005 632"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^4</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>293.15</td> <td>13.5</td> <td>0.220</td> <td>0.236</td> </tr> <tr> <td>298.15</td> <td>13.5</td> <td>0.220</td> <td>0.240</td> </tr> </tbody> </table> <p>The Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	293.15	13.5	0.220	0.236	298.15	13.5	0.220	0.240
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<b>METHOD/APPARATUS/PROCEDURE:</b> A Van Slyke-Neill Manometric Apparatus manufactured by the Eimer and Amend Co. was used. The procedure of Van Slyke (1) for pure liquids was modified (2) so that small solvent samples (2 cm <sup>3</sup> ) could be used with almost complete recovery of the sample. An improved temperature control system was used.													
<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Reduction Co. Purity 99.5 per cent. (2) 1-Chlorohexane. Eastman Kodak Co. Purified, distilled from P <sub>2</sub> O <sub>5</sub> in a N <sub>2</sub> atm. B.p. (746.6 mmHg) t/°C 134.66 (corr.). Refractive index, density, and vapor pressure data are in the thesis.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ <b>REFERENCES:</b> 1. Van Slyke, D. D. <i>J. Biol. Chem.</i> 1939, 130, 545. 2. Ijams, C. C. Ph.D. thesis, 1941 Vanderbilt University												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hexafluorobenzene; C <sub>6</sub> F <sub>6</sub> ; [392-56-3]	<b>ORIGINAL MEASUREMENTS:</b> Evans, D. F.; Battino, R. <i>J. Chem. Thermodyn.</i> <u>1971</u> , <i>3</i> , 753-60.																																						
<b>VARIABLES:</b> T/K = 282.92 - 297.81 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																																						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="319 462 984 662"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>282.92</td> <td>2.479</td> <td>0.491</td> <td>0.509</td> </tr> <tr> <td>283.21</td> <td>2.468</td> <td>0.489</td> <td>0.507</td> </tr> <tr> <td>297.56</td> <td>2.417</td> <td>0.469</td> <td>0.511</td> </tr> <tr> <td>297.81</td> <td>2.422</td> <td>0.471</td> <td>0.513</td> </tr> </tbody> </table> <p>The Bunsen coefficients were calculated by the compiler.            The solubility values were adjusted to an oxygen partial pressure of 101.325 kPa (1 atm) by Henry's law.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -973.1 + 53.371 T</math>            Std. Dev. <math>\Delta G^\circ = 5.7</math>, Coef. Corr. = 0.9992  <math>\Delta H^\circ/\text{J mol}^{-1} = -973.1</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = 53.371 T</math></p> <table border="1" data-bbox="404 909 880 1132"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>278.15</td> <td>2.48</td> <td>13,872</td> </tr> <tr> <td>283.15</td> <td>2.46</td> <td>14,139</td> </tr> <tr> <td>288.15</td> <td>2.45</td> <td>14,406</td> </tr> <tr> <td>293.15</td> <td>2.43</td> <td>14,673</td> </tr> <tr> <td>298.15</td> <td>2.41</td> <td>14,939</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	282.92	2.479	0.491	0.509	283.21	2.468	0.489	0.507	297.56	2.417	0.469	0.511	297.81	2.422	0.471	0.513	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^\circ/\text{J mol}^{-1}$	278.15	2.48	13,872	283.15	2.46	14,139	288.15	2.45	14,406	293.15	2.43	14,673	298.15	2.41	14,939
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans, and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3). Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid N <sub>2</sub> trap until the permanent gas residual pressure drops to 5 microns. Solubility Determination. The degassed solvent is passed in a thin film down a glass helical tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air Products and Chemicals Co. 99.6 per cent. (2) Hexafluorobenzene. Imperiel Smelting Co., Avnomouth, U.K. GC purity 99.7%, density, $\rho_{298.15} = 1.60596 \text{ g cm}^{-3}$ . Purification described <i>Anal. Chem.</i> 1968, <i>40</i> , 224. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.03$ $\delta P/\text{mmHg} = 0.5$ $\delta X_1/X_1 = 0.005$ <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> 1948, 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u> , <i>45</i> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , <i>43</i> , 806.																																						

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<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Imperial Smelting Co Chemicals Ltd., boiling pt. 81.5°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						



<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1,1,1,2,2,3,3,5,5,5-Decafluoro-4-methoxy-4-(trifluoromethyl)-pentane; C<sub>7</sub>H<sub>3</sub>F<sub>13</sub>O; [67728-33-0]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lawson, D.D.; Moacanin, J.; Scherer, K.V.; Terranova, T.F.; Ingham, J.D.</p> <p><i>J. Fluorine Chem.</i> <u>1978</u>, 12, 221-36.</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved sample of liquid analysed by gas chromatography using a molecular sieve to retain the fluorocarbon. Details not given in source but method in ref. (1) was equivalent.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Prepared by Jet Propulsion Laboratory, Caltech.</p>						
<p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 3\%</math></p> <p style="text-align: center;">(estimated by compiler)</p>							
<p>REFERENCES:</p> <p>1. Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>							

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1-Bromoheptane; C <sub>7</sub> H <sub>15</sub> Br; [629-04-9]	<b>ORIGINAL MEASUREMENTS:</b> Ijams, C. C. Ph.D. thesis, <u>1941</u> , Vanderbilt University, Nashville, TN.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="290 466 1014 593"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>1.32</td> <td>0.189</td> <td>0.206</td> </tr> </tbody> </table> <p>The mole fraction and Ostwald coefficient values were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	1.32	0.189	0.206
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1-Bromo-1,1,2,2,3,3,4,4,5,6,6,6-dodecafluoro-5-(trifluoromethyl)-hexane; C<sub>7</sub>F<sub>15</sub>Br; [50279-29-3]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Pennwalt Corp. sample, boiling pt. 120°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						

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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Pennwalt Corp sample boiling pt. 108°C.</p>						
	<p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p>						
	<p>REFERENCES:</p>						

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Undecafluoro (trifluoromethyl) cyclohexane, (Perfluoromethyl-cyclohexane); C <sub>7</sub> F <sub>14</sub> ; [355-02-2]	<b>ORIGINAL MEASUREMENTS:</b> Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.  <i>J. Fluorine Chem.</i> <u>1977</u> , 9, 137-46.						
<b>VARIABLES:</b>  T/K = 298	<b>PREPARED BY:</b>  C. L. Young						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="106 512 1218 701"> <thead> <tr> <th data-bbox="106 512 405 608">T/K</th> <th data-bbox="405 512 711 608">Solubility *</th> <th data-bbox="711 512 1218 608">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td data-bbox="106 608 405 701">298.15</td> <td data-bbox="405 608 711 701">57.2</td> <td data-bbox="711 608 1218 701">0.00456</td> </tr> </tbody> </table> <p data-bbox="155 942 988 1025">* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p data-bbox="155 1055 1060 1109">+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	57.2	0.00456
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$					
298.15	57.2	0.00456					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 $\mu$ l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) ISC Chemicals, Avonmouth, UK sample, boiling pt 76°C.						
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 2\%$							
<b>REFERENCES:</b>							

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hexadecafluoroheptane or Perfluoroheptane; C <sub>7</sub> F <sub>16</sub> ; [335-57-9]	<b>ORIGINAL MEASUREMENTS:</b> Gjaldbaek, J. C. <i>Acta Chem. Scand.</i> <u>1952</u> , <i>6</i> , 623-33.												
<b>VARIABLES:</b> T/K = 298.11 - 298.15 Total P/kPa = 101.325	<b>PREPARED BY:</b> J. Chr. Gjaldbaek												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="335 467 1006 626"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.11</td> <td>5.51</td> <td>0.544</td> <td>0.594</td> </tr> <tr> <td>298.15</td> <td>5.55</td> <td>0.548</td> <td>0.598</td> </tr> </tbody> </table> <p>The mole fraction and Ostwald solubility values were calculated by the compiler.</p>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	298.11	5.51	0.544	0.594	298.15	5.55	0.548	0.598
T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L										
298.11	5.51	0.544	0.594										
298.15	5.55	0.548	0.598										
<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> A calibrated all-glass combined manometer and bulb was enclosed in an air thermostat and shaken until equilibrium. Mercury was used for calibration and as the confining liquid. The solvents were degassed in the apparatus. Details are in references 1 and 2. The absorbed volume of gas was calculated from the initial and final amounts, both saturated with solvent vapor. The amount of solvent was determined by the weight of displaced mercury. The saturation of the liquid with the gas was carried out close to atmospheric pressure. The solubility values were reported for one atmosphere gas pressure assuming Henry's law is obeyed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1)Oxygen. Prepared by heating KMnO <sub>4</sub> , 99.7 percent O <sub>2</sub> , 0.3 percent N <sub>2</sub> . (2)Hexadecafluoroheptane. E. I. duPont Co. Distilled, boiling point 82.3 - 82.4°C at 753.7 mmHg. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta X_1/X_1 = 0.015$ <b>REFERENCES:</b> 1. Lannung, A. <i>J. Am. Chem. Soc.</i> <u>1930</u> , <i>52</i> , 68. 2. Gjaldbaek, J. C. <i>Acta Chem. Scand.</i> <u>1952</u> , <i>6</i> , 623.												

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Benzene, bis(trifluoromethyl)-; C<sub>6</sub>H<sub>4</sub>(CF<sub>3</sub>)<sub>2</sub>; [26545-61-9]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
<p>EXPERIMENTAL VALUES:</p> <table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Solubility *</th> <th style="text-align: center;">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">35.4</td> <td style="text-align: center;">0.00631</td> </tr> </tbody> </table>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	35.4	0.00631
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$					
298.15	35.4	0.00631					
<p>* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>							
<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume for oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Pierce Chem. Co. sample, boiling pt. 116°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 2-Ethoxy-1,1,1,3,3,4,4,5,5,5-decafluoro-2-(trifluoromethyl)-pentane; C<sub>8</sub>H<sub>5</sub>F<sub>13</sub>O; [67728-34-1]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lawson, D.D.; Moacanin, J.; Scherer, K.V.; Terranova, T.F.; Ingham, J.D.</p> <p><i>J. Fluorine Chem.</i> <u>1978</u>, <i>12</i>, 221-36.</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved sample of liquid analysed by gas chromatography using a molecular sieve to retain the fluorocarbon. Details not given in source but method in ref. (1) was equivalent.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Prepared by Jet Propulsion Laboratory, Caltech.</p>						
	<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 3\%</math></p> <p>(estimated by compiler)</p>						
	<p>REFERENCES:</p> <p>1. Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, <i>9</i>, 137-46.</p>						



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Heptafluorotetrahydro(nonafluorobutyl)-furan or Perfluorobutyl perfluorotetrahydrofuran or FC-80; C <sub>8</sub> F <sub>16</sub> O; [40464-54-8]	<b>ORIGINAL MEASUREMENTS:</b> Tham, M. K.; Walker, R. D. Jr.; Modell, J. H. <i>J. Chem. Eng. Data</i> <u>1973</u> , <i>18</i> , 385-6.																																													
<b>VARIABLES:</b> T/K = 298.15 - 323.15 P/kPa = 101.325	<b>PREPARED BY:</b> T. D. Kittredge H. L. Clever																																													
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="306 472 1027 701"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>298.15</td><td>5.60</td><td>0.536</td><td>0.585</td></tr> <tr><td>303.15</td><td>5.58</td><td>0.530</td><td>0.588</td></tr> <tr><td>310.15</td><td>5.50</td><td>0.517</td><td>0.587</td></tr> <tr><td>313.15</td><td>5.50</td><td>0.514</td><td>0.589</td></tr> <tr><td>323.15</td><td>5.40</td><td>0.497</td><td>0.588</td></tr> </tbody> </table> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.</p> <p>Smoothed Data: <math>\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -1187.0 + 47.073 T</math></p> <p>Std. dev. <math>\Delta G^{\circ} = 6.0</math>, Coef. corr. = 0.9997</p> <p><math>\Delta H^{\circ}/J \text{ mol}^{-1} = -1187.0</math>, <math>\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -47.073</math></p> <table border="1" data-bbox="409 913 937 1158"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^{\circ}/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>298.15</td><td>5.61</td><td>12,848</td></tr> <tr><td>303.15</td><td>5.57</td><td>13,083</td></tr> <tr><td>308.15</td><td>5.52</td><td>13,319</td></tr> <tr><td>313.15</td><td>5.48</td><td>13,554</td></tr> <tr><td>318.15</td><td>5.44</td><td>13,789</td></tr> <tr><td>323.15</td><td>5.41</td><td>14,025</td></tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	298.15	5.60	0.536	0.585	303.15	5.58	0.530	0.588	310.15	5.50	0.517	0.587	313.15	5.50	0.514	0.589	323.15	5.40	0.497	0.588	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$	298.15	5.61	12,848	303.15	5.57	13,083	308.15	5.52	13,319	313.15	5.48	13,554	318.15	5.44	13,789	323.15	5.41	14,025
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus and procedure described by Shoor, Walker and Gubbins (1) were used. The solvent was placed in a saturator immersed in a constant temperature bath. The gas was dispersed through the liquid by a fritted glass disk at a rate of about 40 cm <sup>3</sup> m <sup>-1</sup> . After an initial equilibration period of 30 minutes, samples were withdrawn with a Hamilton microliter syringe at 15 minute intervals and analyzed chromatographically (Perkin-Elmer 900 gas chromatograph with thermal conductivity detector). The solubility at one atmosphere partial pressure of the gas was the mean value of three consecutive samples which agreed within the limits of experimental error.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1)Oxygen. Source not given. Minimum purity 99.6 per cent. (2)FC-80. Minnesota Mining and Manufacturing Co. A mixture of several isomers. The authors also measured the density and viscosity of the solvent at several temperatures. At 298.15 K the density is 1.7657 g cm <sup>-3</sup> and the viscosity is 1.3953 centipoise.																																													
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta X_1/X_1 = 0.005$ (Compiler)																																														
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1-Bromo-1,1,2,2,3,3,4,4,5,5,6,6,7,7,8,8,8-heptadecalfluoro-octane (Perfluorooctyl bromide); C<sub>8</sub>F<sub>17</sub>Br; [423-55-2]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9,137-46.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
<p>EXPERIMENTAL VALUES:</p> <table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center; width: 20%;">T/K</th> <th style="text-align: center; width: 30%;">Solubility *</th> <th style="text-align: center; width: 50%;">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">52.7</td> <td style="text-align: center;">0.00566</td> </tr> </tbody> </table>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	52.7	0.00566
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<p>* appears to be the Ostwald coefficient <math>\times 10^2</math>, units were stated as ml/100 ml (total pressure was the barometric pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using the density given in source</p>							
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) A 3M sample, boiling pt 140.5°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Octadecafluorooctane (Perfluorooctane); C<sub>8</sub>F<sub>18</sub>; [307-34-6]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, <i>9</i>, 137-46.</p>						
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298.15	52.1	0.00534					
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COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Zander, R.		
(2) FC-75 which is mostly 2,2,3,3,4-4,5-heptafluorotetrahydro-5-(nonafluorobutyl)furan or perfluorobutyltetrahydrofuran; C <sub>8</sub> F <sub>16</sub> O; [335-36-4]		Res. exp. Med. <u>1974</u> , 164, 97-109.		
VARIABLES:		PREPARED BY:		
T/K= 283.15 - 323.15 P/kPa= 12 - 101		H. L. Clever		
EXPERIMENTAL VALUES:				
Temperature Range T/K	Gas Phase <sup>1</sup> Volume Per Cent Oxygen	Oxygen Partial Pressure <sup>2</sup> p/mmHg	Bunsen Coefficient Regression Equation $\alpha/\text{cm}^3 \text{ cm}^{-3} \text{ atm}^{-1}$	Number of Experimental Points
283.15 - 323.15 (10 - 50 °C)	12	91.2	$\alpha = 0.369 - 0.00041 t/^\circ\text{C}$	24
	35	266	$\alpha = 0.466 - 0.00073 t/^\circ\text{C}$	20
	100	760	$\alpha = 0.491 - 0.00096 t/^\circ\text{C}$	20
<p><sup>1</sup> The gas phase consists of oxygen, water at its equilibrium vapor pressure, solvent (FC-75) at its equilibrium vapor pressure, and nitrogen to bring the total pressure to near one atm. The per cent oxygen in the gas phase was experimentally determined by a Scholander gas analyzer.</p> <p><sup>2</sup> The oxygen partial pressure was calculated by the compiler with the assumption that the gas mixture behaved ideally and that the total pressure was 760 mmHg.</p>				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
<p>Equilibration between the gas and liquid phases was established in 45 minutes in a Tonometer of the Laue (1) design.</p> <p>The oxygen content of the gas phase was determined by a Scholander gas analyzer (see footnote 1 above).</p> <p>The saturated solution was transferred to a Van Slyke apparatus for the solubility determination.</p>		<p>(1) Oxygen. No information.</p> <p>(2) FC-75. Minnesota Mining and Manufacturing Co. Used as received.</p>		
<p>The 64 experimental measurements made at temperatures of 10, 30, and 50 °C were fitted to the equations in the table above. The smoothed data were used to construct a graph of Bunsen coefficient vs. oxygen partial pressure, and a nomogram for the volume percent oxygen as a function of oxygen partial pressure and temperature.</p> <p>The solubility appears to depart from Henry's law above pressures of 100 mmHg oxygen.</p>		<p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.1</math>  <math>\delta \alpha/\alpha = 0.03</math> above 100 mmHg oxygen,  <math>0.05 - 0.10</math> below 100 mmHg.</p>		
		REFERENCES:		
		<p>1. Laue, D.  <i>Pflugers Arch. Gesamte Physiol. Menschen Tiere</i> <u>1951</u>, 254, 142.</p>		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) FC-80, which is mostly a mixture of isomers of perfluorobutyl-tetrahydrofuran. For example 2,2,3,3,4,4,5-heptafluorotetrahydro-5(nonafluorobutyl) furan; C <sub>8</sub> F <sub>16</sub> O; [335-36-4]	<b>ORIGINAL MEASUREMENTS:</b> Sargent, J. W.; Seffl, R. J. <i>Fed. Proc.</i> <u>1970</u> , <i>29</i> , 1699 - 1703.																
<b>VARIABLES:</b> T/K = 298.15, 310.15 Total P/kPa = 101.325	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="363 478 1097 674" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th colspan="2">Temperature</th> <th colspan="2">Oxygen Solubility</th> </tr> <tr> <th>t/°C</th> <th>T/K</th> <th>g O<sub>2</sub> 1000 g<sup>-1</sup></th> <th>cm<sup>3</sup> O<sub>2</sub> 100 cm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td>25</td> <td>298.15</td> <td>0.361</td> <td>48.8</td> </tr> <tr> <td>37</td> <td>310.15</td> <td>0.354</td> <td>48.5</td> </tr> </tbody> </table> <p data-bbox="363 707 1067 756" style="text-align: center;">The authors solubility, cm<sup>3</sup> O<sub>2</sub> 100 cm<sup>-3</sup>, appears to be the Ostwald coefficient times 100.</p>		Temperature		Oxygen Solubility		t/°C	T/K	g O <sub>2</sub> 1000 g <sup>-1</sup>	cm <sup>3</sup> O <sub>2</sub> 100 cm <sup>-3</sup>	25	298.15	0.361	48.8	37	310.15	0.354	48.5
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The equilibrium apparatus is a 50 cm<sup>3</sup> three neck flask equipped with a water condenser, a thermometer, and a gas dispersing tube extending below the fluid surface level. Between 25 and 35 cm<sup>3</sup> of solvent are placed in the flask. Gas is bubbled through the solvent for 2 - 3 h. An 80 micro-liter sample is slowly taken into a gas tight syringe. The sample is injected into a gas chromatograph. The results of three sampling and analyses are averaged.</p> <p>The chromatograph is an F and M Model 720 equipped with a thermal conductivity detector at 320 °C, and a 6' by ¼" stainless steel column packed with 13X molecular sieve at room temperature. The apparatus is calibrated with pure gas samples.</p> <p>Details of the procedure were furnished by R. D. Danielson of the 3 M Co.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Commercial cylinder. (2) FC-80. Minnesota Mining and Manufacturing Co. All H in an organic compound are replaced by F by Simons electrochemical process (1)																
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.1$ $\delta c/c = 0.01$ reproducibility = 0.05 absolute																	
<b>REFERENCES:</b> 1. Simons, J. H., Editor <i>Fluorine Chemistry</i> Academic Press, New York, <u>1950</u> .																	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1,1,1,2,2,3,3-Heptafluoro-4,4-bis (trifluoromethyl)-heptane; C <sub>9</sub> H <sub>7</sub> F <sub>13</sub> ; [67728-31-8]	<b>ORIGINAL MEASUREMENTS:</b> Lawson, D.D.; Moacanin, J.; Scherer, K.V.; Terranova, T.F.; Ingham, J.D. <i>J. Fluorine Chem.</i> <u>1978</u> , <i>12</i> , 221-36.						
<b>VARIABLES:</b>  T/K = 298	<b>PREPARED BY:</b>  C. L. Young						
<b>EXPERIMENTAL VALUES:</b>  <table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center; width: 20%;">T/K</th> <th style="text-align: center; width: 40%;">Solubility *</th> <th style="text-align: center; width: 40%;">Mole fraction <sup>+</sup> of oxygen <sub>x</sub>O<sub>2</sub></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">46.7</td> <td style="text-align: center;">0.00494</td> </tr> </tbody> </table>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen <sub>x</sub> O <sub>2</sub>	298.15	46.7	0.00494
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen <sub>x</sub> O <sub>2</sub>					
298.15	46.7	0.00494					
<p>* appears to be the Ostwald coefficient x 10<sup>2</sup>, units were stated as cm<sup>3</sup>O<sub>2</sub>/100 cm<sup>3</sup> (total pressure was assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>							
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved sample of liquid analysed by gas chromatography using a molecular sieve to retain the fluorocarbon. Details not given in source but method in ref.(1) was equivalent.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) Prepared by Jet Propulsion Laboratory, Caltech.						
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 3\%$ (estimated by compiler)							
<b>REFERENCES:</b> 1. Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr. <i>J. Fluorine Chem.</i> <u>1977</u> , <i>9</i> , 137-146.							

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1,1,1,2,2,3,3,5,5,5-Decafluoro-4-propoxy-4-(trifluoromethyl)-pentane; C <sub>9</sub> H <sub>7</sub> F <sub>13</sub> O; [67728-35-2]	<b>ORIGINAL MEASUREMENTS:</b> Lawson, D.D.; Moacanin, J.; Scherer, K.V.; Terranova, T.F.; Ingham, J.D.  <i>J. Fluorine Chem.</i> <u>1978</u> , <i>12</i> , 221-36.	
<b>VARIABLES:</b>  T/K = 298	<b>PREPARED BY:</b>  C. L. Young	
<b>EXPERIMENTAL VALUES:</b>		
T/K  298.15	Solubility *  45.8	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$  0.00509
<p>* appears to be the Ostwald coefficient x 10<sup>2</sup>, units were stated as cm<sup>3</sup>O<sub>2</sub>/100 cm<sup>3</sup> (total pressure was assumed to be 1 atmosphere)</p> <p><sup>+</sup> calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>		
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1-Chloro-1,1,2,2,3,3,4,4,5,5,6,6,7,8,8,8-hexadecafluoro-7-(trifluoromethyl)-Octane; C<sub>9</sub>F<sub>19</sub>Cl; [63243-38-9]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>						
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume for oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Pennwalt Corp. boiling pt. 151°C.</p> <p>ESTIMATED ERROR: <math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						



COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Eicosfluorononane, (Perfluorononane); C <sub>9</sub> F <sub>20</sub> ; [375-96-2]		ORIGINAL MEASUREMENTS: Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr. <i>J. Fluorine Chem.</i> 1977, 9, 137-46.
VARIABLES:  T/K = 298		PREPARED BY:  C. L. Young
EXPERIMENTAL VALUES:		
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen <sub>O<sub>2</sub></sub>
298.15	49.6	0.00535
<p>* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>		
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		ESTIMATED ERROR: $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 2\%$
		REFERENCES:

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1,1,1,2,2,3,3,4,4,5,5,6,6-Tridecafluoro-6-[1,2,2,2-tetrafluoro-1-(trifluoromethyl)ethoxy]-hexane or Perfluoro-1-isopropoxy hexane or Caroxin-F; C <sub>9</sub> F <sub>20</sub> O; [37340-18-4] or [41719-16-8]	<b>ORIGINAL MEASUREMENTS:</b> Tham, M. K.; Walker, R. D. Jr.; Modell, J. H. <i>J. Chem. Eng. Data</i> <u>1973</u> , <i>18</i> , 385-6.																																													
<b>VARIABLES:</b> T/K = 298.15 - 323.15 P/kPa = 101.325	<b>PREPARED BY:</b> T. D. Kittredge H. L. Clever																																													
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="309 456 1037 676"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr><td>298.15</td><td>6.60</td><td>0.515</td><td>0.562</td></tr> <tr><td>303.15</td><td>6.57</td><td>0.509</td><td>0.565</td></tr> <tr><td>310.15</td><td>6.48</td><td>0.497</td><td>0.564</td></tr> <tr><td>313.15</td><td>6.47</td><td>0.494</td><td>0.566</td></tr> <tr><td>323.15</td><td>6.30</td><td>0.474</td><td>0.561</td></tr> </tbody> </table> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.</p> <p>Smoothed Data: <math>\Delta G^\circ/\text{J mol}^{-1} = -RT \ln X_1 = -1495.4 + 46.727 T</math></p> <p>Std. dev. <math>\Delta G^\circ = 9.9</math>, Coef. corr. 0.9997</p> <p><math>\Delta H^\circ/\text{J mol}^{-1} = -1495.4</math>, <math>\Delta S^\circ/\text{J K}^{-1} \text{ mol}^{-1} = -46.727</math></p> <table border="1" data-bbox="440 887 980 1127"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th><math>\Delta G^\circ/\text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr><td>298.15</td><td>6.63</td><td>12,436</td></tr> <tr><td>303.15</td><td>6.56</td><td>12,670</td></tr> <tr><td>308.15</td><td>6.50</td><td>12,903</td></tr> <tr><td>313.15</td><td>6.44</td><td>13,137</td></tr> <tr><td>318.15</td><td>6.38</td><td>13,371</td></tr> <tr><td>323.15</td><td>6.32</td><td>13,604</td></tr> </tbody> </table>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	6.60	0.515	0.562	303.15	6.57	0.509	0.565	310.15	6.48	0.497	0.564	313.15	6.47	0.494	0.566	323.15	6.30	0.474	0.561	T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ/\text{J mol}^{-1}$	298.15	6.63	12,436	303.15	6.56	12,670	308.15	6.50	12,903	313.15	6.44	13,137	318.15	6.38	13,371	323.15	6.32	13,604
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<b>METHOD/APPARATUS/PROCEDURE:</b> The method of Shoor, Walker and Gubbins (1) was used. The solvent was placed in a saturator immersed in a constant temperature bath. The gas was dispersed through the liquid by a fritted glass disk at a rate of about 40 cm <sup>3</sup> m <sup>-1</sup> . After an initial equilibration period of 30 minutes, samples were withdrawn at 15 minute intervals and analyzed chromatographically (Perkin-Elmer 900 gas chromatograph with thermal conductivity detector). The solubility at one atmosphere partial pressure of the gas was the mean value of three consecutive samples which agreed within the limits of experimental error.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1)Oxygen. Source not given. Minimum purity 99.6 per cent. (2)Caroxin-F. Allied Chemical Corp. Purity > 99.9 per cent as supplied. The authors also measured the density and viscosity of the solvent at several temperatures. At 298.15 K the density is 1.7449 g cm <sup>-3</sup> and the viscosity is 1.5405 centipoise.																																													
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Octadecafluorodecahydronaphthalene, (Perfluorodecalin); C<sub>10</sub>F<sub>18</sub>; [306-94-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Imperial Smelting Co Chemicals Ltd, boiling pt. 142°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p>						
	<p>REFERENCES:</p>						

<b>COMPONENTS:</b> (1)Oxygen; O <sub>2</sub> ; [7782-44-7] (2)1,1,2,2,3,3,4,4-Octafluoro-1,4-bis(1,2,2,2-tetrafluoro-1-(trifluoromethyl)ethoxy) butane or Perfluoro-1,4- diisopropoxy butane or Caroxin-D; C <sub>10</sub> F <sub>22</sub> O <sub>2</sub> ; [23228-90-2]	<b>ORIGINAL MEASUREMENTS:</b> Tham, M. K.; Walker, R. D. Jr.; Modell, J. H.  <i>J. Chem. Eng. Data</i> <u>1973</u> , <i>18</i> , 385-6.																								
<b>VARIABLES:</b> T/K= 298.15 - 323.15 P/kPa =101.325	<b>PREPARED BY:</b> T. D. Kittredge H. L. Clever																								
<b>EXPERIMENTAL VALUES:</b>																									
<table border="1"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>6.50</td> <td>0.449</td> <td>0.490</td> </tr> <tr> <td>303.15</td> <td>6.40</td> <td>0.439</td> <td>0.487</td> </tr> <tr> <td>310.15</td> <td>6.30</td> <td>0.428</td> <td>0.486</td> </tr> <tr> <td>313.15</td> <td>6.28</td> <td>0.424</td> <td>0.486</td> </tr> <tr> <td>323.15</td> <td>6.20</td> <td>0.412</td> <td>0.487</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	298.15	6.50	0.449	0.490	303.15	6.40	0.439	0.487	310.15	6.30	0.428	0.486	313.15	6.28	0.424	0.486	323.15	6.20	0.412	0.487
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<p>Smoothed Data: <math>\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -1489.7 + 46.900 T</math>            Std. dev. <math>\Delta G^{\circ} = 8.9</math>, Coef. corr. = 0.9999  <math>\Delta H^{\circ}/J.\text{mol}^{-1} = -1489.7</math>, <math>\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -46.900</math></p> <table border="1"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^{\circ}/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>6.47</td> <td>12,494</td> </tr> <tr> <td>303.15</td> <td>6.41</td> <td>12,728</td> </tr> <tr> <td>308.15</td> <td>6.35</td> <td>12,963</td> </tr> <tr> <td>313.15</td> <td>6.29</td> <td>13,197</td> </tr> <tr> <td>318.15</td> <td>6.23</td> <td>13,432</td> </tr> <tr> <td>323.15</td> <td>6.18</td> <td>13,666</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$	298.15	6.47	12,494	303.15	6.41	12,728	308.15	6.35	12,963	313.15	6.29	13,197	318.15	6.23	13,432	323.15	6.18	13,666			
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<b>AUXILIARY INFORMATION</b>																									
<b>METHOD/APPARATUS/PROCEDURE:</b> The method of Shoor, Walker and Gubbins was used (1). The solvent was placed in a saturator immersed in a constant temperature bath. The gas was bubbled through the liquid by a fritted glass disk for 30 minutes, then analyzed at 15 minute intervals by gas chromatography. The solubility corrected to one atm partial pressure of the gas was the mean value of three consecutive samples which agree within the limits of experimental error.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1)Oxygen. Source not given. Minimum purity 99.6 per cent. (2)Caroxin-D. Allied Chemical Corp. Purity > 99.9 per cent as supplied. The authors also measured the density and viscosity of the solvent. At 298.15 K the density is 1.7465 g cm <sup>-3</sup> and the viscosity is 2.0579 centi poise.  <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta X_1/X_1 = 0.005(\text{compiler})$  <b>REFERENCES:</b> 1. Shoor, S. K.; Walker, R. D.; Gubbins, K. E. <i>J. Phys. Chem.</i> <u>1969</u> , <i>73</i> , 312.																								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1,1,1,2,3,3-hexafluoro-2 (heptafluoropropoxy)-3-[1,2,2- trifluoro-2-(1,2,2,2-tetra- fluoroethoxy)-1-(trifluoromethyl) ethoxy]-propane; C <sub>11</sub> HF <sub>23</sub> O <sub>3</sub> ; [3330-16-3]	<b>ORIGINAL MEASUREMENTS:</b> Wesseler, E.P.; Iltis, R; Clark, L.C. Jr. <i>J. Fluorine Chem.</i> <u>1977</u> , <i>9</i> , 137-46.						
<b>VARIABLES:</b> T/K =298	<b>PREPARED BY:</b> C. L. Young						
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Solubility *</th> <th style="text-align: center;">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">47.3</td> <td style="text-align: center;">0.00683</td> </tr> </tbody> </table> <p>* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	47.3	0.00683
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$					
298.15	47.3	0.00683					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 $\mu$ l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume for oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) DuPont sample, boiling pt. 152°C.						
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 2\%$							
<b>REFERENCES:</b>							

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 1,1,1,7,7,7-Hexafluoro-2,2,6,6-tetrakis (trifluoromethyl)-heptane; C<sub>11</sub>H<sub>6</sub>F<sub>18</sub>; [67728-37-4]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Lawson, D.D.; Moacanin, J.; Scherer, K.V.; Terranova, T.F.; Ingham, J.D.</p> <p><i>J. Fluorine Chem.</i> <u>1978</u>, <i>12</i>, 221-36.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved sample of liquid analysed by gas chromatography using a molecular sieve to retain the fluorocarbon. Details not given in source but method in ref.(1) was equivalent.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Prepared by Jet Propulsion Laboratory, Caltech.</p> <p>ESTIMATED ERROR:  <math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 3\%</math>        (estimated by compiler)</p> <p>REFERENCES:</p> <p>1. Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, <i>9</i>, 137-46.</p>						



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-3] (2) Heptadecafluorodecahydro (trifluoromethyl)-Naphthalene, (Perfluoromethyldecalin); C <sub>11</sub> F <sub>20</sub> ; [51294-16-7]	<b>ORIGINAL MEASUREMENTS:</b> Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.  <i>J. Fluorine Chem.</i> <u>1977</u> , <i>9</i> , 137-46.						
<b>VARIABLES:</b>  T/K = 298	<b>PREPARED BY:</b>  C. L. Young						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="106 465 1234 711"> <thead> <tr> <th data-bbox="106 465 409 608">T/K</th> <th data-bbox="413 465 668 608">Solubility *</th> <th data-bbox="672 465 1234 608">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td data-bbox="106 614 409 711">298.15</td> <td data-bbox="413 614 668 711">38.4</td> <td data-bbox="672 614 1234 711">0.00406</td> </tr> </tbody> </table> <p data-bbox="106 1001 1234 1089">* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p data-bbox="106 1109 1234 1176">+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	38.4	0.00406
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$					
298.15	38.4	0.00406					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 $\mu$ l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) Imperial Smelting Co. Chemicals Ltd, sample, boiling pt. 160°C.  <b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 2\%$  <b>REFERENCES:</b>						

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Tricyclo[3,3,1,3,7] decane tetradecafluorobis (trifluoromethyl)-(Perfluorodomethyladamantane); C<sub>12</sub>F<sub>20</sub>; [63267-58-3]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
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T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$					
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<p>* appears to be the Ostwald coefficient <math>\times 10^2</math> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>							
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Sun Ventures (Penn) sample, boiling pt. 175-180°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/K = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 3,6,9,12-Tetraoxapentadecane, 1,1,1,2,4,4,5,7,7,8,10,10,11,13, 13,14,14,15,15,15-eicosafuoro- 5,8,11-tris(trifluoromethyl)- C <sub>14</sub> HF <sub>29</sub> O <sub>4</sub> ; [26738-51-2]	<b>ORIGINAL MEASUREMENTS:</b> Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr. <i>J. Fluorine Chem.</i> <u>1977</u> , 9, 137-46.						
<b>VARIABLES:</b> T/K = 298	<b>PREPARED BY:</b> C. L. Young						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="113 532 1227 717"> <thead> <tr> <th data-bbox="113 532 422 638">T/K</th> <th data-bbox="422 532 668 638">Solubility *</th> <th data-bbox="668 532 1227 638">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td data-bbox="113 638 422 717">298.15</td> <td data-bbox="422 638 668 717">42.2</td> <td data-bbox="668 638 1227 717">0.00759</td> </tr> </tbody> </table> <p data-bbox="163 976 1106 1065">* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p data-bbox="163 1095 1031 1149">+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	42.2	0.00759
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298.15	42.2	0.00759					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 $\mu$ l Oressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) DuPont sample, boiling pt. 194°C.						
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 2\%$							
<b>REFERENCES:</b>							

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 3,6,9,12,15-Pentaoxaoctadecane, 1,1,1,2,4,4,5,7,7,8,10,10,11,13,13,14,16,16,17,17,18,18,18-tricosafluoro-5,8,11,14-tetrakis (trifluoromethyl)-; C<sub>17</sub>HF<sub>35</sub>O<sub>5</sub>; [37486-69-4]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P.; Iltis, R.; Clark, L.C. Jr.</p> <p><i>J. Fluorine Chem.</i> 1977, 9, 137-46.</p>						
<p>VARIABLES:</p> <p style="text-align: center;">T/K = 298</p>	<p>PREPARED BY:</p> <p style="text-align: center;">C. L. Young</p>						
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<p>* appears to be the Ostwald coefficient x 10<sup>2</sup> stated as ml/100 ml (total pressure was the barometer pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using density given in source</p>							
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 <math>\mu</math>l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Du Pont sample, boiling pt. 224°C.</p> <p>ESTIMATED ERROR:</p> <p style="text-align: center;"><math>\delta T/k = \pm 0.3</math>; <math>\delta x_{O_2} = \pm 2\%</math></p> <p>REFERENCES:</p>						

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) 3,6,9,12,15,21,24,27-Nonaoxatriacontane, 1,1,1,2,4,4,5,7,7,8,10,10,11,13,13,14,16,16,17,19,19,20,22,22,23,25,25,26,28,28,29,29,30,30,30,-pentacontafuoro- 5,8,11,14,17,20,23,26,octakis (trifluoromethyl) C<sub>29</sub>HF<sub>59</sub>O<sub>9</sub>; [58979-41-2]</p> <p>VARIABLES: T/K = 298</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wesseler, E.P; Iltis, R.; Clark, L.C. Jr. <i>J. Fluorine Chem.</i> <u>1977</u>, 9, 137-46.</p>						
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<p>AUXILIARY INFORMATION</p>							
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 µl Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) No details given.</p> <p>(2) Dupont sample, density 1.848g cm<sup>-3</sup> at 25°C.</p> <p>ESTIMATED ERROR: δT/K = ±03; δx<sub>O<sub>2</sub></sub> = ±2%</p> <p>REFERENCES:</p>						

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Carbon disulfide; CS <sub>2</sub> ; [75-15-0]	<b>ORIGINAL MEASUREMENTS:</b> Gjaldbaek, J. C. <i>Acta Chem. Scand.</i> <u>1952</u> , <i>6</i> , 623-33.												
<b>VARIABLES:</b> T/K = 297.97 - 298.15 Total P/kPa = 101.325	<b>PREPARED BY:</b> J. Chr. Gjaldbaek												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="326 478 997 635"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>297.97</td> <td>0.445</td> <td>0.164</td> <td>0.179</td> </tr> <tr> <td>298.15</td> <td>0.439</td> <td>0.162</td> <td>0.177</td> </tr> </tbody> </table> <p>The mole fraction and Ostwald solubility values were calculated by the compiler.</p>		T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	297.97	0.445	0.164	0.179	298.15	0.439	0.162	0.177
T/K	Mol Fraction $X_1 \times 10^3$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L										
297.97	0.445	0.164	0.179										
298.15	0.439	0.162	0.177										
<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> A calibrated all-glass combined manometer and bulb was enclosed in an air thermostat and shaken until equilibrium. Mercury was used for calibration and as the confining liquid. The solvents were degassed in the apparatus. Details are in references 1 and 2. The absorbed volume of gas was calculated from the initial and final amounts, both saturated with solvent vapor. The amount of solvent was determined by the weight of displaced mercury. The saturation of the liquid with the gas was carried out close to atmospheric pressure. The solubility values were reported for one atmosphere gas pressure assuming Henry's law is obeyed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Prepared by heating KMnO <sub>4</sub> , 99.7 percent O <sub>2</sub> , 0.3 percent N <sub>2</sub> . (2) Carbon disulfide. Merck Co. Analytical reagent grade, boiling point 46.21 - 46.26°C. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ $\delta X_1/X_1 = 0.015$ <b>REFERENCES:</b> 1. Lannung, A. <i>J. Am. Chem. Soc.</i> <u>1930</u> , <i>52</i> , 68. 2. Gjaldbaek, J. C. <i>Acta Chem. Scand.</i> <u>1952</u> , <i>6</i> , 623.												

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfinylbismethane or Dimethyl Sulfoxide; C <sub>2</sub> H <sub>6</sub> OS (CH <sub>3</sub> SOCH <sub>3</sub> ); [67-68-5]	<b>ORIGINAL MEASUREMENTS:</b> Dymond, J. H. <i>J. Phys. Chem.</i> <u>1967</u> , <i>71</i> , 1829-31.								
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="300 491 1022 635" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^4</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">1.57</td> <td style="text-align: center;">0.0494</td> <td style="text-align: center;">0.0539</td> </tr> </tbody> </table> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	1.57	0.0494	0.0539
T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L						
298.15	1.57	0.0494	0.0539						
<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> The liquid is saturated with the gas at a gas partial pressure of 1 atm.  The apparatus is that described by Dymond and Hildebrand (1). The apparatus uses an all-glass pumping system to spray slugs of degassed solvent into the gas. The amount of gas dissolved is calculated from the initial and final gas pressure.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Stuart Oxygen Co. Dried. (2) Dimethyl Sulfoxide. Matheson, Coleman, and Bell Co. Spectro-quality reagent, dried, and a fraction frozen out. Melting pt.: 18.37°C.  <b>ESTIMATED ERROR:</b>  <b>REFERENCES:</b> 1. Dymond, J.; Hildebrand, J. H. <i>Ind. Eng. Chem. Fundam.</i> <u>1967</u> , <i>6</i> , 130.								

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Sulfinylbismethane or dimethyl sulfoxide; C<sub>2</sub>H<sub>6</sub>OS; [67-68-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Baird, W. R.; Foley, R. T.</p> <p><i>J. Chem. Eng. Data</i> <u>1972</u>, <i>17</i>, 355-7.</p>								
<p>VARIABLES:</p> <p>T/K = 298.15</p> <p>P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>P. L. Long</p> <p>H. L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="282 479 1010 632"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha \times 10^2</math></th> <th>Ostwald Coefficient <math>L \times 10^2</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.109</td> <td>3.42 ± 0.08<sup>1</sup></td> <td>3.73</td> </tr> </tbody> </table> <p><sup>1</sup>Average of four measurements ± average deviation.</p> <p>The compiler calculated the mole fraction and Ostwald coefficient values.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha \times 10^2$	Ostwald Coefficient $L \times 10^2$	298.15	0.109	3.42 ± 0.08 <sup>1</sup>	3.73
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298.15	0.109	3.42 ± 0.08 <sup>1</sup>	3.73						
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus and procedure used were based on those described by Morrison and Billett (1). Gas saturation is achieved by allowing a thin film of solvent to flow down a glass helix containing the gas and solvent vapor at a total pressure of one atm. About 100 cm<sup>3</sup> of solvent is saturated at a flow rate of 2 - 3 cm<sup>3</sup> m<sup>-1</sup>.</p> <p>The authors solubility values for oxygen dissolved in water and in dimethylsulfoxide were 3.5 and 21 per cent lower, respectively, than values reported by other workers.</p> <p>The authors reported a Bunsen coefficient which they had calculated from their measured Ostwald coefficients.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. No information.</p> <p>(2) Dimethyl sulfoxide. Matheson, Coleman and Bell. Fractionally distilled under reduced pressure through spinning band column. Use 40 percent from the center of an initial one liter sample.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.5</math></p> <p><math>\delta \alpha/\alpha = 0.023 - 0.050</math> (authors)</p> <p>REFERENCES:</p> <p>1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> 1948, 2033.</p>								



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfinylbismethane or dimethyl sulfoxide; C <sub>2</sub> H <sub>6</sub> OS; [67-68-5]	<b>ORIGINAL MEASUREMENTS:</b> Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I. A. <i>Zh. Fiz. Khim.</i> <u>1979</u> , <i>53</i> , 1989-92. <i>Russ. J. Phys. Chem.</i> <u>1979</u> , <i>53</i> , 1133-4.						
<b>VARIABLES:</b> T/K = 298.15 (?) O <sub>2</sub> P/kPa = ~21.3 (air at one atm)	<b>PREPARED BY:</b> H. L. Clever						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="354 490 998 637" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Mol Fraction <math>x_1 \times 10^4</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Absorption Coefficient cm<sup>3</sup> (STP) cm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td style="border-bottom: 1px solid black;">298.15<sup>1</sup></td> <td style="border-bottom: 1px solid black;">1.96</td> <td style="border-bottom: 1px solid black;">0.063 ± 0.010</td> </tr> </tbody> </table> <p data-bbox="354 656 1017 754"> <sup>1</sup> The temperature is not given in the paper. However, the authors quote values from another of their papers in which all values were measured at 298.15 K.         </p> <p data-bbox="354 774 1049 901">           The solvent was saturated with dry air at a total pressure of one atm. The oxygen partial pressure in dry air is ~0.21 atm. The solubility values above are for that partial pressure of oxygen.         </p>		T/K	Mol Fraction $x_1 \times 10^4$	Absorption Coefficient cm <sup>3</sup> (STP) cm <sup>-3</sup>	298.15 <sup>1</sup>	1.96	0.063 ± 0.010
T/K	Mol Fraction $x_1 \times 10^4$	Absorption Coefficient cm <sup>3</sup> (STP) cm <sup>-3</sup>					
298.15 <sup>1</sup>	1.96	0.063 ± 0.010					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> <p data-bbox="96 1293 618 1440">           The oxygen concentration was determined by an electrochemical sensor. The sensor was calibrated against oxygen saturated ethanol. The Bunsen coefficient of oxygen in ethanol was taken to be 0.213 cm<sup>3</sup> cm<sup>-3</sup> atm<sup>-1</sup>.         </p> <p data-bbox="96 1460 618 1519">           Solutions were saturated in a 20 cm<sup>3</sup> cell in 3 hours without stirring.         </p> <p data-bbox="96 1538 637 1636">           The solvent water content was determined by the Fisher method. Water content of 0.0053 - 0.017 % had no effect on the oxygen solubility.         </p> <p data-bbox="96 1656 592 1705">           The sensitivity of the method with respect to oxygen is 3 μg dm<sup>-3</sup>.         </p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Dry air. (2) Dimethylsulfoxide. Freshly distilled after special purification.						
<b>ESTIMATED ERROR:</b> The authors state that the relative error in O <sub>2</sub> concentration is 9.9 per cent.							
<b>REFERENCES:</b>							

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitromethane; CH <sub>3</sub> NO <sub>2</sub> ; [75-52-5]	<b>ORIGINAL MEASUREMENTS:</b> Chaenko, N. V.; Sukhova, G. I.; Naumenko, N. K.; Kedrinskii, I. A. <i>Zh. Fiz. Khim.</i> <b>1979</b> , <i>53</i> , 1989-92.  <i>Russ. J. Phys. Chem.</i> <b>1979</b> , <i>53</i> , 1133-4.						
<b>VARIABLES:</b> T/K = 298.15 (?) O <sub>2</sub> P/kPa = 21.3 (air at one atm)	<b>PREPARED BY:</b> H. L. Clever						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="377 493 969 644"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^4</math></th> <th>Absorption Coefficient cm<sup>3</sup> (STP) cm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td>298.15<sup>1</sup></td> <td>4.64</td> <td>0.194 ± 0.004</td> </tr> </tbody> </table> <p><sup>1</sup> The temperature is not given in the paper. However, the authors quote values from another of their papers which were measured at 298.15.</p> <p>The solvent was saturated with dry air at a total pressure of one atm. The oxygen partial pressure in dry air is ~0.21 atm. The solubility values above are for the partial pressure of oxygen in air.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Absorption Coefficient cm <sup>3</sup> (STP) cm <sup>-3</sup>	298.15 <sup>1</sup>	4.64	0.194 ± 0.004
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<b>ESTIMATED ERROR:</b> The authors state that the relative error in O <sub>2</sub> concentration is 4 - 5 per cent.							
<b>REFERENCES:</b>							

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) N-methyl-N-nitroso-methanamine or N-nitroso-dimethylamine; C<sub>2</sub>H<sub>6</sub>N<sub>2</sub>O; [62-75-9]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Baird, W. R.; Foley, R. T.</p> <p><i>J. Chem. Eng. Data</i> <u>1972</u>, <i>17</i>, 355-7.</p>								
<p>VARIABLES:</p> <p>T/K = 298.15 P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>P. L. Long H. L. Clever</p>								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="326 506 1050 665"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^3</math></th> <th>Bunsen Coefficient <math>\alpha \times 10^2</math></th> <th>Ostwald Coefficient L <math>\times 10^2</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>0.200</td> <td>6.05 <math>\pm</math> 0.20<sup>1</sup></td> <td>6.60</td> </tr> </tbody> </table> <p><sup>1</sup>Average of four measurements <math>\pm</math> average deviation.</p> <p>The mole fraction and Ostwald coefficient values were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^3$	Bunsen Coefficient $\alpha \times 10^2$	Ostwald Coefficient L $\times 10^2$	298.15	0.200	6.05 $\pm$ 0.20 <sup>1</sup>	6.60
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<p>AUXILIARY INFORMATION</p>									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus and procedure used were based on those described by Morrison and Billett (1). Gas saturation is achieved by allowing a thin film of solvent to flow down a glass helix containing the gas and solvent vapor at a total pressure of one atm. About 100 cm<sup>3</sup> of solvent is saturated at a flow rate of 2 - 3 cm<sup>3</sup> m<sup>-1</sup>.</p> <p>The authors solubility values for oxygen dissolved in water and in dimethylsulfoxide were 3.5 and 21 per cent lower, respectively, than values reported by other workers.</p> <p>The authors reported a Bunsen coefficient which they had calculated from their measured Ostwald coefficients.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. No information.</p> <p>(2) N-nitroso-dimethylamine. Matheson, Coleman and Bell. Fractionally distilled under reduced pressure through spinning band column. Use 40 percent from the center of an initial one liter sample.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.5</math> <math>\delta \alpha/\alpha = 0.023 - 0.050</math> (authors)</p> <p>REFERENCES:</p> <p>1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u>, 2033.</p>								

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitric acid, propyl ester or 1-propyl nitrate; C <sub>3</sub> H <sub>7</sub> NO <sub>3</sub> ; [627-13-4]		Amster, A. B.; Levy, J. B. <i>J. Am. Rocket Soc.</i> <u>1959</u> , <i>29</i> , 870-1.			
VARIABLES:		PREPARED BY:			
T/K = "Room temperature" P/kPa = 28.0 - 84.66		M. E. Derrick H. L. Clever			
EXPERIMENTAL VALUES:					
Pressure		Solubility <sup>1</sup>	Mol Fraction	Bunsen Coefficient	Ostwald Coefficient
P/mmHg <sup>1</sup>	P/kPa	mol g <sup>-1</sup> x 10 <sup>6</sup>	x <sub>1</sub> x 10 <sup>4</sup>	α	L
210	28.0	1.9	2.0	0.17	0.18
225	30.0	2.0	2.1	0.16	0.17
230	30.7	1.9	2.0	0.15	0.16
400	53.3	4.2	4.4	0.19	0.20
410	54.7	4.1	4.3	0.18	0.19
425	56.7	4.5	4.7	0.19	0.20
440	58.7	3.8	4.0	0.16	0.17
620	82.7	7.3	7.7	0.21	0.23
630	84.0	7.1	7.5	0.20	0.22
635	84.7	7.2	7.6	0.20	0.22
<p><sup>1</sup> The compiler read values of pressure and solubility from a graph in the author's paper. The pressure is the total pressure minus the equilibrium vapor pressure of pure nitric acid propyl ester.</p> <p>The compiler calculated the mole fraction, Bunsen coefficient, and the Ostwald coefficient values assuming a temperature of 293.15 K. Density values for the solvent were available at the temperature.</p>					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
<p>The apparatus consists of an absorption flask connected by a flexible spiral to a mercury filled capillary (1).</p> <p>The gas is shaken with the degassed liquid. A weighed quantity of liquid is placed in the flask. The volume of the gas is taken as the volume of the flask minus the liquid volume. The solubility is calculated from</p> $\text{Solubility/mol g}^{-1} = \frac{V\Delta P}{WRT}$ <p>where V is the gas volume, ΔP is the pressure change, W is the weight of liquid.</p>			<p>(1) Oxygen. Technical grade. 99.5 per cent. Passed through a drying tube.</p> <p>(2) Nitric acid, propyl ester. Source and purity not given.</p>		
			ESTIMATED ERROR:		
			$\delta P/\text{mmHg} = 5$ $\delta T/K = 2$ $\delta \alpha/\alpha = 0.15$		
			REFERENCES:		
			<p>1. Levy, J. B.; Taft, R. W. Jr.; Aaron, D.; Hammett, L. P. <i>J. Am. Chem. Soc.</i> <u>1953</u>, <i>75</i>, 3955.</p>		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Cyclic amines; C <sub>4</sub> H <sub>9</sub> N, C <sub>5</sub> H <sub>5</sub> N, and C <sub>5</sub> H <sub>10</sub> N	<b>ORIGINAL MEASUREMENTS:</b> Guerry, D. Jr. Ph.D. thesis, 1944, Vanderbilt University, Nashville, TN.																																								
<b>VARIABLES:</b> T/K = 293-298 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Mol Fraction <math>x_1 \times 10^4</math></th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Pyrrolidine; C<sub>4</sub>H<sub>9</sub>N; [123-75-1]</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">6.04</td> <td style="text-align: center;">0.163</td> <td style="text-align: center;">0.175</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">6.06</td> <td style="text-align: center;">0.163</td> <td style="text-align: center;">0.178</td> </tr> <tr> <td colspan="4" style="text-align: center;">Pyridine; C<sub>5</sub>H<sub>5</sub>N; [110-86-1]</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">4.55</td> <td style="text-align: center;">0.127</td> <td style="text-align: center;">0.136</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">4.58</td> <td style="text-align: center;">0.127</td> <td style="text-align: center;">0.139</td> </tr> <tr> <td colspan="4" style="text-align: center;">Piperidine; C<sub>5</sub>H<sub>11</sub>N; [110-89-4]</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">7.44</td> <td style="text-align: center;">0.169</td> <td style="text-align: center;">0.181</td> </tr> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">7.35</td> <td style="text-align: center;">0.166</td> <td style="text-align: center;">0.181</td> </tr> </tbody> </table> <p>The Ostwald coefficients were calculated by the compiler.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	Pyrrolidine; C <sub>4</sub> H <sub>9</sub> N; [123-75-1]				293.15	6.04	0.163	0.175	298.15	6.06	0.163	0.178	Pyridine; C <sub>5</sub> H <sub>5</sub> N; [110-86-1]				293.15	4.55	0.127	0.136	298.15	4.58	0.127	0.139	Piperidine; C <sub>5</sub> H <sub>11</sub> N; [110-89-4]				293.15	7.44	0.169	0.181	298.15	7.35	0.166	0.181
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293.15	4.55	0.127	0.136																																						
298.15	4.58	0.127	0.139																																						
Piperidine; C <sub>5</sub> H <sub>11</sub> N; [110-89-4]																																									
293.15	7.44	0.169	0.181																																						
298.15	7.35	0.166	0.181																																						
<b>AUXILIARY INFORMATION</b>																																									
<b>METHOD/APPARATUS/PROCEDURE:</b> A Van Slyke-Neill Manometric Apparatus manufactured by the Eimer and Amend Co. was used. The procedure of Van Slyke (1) for pure liquids was modified (2) so that small solvent samples (2 cm <sup>3</sup> ) could be used with almost complete recovery of the sample. An improved temperature control system was used.	<b>SOURCE AND PURITY OF MATERIALS:</b> Pyrrolidine. Pyrrole was prepared and catalytically reduced to pyrrolidine. B.p. (750 mmHg) t/°C 88.12 - 88.26 (corr.). Pyridine. Mallinckrodt Chemical Co. Purified and distilled. B.p. (743.9 mmHg) t/°C 114.96 - 115.06 (corr.). Piperidine. Part was a commercial sample (Eastman Kodak Co.), part prepared by reduction of pyridine. B.p. (752.4 mmHg) t/°C 106.00 - 106.17.																																								
<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air reduction Co. Purity 99.5 per cent. (2) Cyclic amines. The pyridine and pyrrolidine were distilled from BaO under a N <sub>2</sub> atmosphere. The piperidine was distilled from KOH under a N <sub>2</sub> atmosphere. Experimental data on refractive index, density and vapor pressure are in the thesis.	<b>ESTIMATED ERROR:</b> $\delta T/K = 0.05$ <b>REFERENCES:</b> 1. Van Slyke, D. D. <i>J. Biol. Chem.</i> 1939, 130, 545. 2. Ijams, C. C. Ph.D. thesis, 1941 Vanderbilt University																																								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitrobenzene; C <sub>6</sub> H <sub>5</sub> NO <sub>2</sub> ; [98-95-3]	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim. (Leningrad)</i> <u>1969</u> , 42, 2522-8. <i>J. Appl. Chem. USSR</i> , <u>1969</u> , 42, 2376-81.								
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever								
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="303 485 1089 618"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>x_1 \times 10^4</math></th> <th>Bunsen Coefficient <math>\alpha</math></th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>4.95</td> <td>0.108 ± 0.0041</td> <td>0.118</td> </tr> </tbody> </table> <p>The Ostwald coefficient values were calculated by the compiler.</p> <p>The absolute errors are calculated from the results of three or four determinations.</p>		T/K	Mol Fraction $x_1 \times 10^4$	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	298.15	4.95	0.108 ± 0.0041	0.118
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<b>AUXILIARY INFORMATION</b>									
<b>METHOD/APPARATUS/PROCEDURE:</b> The oxygen solubility was determined by a volumetric gas method. The liquids were deaerated for 20 to 30 minutes under reduced pressure with the aid of an oil pump. The deaeration was monitored from the readings of a thermocouple vacuum gage. The liquids were saturated with oxygen under an oxygen partial pressure of about 760 mmHg at 25°C for 2 hours. The amount of gas absorbed was then determined. Details of the method are given in an earlier paper (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> The source and purity of the materials were not given. <b>ESTIMATED ERROR:</b> $\delta T/K = 0.1$ $\delta \alpha/\alpha = 0.023$ (relative) <b>REFERENCES:</b> 1. Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim.</i> <u>1969</u> , 42, 2090.								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Aromatic amines; C <sub>6</sub> H <sub>7</sub> N, C <sub>7</sub> H <sub>9</sub> N, C <sub>8</sub> H <sub>11</sub> N, and C <sub>10</sub> H <sub>15</sub> N	<b>ORIGINAL MEASUREMENTS:</b> Naumenko, N. K.; Mukhin, N. N. Aleskovskii, V. B. <i>Zh. Prikl. Khim. (Leningrad)</i> <u>1969</u> , <i>42</i> , 2522-28. <i>J. Appl. Chem. USSR</i> , <u>1969</u> , <i>42</i> , 2376-81.																																																												
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) N,N,N-Triethyl ethanaminium bromide or tetraethyl ammonium bromide; C <sub>8</sub> H <sub>20</sub> NBr; [71-91-0] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Morrison, T. J.; Johnstone, N. B. B. <i>J. Chem. Soc.</i> <u>1955</u> , 3655-9.						
<b>VARIABLES:</b> T/K = 298.15 P/kPa = 101.325 $m_{\text{C}_8\text{H}_{20}\text{NBr}}/\text{mol kg}^{-1} = 0, 1.0$	<b>PREPARED BY:</b> H. L. Clever						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="286 526 1029 675"> <thead> <tr> <th>T/K</th> <th><math>k_s =</math> (1/m) log(S<sup>0</sup>/S)</th> <th><math>k_{sx} =</math> (1/m) log(x<sup>0</sup>/x)</th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>-0.046</td> <td>-0.031</td> </tr> </tbody> </table> <p>The salt effect parameter was calculated from two measurements. The solubility of oxygen in water, S<sup>0</sup>/cm<sup>3</sup> (STP) kg<sup>-1</sup>, and in one molal salt solution, S/cm<sup>3</sup> (STP) kg<sup>-1</sup>. Neither solubility value is given in the paper. Only the k<sub>s</sub> value is given. The compiler calculated the value of the salt effect parameter using the mole fraction oxygen solubility ratio.</p>		T/K	$k_s =$ (1/m) log(S <sup>0</sup> /S)	$k_{sx} =$ (1/m) log(x <sup>0</sup> /x)	298.15	-0.046	-0.031
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298.15	-0.046	-0.031					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> The degassed salt solution flows in a thin film down as absorption helix containing the oxygen gas and solvent vapor at a total pressure of one atm. The volume of gas absorbed is measured in an attached buret system (1,2).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. British Oxygen Co., Ltd. (2) Tetraethyl ammonium bromide. No information given. (3) Water. No information given.  <b>ESTIMATED ERROR:</b> $\delta k_s = 0.010$ (authors)  <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u> , 2033; <i>ibid.</i> <u>1952</u> , 3819.						



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-3] (2) 1,1,2,2,3,3,4,4,4-nonafluoro-N,N-bis (nonafluorobutyl) -1-butanamine, (Perfluorotributylamine); C <sub>12</sub> F <sub>27</sub> N; [311-89-7]	<b>ORIGINAL MEASUREMENTS:</b> Wesseler, E.P.; Iltis, R.; Clark, L. C. Jr. <i>J. Fluorine Chem.</i> <u>1977</u> , 9, 134-46.						
<b>VARIABLES:</b> T/K = 298	<b>PREPARED BY:</b> C. L. Young						
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Solubility *</th> <th style="text-align: center;">Mole fraction <sup>+</sup> of oxygen <math>x_{O_2}</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">298.15</td> <td style="text-align: center;">38.4</td> <td style="text-align: center;">0.00552</td> </tr> </tbody> </table> <p>* appears to be the Ostwald coefficient x 10<sup>2</sup>, units were stated as ml/100 ml (total pressure was the barometric pressure, assumed to be 1 atmosphere)</p> <p>+ calculated by compiler for a total pressure of 101.325 kPa using the density given in source</p>		T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$	298.15	38.4	0.00552
T/K	Solubility *	Mole fraction <sup>+</sup> of oxygen $x_{O_2}$					
298.15	38.4	0.00552					
<b>AUXILIARY INFORMATION</b>							
<b>METHOD/APPARATUS/PROCEDURE:</b> Oxygen bubbled through fluorocarbon in stirred cell. When saturation achieved samples of liquid removed with a hypodermic Precision Sampling 50 $\mu$ l Pressure-Lok syringe. At least 15 samples taken and chromatographed. Average peak height compared with that of average peak height for injection of the same volume of oxygen. Chromatographic column consisted of 13X molecular sieve at 70°C. Helium was used as carrier gas.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) A 3M sample, boiling pt 174°C.						
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.3$ ; $\delta x_{O_2} = \pm 2\%$							
<b>REFERENCES:</b>							

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) FC-47, which is largely perfluorotributylamine or 1,1,2,2,3,3,4,4,4-nonafluoro-N,N-bis(nonafluorobutyl)-1-butanamine; C <sub>12</sub> F <sub>27</sub> N; [311-89-7]	<b>ORIGINAL MEASUREMENTS:</b> Sargent, J. W.; Seffl, R. J. <i>Fed. Proc.</i> <u>1970</u> , <i>29</i> , 1699 - 1703.																
<b>VARIABLES:</b> T/K = 298-310 Total P/kPa = 101.325	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="296 493 1023 665" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th colspan="2">Temperature</th> <th colspan="2">Oxygen Solubility</th> </tr> <tr> <th>t/°C</th> <th>T/K</th> <th>g O<sub>2</sub> 1000 g<sup>-1</sup></th> <th>cm<sup>3</sup> O<sub>2</sub> 100 cm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td>25</td> <td>298.15</td> <td>0.272</td> <td>38.9</td> </tr> <tr> <td>37</td> <td>310.15</td> <td>0.276</td> <td>40.3</td> </tr> </tbody> </table> <p>The authors solubility, cm<sup>3</sup> O<sub>2</sub> 100 cm<sup>-3</sup>, appears to be the Ostwald coefficient times 100.</p>		Temperature		Oxygen Solubility		t/°C	T/K	g O <sub>2</sub> 1000 g <sup>-1</sup>	cm <sup>3</sup> O <sub>2</sub> 100 cm <sup>-3</sup>	25	298.15	0.272	38.9	37	310.15	0.276	40.3
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The equilibrium apparatus is a 50 cm<sup>3</sup> three neck flask equipped with a water condenser, a thermometer, and a gas dispersing tube extending below the fluid surface level. Between 25 and 35 cm<sup>3</sup> of solvent are placed in the flask. Gas is bubbled through the solvent for 2 - 3 h. An 80 micro-liter sample is slowly taken into a gas tight syringe. The sample is injected into a gas chromatograph. The results of three sampling and analyses are averaged.</p> <p>The chromatograph is an F and M Model 720 equipped with a thermal conductivity detector at 320 °C, and a 6' by ¼" stainless steel column packed with 13X molecular sieve at room temperature. The apparatus is calibrated with pure gas samples.</p> <p>Details of the procedure were furnished by R. D. Danielson of the 3 M Co.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Commercial cylinder. (2) FC-47. Minnesota Mining and Manufacturing Co. All H in an organic compound are replaced by F by Simons electrochemical process (1).																
<b>ESTIMATED ERROR:</b> $\delta T/K = 0.1$ $\delta c/c = 0.01$ (reproducibility) $= 0.05$ (absolute)																	
<b>REFERENCES:</b> 1. Simons, J. H., Editor <i>Fluorine Chemistry</i> Academic Press, New York, <u>1950</u> .																	

<b>COMPONENTS:</b> (1)Oxygen; O <sub>2</sub> ; [7782-44-7] (2)1,1,2,2,3,3,4,4,4-Nonfluoro-N,N-bis(nonfluorobutyl)-1-butamine; (C <sub>4</sub> F <sub>9</sub> ) <sub>3</sub> N; [311-89-7]	<b>ORIGINAL MEASUREMENTS:</b> Kobatake, Y.; Hildebrand, J. H. <i>J. Phys. Chem.</i> <u>1961</u> , <i>65</i> , 331-5.																																						
<b>VARIABLES:</b> T/K = 278.80 - 304.65 P/kPa = 101.325	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever																																						
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="348 487 1019 675"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>278.80</td> <td>5.542</td> <td>0.365</td> <td>0.373</td> </tr> <tr> <td>287.50</td> <td>5.395</td> <td>0.349</td> <td>0.367</td> </tr> <tr> <td>297.16</td> <td>5.218</td> <td>0.330</td> <td>0.359</td> </tr> <tr> <td>304.65</td> <td>5.096</td> <td>0.317</td> <td>0.358</td> </tr> </tbody> </table> <p>The Bunsen and Ostwald coefficients were calculated by the compiler.            Smoothed Data: <math>\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln X_1 = -2,312.6 + 51.480 T</math>            Std. Dev. <math>\Delta G^{\circ} = 2.9</math>, Coef. Corr. = 0.9999  <math>\Delta H^{\circ}/J \text{ mol}^{-1} = -2,312.6</math>, <math>\Delta S^{\circ}/J \text{ K}^{-1} \text{ mol}^{-1} = -51.480</math></p> <table border="1" data-bbox="434 864 914 1093"> <thead> <tr> <th>T/K</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th><math>\Delta G^{\circ}/J \text{ mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>283.15</td> <td>5.465</td> <td>12,264</td> </tr> <tr> <td>288.15</td> <td>5.372</td> <td>12,521</td> </tr> <tr> <td>293.15</td> <td>5.285</td> <td>12,779</td> </tr> <tr> <td>298.15</td> <td>5.201</td> <td>13,036</td> </tr> <tr> <td>303.15</td> <td>5.122</td> <td>13,294</td> </tr> </tbody> </table>		T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Ostwald Coefficient L	278.80	5.542	0.365	0.373	287.50	5.395	0.349	0.367	297.16	5.218	0.330	0.359	304.65	5.096	0.317	0.358	T/K	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	$\Delta G^{\circ}/J \text{ mol}^{-1}$	283.15	5.465	12,264	288.15	5.372	12,521	293.15	5.285	12,779	298.15	5.201	13,036	303.15	5.122	13,294
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<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus consists of a gas-measuring buret, an absorption pipet, and reservoir for solvent. The buret is thermostated at 25°C, the pipet at any temperature from 5 to 30°C. The solvent is degassed by freezing with liquid nitrogen, evacuating, then boiling with a heat lamp. The solvent never comes into contact with stopcock grease. The amount of gas is determined by P-V measurements in the gas buret before and after admission of the gas into the pipet. No solvent vapor is allowed into the buret system. The solvent is magnetically stirred for up to 24 hours until equilibrium is reached. Ideal gas behavior and Henry's law are assumed to calculate the mole fraction solubility at a gas partial pressure of one atm.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Linde Oxygen Co. Standard grade, 99.7 % oxygen. (2) (C <sub>4</sub> F <sub>9</sub> ) <sub>3</sub> N. Minnesota Mining and Manufacturing Co. dried, fractionated, bp. 178.5 - 179.0°C. <b>ESTIMATED ERROR:</b> $\delta X_1/X_1 = 0.003$ <b>REFERENCES:</b>																																						

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Zander, R.		
(2) FC-43 which is 1,1,2,2,3,3,4,4,4-nonafluoro-N,N-bis(nonafluorobutyl)-1-butanamine or perfluorotributylamine; C <sub>12</sub> F <sub>27</sub> N; [311-89-7]		Res. exp. Med. <u>1974</u> , 164, 97-109.		
VARIABLES: T/K = 283.15 - 323.15 P/kPa = 6 - 101		PREPARED BY:  H. L. Clever		
EXPERIMENTAL VALUES:				
Temperature Range, T/K	Gas Phase; <sup>1</sup> Volume Per Cent Oxygen	Oxygen Partial Pressure <sup>2</sup> p/mmHg	Bunsen Coefficient Regression Equation $\alpha/\text{cm}^3 \text{ cm}^{-3} \text{ atm}^{-1}$	Number of Experimental Points
283.15 - 323.15	6	45.6	$\alpha = 0.223 + 0.00005 t/^{\circ}\text{C}$	38
	12	91.2	$\alpha = 0.282 - 0.00021 t/^{\circ}\text{C}$	25
	25	190	$\alpha = 0.353 - 0.00071 t/^{\circ}\text{C}$	31
	50	380	$\alpha = 0.383 - 0.00083 t/^{\circ}\text{C}$	59
	100	760	$\alpha = 0.398 - 0.00093 t/^{\circ}\text{C}$	82
<p><sup>1</sup> The gas phase consists of oxygen, water at its equilibrium vapor pressure, solvent (FC-43) at its equilibrium vapor pressure, and nitrogen to bring the total pressure near one atm. The per cent oxygen in the gas phase was experimentally determined by a Scholander gas analyzer.</p> <p><sup>2</sup> The oxygen partial pressure was calculated by the compiler with the assumptions that the gas mixture behaved ideally and that the total pressure was 760 mmHg.</p> <p>In an abstract the author (1) reported the Bunsen coefficient at 310.15 K (37 °C) to be <math>0.362 \pm 0.007</math>. The 100 % O<sub>2</sub> equation above gives 0.364.</p>				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
Equilibration between the gas and liquid phases was established in 45 minutes in a Tonometer of the Laue (2) design.		(1) Oxygen. No information.		
The oxygen content of the gas phase was determined by a Scholander gas analyzer (see footnote <sup>1</sup> above).		(2) FC-43. Minnesota Mining and Manufacturing Co. Used as received.		
The saturated solution was transferred to a Van Slyke apparatus for the solubility determination.		The solubility measurements were made at the five temperatures 10, 20, 30, 40, and 50 °C.		
The 235 experimental measurements were fitted to the equations in the table above. The smoothed data were used to construct a graph of Bunsen coefficient vs. oxygen partial pressure and a nomogram for the volume per cent of oxygen as a function of oxygen partial pressure and temperature.		ESTIMATED ERROR: $\delta T/K = 0.1$ $\delta \alpha/\alpha = 0.03$ above 100 mmHg O <sub>2</sub> 0.05 - 0.10 below.		
The solubility appears to depart from Henry's law above 100 mmHg O <sub>2</sub> .		REFERENCES: 1. Zander, R. <i>Pflug. Arch.</i> <u>1973</u> , 343, R5. 2. Laue, D. <i>Pflugers Arch. Gesamte Physiol. Menschen Tiere</i> <u>1951</u> , 254, 142.		

COMPONENTS:		ORIGINAL MEASUREMENTS:				
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Matheson, I. B. C.; King, A. D.				
(2) 1-Hexadecanaminium, N,N,N-trimethyl bromide (Cetyl trimethyl ammonium bromide or CTAB); C <sub>19</sub> H <sub>42</sub> N.Br; [57-09-0]		J. Coll. Interface Sci. 1978, 66, 464-9.				
(3) Water; H <sub>2</sub> O; [7732-18-5]						
VARIABLES:		PREPARED BY:				
T/K = 298.15 P/kPa = 273.7 - 954.9 (39.7-138.5 psig) CTAB/mol kg <sup>-1</sup> H <sub>2</sub> O = 0 - 0.300		H. L. Clever				
EXPERIMENTAL VALUES:						
T/K	1-Hexadecanaminium, N,N,N-trimethyl ammonium bromide mol kg <sup>-1</sup> H <sub>2</sub> O	Pressure pounds per square inch, gauge	Volume gas evolved ml	Ambient Pressure mmHg	Ambient Temperature °C	Henry's constant K x 10 <sup>3</sup> mol Ar kg <sup>-1</sup> H <sub>2</sub> O atm <sup>-1</sup>
298.15	0	49.3	12.5	746.3	25.1	1.41±0.02
		71.5	18.0	743.5	25.2	
		74.7	18.6	745.5	24.8	
		108.5	26.2	747.0	24.8	
		122.0	29.7	745.5	25.9	
	0.100	46.0	12.2	745.3	25.8	1.50±0.02
		81.3	21.8	747.1	27.0	
		88.3	23.4	747.0	25.1	
		122.0	31.3	746.6	26.1	
		138.5	36.1	742.0	24.7	
	0.200	41.0	11.5	745.8	23.0	1.64±0.02
		78.3	22.4	747.9	22.0	
		100.5	28.2	747.8	22.4	
	0.300	39.7	13.1	735.9	23.0	1.82±0.03
		71.0	21.9	743.7	22.5	
		92.3	28.9	742.6	22.5	
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:			
<p>The apparatus consists of a jacketed thermostated thick-walled cylindrical brass bomb which rests on a variable speed magnetic stirrer. An inlet line to the bomb is connected to a gas manifold, and an exit line is connected to a Warburg manometer. Bourden gauges are used to record the pressure.</p> <p>The solution, consisting of 100 g of water and the colloidal electrolyte, is contained in a glass liner inside of the bomb. The solution is degassed by evacuation to just above water vapor pressure and then stirring for several hours. The gas is introduced over the solution at the desired pressure and the solution is stirred for a minimum of five hours.</p> <p>The gas is vented to atmospheric pressure. The gas from the supersaturated solution is collected in the Warburg manometer and its volume measured at atmospheric pressure and ambient temperature. Corrections for gas lost during venting and thermal equilibration and for water vapor pressure are made. The solubility is reported as Henry's constant, K/mol gas kg<sup>-1</sup> water atm<sup>-1</sup> = gas molality/pressure, m/p.</p>			<p>(1) Oxygen. Source not given. Chemically pure or equivalent of 99.5 mol per cent purity or better.</p> <p>(2) 1-Hexadecanaminium, N,N,N-trimethyl bromide. Eastman Chemical. Technical grade, recrystallized from ethyl acetate-ethanol mixture and dried <u>in vacuo</u>.</p> <p>(3) Water. Laboratory distilled.</p>			
			ESTIMATED ERROR:			
			δK/K = 0.02			

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Triglyceride oil (herring)				ORIGINAL MEASUREMENTS: Ke, P. J.; Ackman, R. G.  <i>J. Am. Oil Chemists' Soc.</i> <u>1973</u> , 50, 429-35.		
VARIABLES: T/K = 293.15 - 353.15 P/kPa = partial pressure of oxygen in air at 101.325 kPa				PREPARED BY:  P. L. Long H. L. Clever		
EXPERIMENTAL VALUES:						
Temperature	Density	Peroxide	Bunsen Coefficient/ $\alpha^1$			
t/°C	T/K	$\rho/g\text{ cm}^{-3}$	Value	Polarographic	Chemical	Displacement
			meq kg <sup>-1</sup>	Exponential	Method <sup>2</sup>	Method <sup>3</sup>
				Dilution		
				Method		
40 [sic]		0.9114	63.8	0.113 (+6%)	0.192 (+19%)	---
20	293.15	0.9151	2.0	0.110 ( $\bar{+}$ 6%)	0.124 ( $\bar{+}$ 11%)	0.113 (+8%)
20		0.9151	21.4	0.108 ( $\bar{+}$ 6%)	0.149 (+18%)	0.119 ( $\bar{+}$ 7%)
20		0.9151	79.5	0.113 ( $\bar{+}$ 6%)	0.214 (-)	---
40	313.15	0.9034	2.3	0.128 (+6%)	0.141 (+9%)	---
40		0.9034	84.0	0.122 ( $\bar{+}$ 6%)	0.289 (-)	---
<sup>1</sup> Values are the average of three determinations. Numbers in ( ) are the percentage relative error.						
<sup>2</sup> Chemical method of McDowell, A. K. R. <i>J. Dairy Res.</i> <u>1963</u> , 30, 399.						
<sup>3</sup> Displacement method of Becker, E.; Neiderstebruch, A. <i>Fett Seifen Anstrichm.</i> <u>1966</u> , 68, 135. Details of neither method given in the paper.						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE: Polarographic exponential dilution method (1).  The oil was degassed by the method of Battino et al. (2).  A 155-159 cm <sup>3</sup> sample of degassed oil was transferred to a glass vessel and weighed. The vessel was so constructed that the ratio $V_{\text{top air space}}/V_{\text{oil}}$ was between 0.0704 and 0.0981. A magnetic stirring bar (120 rpm) and a polarographic oxygen sensor were placed in the sample. Air was bubbled through the sample at 15 cm <sup>3</sup> m <sup>-1</sup> for two hours. The air was stopped, and helium gas preheated to the sample temperature was introduced into the oil at a rate of 7-10 cm <sup>3</sup> m <sup>-1</sup> . The oxygen concentration was measured as a function of the volume of helium passed through the solution. A plot of log (O <sub>2</sub> ) vs. $V_{\text{helium}}$ is linear. The slope is a function of the Ostwald coefficient. The Ostwald coefficient was converted to Bunsen coefficient.				SOURCE AND PURITY OF MATERIALS: (1) Oxygen. Breathing grade compressed air.  (2) Herring oil. Oil from whole herring ( <i>chi pea harengus</i> ) obtained from local commercial reduction plant in Nova Scotia.		
				ESTIMATED ERROR:		
				REFERENCES: 1. Aho, L.; Wahlroos, O. <i>J. Am. Oil Chem. Soc.</i> <u>1967</u> , 44, 65. 2. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , 45, 806.		

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Triglyceride oils</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Ke, P. J.; Ackman, R. G.</p> <p><i>J. Am. Oil Chemists' Soc.</i> <u>1973</u>, 50, 429-35.</p>
<p>VARIABLES:</p> <p>T/K = 293.15 - 353.15 P/kPa = Oxygen at partial pressure in air at 101.325 (1 atm).</p>	<p>PREPARED BY:</p> <p>P. L. Long H. L. Clever</p>
<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Breathing grade compressed air.</p> <p>(2) Triglyceride oils.</p> <p>Redfish oil.<sup>3</sup> Oil from redfish (<u>sebastes marinus</u>) viscera and scrap. Capelin oil.<sup>3</sup> Oil from whole capelin (<u>mallofus villosus</u>). Herring oil.<sup>4</sup> Oil from whole herring (<u>chi pea harengus</u>). Mackerel oil.<sup>3</sup> Oil from mackerel (<u>scomber scombrus</u>). Harp seal oil.<sup>4</sup> Oil from harp seal (<u>Phoca groenlandica</u>) blubber. Flounder oil.<sup>3</sup> Oil from flounder (<u>Pseudopleuronectes americanus</u>) viscera and scrap. Cod liver oil.<sup>4</sup> Oil from cod (<u>Gadus morhua</u>) livers.</p> <p><sup>3</sup>Oils obtained from local commercial reduction plants in Nova Scotia.</p> <p><sup>4</sup>Oils produced in a pilot scale reduction plant at the Vancouver Lab of The Fisheries Research Board of Canada.</p> <p>All oils were kept under nitrogen in cold storage (3°C) except when the experiment was in progress.</p> <p style="text-align: right;">continued on following page</p>	
<p>AUXILIARY INFORMATION</p>	
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Polarographic exponential dilution method (1).</p> <p>The oil was degassed by the method of Battino <i>et al.</i> (2).</p> <p>A 155 - 159 cm<sup>3</sup> sample of degassed oil was transferred to a glass vessel and weighed. The vessel was so constructed that the ratio V<sub>top air space</sub>/V<sub>oil</sub> was between 0.0704 and 0.0981. A magnetic stir- ring bar (120 rpm) and a polarographic oxygen sensor were placed in the sample. Air was bubbled through the sample at 15 cm<sup>3</sup> m<sup>-1</sup> for two hours. The air was stopped, and helium gas preheated to the sample temperature was introduced into the oil at a rate of 7 - 10 cm<sup>3</sup> m<sup>-1</sup>. The oxygen concentration was measured as a function of the volume of helium passed through the solution. A plot of log (O<sub>2</sub>) vs. V<sub>helium</sub> is linear. The slope is a function of the Ostwald coefficient. The Ostwald coefficient was converted to Bunsen coefficient.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>See above.</p>
	<p>ESTIMATED ERROR:</p> <p>Solubility values are the average of three determinations with relative standard deviation of 7 % or less.</p>
	<p>REFERENCES:</p> <p>1. Aho, L.; Wahlroos, O. <i>J. Am. Oil Chem. Soc.</i> <u>1967</u>, 44, 65.</p> <p>2. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u>, 45, 806.</p>

COMPONENTS:  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) Triglyceride oils	ORIGINAL MEASUREMENTS:  Ke, P. J.; Ackman, R. G.  <i>J. Am. Oil Chemists' Soc.</i> <u>1973</u> , 50, 429-35.
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## EXPERIMENTAL VALUES: continued

Temperature		Density	Bunsen	Parts per	cm <sup>3</sup> (STP) O <sub>2</sub>
t/°C	T/K	ρ/g cm <sup>-3</sup>	Coefficient <sup>1</sup>	Million <sup>2</sup>	100 cm <sup>-3</sup>
			α	μg g <sup>-1</sup>	of oil <sup>2</sup>
Redfish oil					
20	293.15	0.9184	0.074	24.2	1.55
40	313.15	0.9061	0.078	25.8	1.64
60	333.15	0.8931	0.088	29.6	1.84
80	353.15	0.8814	0.012	4.1	0.25
Capelin oil					
20	293.15	0.9163	0.060	19.5	1.25
40	313.15	0.9049	0.081	26.6	1.68
60	333.15	0.8920	0.103	34.4	2.14
80	353.15	0.8798	0.025	8.5	0.52
Herring oil					
20	293.15	0.9151	0.110	35.8	2.29
40	313.15	0.9034	0.128	42.2	2.26
60	333.15	0.8904	0.135	45.2	2.81
80	353.15	0.8785	0.076	25.8	1.58
Mackerel oil					
20	293.15	0.9192	0.042	13.6	0.87
40	313.15	0.9074	0.078	25.6	1.62
60	333.15	0.8952	0.086	28.7	1.79
80	353.15	0.8828	0.011	3.7	0.23
Harp seal oil					
20	293.15	0.9220	0.090	29.1	1.87
40	313.15	0.9087	0.108	35.7	2.26
60	333.15	0.8970	0.114	37.9	2.37
80	353.15	0.8844	0.030	10.1	0.62
Flounder oil					
20	293.15	0.9234	0.075	23.2	1.55
40	313.15	0.9115	0.078	25.6	1.63
60	333.15	0.8977	0.081	26.9	1.69
80	353.15	0.8853	0.029	9.6	0.59
Cod liver oil					
20	293.15	0.9205	0.124	39.9	2.58
40	313.15	0.9139	0.146	47.6	3.04
60	333.15	0.9002	0.130	43.0	2.70
80	353.15	0.8896	0.018	6.0	0.37

<sup>1</sup>The Bunsen coefficients are for an oxygen partial pressure of 101.325 kPa (1 atm or 760 mmHg).

<sup>2</sup>The parts per million and the volume O<sub>2</sub> (STP) per 100 cm<sup>3</sup> oil are for the partial pressure of oxygen in air (ca. 0.21 atm or 160 mmHg).



<b>COMPONENTS:</b> (1) Oxygen: O <sub>2</sub> ; [7782-44-7] (2) Soybean Oil	<b>ORIGINAL MEASUREMENTS:</b> Tomoto, N.; Kusano, K. <i>Yukagaku</i> 1967, 16, 108-13. <i>Chem. Abstr.</i> 1967, 66, 106141z.												
<b>VARIABLES:</b> T/K = 303-343	<b>PREPARED BY:</b> R. Battino												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="221 504 1159 707" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">t/°C</th> <th style="text-align: center;">T<sup>a</sup>/K</th> <th style="text-align: center;"><math>\alpha^b / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">30</td> <td style="text-align: center;">303</td> <td style="text-align: center;">0.141</td> </tr> <tr> <td style="text-align: center;">50</td> <td style="text-align: center;">323</td> <td style="text-align: center;">0.143</td> </tr> <tr> <td style="text-align: center;">70</td> <td style="text-align: center;">343</td> <td style="text-align: center;">0.251</td> </tr> </tbody> </table> <p data-bbox="221 751 585 781"> <sup>a</sup> Calculated by compiler.         </p> <p data-bbox="221 795 526 825"> <sup>b</sup> Bunsen coefficient.         </p>		t/°C	T <sup>a</sup> /K	$\alpha^b / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$	30	303	0.141	50	323	0.143	70	343	0.251
t/°C	T <sup>a</sup> /K	$\alpha^b / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$											
30	303	0.141											
50	323	0.143											
70	343	0.251											
<b>AUXILIARY INFORMATION</b>													
<b>METHOD/APPARATUS/PROCEDURE:</b> Described in the paper	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) (2) Saponification value: 192.0; acid value: 0.17; iodine value: 128.5; unsaponifiable: 0.33%; d <sub>30</sub> : 0.9132 g cm <sup>-3</sup> ; M.W.: 877 g mol <sup>-1</sup> ; molar volume: 960.4 cm <sup>3</sup> mol <sup>-1</sup> . <b>ESTIMATED ERROR:</b> $\delta\alpha/\alpha = \pm 0.02$ , compiler's estimate. <b>REFERENCES:</b>												

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Vegetable oils</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Aho, L.; Wahlroos, O.</p> <p><i>J. Am. Oil Chemists' Soc.</i> <u>1967</u>, 44, 65-6.</p>																														
<p>VARIABLES:</p> <p>T/K = 295 - 296</p>	<p>PREPARED BY:</p> <p>P. L. Long H. L. Clever</p>																														
<p>EXPERIMENTAL VALUES:</p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th colspan="2" style="text-align: center;">Temperature</th> <th style="text-align: center;">Ostwald Coefficient</th> </tr> <tr> <th style="text-align: center;"><u>t/°C</u></th> <th style="text-align: center;"><u>T/K</u></th> <th style="text-align: center;"><u>L</u></th> </tr> </thead> <tbody> <tr> <td colspan="3" style="padding-top: 10px;">Soybean oil, raw</td> </tr> <tr> <td style="text-align: center;">22-23</td> <td style="text-align: center;">~295.6</td> <td style="text-align: center;">0.173</td> </tr> <tr> <td colspan="3" style="padding-top: 10px;">Soybean oil, refined</td> </tr> <tr> <td style="text-align: center;">22-23</td> <td style="text-align: center;">~295.6</td> <td style="text-align: center;">0.170</td> </tr> <tr> <td colspan="3" style="padding-top: 10px;">Sunflower seed oil, raw</td> </tr> <tr> <td style="text-align: center;">22-23</td> <td style="text-align: center;">~295.6</td> <td style="text-align: center;">0.151</td> </tr> <tr> <td colspan="3" style="padding-top: 10px;">Sunflower seed oil, refined</td> </tr> <tr> <td style="text-align: center;">22-23</td> <td style="text-align: center;">~295.6</td> <td style="text-align: center;">0.100</td> </tr> </tbody> </table>		Temperature		Ostwald Coefficient	<u>t/°C</u>	<u>T/K</u>	<u>L</u>	Soybean oil, raw			22-23	~295.6	0.173	Soybean oil, refined			22-23	~295.6	0.170	Sunflower seed oil, raw			22-23	~295.6	0.151	Sunflower seed oil, refined			22-23	~295.6	0.100
Temperature		Ostwald Coefficient																													
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus consisted of a sample vessel with magnetic stirrer, a gas buret, a silver/gold oxygen sensing electrode, and various recorders.</p> <p>Exponential dilution method. The apparatus was filled with a known volume of liquid. Helium, flow rate 4 - 7 cm<sup>3</sup> m<sup>-1</sup>, was the dilution gas. The gas volumes which had flowed through, and the oxygen electrode readings were corrected for the pressure of gas in the buret.</p> <p>The method was tested on O<sub>2</sub> + H<sub>2</sub>O with argon as the carrier gas. A distribution (Ostwald) coefficient of 0.031 was measured at 22 °C.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. No information.</p> <p>(2) Vegetable oils. No information. The peroxide values of each oil were measured.</p> <hr/> <p>ESTIMATED ERROR:</p> <p style="text-align: center;">Standard deviation 3 % (authors)</p> <hr/> <p>REFERENCES:</p>																														

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Animal and vegetable oils</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Vibrans, F. C.</p> <p><i>Oil and Soap</i> <u>1935</u>, 12, 14-5.</p>																																																																						
<p>VARIABLES:</p> <p>T/K = 296-299, 318.15</p> <p>P/kPa = 101.3</p>	<p>PREPARED BY:</p> <p>P. L. Long</p> <p>H. L. Clever</p>																																																																						
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>;[7782-44-7]</p> <p>(2) Animal and vegetable oils</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Schaffer, P. S.; Haller, H. S. <i>Oil and Soap</i> <u>1943</u>, 20, 161-2.</p>																								
<p>VARIABLES:</p> <p>T/K = 313.15, 333.15 P/kPa = 101.325</p>	<p>PREPARED BY:</p> <p>P. L. Long H. L. Clever</p>																								
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus consists of a reaction flask connected to a water jacketed gas buret, a mercury leveling bulb, and a differential manometer. The reaction vessel is attached to a shaking mechanism in an air bath.</p> <p>A 50 cm<sup>3</sup> sample of oil is placed in the flask. Heat and vacuum are applied to remove dissolved gases. The sample is cooled to the temperature of the measurement. Oxygen gas is admitted, a zero reading is taken. The system is shaken until the sample takes up no more gas at a pressure of 1 atm. Three determinations were made on each sample.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. From commercial cylinders, source and purity not given, used as received.</p> <p>(2) Cottonseed oil. Good grade commercial product.</p> <p>Butter oil. Obtained from butter prepared in the lab from fresh cream.</p> <p>Lard. Good grade commercial product.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = 0.5</math> <math>\delta c/c = 0.003</math> (authors, error among three determinations)</p> <p>REFERENCES:</p>																								

<b>COMPONENTS:</b>  (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Olive Oil, Tetralin, Lard	<b>ORIGINAL MEASUREMENTS:</b>  Davidson, D.; Eggleton, P.; Foggie, P.  <i>Quart. J. Exptl. Physiol.</i> <u>1952</u> , 37, 91-105.																					
<b>VARIABLES:</b> T/K = 299, 323	<b>PREPARED BY:</b>  R. Battino																					
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">t/°C</th> <th style="text-align: center;">T<sup>a</sup>/K</th> <th style="text-align: center;">L<sup>b</sup></th> </tr> </thead> <tbody> <tr> <td></td> <td style="text-align: center;">Olive Oil</td> <td></td> </tr> <tr> <td style="text-align: center;">25.3</td> <td style="text-align: center;">298.5</td> <td style="text-align: center;">0.1117</td> </tr> <tr> <td></td> <td style="text-align: center;">Tetralin</td> <td></td> </tr> <tr> <td style="text-align: center;">25.3</td> <td style="text-align: center;">298.5</td> <td style="text-align: center;">0.1186</td> </tr> <tr> <td></td> <td style="text-align: center;">Lard (liquid)</td> <td></td> </tr> <tr> <td style="text-align: center;">50</td> <td style="text-align: center;">323</td> <td style="text-align: center;">0.114</td> </tr> </tbody> </table> <p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Ostwald coefficient.</p>		t/°C	T <sup>a</sup> /K	L <sup>b</sup>		Olive Oil		25.3	298.5	0.1117		Tetralin		25.3	298.5	0.1186		Lard (liquid)		50	323	0.114
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<b>METHOD/APPARATUS/PROCEDURE:</b>  Combined with diffusion measurements. Measurement based on knowing gas phase and liquid phase volumes and the initial (before any gas dissolved) pressure and the final equilibrium pressure.	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details given.																					
<b>ESTIMATED ERROR:</b>  $\delta L/L = \pm 0.08$ , compiler's estimate. $\delta T/K = \pm 0.01$ , but reported to 0.1°C or 1°C.																						
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Olive Oil	<b>ORIGINAL MEASUREMENTS:</b> Battino, R.; Evans, F. D.; Danforth, W. F.  <i>J. Am. Oil Chemists' Soc.</i> <u>1968</u> , <i>45</i> , 830-3.																				
<b>VARIABLES:</b> T/K = 298.26 - 327.93 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																				
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<p>Smoothed Data: <math>\Delta G^\circ / \text{J mol}^{-1} = -RT \ln X_1 = 1240.9 + 39.809 T</math></p> <p>Std. Dev. <math>\Delta G^\circ = 11.2</math>, Coef. Corr. = 0.9999</p> <p><math>\Delta H^\circ / \text{J mol}^{-1} = 1240.9</math>, <math>\Delta S^\circ / \text{J K}^{-1} \text{ mol}^{-1} = -39.809</math></p> <table border="1"> <thead> <tr> <th>T/K</th> <th>Mol Fraction <math>X_1 \times 10^3</math></th> <th><math>\Delta G^\circ / \text{J mol}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>5.05</td> <td>13,110</td> </tr> <tr> <td>308.15</td> <td>5.13</td> <td>13,508</td> </tr> <tr> <td>318.15</td> <td>5.21</td> <td>13,906</td> </tr> <tr> <td>328.15</td> <td>5.29</td> <td>14,304</td> </tr> </tbody> </table>		T/K	Mol Fraction $X_1 \times 10^3$	$\Delta G^\circ / \text{J mol}^{-1}$	298.15	5.05	13,110	308.15	5.13	13,508	318.15	5.21	13,906	328.15	5.29	14,304					
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<b>AUXILIARY INFORMATION</b>																					
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus is based on the design by Morrison and Billett (1) and the version used is a modification of the apparatus of Clever, Battino, Saylor and Gross (2).</p> <p>Degassing. The solvent is sprayed into an evacuated chamber of an all glass apparatus; it is stirred and heated until the pressure drops to the vapor pressure of the liquid.</p> <p>Solubility Determination. The degassed liquid passes in a thin film down a glass spiral tube at a total pressure of one atm of solute gas plus solvent vapor. The gas absorbed is measured in the attached buret system, and the solvent is collected in a tared flask and weighed.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Matheson Co., Inc. min. vol. % purity 99.999. (2) Olive Oil. A. U.S.P., Fisher Scientific Company., 0.58% free fatty acid. B. Nutritional Biochemicals Corp., 0.30% free fatty acid. The density was measured and fitted to the equation $\rho / \text{g cm}^{-3} = 0.9152 - 0.000468 t / \text{C}$ . The average mol wt is $884 \pm 45$ (3).																				
	<b>ESTIMATED ERROR:</b> $\delta T / \text{K} = 0.03$ $\delta P / \text{mmHg} = 0.5$ $\delta X_1 / X_1 = 0.005$																				
	<b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u> , 2033. 2. Clever, H. L.; Battino, R.; Saylor, J. H.; Gross, P. M. <i>J. Phys. Chem.</i> <u>1957</u> , <i>61</i> , 1078. 3. Johnson, L. F.; Shooley, J. N. <i>Anal. Chem.</i> <u>1962</u> , <i>34</i> , 1136.																				

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Olive oil.		Power, G.G.; Stegall, H. <i>J. Appl. Physiol.</i> <u>1970</u> , <i>19</i> , 145-9.	
VARIABLES:		PREPARED BY:	
T/K = 285-310		C.L. Young	
EXPERIMENTAL VALUES:			
T/K	Bunsen coefficient, $\alpha$	S.D. *	No. of measurements
310.15	0.117	0.002	5
298.15	0.119	0.001	5
285.15	0.121	0.002	5
* Standard deviation.			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Liquid saturated with gas in a stirred cell. 5.0 cm <sup>3</sup> samples of liquid removed in a calibrated syringe and amount of gas extracted by two extraction in a van Slyke apparatus determined. Details in source and ref. (1).		(1) Matheson Co. sample, purity better than 99.7 mole per cent. (2) No details given.	
		ESTIMATED ERROR: $\delta T/K = \pm 0.1$	
		REFERENCES: 1. Power, G.G. <i>J. Appl. Physiol.</i> <u>1968</u> , <i>24</i> , 468.	

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Olive oil				ORIGINAL MEASUREMENTS: Ke, P. J.; Ackman, R. G. <i>J. Am. Oil Chemists' Soc.</i> <u>1973</u> , 50, 429-35.		
VARIABLES: T/K = 293.15 - 353.15 P/kPa = partial pressure of oxygen in air at 101.325 kPa				PREPARED BY:  P. L. Long H. L. Clever		
EXPERIMENTAL VALUES:						
Temperature t/°C	Density T/K ρ/g cm <sup>-3</sup>	Peroxide Value meq kg <sup>-1</sup>	Bunsen Coefficient/α <sup>1</sup>			
			Polarographic Exponential Dilution Method	Chemical Method <sup>2</sup>	Displacement Method <sup>3</sup>	
20	293.15	0.9235 0.9235	0.9 41.5	0.102(+6%) 0.106(±6%)	0.109(+8%) 0.150(±15%)	0.098(+6%) 0.107(±8%)
40	313.15	0.9114	1.0	0.110(+5%)	0.121(+10%)	---
<p><sup>1</sup> Values are the average of three determinations. Numbers in ( ) are the percentage relative error.</p> <p><sup>2</sup> Chemical method of McDowell, A. K. R. <i>J. Dairy Res.</i> <u>1963</u>, 30, 399.</p> <p><sup>3</sup> Displacement method of Becker, E.; Neiderstebruch, A. <i>Fett Seifen Anstrichm.</i> <u>1966</u>, 68, 135. Details of neither method given in the paper.</p>						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE: Polarographic exponential dilution method (1).  The oil was degassed by the method of Battino et al. (2).  A 155-159 cm <sup>3</sup> sample of degassed oil was transferred to a glass vessel and weighed. The vessel was so constructed that the ratio $V_{\text{top air space}}/V_{\text{oil}}$ was between 0.0704 and 0.0981. A magnetic stirring bar (120 rpm) and a polarographic oxygen sensor were placed in the sample. Air was bubbled through the sample at 15 cm <sup>3</sup> m <sup>-1</sup> for two hours. The air was stopped, and helium gas preheated to the sample temperature was introduced into the oil at a rate of 7-10 cm <sup>3</sup> m <sup>-1</sup> . The oxygen concentration was measured as a function of the volume of helium passed through the solution. A plot of log (O <sub>2</sub> ) vs. $V_{\text{helium}}$ is linear. The slope is a function of the Ostwald coefficient. The Ostwald coefficient was converted to Bunsen coefficient.				SOURCE AND PURITY OF MATERIALS: (1) Oxygen. Breathing grade compressed air.  (2) Olive oil. Italian origin. Bought in retail store.		
				ESTIMATED ERROR: Solubility values are the average of three determinations with relative standard deviation of 7% or less.		
				REFERENCES: 1. Aho, L.; Wahlroos, O. <i>J. Am. Oil Chem. Soc.</i> <u>1967</u> , 44, 65. 2. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , 45, 806.		



EXPERIMENTAL VALUES:		T/K = 310.15		
Treatment	$P_{O_2}$ /mmHg	$P_{O_2}$ /kPa	Bunsen Coefficient, $\alpha/cm^3$ (STP) $cm^{-3}atm^{-1}$	Corrected Bunsen Coefficient, $\alpha/cm^3$ (STP) $cm^{-3}atm^{-1}$
K <sub>3</sub> Fe(CH) <sub>6</sub> , 3.2g/100 ml saponin	706	94.1	0.0231	0.0249
	375	50.0	0.0218	0.0236
K <sub>3</sub> Fe(CN) <sub>6</sub> , 3.2g/100 ml	382	50.9	0.0204	0.0222
	382	50.9	0.0209	0.0227
Triton-X	382	50.9	0.0202	0.0220
	398	53.1	0.0221	0.0225
NaNO <sub>2</sub> , 0.05g/100 ml	398	53.1	0.0216	0.0220
	398	53.1	0.0216	0.0220
	382	50.9	0.0219	0.0227
NaNO <sub>2</sub> , 1.0g/100 ml	382	50.9	0.0217	0.0225
	382	50.9	0.0219	0.0227
	382	50.9	0.0221	0.0229
	382	50.9	0.0215	0.0223
	366	48.8	0.0234	0.0242
NaNO <sub>2</sub> , (1.0g/100 ml) freeze-thaw hemolysis	366	48.8	0.0223	0.0231
	366	48.8	0.0217	0.0225
	366	48.8	0.0228	0.0236
	366	48.8	0.0229	0.0237
	366	48.8	0.0233	0.0241
Average .. 0.0230 ± 0.0008				
AUXILIARY INFORMATION				
METHOD / APPARATUS / PROCEDURE:			SOURCE AND PURITY OF MATERIALS:	
Liquid samples were equilibrated with gas and then the dissolved gas was stripped out under vacuum and measured in a manometric Van Slyke apparatus. Various amounts of K <sub>3</sub> Fe(CN) <sub>6</sub> or NaNO <sub>2</sub> were added to the blood to prevent the formation of oxyhemoglobin. The above results have been corrected for the decrease in solubility due to the presence of these salts.			Details given under method.	
			ESTIMATED ERROR:	
			$\delta T/K = \pm 0.03$ .	
			REFERENCES:	

COMPONENTS:

(1) Oxygen; O<sub>2</sub>; [7782-44-7]

(2) Human blood

ORIGINAL MEASUREMENTS:

Power, G. G.

*J. Appl. Physiol.* 1968, 24, 468-74.

VARIABLES:

PREPARED BY:

C. L. Young

<b>COMPONENTS:</b> (1) Oxygen: O <sub>2</sub> ; [7782-44-7] (2) Human blood (3) Krebs-Henseleit solution, human blood, and human plasma with added NaNO <sub>2</sub>	<b>ORIGINAL MEASUREMENTS:</b> Christoforides, C.: Hedley-Whyte, J. <i>J. Appl. Physiol.</i> <u>1969</u> , 27, 592-6.																												
<b>VARIABLES:</b> T/K = 291-310 Concentration	<b>PREPARED BY:</b> R. Battino																												
<b>EXPERIMENTAL VALUES:</b> $10^2 \alpha^a / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$ <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th>Hb<sup>b</sup> concn./ (g/100 ml)</th> <th>18</th> <th>28</th> <th>37</th> </tr> </thead> <tbody> <tr> <td>2.5</td> <td>2.90</td> <td>2.49</td> <td>2.19</td> </tr> <tr> <td>7.8</td> <td>2.93</td> <td>2.50</td> <td>2.20</td> </tr> <tr> <td>13.3</td> <td>2.96</td> <td>2.52</td> <td>2.22</td> </tr> <tr> <td>17.1</td> <td>2.99</td> <td>2.55</td> <td>2.25</td> </tr> <tr> <td>20.5</td> <td>3.04</td> <td>2.60</td> <td>2.29</td> </tr> <tr> <td>27.8</td> <td>3.14</td> <td>2.70</td> <td>2.38*</td> </tr> </tbody> </table>		Hb <sup>b</sup> concn./ (g/100 ml)	18	28	37	2.5	2.90	2.49	2.19	7.8	2.93	2.50	2.20	13.3	2.96	2.52	2.22	17.1	2.99	2.55	2.25	20.5	3.04	2.60	2.29	27.8	3.14	2.70	2.38*
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<p><sup>a</sup> Bunsen coefficient. Values are averages of 14 determinations, except the asterisked value which is for 13 determinations.</p> <p><sup>b</sup> Hemoglobin concentration.</p> $10^2 \alpha^a / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$ <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th rowspan="2">Solvent</th> <th rowspan="2">No. Dets.</th> <th colspan="4">NaNO<sub>2</sub> concn/(g/100 ml)</th> </tr> <tr> <th>0</th> <th>0.01</th> <th>0.5</th> <th>1.0</th> </tr> </thead> <tbody> <tr> <td>Krebs-Henseleit</td> <td>14</td> <td>2.27</td> <td></td> <td>2.25</td> <td>2.20</td> </tr> <tr> <td>Human Blood</td> <td>14</td> <td></td> <td></td> <td>2.225</td> <td>2.18</td> </tr> <tr> <td>Human Plasma</td> <td>12</td> <td></td> <td>2.16</td> <td>2.135</td> <td>2.085</td> </tr> </tbody> </table>		Solvent	No. Dets.	NaNO <sub>2</sub> concn/(g/100 ml)				0	0.01	0.5	1.0	Krebs-Henseleit	14	2.27		2.25	2.20	Human Blood	14			2.225	2.18	Human Plasma	12		2.16	2.135	2.085
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<b>METHOD/APPARATUS/PROCEDURE:</b> Solubilities determined by the Van Slyke method. Smoothed recommended values for oxygen solubility in human blood reported 15-40°C in 1K intervals, and for four H <sub>b</sub> concentrations.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Argon-free, 99.99%, from Precision Gas Products. (2) From each of six normal and healthy men, aged 22-42 years. See original paper for details.																												
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.05$ $\delta \alpha / \alpha = \pm 0.01$																													
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COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Human blood		Roughton, F.J.W.; Severinghaus, J.W. <i>J. Appl. Physiol.</i> <u>1973</u> , 35, 861-9.	
VARIABLES:		PREPARED BY:	
T/K = 273 - 310		R. Battino	
EXPERIMENTAL VALUES:			
t/°C	T/K <sup>a</sup>	Bunsen Coefficient 10 <sup>2</sup> α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>	Ostwald Coefficient <sup>a</sup>
0	273	4.59 <sup>b</sup>	4.59
0	273	4.58 <sup>c</sup>	4.58
22	295	2.91 <sup>d</sup>	3.14
37	310	2.387 <sup>e</sup>	2.710
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Mean of 27 determinations using electrode method.</p> <p><sup>c</sup> Mean of 4 determinations using Van Slyke method.</p> <p><sup>d</sup> Mean of 10 determinations using electrode method.</p> <p><sup>e</sup> Mean of 22 determinations using electrode method.</p> <p><sup>f</sup> α(t°C, blood) = α(t°C, water) × (0.9373 + 0.00160 t/°C); relationship given by authors relating solubility in pure water to that in human blood.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
They used the Van Slyke method for checking at 0°C. The other measurements were made using a Radiometer oxygen electrode which was covered with 25 micron polyethylene. Temperature was controlled to +0.05°C. Solutions were degassed by shaking in oiled syringes with a vacuum. Details are given in the paper.		(1) No details given.	
		(2) 50 cm <sup>3</sup> of venous blood drawn each from four normal non-smoking males into a heparinized glass syringe. Hb concentration averaged 15.5 g/100 cm <sup>3</sup> (range 15.0 - 16.8).	
		ESTIMATED ERROR:	
		δα/α = ±0.03 (compiler's estimate)	
		REFERENCES:	

<p>COMPONENTS:</p> <p>(1) Oxygen: O<sub>2</sub>: [7782-44-7]</p> <p>(2) Human blood</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Christoforides, C.; Hedley-Whyte, J.  <i>J. Appl. Physiol.</i> <u>1976</u>, <i>40</i>, 815-8.</p>																								
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<p>EXPERIMENTAL VALUES:</p> $10^2 \alpha^a / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$ <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">Hb<sup>b</sup> concn/(g/100 ml)</th> <th colspan="3" style="text-align: center;">t/°C</th> </tr> <tr> <th></th> <th style="text-align: center;">0</th> <th style="text-align: center;">6</th> <th style="text-align: center;">12</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">5.6</td> <td style="text-align: center;">4.40</td> <td style="text-align: center;">3.76</td> <td style="text-align: center;">3.23</td> </tr> <tr> <td style="text-align: center;">10.2</td> <td style="text-align: center;">4.43</td> <td style="text-align: center;">3.78</td> <td style="text-align: center;">3.28</td> </tr> <tr> <td style="text-align: center;">15.7</td> <td style="text-align: center;">4.52</td> <td style="text-align: center;">3.86</td> <td style="text-align: center;">3.34</td> </tr> <tr> <td style="text-align: center;">22.5</td> <td style="text-align: center;">4.67</td> <td style="text-align: center;">4.05</td> <td style="text-align: center;">3.45</td> </tr> </tbody> </table>		Hb <sup>b</sup> concn/(g/100 ml)	t/°C				0	6	12	5.6	4.40	3.76	3.23	10.2	4.43	3.78	3.28	15.7	4.52	3.86	3.34	22.5	4.67	4.05	3.45
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Solubilities determined by the van Slyke method. Smoothed recommended values at four Hb concentrations and 0 to 15°C at 1K intervals also given.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Argon-free, 99.99%, from Precision Gas Products.</p> <p>(2) From four healthy non-smoking men, aged 25-41. See original paper for details of handling.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = \pm 0.05</math></p> <p><math>\delta \alpha/\alpha = \pm 0.01</math></p> <p>REFERENCES:</p>																								

COMPONENTS:		ORIGINAL MEASUREMENTS:					
(1) Oxygen: O <sub>2</sub> ; [7732-44-7]		Christoforides, C.; Laasberg, L.H.; Hedley-Whyte, J.					
(2) Human blood plasma		J. Appl. Physiol. 1969, 26, 56-60. (cf. <i>ibid.</i> 1969, 26, R12 for corr.)					
VARIABLES:		PREPARED BY:					
T/K = 291 - 310		R. Battino					
P/kPa = 20 - 98							
EXPERIMENTAL VALUES:							
t <sup>a</sup> /°C	T/K <sup>b</sup>	P <sub>O<sub>2</sub></sub> /mm Hg	10 <sup>2</sup> L <sup>b,c</sup>	10 <sup>2</sup> $\frac{\alpha^d}{\text{cm}^3 \text{atm}^{-1}}$	No. Detns. <sup>e</sup>	$\sigma^f$	
18	291.15	737.4	3.04	2.85	10	0.009	
28	301.15	724.4	2.71	2.46	12	0.017	
37	310.15	149.6	2.42	2.13	11	0.012	
37	310.15	355.2	2.43	2.14	10	0.006	
37	310.15	534.1	2.44	2.15	12	0.006	
37	310.15	705.6	2.44	2.15	13	0.008	
<p>a Controlled to <math>\pm 0.05</math> K.</p> <p>b Calculated by compiler.</p> <p>c Ostwald coefficient.</p> <p>d Bunsen coefficient.</p> <p>e Number of determinations at that partial pressure of oxygen.</p> <p>f Authors' calculated standard deviation.</p>							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:				
Standard van Slyke manometric technique employed. Also some measurements made with an oxygen electrode. Paper reports calculated values at 1K intervals from 0 to 40°C.			(1) Argon-free, 99.99% from Precision Gas Products				
			(2) Blood obtained from a 31 year-old healthy man, and the plasma separated. Details given in the original paper.				
			ESTIMATED ERROR:				
			$\delta T/K = \pm 0.05$				
			$\delta \alpha/\alpha = \pm 0.01$ , authors' estimate				
			REFERENCES:				

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Wise, D.L.; Houghton, G.			
(2) Human hemoglobin		<i>Biophys. J.</i> <u>1969</u> , 9,36-53.			
(3) Water; H <sub>2</sub> O; [7732-18-5]					
VARIABLES:		PREPARED BY:			
T/K = 283 - 333 concentration		R. Battino			
EXPERIMENTAL VALUES:					
t/°C	T/K <sup>a</sup>	10 <sup>2</sup> L <sup>a,b</sup>	10 <sup>2</sup> α <sup>c</sup> / cm <sup>3</sup> (STP)cm <sup>-3</sup> atm <sup>-1</sup>	S <sub>0</sub> <sup>d</sup>	
5 wt % packed red cells					
10	283.2	4.73	4.61	46.1	
20	293.2	3.96	3.69	37.0	
30	303.2	3.33	3.00	30.1	
40	313.2	3.10	2.70	27.2	
50	323.2	3.04	2.57	26.0	
60	333.2	2.85	2.34	23.8	
10 wt % packed red cells					
10	283.2	6.85	6.61	66.1	
20	293.2	5.36	4.99	49.9	
30	303.2	4.67	4.21	42.3	
40	313.2	4.10	3.58	36.1	
50	323.2	4.01	3.39	34.3	
60	333.2	3.56	2.92	29.7	
20 wt % packed red cells					
10	283.2	9.59	9.25	92.6	
20	293.2	8.08	7.53	75.4	
30	303.2	6.75	6.08	61.1	
40	313.2	5.62	4.90	49.4	
50	323.2	4.74	4.01	40.6	
60	333.2	4.21	3.45	35.6	
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Used an adaptation of the Morrison and Billett apparatus(1), but with the gas capacity of the manometer-buret system being about 15 cm <sup>3</sup> . The storage spiral, the absorption spiral, and the manometer-buret system were thermostatted in glass jackets through which water from a thermostat circulated.			(1) No details given.		
			(2) Prepared from just out-dated human red blood cells. Mixed with degassed water to make up solutions.		
			(3) Boiled and deionized.		
			ESTIMATED ERROR:		
			δα/α = ±0.01		
			δT/K = ±0.1		
			REFERENCES:		
			1. Morrison, T.J.; Billett, F. <i>J. Chem. Soc.</i> <u>1952</u> , 3819-22.		

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Human hemoglobin (3) Water; H <sub>2</sub> O; [7732-18-5]	EVALUATOR: Wise, D.L.; Houghton, G. <i>Biophys. J.</i> <u>1969</u> , 9, 36-53.
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## CRITICAL EVALUATION:

continued

<sup>a</sup> Calculated by compiler.

<sup>b</sup> Ostwald coefficient.

<sup>c</sup> Bunsen coefficient.

<sup>d</sup> Solubility in cm<sup>3</sup> (STP)/1000 g of solution. Solubilities fitted to:  $\log_{10} S_0 = -A + B/(T/K) + C \log_{10}(T/K)$ .

wt %	A	B	C
5	19.497	1406.59	6.59453
10	16.1187	1339.30	5.37665
20	-0.9971	724.42	-0.64668

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hemoglobin (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R.  <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.																								
<b>VARIABLES:</b> T/K = 310.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																								
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Hemoglobin g 100 cm<sup>-3</sup></th> <th style="text-align: center;">Bunsen Coefficient 10<sup>4</sup>α/cm<sup>3</sup>cm<sup>-3</sup> atm<sup>-1</sup></th> <th style="text-align: center;">Constant<sup>1</sup> k=(1/c) ln (α/α<sub>0</sub>)</th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">310.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">241</td> <td></td> </tr> <tr> <td></td> <td style="text-align: center;">10</td> <td style="text-align: center;">241 ± 7</td> <td></td> </tr> <tr> <td></td> <td style="text-align: center;">20</td> <td style="text-align: center;">245 ± 8</td> <td></td> </tr> <tr> <td></td> <td style="text-align: center;">25</td> <td style="text-align: center;">245 ± 10</td> <td></td> </tr> <tr> <td colspan="3"></td> <td style="text-align: center;">+0.00070</td> </tr> </tbody> </table> <p><sup>1</sup> k/g<sup>-1</sup>100 cm<sup>3</sup></p>		T/K	Hemoglobin g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )	310.15	0	241			10	241 ± 7			20	245 ± 8			25	245 ± 10					+0.00070
T/K	Hemoglobin g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )																						
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			+0.00070																						
<b>AUXILIARY INFORMATION</b>																									
<b>METHOD/APPARATUS/PROCEDURE:</b> Classical Van Slyke method (1).  The apparatus sample volume and constant gas volume are carefully calibrated. The correction for unextracted gas is made, but the reabsorption correction is not necessary for oxygen.  Equilibration is undertaken in a thermostated tonometer. A 2 cm <sup>3</sup> sample is directly transferred to the Van Slyke apparatus for analysis.  The solubility of oxygen in water value is from the authors analysis of ten literature values (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Linde Co. Purity 99.9 per cent by volume.  (2) Hemoglobin. No information.  (3) Water. Distilled.  <b>ESTIMATED ERROR:</b> δT/K = 0.1 δα/α = 0.01																								
	<b>REFERENCES:</b> 1. Van Slyke, D. D.; Neill, J. M. <i>J. Biol. Chem.</i> <u>1924</u> , 61, 523. 2. Zander, R.; Euler, R. <i>Measurement of Oxygen</i> , Edited by Degn, H.; Balslev, I.; Brook, R. Elsevier, Amsterdam, 1976, p.271.																								



<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Human Serum</p> <p>(3) Corticosteroids; [50-04-4], [125-04-2], [151-73-5], [1715-33-9], [2375-03-3], and [2392-39-4]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Gainer, J. V. Jr.; Gainer, J. L.; Kelly, R.</p> <p><i>Steroids</i> 1976, 28, 307-10.</p>
<p>VARIABLES:</p> <p>T/K = 298.15</p> <p>O<sub>2</sub> P/kPa = about 101.325</p> <p>Corticosteroid/μg cm<sup>-3</sup> = 0 - 200</p>	<p>PREPARED BY:</p> <p>H. L. Clever</p>
<p>EXPERIMENTAL VALUES:</p> <p style="text-align: center;">continued on following page</p>	
<p style="text-align: center;">AUXILIARY INFORMATION</p>	
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Reconstituted human serum was placed in a beaker, antifoaming agent (Anti-foamer-A, Dow Corning) was added, oxygen was bubbled through the solution for 10 minutes, and a sample was taken in an airtight syringe. The sample was injected into a gas chromatograph for the determination of the oxygen by the method of Navarri (1). The sample passed through a drying tube of CaSO<sub>4</sub>. The chromatograph used a Beckman GC2A thermal conductivity detector and was fitted with a molecular sieve column. Preliminary tests showed that the O<sub>2</sub> solubility was the same in plasma and serum, that the anti-foamer did not change the solubility, and that O<sub>2</sub> was not absorbed in the drying column.</p> <p>Data read from small graphs.</p> <p>Evaluator's Comment. The large changes in O<sub>2</sub> solubility with small concentrations of corticosteroids are startling. Confirmation by other workers is desirable.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Source not given. 99 per cent purity.</p> <p>(2) Human serum. Lyophilized human serum was reconstituted for use.</p> <p>(3) Corticosteroids. Commercial samples. Sources given in table above, along with Chem. Abstr. index formulas.</p> <p>ESTIMATED ERROR: <math>\delta T/K = 1</math></p> <p>Authors say values were average of repeated tests with values falling within a 5 per cent range.</p> <p>REFERENCES:</p> <p>1. Navarri, R. M. Mass Transport in Biological Systems. Ph.D. Dissertation, University of Virginia, Charlottesville, VA 1970.</p>

COMPONENTS:	ORIGINAL MEASUREMENTS:				
(1)Oxygen; O <sub>2</sub> ; [7782-44-7]	Gainer, J. V. Jr.; Gainer, J. L.; Kelly, R. <i>Steroids</i> 1976, 28, 307-10.				
(2)Human Serum					
(3)Corticosteroids; [50-04-4], [125-04-2], [151-73-5], [1715-33-9], [2375-03-3], and [2392-39-4]					
EXPERIMENTAL VALUES: <span style="float: right;">continued</span>					
9-Fluoro-11 $\beta$ ,17,21-trihydroxy-16 $\alpha$ -methyl-1,4-pregnadiene-3,20-dione or Dexamethasone sodium phosphate or Decadron <sup>R</sup> , Merck, Sharpe and Dohme; C <sub>22</sub> H <sub>30</sub> F <sub>08</sub> P.2Na; [2392-39-4]					
Solubility Ratio:					
(O <sub>2</sub> in serum + steroid/O <sub>2</sub> in serum)x100 Steroid/ $\mu$ g cm <sup>-3</sup>					
	+42	+38	+37	+ 5	- 5
	0.5	2.5	5.	25.	100.
9-Fluoro-11 $\beta$ , 17, 21-trihydroxy-16 $\beta$ -methyl-1,4-pregnadiene-3, 20-dione or Betamethasone sodium phosphate or Celestone <sup>R</sup> , Schering; C <sub>22</sub> H <sub>30</sub> F <sub>08</sub> P.2Na; [151-73-5]					
Solubility Ratio:					
(O <sub>2</sub> in serum + steroid/O <sub>2</sub> in serum)x100 Steroid/ $\mu$ g cm <sup>-3</sup>					
	+42	+38	+35	+15	+ 2
	0.625	2.5	5.	10.	20.
Cortisone acetate, Upjohn Co.; C <sub>23</sub> H <sub>30</sub> O <sub>6</sub> ; [50-04-4]					
Solubility Ratio:					
(O <sub>2</sub> in serum + steroid/O <sub>2</sub> in serum)x100 Steroid/ $\mu$ g cm <sup>-3</sup>					
	0	-20	-19	-10	-12
	1.	12.	30.	110.	225.
11 $\beta$ , 17, 21-trihydroxy-1,4-pregnadiene-3, 20-dione or Prednisolone sodium succinate or Meticortelone <sup>R</sup> , Schering, Co.; C <sub>25</sub> H <sub>32</sub> O <sub>8</sub> .Na; [1715-33-9]					
Solubility Ratio:					
(O <sub>2</sub> in serum + steroid/O <sub>2</sub> in serum)x100 Steroid/ $\mu$ g cm <sup>-3</sup>					
	-20	-17	-24	-12	
	2.5	5.	40.	80.	
The two compounds listed below were stated to behave similarly to the cortisone and the prednisolone but no data were given.					
Hydrocortisone sodium succinate or Solu Cortef <sup>R</sup> , Upjohn Co.; C <sub>25</sub> H <sub>34</sub> O <sub>8</sub> .Na; [125-04-2]					
11 $\beta$ ,17,21-trihydroxy-6 $\alpha$ -methyl-1,4-pregnadiene-3,20-dione or Methylprednisolone sodium succinate or Solu Medrol <sup>R</sup> , Upjohn Co.; C <sub>26</sub> H <sub>34</sub> O <sub>8</sub> .Na; [2375-03-3]					

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Phosphate buffer and human red cell ghosts in phosphate buffer.</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Power, G.G.; Stegall, H. <i>J. Appl. Physiol.</i> 1970, 29, 145-9.</p>																								
<p>VARIABLES:</p> <p>T/K = 310</p>	<p>PREPARED BY:</p> <p>C.L. Young</p>																								
<p>EXPERIMENTAL VALUES:</p>																									
<table border="1"> <thead> <tr> <th>T/K</th> <th>Bunsen coefficient, <math>\alpha</math></th> <th>S.D.*</th> <th>No. of measurements.</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Phosphate Buffer</td> </tr> <tr> <td>310.15</td> <td>0.02375</td> <td>0.00055</td> <td>7</td> </tr> <tr> <td colspan="4" style="text-align: center;">Ghosts suspension in buffer</td> </tr> <tr> <td>310.15</td> <td>0.02440</td> <td>0.00128</td> <td>6</td> </tr> <tr> <td>310.15</td> <td>0.0252§</td> <td>0.0011</td> <td>3</td> </tr> </tbody> </table>		T/K	Bunsen coefficient, $\alpha$	S.D.*	No. of measurements.	Phosphate Buffer				310.15	0.02375	0.00055	7	Ghosts suspension in buffer				310.15	0.02440	0.00128	6	310.15	0.0252§	0.0011	3
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<p>* Standard deviation</p> <p>§ Disrupted membranes</p> <p><math>\alpha^\circ</math> ghost = (<math>\alpha</math> ghost suspension - <math>\alpha</math> buffer) / g ghost cm<sup>-3</sup> = 0.113 ± 0.097</p>																									
<p style="text-align: center;">AUXILIARY INFORMATION</p>																									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>5 to 12 cm<sup>-3</sup> samples placed in a stirrer cell and gas, saturated with water vapor passed through liquid for 30 -60 mins. Samples of saturated liquid withdrawn and transferred to Van Slyke apparatus. Dissolved gas removed under reduced pressure. Red cell ghosts prepared by centrifugation of human blood and lysing the cells using phosphate buffer of pH 7.4. Ghost separated by high speed centrifugation. Washed with phosphate buffer containing 0.01M sodium nitrite.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Matheson sample, purity better than 99.7 mole per cent.</p> <p>(2) See method.</p> <hr/> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = \pm 0.1</math></p> <hr/> <p>REFERENCES:</p>																								

COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Human pulmonary tissue		Power, G. G. <i>J. Appl. Physiol.</i> 1968, 24, 468-74.		
VARIABLES:		PREPARED BY:		
T/K = 310		C. L. Young		
EXPERIMENTAL VALUES:				
T/K = 310.15				
Treatment	P <sub>O<sub>2</sub></sub> /mmHg	P <sub>O<sub>2</sub></sub> /kPa	Bunsen Coefficient, α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>	Corrected Bunsen Coefficient, α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>
NaNO <sub>2</sub> , 1.0g/100 ml	372	49.6	0.0212	0.0220
	372	49.6	0.0201	0.0209
	372	49.6	0.0198	0.0206
	372	49.6	0.0220	0.0228
	372	49.6	0.0224	0.0232
	372	49.6	0.0204	0.0212
	372	49.6	0.0202	0.0210
	372	49.6	0.0205	0.0213
K <sub>3</sub> Fe(CN) <sub>6</sub> , 3.2g/100 ml saponin	365	48.7	0.0194	0.0212
	365	48.7	0.0190	0.0208
	365	48.7	0.0195	0.0213
	365	48.7	0.0186	0.0204
	365	48.7	0.0184	0.0202
	365	48.7	0.0199	0.0217
	365	48.7	0.0186	0.0204
	365	48.7	0.0206	0.0224
Average ..				0.0213 ± 0.0008
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
Sample of tissue homogenised; no effort was made to remove blood. Samples were equilibrated with gas and then dissolved gas was stripped out under vacuum and measured in a manometric Van Slyke apparatus. Various amounts of K <sub>3</sub> Fe(CN) <sub>6</sub> or NaNO <sub>2</sub> were added to the tissue to prevent formation of oxyhemoglobin. The above results have been corrected for the decrease in solubility due to the presence of these salts.		Details given under method.		
		ESTIMATED ERROR: δT/K = ±0.03.		
		REFERENCES:		

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sheep placental tissue		Power, G. G. <i>J. Appl. Physiol.</i> 1968, 24, 468-74.			
VARIABLES:		PREPARED BY:			
T/K = 310		C. L. Young			
EXPERIMENTAL VALUES:					
T/K = 310.15					
Treatment	P <sub>O<sub>2</sub></sub> /mmHg	P <sub>O<sub>2</sub></sub> /kPa	Bunsen Coefficient, α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>	Corrected Bunsen Coefficient, α/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>	
K <sub>3</sub> Fe(CN) <sub>6</sub> , 2.9g/100 ml	366	48.8	0.0198	0.0214	
Triton-X	366	48.8	0.0207	0.0223	
	366	48.8	0.0198	0.0214	
NaNO <sub>2</sub> , 0.9g/100 ml	366	48.8	0.0217	0.0244	
Triton-X	366	48.8	0.0214	0.0221	
	366	48.8	0.0206	0.0213	
NaNO <sub>2</sub> , 1.0g/100 ml	368	49.1	0.0178	0.0186	
	368	49.1	0.0189	0.0197	
	368	49.1	0.0194	0.0202	
	368	49.1	0.0183	0.0191	
Average ..				0.0209 ± 0.0012	
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Samples of tissue homogenised; no effort was made to remove blood. Samples were equilibrated with gas and then dissolved gas stripped out under vacuum and measured in a manometric Van Slyke apparatus. Various amounts of K <sub>3</sub> Fe(CN) <sub>6</sub> or NaNO <sub>2</sub> were added to the tissue to prevent formation of oxyhemoglobin. The above results have been corrected for the decrease in solubility due to the presence of these salts.			Details given under method.		
			ESTIMATED ERROR:		
			δT/K = ±0.03.		
			REFERENCES:		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Krebs solution (3) FC-80 which is mostly a mixture of isomers of perfluorobutyl-tetrahydrofuran; C <sub>8</sub> F <sub>16</sub> O; e.g. see [335-36-4]	<b>ORIGINAL MEASUREMENTS:</b> Wong, S. S.; DiMicco, J. A.; Standaert, D. G.; Dretchen, K. L. <i>J. Gen. Physiol.</i> 1977, 69, 655-66.																										
<b>VARIABLES:</b> T/K = 310.15 P/kPa = 91.9 - 94.8 FC-80 emulsion/per cent = 20	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																										
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Oxygen Tension p/mmHg</th> <th style="text-align: center;">Time after oxygen bubbling ceases, t/m</th> <th style="text-align: center;">Volume Per<sub>3</sub>Cent Oxygen, cm<sup>3</sup> 100 cm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Krebs solution</td> </tr> <tr> <td rowspan="2" style="text-align: center;">310.15</td> <td style="text-align: center;">690.0 ± 11.6 graph</td> <td style="text-align: center;">0</td> <td style="text-align: center;">2.23 ± 0.03</td> </tr> <tr> <td></td> <td style="text-align: center;">60</td> <td style="text-align: center;">1.43 ± 0.03</td> </tr> <tr> <td colspan="4" style="text-align: center;">Emulsion: 80 per cent Krebs solution, 20 per cent FC-80</td> </tr> <tr> <td rowspan="2" style="text-align: center;">310.15</td> <td style="text-align: center;">711.6 ± 9.29 graph</td> <td style="text-align: center;">0</td> <td style="text-align: center;">8.03 ± 0.44</td> </tr> <tr> <td></td> <td style="text-align: center;">60</td> <td style="text-align: center;">7.53 ± 0.41</td> </tr> </tbody> </table> <p>The uncertainties are standard error.</p>		T/K	Oxygen Tension p/mmHg	Time after oxygen bubbling ceases, t/m	Volume Per <sub>3</sub> Cent Oxygen, cm <sup>3</sup> 100 cm <sup>-3</sup>	Krebs solution				310.15	690.0 ± 11.6 graph	0	2.23 ± 0.03		60	1.43 ± 0.03	Emulsion: 80 per cent Krebs solution, 20 per cent FC-80				310.15	711.6 ± 9.29 graph	0	8.03 ± 0.44		60	7.53 ± 0.41
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<b>AUXILIARY INFORMATION</b>																											
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The emulsion was formed by sonicating a mixture of FC-80 and Krebs solution for 30 minutes.</p> <p>The Krebs solution or the emulsion were thermostated at 36 - 38 °C. A mixture of 95 per cent oxygen and 5 per cent carbon dioxide was bubbled through the solvent for 60 minutes.</p> <p>Total oxygen was measured with an oxygen analyzer and oxygen tension was measured with a pO<sub>2</sub> electrode.</p> <p>The Krebs solution composition in g dm<sup>-3</sup> was:</p> <table style="width: 100%;"> <tbody> <tr><td>NaCl</td><td></td></tr> <tr><td>KCl</td><td style="text-align: right;">0.35</td></tr> <tr><td>MgSO<sub>4</sub>·7H<sub>2</sub>O</td><td style="text-align: right;">0.29</td></tr> <tr><td>CaCl<sub>2</sub></td><td style="text-align: right;">0.28</td></tr> <tr><td>KH<sub>2</sub>PO<sub>4</sub></td><td style="text-align: right;">0.16</td></tr> <tr><td>NaHCO<sub>3</sub></td><td style="text-align: right;">2.1</td></tr> <tr><td>Dextrose</td><td></td></tr> </tbody> </table> <p>Emulsifying agent was Pluronic F68 150 mg per 100 cm<sup>3</sup></p>	NaCl		KCl	0.35	MgSO <sub>4</sub> ·7H <sub>2</sub> O	0.29	CaCl <sub>2</sub>	0.28	KH <sub>2</sub> PO <sub>4</sub>	0.16	NaHCO <sub>3</sub>	2.1	Dextrose		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. No information. (2) Krebs solution. Prepared in distilled water. See bottom of left column. (3) FC-80. Minnesota Mining and Manufacturing Co. Used as received.												
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<b>ESTIMATED ERROR:</b> $\delta T/K = 1$ The maximum standard error is 5.5 % of the mean.																											
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COMPONENTS:		ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Navari, R. M.; Rosenblum, W. I.; Kontos, H. A.; Patterson, J. L.		
(2) Aqueous physiologic salt solution		<i>Res. Exp. Med.</i> <u>1977</u> , <i>170</i> , 169-80.		
(3) FC-47, which is largely 1,1,2,2,3,3,4,4,4-nonafluoro-N,N-bis(nonafluorobutyl)-1-butanamine; C <sub>12</sub> F <sub>27</sub> N; [311-89-7]				
VARIABLES:		PREPARED BY:		
T/K = 310.15 P/kPa = 6.66 - 101.325		H. L. Clever		
Emulsion of several concentrations				
EXPERIMENTAL VALUES:				
T/K	Oxygen Pressure p/mmHg	Emulsion Composition g FC-47 per 100 cm <sup>3</sup>	Oxygen Solubility <sup>1</sup> cm <sup>3</sup> O <sub>2</sub> /cm <sup>3</sup>	Diffusion Coefficient <sup>2</sup> 10 <sup>-5</sup> D/cm <sup>2</sup> s <sup>-1</sup>
310.15	50	22	0.0040±0.0010	2.43±0.07
	100		0.0090±0.0010	2.79±0.10
	150		0.0143±0.0011	2.88±0.08
	760		0.0797±0.0011	2.93±0.09
	150	25	0.0180±0.0010	2.84±0.01
	760		0.0932±0.0011	3.03±0.09
	150	33	0.0200±0.0010	2.96±0.09
	760		0.1173±0.0082	3.21±0.14
	50	* <sup>3</sup>	0.23 <sup>4</sup>	
	100		0.28 <sup>4</sup>	
	150		0.31 <sup>4</sup>	
	760		0.36 <sup>4</sup>	
<sup>1</sup> Mean of five determinations ± standard deviation. <sup>2</sup> Mean of three determinations ± standard deviation. <sup>3</sup> Pure FC-47, not an emulsion. <sup>4</sup> Values read from a graph (Fig 2) in the paper.				
The solubility values read from the graph appear to be Bunsen coefficients. The authors call it a solubility coefficient. They do not describe how it is calculated.				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:		
The solubilities were measured by the gas chromatograph method of Shoor <i>et al.</i> (1). The gas, presaturated with solvent vapor, was passed through the degassed liquid in the saturation cell at a rate of 50 ml m <sup>-1</sup> . Twenty microliter samples of the gas-saturated liquid were withdrawn and analyzed chromatographically at 15 m intervals. When readings remained constant for one hour the solution was assumed to be saturated. The time for saturation was less than 2 hours. The apparatus was calibrated with pure dry oxygen.		(1) Oxygen. No information.		
The results confirm the report of Zander (2) that oxygen solubility in FC-47 does not obey Henry's law in either the pure liquid or the emulsion. The departure from Henry's law appears to be more pronounced at oxygen partial pressures below 150 mmHg.		(2) Physiologic salt solution.  Ion Na K Ca Cl Lactate meq dm <sup>-3</sup> 154 4 3 109 28  A non-ionic detergent, Pluronic F-68/g dm <sup>-3</sup> 48; Tris buffer to adjust the pH to 7.30 ± 0.10. Emulsion osmolarity/mOsm dm <sup>-3</sup> 272 - 292.		
Emulsion prepared by sonication.		(3) FC-47. 3 M Co.		
		ESTIMATED ERROR:		
		REFERENCES:		
		1. Shoor, S. K.; Walker, R. D. Jr.; Gubbins, K. E. <i>J. Phys. Chem.</i> <u>1969</u> , <i>73</i> , 312.		
		2. Zander, R. <i>Res. Exp. Med.</i> <u>1974</u> , <i>164</i> , 97.		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Globulins, bovine (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R.  <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.																																								
<b>VARIABLES:</b> T/K = 310.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																																								
<b>EXPERIMENTAL VALUES:</b>																																									
<table border="1"> <thead> <tr> <th>T/K</th> <th>Globulins, bovine g 100 cm<sup>-3</sup></th> <th>Bunsen Coefficient 10<sup>4</sup>α/cm<sup>3</sup>cm<sup>-3</sup> atm<sup>-1</sup></th> <th>Constant<sup>1</sup> k=(1/c) ln (α/α<sub>0</sub>)</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align:center">α-Globulin, bovine</td> </tr> <tr> <td rowspan="3">310.15</td> <td>0</td> <td>241</td> <td rowspan="3">-0.00703</td> </tr> <tr> <td>5</td> <td>237 ± 4</td> </tr> <tr> <td>10</td> <td>224 ± 5</td> </tr> <tr> <td colspan="4" style="text-align:center">β-Globulin, bovine</td> </tr> <tr> <td rowspan="3">310.15</td> <td>0</td> <td>241</td> <td rowspan="3">-0.00856</td> </tr> <tr> <td>10</td> <td>220 ± 5</td> </tr> <tr> <td>15</td> <td>213 ± 5</td> </tr> <tr> <td colspan="4" style="text-align:center">-Globulin, bovine</td> </tr> <tr> <td rowspan="3">310.15</td> <td>0</td> <td>241</td> <td rowspan="3">-0.00589</td> </tr> <tr> <td>10</td> <td>232 ± 3</td> </tr> <tr> <td>20</td> <td>214 ± 7</td> </tr> </tbody> </table>		T/K	Globulins, bovine g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )	α-Globulin, bovine				310.15	0	241	-0.00703	5	237 ± 4	10	224 ± 5	β-Globulin, bovine				310.15	0	241	-0.00856	10	220 ± 5	15	213 ± 5	-Globulin, bovine				310.15	0	241	-0.00589	10	232 ± 3	20	214 ± 7
T/K	Globulins, bovine g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )																																						
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<b>METHOD/APPARATUS/PROCEDURE:</b> Classical Van Slyke method (1).  The apparatus sample volume and constant gas volume are carefully calibrated. The correction for unextracted gas is made, but the reabsorption correction is not necessary for oxygen.  Equilibration is undertaken in a thermostated tonometer. A 2 cm <sup>3</sup> sample is directly transferred to the Van Slyke apparatus for analysis.  The solubility of oxygen in water value is from the authors analysis of ten literature values (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Linde Co. Purity 99.9 per cent by volume.  (2) Globulins, bovine. No information.  (3) Water. Distilled.  <b>ESTIMATED ERROR:</b> δT/K = 0.1 δα/α = 0.01																																								
	<b>REFERENCES:</b> 1. Van Slyke, D. D.; Neill, J. M. <i>J. Biol. Chem.</i> <u>1924</u> , 61, 523. 2. Zander, R.; Euler, R. <i>Measurement of Oxygen</i> , Edited by Degn, H.; Balslev, I.; Brook, R. Elsevier, Amsterdam, 1976, p.271.																																								



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Various solutions - see below		<b>ORIGINAL MEASUREMENTS:</b> Shkol'nikova, R.I. <i>Uch. Zap. Leningr. Gos. Univ., Ser. Khim. Nauk.</i> 1959, [18], 64-86. <i>Chem. Abstr.</i> 1961, 55, 25443b.							
<b>VARIABLES:</b> T/K = 283-313 P/kPa = 101 Concentration		<b>PREPARED BY:</b> V. Katovic							
<b>EXPERIMENTAL VALUES:</b> Solubility of Oxygen in Serum Albumin									
		0.575%		1.15%		1.68%		1.99%	
t/°C	T <sup>a</sup> /K	10 <sup>3</sup> <sub>α</sub> <sup>b</sup>	10 <sup>3</sup> <sub>L</sub> <sup>c</sup>	10 <sup>3</sup> <sub>α</sub>	10 <sup>3</sup> <sub>L</sub>	10 <sup>3</sup> <sub>α</sub>	10 <sup>3</sup> <sub>L</sub>	10 <sup>3</sup> <sub>α</sub>	10 <sup>3</sup> <sub>L</sub>
10	283	34.8	36.1	30.9	32.0	28.2	29.2	26.3	27.3
15	288	31.1	32.8	28.1	29.6	26.0	27.4	24.5	25.8
20	293	28.3	30.4	24.3	26.1	22.1	23.7	21.4	23.0
25	298	25.7	28.1	23.0	25.1	20.4	22.3	18.1	19.8
30	303	23.1	25.6	21.9	24.3	18.2	20.2	17.8	19.7
35	308	21.3	24.0	20.4	23.0	17.8	20.1	16.2	18.4
40	313	19.6	22.5	18.1	20.7	16.0	18.4	15.4	17.6
<sup>a</sup> Calculated by compiler. <sup>b</sup> Bunsen coefficient in cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup> . <sup>c</sup> Ostwald coefficient.									
continued on following page									
AUXILIARY INFORMATION									
<b>METHOD/APPARATUS/PROCEDURE:</b> Solubility determined by a manometric/volumetric apparatus described in the paper.					<b>SOURCE AND PURITY OF MATERIALS:</b> (1) 99.98-99.99% pure (2) Serum and egg albumin were purified by dialysis.				
					<b>ESTIMATED ERROR:</b> δα/α = ±0.015, author's estimate				
					<b>REFERENCES:</b>				

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Various solutions - see below	EVALUATOR: Shkolnikova, R.I. <i>Uch. Zap. Leningr. Gos. Univ., Ser. Khim. Nauk.</i> 1959, [18], 64-86. <i>Chem. Abstr.</i> 1961, 55, 25443b.
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## CRITICAL EVALUATION:

continued

## Solubility of Oxygen in Gelatin

t/°C	T <sup>a</sup> /K	1%			5%		10%	
		10 <sup>3</sup> <sub>α</sub> <sup>b</sup>	10 <sup>3</sup> <sub>L</sub> <sup>c</sup>	10 <sup>3</sup> <sub>α</sub>	10 <sup>3</sup> <sub>L</sub>	10 <sup>3</sup> <sub>α</sub>	10 <sup>3</sup> <sub>L</sub>	
10	283	34.9	36.2	29.4	30.5	26.2	27.2	
15	288	32.3	34.7	28.0	29.2	24.1	25.5	
20	293	30.0	32.2	26.9	28.9	22.6	24.2	
25	298	26.6	29.0	22.4	24.4	19.3	22.1	
30	303	21.0	23.3	18.1	20.2	16.0	17.7	
35	308	19.3	21.8	17.9	20.0	14.7	16.6	
40	313	17.1	19.6	14.5	16.6	12.9	14.3	

<sup>a</sup> Calculated by compiler.<sup>b</sup> Bunsen coefficient in cm<sup>3</sup>(STP) cm<sup>-3</sup> atm<sup>-1</sup>.<sup>c</sup> Ostwald coefficient.

## Solubility of Oxygen in Egg Albumin

t/°C	T <sup>a</sup> /K	0.575%		1.15%	
		10 <sup>3</sup> <sub>α</sub> <sup>b</sup>	10 <sup>3</sup> <sub>L</sub> <sup>c</sup>	10 <sup>3</sup> <sub>α</sub>	10 <sup>3</sup> <sub>L</sub>
10	283	35.5	36.8	31.4	32.5
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<sup>a</sup> Calculated by compiler.<sup>b</sup> Bunsen coefficient in cm<sup>3</sup>(STP) cm<sup>-3</sup> atm<sup>-1</sup>.<sup>c</sup> Ostwald coefficient.

t/°C	T <sup>a</sup> /K	Hydrated Iron Oxide			Hydrated Aluminum Oxide		
		0.1%	10 <sup>3</sup> <sub>b</sub>	0.5%	0.8%	0.1%	10 <sup>3</sup> <sub>b</sub>
20	293	30.1	29.6	27.9	31.0	28.7	26.0
30	303	25.3	21.5	20.1	26.5	26.5	21.1
40	313	21.3	16.1	13.0	23.1	23.1	16.5

<sup>a</sup> Calculated by compiler.<sup>b</sup> Bunsen coefficient in cm<sup>3</sup>(STP) cm<sup>-3</sup> atm<sup>-1</sup>.<sup>c</sup> Concentrations are presumably in wt per cent.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Serum Albumin (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Shkol'nikova, R. I.  <i>Uch. Zap. Leningr. Gos. Univ., Ser. Khim. Nauk.</i> 1959, Nr. 18, 64-86.  <i>Chem. Abstr.</i> 1961, 55, 25443b.																																																
<b>VARIABLES:</b> T/K = 283.15 - 313.15 P/kPa = 101.325 serum albumin/Wt % = 0.575 - 1.99	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																																																
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<b>VARIABLES:</b> T/K = 310.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																																				
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<b>METHOD/APPARATUS/PROCEDURE:</b> Classical Van Slyke method (1).  The apparatus sample volume and constant gas volume are carefully calibrated. The correction for unextracted gas is made, but the reabsorption correction is not necessary for oxygen.  Equilibration is undertaken in a thermostated tonometer. A 2 cm <sup>3</sup> sample is directly transferred to the Van Slyke apparatus for analysis.  The solubility of oxygen in water value is from the authors analysis of ten literature values (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Linde Co. Purity 99.9 per cent by volume.  (2) Albumins. No information.  (3) Water. Distilled  <b>ESTIMATED ERROR:</b> δT/K = 0.1 δα/α = 0.01																																				
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 2-Methyl-1-propanol or Isobutanol; C <sub>4</sub> H <sub>10</sub> O; [78-83-1] (3) Cholest-5-en-3β-ol or Cholesterol; C <sub>27</sub> H <sub>46</sub> O; [57-88-5]	<b>ORIGINAL MEASUREMENTS:</b> Byrne, J. E.; Battino, R.; Danforth, W. F. <i>J. Chem. Thermodyn.</i> <u>1974</u> , <i>6</i> , 245-50.																
<b>VARIABLES:</b> T/K = 310.65 Total P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3).  Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid nitrogen trap until the permanent gas residual pressure drops to 5 microns.  Solubility Determination. The degassed solvent is passed in a thin film down a glass helical tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Matheson Co., Inc. 99.995 per cent. (2) 2-methyl-1-propanol or isobutanol. Fisher Scientific Certified. 99 mol per cent. (3) Cholesterol. Source not given. Recrystallized from benzene.  <b>ESTIMATED ERROR:</b> δT/K = 0.01 δP/mmHg = 0.5 δL <sub>O</sub> /L <sub>O</sub> = 0.01 δL <sub>W</sub> /L <sub>W</sub> = 0.02  <b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> <u>1948</u> , 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> <u>1968</u> , <i>45</i> , 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , <i>43</i> , 806.																

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2] (3) Cephalin		<b>ORIGINAL MEASUREMENTS:</b> Byrne, J. E.; Battino, R.; Danforth, W. F.  <i>J. Chem. Thermodyn.</i> 1974, 6, 245-50.	
<b>VARIABLES:</b> T/K = 310.65 Total P/kPa = 101.325		<b>PREPARED BY:</b> H. L. Clever	
<b>EXPERIMENTAL VALUES:</b>			
T/K	Mass Fraction Cephalin W <sub>3</sub>	Ostwald Coefficient L	"Salting Out" Parameter k = (1/W <sub>3</sub> ) log (L <sub>O</sub> /L <sub>W</sub> )
310.59	0.0	0.2379	
310.61	0.0	0.2349	
310.64	0.0	0.2326	
310.66	0.0	0.2318	
310.60	0.1008	0.222	
310.63	0.1008	0.221	0.25 ± 0.09
310.65	0.1996	0.204	
310.68	0.1996	0.205	0.30 ± 0.05
310.62	0.3015	0.191	
310.63	0.3015	0.186	0.32 ± 0.03
310.65	1.0	0.112*	
<p>*Extrapolated oxygen solubility in hypothetical liquid cephalin.</p> <p>L<sub>O</sub> and L<sub>W</sub> are the oxygen Ostwald coefficients in benzene and in the benzene + cephalin solution, respectively.</p>			
<b>AUXILIARY INFORMATION</b>			
<b>METHOD/APPARATUS/PROCEDURE:</b> The solubility apparatus is based on the design of Morrison and Billett (1) and the version used is described by Battino, Evans and Danforth (2). The degassing apparatus is that described by Battino, Banzhof, Bogan, and Wilhelm (3).  Degassing. Up to 500 cm <sup>3</sup> of solvent is placed in a flask of such size that the liquid is about 4 cm deep. The liquid is rapidly stirred, and vacuum is intermittently applied through a liquid nitrogen trap until the permanent gas residual pressure drops to 5 microns.  Solubility Determination. The degassed solvent is passed in a thin film down a glass helical tube containing solute gas plus the solvent vapor at a total pressure of one atm. The volume of gas absorbed is found by difference between the initial and final volumes in the buret system. The solvent is collected in a tared flask and weighed.		<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Matheson Co., Inc. 99.995 per cent. (2) Benzene. J. T. Baker Analyzed Reagent Grade. 99.9 mol per cent, thiophene free. (3) Cephalin. Nutritional Biochemicals Corp. Homostatic phosphatide obtained from bovine brain tissue, used as received.	
		<b>ESTIMATED ERROR:</b> δT/K = 0.01 δP/mmHg = 0.5 δL <sub>O</sub> /L <sub>O</sub> = 0.01 δL <sub>W</sub> /L <sub>W</sub> = 0.02	
		<b>REFERENCES:</b> 1. Morrison, T. J.; Billett, F. <i>J. Chem. Soc.</i> 1948, 2033. 2. Battino, R.; Evans, F. D.; Danforth, W. F. <i>J. Am. Oil Chem. Soc.</i> 1968, 45, 830. 3. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> 1971, 43, 806.	

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Benzene; C<sub>6</sub>H<sub>6</sub>; [71-43-2]</p> <p>(3) Lecithin.</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Byrne, J. E.; Battino, R.; Danforth, W. F.</p> <p><i>J. Chem. Thermodyn.</i> <u>1974</u>, <i>6</i>, 245-50.</p>																																																								
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<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="234 473 1093 1009"> <thead> <tr> <th>T/K</th> <th>Mass Fraction Lecithin W<sub>3</sub></th> <th>Ostwald Coefficient L</th> <th>"Salting Out" Parameter k = (1/W<sub>3</sub>) log (L<sub>O</sub>/L<sub>w</sub>)</th> </tr> </thead> <tbody> <tr><td>310.59</td><td>0.0</td><td>0.2379</td><td></td></tr> <tr><td>310.61</td><td>0.0</td><td>0.2349</td><td></td></tr> <tr><td>310.64</td><td>0.0</td><td>0.2326</td><td></td></tr> <tr><td>310.66</td><td>0.0</td><td>0.2318</td><td></td></tr> <tr><td>310.62</td><td>0.1007</td><td>0.216</td><td></td></tr> <tr><td>310.63</td><td>0.1007</td><td>0.217</td><td>0.34 ± 0.09</td></tr> <tr><td>310.63</td><td>0.2025</td><td>0.203</td><td></td></tr> <tr><td>310.64</td><td>0.2025</td><td>0.206</td><td>0.29 ± 0.05</td></tr> <tr><td>310.59</td><td>0.2993</td><td>0.193</td><td></td></tr> <tr><td>310.61</td><td>0.2993</td><td>0.192</td><td>0.28 ± 0.03</td></tr> <tr><td>310.59</td><td>0.3986</td><td>0.178</td><td></td></tr> <tr><td>310.60</td><td>0.3986</td><td>0.178</td><td>0.30 ± 0.02</td></tr> <tr><td>310.65</td><td>1.0</td><td>0.117*</td><td></td></tr> </tbody> </table> <p>*Extrapolated oxygen solubility in hypothetical liquid lecithin.</p> <p>L<sub>O</sub> and L<sub>w</sub> are the oxygen Ostwald coefficients in benzene and in the benzene + lecithin solution, respectively.</p>		T/K	Mass Fraction Lecithin W <sub>3</sub>	Ostwald Coefficient L	"Salting Out" Parameter k = (1/W <sub>3</sub> ) log (L <sub>O</sub> /L <sub>w</sub> )	310.59	0.0	0.2379		310.61	0.0	0.2349		310.64	0.0	0.2326		310.66	0.0	0.2318		310.62	0.1007	0.216		310.63	0.1007	0.217	0.34 ± 0.09	310.63	0.2025	0.203		310.64	0.2025	0.206	0.29 ± 0.05	310.59	0.2993	0.193		310.61	0.2993	0.192	0.28 ± 0.03	310.59	0.3986	0.178		310.60	0.3986	0.178	0.30 ± 0.02	310.65	1.0	0.117*	
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2] (3) Cholest-5-en-3β-ol or Cholesterol; C <sub>27</sub> H <sub>46</sub> O; [57-88-5]	<b>ORIGINAL MEASUREMENTS:</b> Byrne, J. E.; Battino, R.; Danforth, W. F. <i>J. Chem. Thermodyn.</i> <u>1974</u> , <i>6</i> , 245-50.																																																
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T/K	Mass Fraction Cholesterol W <sub>3</sub>	Ostwald Coefficient L	"Salting Out" Parameter k = (1/W <sub>3</sub> ) log (L <sub>O</sub> /L <sub>W</sub> )																																														
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The solubility of oxygen at 310.15 K (37 °C) in some complex aqueous mixtures.											EXPERIMENTAL VALUES:	COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Various substances given in table below (3) Water; H <sub>2</sub> O; [7732-18-5]	ORIGINAL MEASUREMENTS: Zander, R. Z. Naturforsch., C: Biosci. 1976, 31C, 339-52.
Solute, g per 100 cm <sup>3</sup>	1.	2.	3.	4.	5.	6.	7.	8.	9.	10.			
Component D-Glucose; C <sub>6</sub> H <sub>12</sub> O <sub>6</sub> ; [50-99-7]	10	10	-	-	10	7.5	-	5	10	10			
Sodium chloride; NaCl; [7647-14-5]	2.9	2.9	1.34	2.5	0.18	2.41	-	1.16	5	7.5			
Ovalbumin	10	-	-	-	-	-	10	4	-	-			
4-Hydroxyproline; C <sub>5</sub> H <sub>9</sub> NO <sub>3</sub> ; [6912-67-0]	-	10	-	-	-	-	-	4	-	-			
Albumin, bovine	-	-	2	-	-	-	-	-	-	-			
Choline chloride; C <sub>6</sub> H <sub>15</sub> N <sub>2</sub> O <sub>2</sub> .Cl [51-83-2]	-	-	8	4	-	-	-	-	15	15			
Lysine; C <sub>6</sub> H <sub>9</sub> N <sub>2</sub> O <sub>2</sub> ; [6899-06-5] <sup>14 2 2</sup>	-	-	10	-	-	-	-	-	10	10			
α-Globin, bovine	-	-	-	1	2	1	-	-	-	-			
γ-Globin, bovine	-	-	-	-	-	2	-	-	-	-			
Chondroitinsulfuric acid	-	-	-	4	4	-	-	-	-	-			
Urea; CH <sub>2</sub> N <sub>2</sub> O; [57-13-6] <sup>2</sup>	-	-	-	-	-	-	15	6	20	20			
Bunsen coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	174±3	138±4	143±4	182±3	188±3	188±3	195±10	180±3	37±6	9±4			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Urea; CH <sub>4</sub> N <sub>2</sub> O; [57-13-6] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R.  <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.																														
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T/K	Urea g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )																												
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<b>AUXILIARY INFORMATION</b>																															
<b>METHOD/APPARATUS/PROCEDURE:</b> Classical Van Slyke method (1).  The apparatus sample volume and constant gas volume are carefully calibrated. The correction for unextracted gas is made, but the reabsorption correction is not necessary for oxygen.  Equilibration is undertaken in a thermostated tonometer. A 2 cm <sup>3</sup> sample is directly transferred to the Van Slyke apparatus for analysis.  The solubility of oxygen in water value is from the authors analysis of ten literature values (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Linde Co. Purity 99.9 per cent by volume. (2) Urea. No information. (3) Water. Distilled.  <b>ESTIMATED ERROR:</b> δT/K = 0.1 δα/α = 0.01  <b>REFERENCES:</b> 1. Van Slyke, D. D.; Neill, J. M. <i>J. Biol. Chem.</i> <u>1924</u> , <i>61</i> , 523. 2. Zander, R.; Euler, R. <i>Measurement of Oxygen</i> , Edited by Degn, H.; Balslev, I.; Brook, R. Elsevier, Amsterdam, 1976, p.271.																														

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]  (2) Urea; CH<sub>4</sub>N<sub>2</sub>O; [57-13-6]  (3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Popovic, M.; Niebelschutz, H.;  Reuss, M.</p> <p><i>European. J. Appl. Microbiol. Biotechnol.</i> <u>1979</u>, <i>8</i>, 1-15.</p>	
<p>VARIABLES:</p> <p>Concentration  T/K = 298</p>	<p>PREPARED BY:</p> <p>C.L. Young</p>	
<p>EXPERIMENTAL VALUES:</p>		
<p>T/K</p>	<p>Concentration  /g dm<sup>-3</sup></p>	<p>Oxygen solubility  S x 10<sup>3</sup>/mol dm<sup>-3</sup></p>
<p>298.15</p>	<p>6.75  13.50</p>	<p>1.239  1.217</p>
<p>AUXILIARY INFORMATION</p>		
<p>METHOD APPARATUS/PROCEDURE:</p> <p>Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = \pm 0.1</math>; <math>\delta S = \pm 2\%</math>  (estimated by compiler).</p> <p>REFERENCES:</p> <p>1. Krauss, W.; Gestrich, W.  <i>Chem. Ing. Techn.</i> <u>1977</u>, <i>6</i>, 35.</p>	

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Zander, R.	
(2) Amino acids		<i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES:		PREPARED BY:	
T/K = 310.15 P/kPa = 101.325		H. L. Clever	
EXPERIMENTAL VALUES:			
T/K	Amino acids g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup> atm <sup>-1</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )
Glycine; C <sub>2</sub> H <sub>5</sub> NO <sub>2</sub> ; [56-40-6]			
310.15	0	241	
	10	177 ± 2	
	20	139 ± 1	-0.02868
4-Hydroxyproline; C <sub>5</sub> H <sub>9</sub> NO <sub>3</sub> ; [6912-67-0]			
310.15	0	241	
	10	202 ± 1	
	20	168 ± 1	-0.01799
L-Alanine; C <sub>3</sub> H <sub>7</sub> NO <sub>2</sub> ; [56-41-7]			
310.15	0	241	
	10	190 ± 2	
	20	149 ± 4	
	30	117 ± 1	-0.02390
Cysteine; C <sub>3</sub> H <sub>7</sub> NO <sub>2</sub> S; [4371-52-2], see [52-90-4]			
310.15	0	241	
	10	128 ± 3	
	20	97 ± 4	-0.05255
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Classical Van Slyke method (1).		(1) Oxygen. Linde Co. Purity 99.9 per cent by volume.	
The apparatus sample volume and constant gas volume are carefully calibrated. The correction for unextracted gas is made, but the reabsorption correction is not necessary for oxygen.		(2) Amino acids. No information.	
Equilibration is undertaken in a thermostated tonometer. A 2 cm <sup>3</sup> sample is directly transferred to the Van Slyke apparatus for analysis.		(3) Water. Distilled.	
The solubility of oxygen in water value is from the authors analysis of ten literature values (2).		ESTIMATED ERROR:	
		δT/K = 0.1 δα/α = 0.01	
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<sup>1</sup> k/g <sup>-1</sup> 100 cm <sup>3</sup>			

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Lysine; C <sub>6</sub> H <sub>14</sub> N <sub>2</sub> O <sub>2</sub> ; [6899-06-5] see also [56-87-1] and [70-54-2] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R. <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.																																
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) 1,2,3-Propanetriol or glycerine; C <sub>3</sub> H <sub>8</sub> O <sub>3</sub> ; [56-81-5] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R. <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.																												
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]  (2) 1,2,3-Propanetricarboxylic acid,  2-hydroxy-, (Citric acid);  C<sub>6</sub>H<sub>8</sub>O<sub>7</sub>; [77-92-9]  (3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Popovic, M.; Niebelschutz, H.;  Reuss, M.   <i>European. J. Appl. Microbiol.</i>  <i>Biotechnol.</i> <u>1979</u>, <i>8</i>, 1-15.</p>																		
<p>VARIABLES:</p> <p>Concentration  T/K = 298</p>	<p>PREPARED BY:</p> <p>C.L. Young</p>																		
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="89 497 1210 815"> <thead> <tr> <th>T/K</th> <th>Concentration /g dm<sup>-3</sup></th> <th>Oxygen solubility, S x 10<sup>3</sup> /mol dm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="7">298.15</td> <td>25</td> <td>1.242</td> </tr> <tr> <td>40</td> <td>1.196</td> </tr> <tr> <td>50</td> <td>1.183</td> </tr> <tr> <td>75.6</td> <td>1.148</td> </tr> <tr> <td>100</td> <td>1.137</td> </tr> <tr> <td>150</td> <td>1.083</td> </tr> <tr> <td>200</td> <td>0.983</td> </tr> </tbody> </table>		T/K	Concentration /g dm <sup>-3</sup>	Oxygen solubility, S x 10 <sup>3</sup> /mol dm <sup>-3</sup>	298.15	25	1.242	40	1.196	50	1.183	75.6	1.148	100	1.137	150	1.083	200	0.983
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<p>METHOD APPARATUS/PROCEDURE:</p> <p>Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = \pm 0.1</math>; <math>\delta S = \pm 2\%</math>  (estimated by compiler).</p> <p>REFERENCES:</p> <p>1. Krauss, W.; Gestrich, W.  <i>Chem. Ing. Techn.</i> <u>1977</u>, <i>6</i>, 35.</p>																		

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]  (2) Gluconic acid; C<sub>6</sub>H<sub>12</sub>O<sub>7</sub>; [133-42-6]  (3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Popovic, M.; Niebelschutz, H.; Reuss, M.</p> <p><i>European. J. Appl. Microbiol. Biotechnol.</i> <u>1979</u>, 8, 1-15.</p>																																							
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COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7732-44-7]		Müller, C.	
(2) d-Glucose; C <sub>6</sub> H <sub>12</sub> O <sub>6</sub> ; [50-99-7]		Z. Physik. Chem. <u>1912</u> , 81, 483-503.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES:		PREPARED BY:	
T/K = 293 - 295		R. Battino	
P/kPa = 101.325			
EXPERIMENTAL VALUES:			
T/K <sup>a</sup>	Weight Percentage d-Glucose	Ostwald Coeff. <sup>b</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>c</sup> 10 <sup>2</sup> <sub>a</sub>
294.35	10.84	2.856	2.650
294.65	20.7	2.375	2.202
293.05	33.8	1.946	1.814
293.65	51.9	1.491	1.378
294.85	58.84	1.318	1.221
<p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>c</sup> Bunsen coefficient.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Water is degassed by pumping under vacuum. The absorption vessel is about 600 cm <sup>3</sup> and is separately thermostatted from the buret gas measuring system. Both are connected by a copper capillary tube. Gas uptake is measured on gas burets. The absorption flask volume and all liquid volumes were calibrated with mercury. The original paper contains details and a drawing of the apparatus. Solubilities were also reported in aqueous solutions of sucrose, glycerol, and chloral hydrate.		<p>(1) From the heating of KMnO<sub>4</sub> and washed in concentrated KOH solution.</p> <p>(2) d-Glucose - from Merck.</p> <p>(3) No comment by author.</p>	
		ESTIMATED ERROR:	
		δ <sub>a</sub> /α = ±0.01, estimated by compiler.	
		REFERENCES:	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) D-Glucose, C <sub>6</sub> H <sub>12</sub> O <sub>6</sub> ; [50-99-7] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R.  <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 31C, 339-52.																								
<b>VARIABLES:</b> T/K = 310.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever																								
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COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [57-50-1] (3) Water; H <sub>2</sub> O; [7732-18-5]		Müller, C. <i>Z. Physik. Chem.</i> <u>1912</u> , <i>81</i> , 493-503.	
VARIABLES:		PREPARED BY:	
T/K = 289-290 P/kPa = 101.325		R. Battino	
EXPERIMENTAL VALUES:			
T/K <sup>a</sup>	Weight Percentage Sucrose	Ostwald Coeff. <sup>b</sup> 10 <sup>2</sup> L	Bunsen Coeff. <sup>c</sup> 10 <sup>2</sup> α
289.15	12.1	3.082	2.911
288.75	24.38	2.502	2.367
289.75	28.44	2.241	2.113
288.75	42.96	1.672	1.582
289.35	49.25	1.428	1.348
290.35	50.	1.384	1.302
<p><sup>a</sup> Temperature reported to 0.1°C.</p> <p><sup>b</sup> Ostwald coefficient calculated by compiler.</p> <p><sup>c</sup> Bunsen coefficient.</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Water is degassed by pumping under vacuum. The absorption vessel is about 600 cm <sup>3</sup> and is separately thermostatted from the buret gas measuring system. Both are connected by a copper capillary tube. Gas uptake is measured on the gas burets. The absorption flask volume and all liquid volumes were calibrated with mercury. The original paper contains details and a drawing of the apparatus. Solubilities were also reported in aqueous solutions of d-glucose, glycerol, and chloral hydrate.		(1) From the heating of KMnO <sub>4</sub> and washed in concentrated KOH solution.	
		(2) Chemically pure from Merck in Darmstadt.	
		(3) No comment by author	
		ESTIMATED ERROR:	
		δ $\alpha$ /α = ± 0.01, estimated by compiler.	
		REFERENCES:	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [57-50-1] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> MacArthur, C. G.  <i>J. Phys. Chem.</i> <u>1916</u> , 20, 495-502.																							
<b>VARIABLES:</b> T/K = 298.15 O <sub>2</sub> P/kPa = ~ 21.2 (O <sub>2</sub> in air at one atm) c <sub>3</sub> /mol dm <sup>-3</sup> = 0 - 2	<b>PREPARED BY:</b> H. L. Clever																							
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="339 466 1023 746"> <thead> <tr> <th>T/K</th> <th>Sucrose c<sub>3</sub>/mol dm<sup>-3</sup></th> <th>Solution density<sup>1</sup> ρ/g cm<sup>-3</sup></th> <th>Solubility<sup>2</sup> cm<sup>3</sup> (STP) O<sub>2</sub> per dm<sup>3</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="7">298.15</td> <td>0.0</td> <td>1.000</td> <td>5.78</td> </tr> <tr> <td>0.125</td> <td>1.015</td> <td>5.40</td> </tr> <tr> <td>0.25</td> <td>1.033</td> <td>4.82</td> </tr> <tr> <td>0.5</td> <td>1.068</td> <td>4.39</td> </tr> <tr> <td>1</td> <td>1.147</td> <td>3.20</td> </tr> <tr> <td>2</td> <td>1.336</td> <td>1.84</td> </tr> </tbody> </table> <p data-bbox="119 770 1126 844"><sup>1</sup> The author calculated the densities from data in the <i>International Critical Tables</i>. Use the density values with caution, some of them appear to be in error.</p> <p data-bbox="119 864 1172 913"><sup>2</sup> The solubility in water is about 3 per cent smaller than the presently accepted value.</p>		T/K	Sucrose c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>	298.15	0.0	1.000	5.78	0.125	1.015	5.40	0.25	1.033	4.82	0.5	1.068	4.39	1	1.147	3.20	2	1.336	1.84
T/K	Sucrose c <sub>3</sub> /mol dm <sup>-3</sup>	Solution density <sup>1</sup> ρ/g cm <sup>-3</sup>	Solubility <sup>2</sup> cm <sup>3</sup> (STP) O <sub>2</sub> per dm <sup>3</sup>																					
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solutions were thermostated in tall cylinder open to the air. They were shaken by hand several times a day for a period of four days.  A sample of 250 cm <sup>3</sup> was analyzed for oxygen by a modified Winkler method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Air at one atm. (2) Sucrose. No information. (3) Water. No information.  <b>ESTIMATED ERROR:</b> The solubility values may be in 5 to 10 per cent error. The salt concentrations above one mol dm <sup>-3</sup> may be in error by 10 per cent.  <b>REFERENCES:</b>																							

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; (3) Water; H <sub>2</sub> O; [7732-18-5]		Hikita, H.; Asai, S.; Azuma, Y. <i>Can. J. Chem. Eng.</i> <u>1978</u> , <i>56</i> , 371-4.			
VARIABLES:		PREPARED BY:			
T/K = 288-318 Concentration		R. Battino			
EXPERIMENTAL VALUES:					
t/°C	T <sup>a</sup> /K	Sucrose Conc.		P/kg m <sup>-3</sup>	10 <sup>3</sup> C <sup>*</sup> /kmol m <sup>-3</sup>
		wt %	kmol m <sup>-3</sup>		
25	298	0	0	997	1.26 <sup>b</sup>
25	298	12.0	0.367	1047	1.06
25	298	23.5	0.754	1097	0.883
25	298	33.5	1.12	1144	0.738
25	298	43.0	1.49	1188	0.626
25	298	54.0	1.97	1248	0.480
15	288	54.0	1.98	1253	0.563
35	308	54.0	1.95	1237	0.425
45	318	54.0	1.95	1232	0.381
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> For pure water. Corresponds to a mole fraction solubility at 101.325 kPa partial pressure of gas of 2.28 x 10<sup>-5</sup>.</p>					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Used the method of Markham and Kobe (1). A known volume of gas is brought into contact with a known quantity of gas-free solution, the latter attained by boiling under vacuum for about ten hours. Equilibrium is established by agitation and the volume of remaining gas measured.			No details given.		
			ESTIMATED ERROR:		
			δC <sup>*</sup> /C <sup>*</sup> = ±0.01, compiler's estimate		
			REFERENCES:		
			1. Markham, A. E.; Kobe, K. A. <i>J. Am. Chem. Soc.</i> <u>1941</u> , <i>63</i> , 449.		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Disaccharides; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zander, R. <i>Z. Naturforsch., C: Biosci.</i> <u>1976</u> , 339-52.																																											
<b>VARIABLES:</b> T/K = 310.15 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever																																											
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Disaccharide g 100 cm<sup>-3</sup></th> <th style="text-align: center;">Bunsen Coefficient 10<sup>4</sup>α/cm<sup>3</sup>cm<sup>-3</sup></th> <th style="text-align: center;">Constant<sup>1</sup> k=(1/c) ln (α/α<sub>0</sub>)</th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">β-D-fructofuranosyl-α-D-glucopyranoside or sucrose; C<sub>12</sub>H<sub>22</sub>O<sub>11</sub>; [57-50-1]</td> </tr> <tr> <td rowspan="4" style="vertical-align: top;">310.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">241</td> <td></td> </tr> <tr> <td style="text-align: center;">2</td> <td style="text-align: center;">234 ± 1</td> <td></td> </tr> <tr> <td style="text-align: center;">10</td> <td style="text-align: center;">215 ± 3</td> <td></td> </tr> <tr> <td style="text-align: center;">20</td> <td style="text-align: center;">189 ± 4</td> <td style="text-align: center;">-0.01195</td> </tr> <tr> <td colspan="4" style="text-align: center;">4-O-α-D-glucopyranosyl-D-glucose or maltose; C<sub>12</sub>H<sub>22</sub>O<sub>11</sub>; [69-79-4]</td> </tr> <tr> <td rowspan="2" style="vertical-align: top;">310.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">241</td> <td></td> </tr> <tr> <td style="text-align: center;">20</td> <td style="text-align: center;">190 ± 1</td> <td></td> </tr> <tr> <td colspan="4" style="text-align: center;">4-O-β-D-galactopyranosyl-D-glucose or lactose; C<sub>12</sub>H<sub>22</sub>O<sub>11</sub>; [63-42-3].</td> </tr> <tr> <td rowspan="2" style="vertical-align: top;">310.15</td> <td style="text-align: center;">0</td> <td style="text-align: center;">241</td> <td></td> </tr> <tr> <td style="text-align: center;">20</td> <td style="text-align: center;">187 ± 3</td> <td></td> </tr> </tbody> </table> <p><sup>1</sup> k/g<sup>-1</sup>100 cm<sup>3</sup></p>		T/K	Disaccharide g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )	β-D-fructofuranosyl-α-D-glucopyranoside or sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [57-50-1]				310.15	0	241		2	234 ± 1		10	215 ± 3		20	189 ± 4	-0.01195	4-O-α-D-glucopyranosyl-D-glucose or maltose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [69-79-4]				310.15	0	241		20	190 ± 1		4-O-β-D-galactopyranosyl-D-glucose or lactose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [63-42-3].				310.15	0	241		20	187 ± 3	
T/K	Disaccharide g 100 cm <sup>-3</sup>	Bunsen Coefficient 10 <sup>4</sup> α/cm <sup>3</sup> cm <sup>-3</sup>	Constant <sup>1</sup> k=(1/c) ln (α/α <sub>0</sub> )																																									
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<b>METHOD/APPARATUS/PROCEDURE:</b> Classical Van Slyke method (1). The apparatus sample volume and constant gas volume are carefully calibrated. The correction for unextracted gas is made, but the reabsorption correction is not necessary for oxygen. Equilibration is undertaken in a thermostated tonometer. A 2 cm <sup>3</sup> sample is directly transferred to the Van Slyke apparatus for analysis. The solubility of oxygen in water value is from the authors analysis of ten literature values (2).	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Linde Co. Purity 99.9 per cent by volume. (2) Disaccharides. No information. (3) Water. Distilled. <b>ESTIMATED ERROR:</b> δT/K = 0.1 δα/α = 0.01 <b>REFERENCES:</b> 1. Van Slyke, D. D.; Neill, J. M. <i>J. Biol. Chem.</i> <u>1924</u> , <i>61</i> , 523. 2. Zander, R.; Euler, R. <i>Measurement of Oxygen</i> , Edited by Degn, H.; Balslev, I.; Brook, R. Elsevier, Amsterdam, 1976, p. 271.																																											

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> : [7782-44-7] (2) Fermentation medium	<b>ORIGINAL MEASUREMENTS:</b> Liu, M.S.; Branion, R.M.R.; Duncan, D.W.  <i>Biotechnol. Bioeng.</i> <u>1973</u> , <i>15</i> , 213-6.										
<b>VARIABLES:</b> T/K = 308 Concentration	<b>PREPARED BY:</b> P. Battino										
<b>EXPERIMENTAL VALUES:</b> <span style="float: right;">35°C; 308 K</span> <table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center; width: 50%;">Concentration</th> <th style="text-align: center; width: 50%;">Solubility<sub>1</sub> /mg liter<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">4.5 K<sup>a</sup></td> <td style="text-align: center;">6.92</td> </tr> <tr> <td style="text-align: center;">9 K</td> <td style="text-align: center;">6.68</td> </tr> <tr> <td style="text-align: center;">13.5 K</td> <td style="text-align: center;">6.66</td> </tr> <tr> <td style="text-align: center;">18 K</td> <td style="text-align: center;">7.06</td> </tr> </tbody> </table>		Concentration	Solubility <sub>1</sub> /mg liter <sup>-1</sup>	4.5 K <sup>a</sup>	6.92	9 K	6.68	13.5 K	6.66	18 K	7.06
Concentration	Solubility <sub>1</sub> /mg liter <sup>-1</sup>										
4.5 K <sup>a</sup>	6.92										
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18 K	7.06										
<sup>a</sup> Fermentation medium of Silverman and Lundgren (1) with 4.5 g liter <sup>-1</sup> ferrous ion.											
<b>AUXILIARY INFORMATION</b>											
<b>METHOD/APPARATUS/PROCEDURE:</b> Saturation solubilities were derived from determining oxygen partial pressures with a polarographic oxygen electrode as a function of time with the electrode being in the stirred medium.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.										
	<b>ESTIMATED ERROR:</b> ±3% in solubility (estimated by compiler).										
	<b>REFERENCES:</b> 1. Silverman, M.P.; Lundgren, D.G. <i>J. Bacteriol.</i> <u>1959</u> , <i>78</i> , 326.										

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]  (2) Fermentation medium.  (3) Methanol; CH<sub>4</sub>O; [67-56-1]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Popovic, M.; Niebelschutz, H.;  Reuss, M.</p> <p><i>European J. Appl. Microbiol. Biotechnol.</i> <u>1979</u>, 8, 1-15.</p>	
<p>VARIABLES:</p> <p>T/K = 298  Concentration</p>	<p>PREPARED BY:</p> <p>C.L. Young</p>	
<p>EXPERIMENTAL VALUES:</p>		
<p>T/K</p>	<p>Concentration of  methanol (volume%)</p>	<p>Oxygen solubility,  x 10<sup>3</sup> /mol dm<sup>-3</sup></p>
<p>298.15</p>	<p>1  2  3</p>	<p>1.200  1.175  1.150</p>
<p>AUXILIARY INFORMATION</p>		
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(2)Medium contained 6.0 g dm<sup>-3</sup> (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>; 0.94 g dm<sup>-3</sup> K<sub>2</sub>HPO<sub>4</sub>; 0.71 g dm<sup>-3</sup> KH<sub>2</sub>PO<sub>4</sub>; 0.82 g dm<sup>-3</sup> MgSO<sub>4</sub>.7H<sub>2</sub>O; 0.08 g dm<sup>-3</sup> NaCl; 0.06 g dm<sup>-3</sup> CaCl<sub>2</sub>. 2H<sub>2</sub>O: Remainder H<sub>2</sub>O.</p> <p>ESTIMATED ERROR:</p> <p>δT/K = ±0.1; δS = ±2%  (estimated by compiler)</p> <p>REFERENCES:</p> <p>1. Krauss, W.; Gestrich, W.  <i>Chem. Ing. Techn.</i> <u>1977</u>, 6, 35.</p>	



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Corn steep liquor. (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b>  Popovic, M.; Niebelschutz, H.; Reuss, M.  <i>European. J. Appl. Microbiol.</i> <i>Biotechnol.</i> <u>1979</u> , <i>8</i> , 1-15.	
<b>VARIABLES:</b>  Concentration T/K = 298	<b>PREPARED BY:</b>  C.L. Young	
<b>EXPERIMENTAL VALUES:</b>		
T/K	Concentration /g dm <sup>-3</sup>	Oxygen solubility, <i>S</i> x 10 <sup>3</sup> /mol dm <sup>-3</sup>
298.15	10 50 100	1.205 1.189 1.154
<b>AUXILIARY INFORMATION</b>		
<b>METHOD / APPARATUS / PROCEDURE:</b>  Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details given.	
	<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1$ ; $\delta S = \pm 2\%$ (estimated by compiler)	
	<b>REFERENCES:</b> 1. Krauss, W.; Gestrich, W. <i>Chem. Ing. Techn.</i> <u>1977</u> , <i>6</i> , 35.	

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]  (2) Yeast extract.  (3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Popovic, M.; Niebelschutz, H.;  Reuss, M.</p> <p><i>European. J. Appl. Microbiol. Biotechnol.</i> <u>1979</u>, <i>8</i>, 1-15.</p>									
<p>VARIABLES:</p> <p>T/K = 298  Concentration</p>	<p>PREPARED BY:</p> <p>C.L. Young</p>									
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="93 486 1221 676"> <thead> <tr> <th>T/K</th> <th>Concentration /g dm<sup>-3</sup></th> <th>Oxygen solubility, S x 10<sup>3</sup> /mol dm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td>298.15</td> <td>5</td> <td>1.255</td> </tr> <tr> <td></td> <td>10</td> <td>1.228</td> </tr> </tbody> </table>		T/K	Concentration /g dm <sup>-3</sup>	Oxygen solubility, S x 10 <sup>3</sup> /mol dm <sup>-3</sup>	298.15	5	1.255		10	1.228
T/K	Concentration /g dm <sup>-3</sup>	Oxygen solubility, S x 10 <sup>3</sup> /mol dm <sup>-3</sup>								
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	10	1.228								
<p>AUXILIARY INFORMATION</p>										
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:  <math>\delta T/K = \pm 0.1</math>; <math>\delta S = \pm 2\%</math>  (estimated by compiler)</p> <p>REFERENCES:  1. Krauss, W.; Gestrich, W.  <i>Chem. Ing. Techn.</i> <u>1977</u>, <i>6</i>, 35.</p>									

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]  (2) Molasses  (3) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Popovic, M.; Niebelschutz, H.;  Reuss, M.</p> <p><i>European. J. Appl. Microbiol.,  Biotechnol. 1979, 8, 1-15.</i></p>	
<p>VARIABLES:</p> <p>Concentration  T/K = 298</p>	<p>PREPARED BY: C.L. Young</p>	
<p>EXPERIMENTAL VALUES:</p>		
<p>T/K</p> <p>298.15</p>	<p>Concentration  /g dm<sup>-3</sup></p> <p>5  66  80  106  150  238  278</p>	<p>Oxygen solubility,  S x 10<sup>3</sup> /mol dm<sup>-3</sup></p> <p>1.243  1.192  1.752  1.128  1.112  1.019  0.840</p>
<p>AUXILIARY INFORMATION</p>		
<p>METHOD APPARATUS/PROCEDURE:</p> <p>Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta T/K = \pm 0.1</math>; <math>\delta S = \pm 2\%</math>  (estimated by compiler)</p> <p>REFERENCES:</p> <p>1. Krauss, W.; Gestrich, W.  <i>Chem. Ing. Techn. 1977, 6, 35</i></p>	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Antifoam. (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Popovic, M.; Niebelschutz, H.; Reuss, M. <i>European, J. Appl. Microbiol. Biotechnol.</i> <u>1979</u> , 8, 1-15.	
<b>VARIABLES:</b> Concentration T/K = 296	<b>PREPARED BY:</b> C.L. young	
<b>EXPERIMENTAL VALUES:</b>		
T/K 295.75	Concentration x 10 <sup>3</sup> vol/vol 0.01 0.02 0.05 0.07 0.10 0.15 0.20 0.50 0.80 1.20 1.50	Oxygen solubility, S x 10 <sup>3</sup> /mol dm <sup>-3</sup> 1.320 1.328 1.329 1.336 1.344 1.327 1.300 1.290 1.286 1.271 1.240
AUXILIARY INFORMATION		
<b>METHOD APPARATUS/PROCEDURE:</b> Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).	<b>SOURCE AND PURITY OF MATERIALS:</b> (2) Antifoam was Contraspum 210 supplied by Zoehiemmer and Schwarz, Lahnstein Rhein. <b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.1$ ; $\delta S = \pm 2\%$ (estimated by compiler) <b>REFERENCES:</b> 1. Krauss, W.; Gestrich, W. <i>Chem. Ing. Techn.</i> <u>1977</u> , 6, 35	

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Popovic, M.; Niebelschutz, H.; Reuss, M.	
(2) Xanthan		<i>European J. Appl. Microbiol.</i> <i>Biotechnol.</i> <u>1979</u> , 8, 1-15.	
(3) Water; H <sub>2</sub> O; [7732-18-5]			
VARIABLES:		PREPARED BY:	
T/K = 298 Concentration		C.L. Young	
EXPERIMENTAL VALUES:			
T/K	Concentration /g dm <sup>-3</sup>	Oxygen solubility, S x 10 <sup>3</sup> /mol dm <sup>-3</sup>	
298.15	1 5	1.250 1.251	
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).		No details given.	
		ESTIMATED ERROR:	
		$\delta T/K = \pm 0.1$ ; $\delta S = \pm 2\%$ (estimated by compiler)	
		REFERENCES:	
		1. Krauss, W.; Gestrinch, W. <i>Chem. Ing. Techn.</i> <u>1977</u> , 6, 35	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Pullulan (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Popovic, M.; Niebelschutz, H.; Reuss, M.  <i>European. J. Appl. Microbiol. Biotechnol.</i> <u>1979</u> , 8, 1-15.	
<b>VARIABLES:</b> Concentration T/K = 298	<b>PREPARED BY:</b> C.L. Young	
<b>EXPERIMENTAL VALUES:</b>		
T/K	Concentration /g dm <sup>-3</sup>	Oxygen solubility, S x 10 <sup>3</sup> /mol dm <sup>-3</sup>
298.15	1 10 20	1.266 1.241 1.240
<b>AUXILIARY INFORMATION</b>		
<b>METHOD/APPARATUS/PROCEDURE:</b>  Stirred equilibrium cell. Volumetric apparatus in which known volume of gas was added to a known volume of liquid and the equilibrium pressure measured. Details in source and ref. (1).	<b>SOURCE AND PURITY OF MATERIALS:</b>  No details given.	
	<b>ESTIMATED ERROR:</b>  $\delta T/K = \pm 0.1$ ; $\delta S = \pm 2\%$ (estimated by compiler)	
	<b>REFERENCES:</b> 1. Krauss, W.; Gestrich, W. <i>Chem. Ing. Techn.</i> <u>1977</u> , 6, 35.	

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [57-50-1] (3) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (4) Water; H <sub>2</sub> O; [7732-18-5] (5) Various wines		Moditis, I.Z.  Izv. Vyssh. Uchebn. Zaved. Pisch. Tehnolog, 1976, (3), 193-41.  Chem. Abstr. 85; 175431g.	
VARIABLES:		PREPARED BY:	
T/K = 298		V. Katovic	
EXPERIMENTAL VALUES:			
	Alcohol %	Sucrose %	Solubility of oxygen <sup>a</sup> Obtained
Water	-	-	8.4
Alcohol solution	10	-	9.0
Alcohol solution	20	-	9.0
Sugar solution	-	5	7.9
	-	10	7.8
<u>Wines</u>			
Port wine	18	10	7.9
Muscatel	16	16	7.1
Madeira	19	4	8.4
"Heres"	20	3	8.3
<sup>a</sup> Solubility of oxygen at 25°C (298 K) in mgO <sub>2</sub> per liter of solution.			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
The amount of oxygen was determined using a gas chromatograph. Columns packed with silica gel and molecular sieves 13X were used.		No details given.	
		ESTIMATED ERROR:	
		Error in solubility ca. ±2% (compiler's estimate).	
		REFERENCES:	

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [57-50-1] (3) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5] (4) Water; H <sub>2</sub> O; [7732-18-5] (5) Various wines	<b>ORIGINAL MEASUREMENTS:</b> Fal'kovich, Yu.E.; Dimenov. A.T.; Moditis, I.Z.; Strukova, V.E. Izv. Vyssh. Uchebn. Zaved. Pisch. Tekhnolog., <u>1977</u> , (7), 56-9. Chem. Abstr. , 87, 66545j.																																																																								
<b>VARIABLES:</b> T/K = 288-308 Concentration	<b>PREPARED BY:</b> R. Battino																																																																								
<b>EXPERIMENTAL VALUES:</b> <table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">Water solution C<sub>O</sub><sup>a</sup></th> <th style="text-align: center;">15°C</th> <th style="text-align: center;">25°C</th> <th style="text-align: center;">35°C</th> </tr> </thead> <tbody> <tr> <td colspan="4"><hr/></td> </tr> <tr> <td>Ethanol/(%)</td> <td></td> <td></td> <td></td> </tr> <tr> <td>0</td> <td style="text-align: center;">10.2</td> <td style="text-align: center;">8.4</td> <td style="text-align: center;">7.2</td> </tr> <tr> <td>10</td> <td style="text-align: center;">11.6</td> <td style="text-align: center;">9.0</td> <td style="text-align: center;">7.8</td> </tr> <tr> <td>15</td> <td style="text-align: center;">11.4</td> <td style="text-align: center;">8.9</td> <td style="text-align: center;">7.5</td> </tr> <tr> <td>20</td> <td style="text-align: center;">11.6</td> <td style="text-align: center;">9.0</td> <td style="text-align: center;">8.0</td> </tr> <tr> <td>40</td> <td style="text-align: center;">10.4</td> <td style="text-align: center;">10.4</td> <td style="text-align: center;">10.0</td> </tr> <tr> <td>70</td> <td style="text-align: center;">21.0</td> <td style="text-align: center;">21.2</td> <td style="text-align: center;">21.2</td> </tr> <tr> <td colspan="4"><hr/></td> </tr> <tr> <td>Sucrose g/100 ml</td> <td></td> <td></td> <td></td> </tr> <tr> <td>5</td> <td style="text-align: center;">9.7</td> <td style="text-align: center;">7.9</td> <td style="text-align: center;">7.0</td> </tr> <tr> <td>10</td> <td style="text-align: center;">9.1</td> <td style="text-align: center;">7.8</td> <td style="text-align: center;">6.5</td> </tr> <tr> <td>15</td> <td style="text-align: center;">8.3</td> <td style="text-align: center;">7.4</td> <td style="text-align: center;">6.2</td> </tr> <tr> <td>20</td> <td style="text-align: center;">7.3</td> <td style="text-align: center;">6.6</td> <td style="text-align: center;">5.9</td> </tr> <tr> <td>25</td> <td style="text-align: center;">6.4</td> <td style="text-align: center;">6.0</td> <td style="text-align: center;">5.7</td> </tr> <tr> <td>30</td> <td style="text-align: center;">5.6</td> <td style="text-align: center;">5.2</td> <td style="text-align: center;">4.9</td> </tr> <tr> <td>60</td> <td style="text-align: center;">2.2</td> <td style="text-align: center;">2.1</td> <td style="text-align: center;">2.0</td> </tr> </tbody> </table> <p><sup>a</sup> Solubility of oxygen in mgO<sub>2</sub> per 1 liter of solution.</p> <p style="text-align: right;">continued on following page</p>		Water solution C <sub>O</sub> <sup>a</sup>	15°C	25°C	35°C	<hr/>				Ethanol/(%)				0	10.2	8.4	7.2	10	11.6	9.0	7.8	15	11.4	8.9	7.5	20	11.6	9.0	8.0	40	10.4	10.4	10.0	70	21.0	21.2	21.2	<hr/>				Sucrose g/100 ml				5	9.7	7.9	7.0	10	9.1	7.8	6.5	15	8.3	7.4	6.2	20	7.3	6.6	5.9	25	6.4	6.0	5.7	30	5.6	5.2	4.9	60	2.2	2.1	2.0
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<b>METHOD/APPARATUS/PROCEDURE:</b> The solutions were saturated with air for 30 minutes at constant temperature. The dissolved oxygen was determined by gas chromatography.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From air. (2,3,4) No details given. <hr/> <b>ESTIMATED ERROR:</b> <hr/> <b>REFERENCES:</b>																																																																								



COMPONENTS:	EVALUATOR:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]	Fal'kovich, Yu.E.; Pinenov, A.T.; Moditis, I.Z., Strukova, V.E.  Izv. Vyssh. Uchebn. Zaved. Pisch. Tekhnolog. 1977, (7), 56-9.  Chem. Abstr. , 87, 66545j.
(2) Sucrose; C <sub>12</sub> H <sub>22</sub> O <sub>11</sub> ; [57-50-1]	
(3) Ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	
(4) Water; H <sub>2</sub> O; [7732-18-5]	
(5) Various wines	

## EXPERIMENTAL VALUES:

continued

Sucrose g/100 ml	C <sub>O</sub> <sup>a</sup> at different % of alcohol					
	0	10	15	20	40	70
0	8.4	9.0	8.9	9.0	10.4	21.2
1	-	9.0	8.9	9.0	10.4	21.2
2	-	8.9	-	8.9	10.2	21.0
3	-	8.7	8.9	8.8	-	-
4	-	8.6	-	8.7	10.0	20.2
5	8.0	-	8.6	8.6	-	-
8	-	8.4	-	8.4	-	-
10	7.8	-	-	8.0	-	-
12	-	8.0	-	7.8	-	-
15	7.4	-	-	-	-	-
16	-	7.6	-	7.1	-	-
18	-	-	6.9	6.9	-	-
20	6.6	6.8	-	-	-	-

<sup>a</sup> Solubility of oxygen in mgO<sub>2</sub> per liter of solution.

	Alcohol %	Sucrose g/100ml	C <sub>O</sub> <sup>a</sup>	
			50°C	25°C
Type of wine:				
dry	10-11	-	12.8	8.9
"madeira" "heres"	16-19	3-4	12.2	8.4
port wine	17-19	7-10	11.7	7.9
dessert	16	16	10.2	6.8
must	-	15	9.4	7.4
must	-	20	8.2	6.5
Cognac:				
3*	40	1.5	10.5	10.2
4*	41	1.5	10.6	10.3
Wine Distillate	68	-	20.3	20.2

<sup>a</sup> Solubility of oxygen in mgO<sub>2</sub> per 1 liter of solution.

COMPONENTS:	ORIGINAL MEASUREMENTS:																																																														
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water solutions of alcohol and sugar (3) Wines	Moditis, I.Z.; Strukova, V.E.; Fal'kovich, Yu.E. <i>Vinodel Vinograd. SSSR 1977, (4),</i> 15-8. <i>Chem. Abstr. 1977, 87; 515 87a.</i>																																																														
VARIABLES:	PREPARED BY:																																																														
T/K = 298 Concentration	V. Katovic																																																														
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COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hydrogen fluoride; HF; [7664-39-3]		ORIGINAL MEASUREMENTS: Rewick, R. T.; Tolberg, W. E.; <i>J. Chem. Eng. Data</i> <u>1970</u> , 15, 527-30.		
VARIABLES: T/K = 273-293		PREPARED BY: C. L. Young		
EXPERIMENTAL VALUES:				
T/K	Total pressure P/kPa	Partial pressure P/kPa	Conc. of oxygen /mol kg <sup>-1</sup>	Mole fraction* of oxygen, x <sub>O<sub>2</sub></sub>
292.95	843.9	741.3	0.160	0.00320
272.94	726.6	678.6	0.153	0.00307
* calculated by compiler				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE: Static equilibrium cell made of Monel metal. Known amounts of oxygen added to known amount of hydrogen fluoride in cell. Quantity of gas absorbed calculated from equilibrium pressure and cell volume.		SOURCE AND PURITY OF MATERIALS: (1) High purity sample obtained from General Dynamics Corp. (2) Anhydrous sample obtained from Olin Corp. Conductivity 3 × 10 <sup>5</sup> ohm <sup>-1</sup> cm <sup>-1</sup> .		
		ESTIMATED ERROR: δT/K = ±0.02; δx <sub>O<sub>2</sub></sub> = ±2% (estimated by compiler).		
		REFERENCES:		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Sulfur dioxide; SO <sub>2</sub> ;	<b>ORIGINAL MEASUREMENTS:</b> Dornte, R.W.; Ferguson, C.V. <i>Ind. Eng. Chem.</i> <u>1939</u> , <i>31</i> , 112-3.																																				
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<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; text-align: center;"> <thead> <tr> <th>t/°C</th> <th>T/K<sup>a</sup></th> <th>K<sup>b</sup></th> </tr> </thead> <tbody> <tr><td>-60</td><td>213.2</td><td>0.12</td></tr> <tr><td>-60</td><td>213.2</td><td>0.59</td></tr> <tr><td>-50</td><td>223.2</td><td>1.63</td></tr> <tr><td>-50</td><td>223.2</td><td>2.14</td></tr> <tr><td>-40</td><td>233.2</td><td>5.2</td></tr> <tr><td>-40</td><td>233.2</td><td>4.05<sup>c</sup></td></tr> <tr><td>-30</td><td>243.2</td><td>10.2</td></tr> <tr><td>-30</td><td>243.2</td><td>11.0</td></tr> <tr><td>-20</td><td>253.2</td><td>25.2</td></tr> <tr><td>-20</td><td>253.2</td><td>24.8</td></tr> <tr><td>-20</td><td>253.2</td><td>30.1<sup>c</sup></td></tr> </tbody> </table>		t/°C	T/K <sup>a</sup>	K <sup>b</sup>	-60	213.2	0.12	-60	213.2	0.59	-50	223.2	1.63	-50	223.2	2.14	-40	233.2	5.2	-40	233.2	4.05 <sup>c</sup>	-30	243.2	10.2	-30	243.2	11.0	-20	253.2	25.2	-20	253.2	24.8	-20	253.2	30.1 <sup>c</sup>
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<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Kuenan coefficient, cm<sup>3</sup>(STP) of gas dissolved in 1 g of solvent at 101.32 kPa partial pressure of gas.</p> <p><sup>c</sup> By the circulation method; all other points by the static method. Authors give <math>\log_{10} K = 9.710 - 9650/(4.58 T/K)</math> as a smoothing equation good to <math>\pm 10\%</math>.</p>																																					
<b>AUXILIARY INFORMATION</b>																																					
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus consisted of a gas buret, a differential manometer, and two 10 cm <sup>3</sup> bulbs. The bulbs were in a dewar flask whose temperature was controlled manually by adding dry ice. Measurements could be taken while the gas was circulating or static. Gas uptake was read on the buret. Corrections were applied for the lines being at different temperatures.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given. <table border="1" style="width: 100%; margin-top: 10px;"> <tbody> <tr> <td data-bbox="633 1592 1188 1721"> <b>ESTIMATED ERROR:</b>  <math>\delta K/K = \pm 0.1</math>  <math>\delta T/K = \pm 0.5</math> </td> </tr> <tr> <td data-bbox="633 1721 1188 1926"> <b>REFERENCES:</b> </td> </tr> </tbody> </table>	<b>ESTIMATED ERROR:</b> $\delta K/K = \pm 0.1$ $\delta T/K = \pm 0.5$	<b>REFERENCES:</b>																																		
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitrogen oxide or dinitrogen tetraoxide; N <sub>2</sub> O <sub>4</sub> ; [10544-72-6]	<b>ORIGINAL MEASUREMENTS:</b> Chang, E. T.; Gokcen, N. A. <i>J. Phys. Chem.</i> <u>1966</u> , <i>70</i> , 2394-9.
<b>VARIABLES:</b> T/K = 262.02 - 303.16 P/kPa = 26.780 - 201.383	<b>PREPARED BY:</b> P. L. Long H. L. Clever
<b>EXPERIMENTAL VALUES:</b> <p>The authors discuss the system further (1, 2), but present no additional solubility data.</p> <p>The authors point out that their method of purification (double distillation) is not capable of removing trace amounts of N<sub>2</sub>O<sub>3</sub> in the N<sub>2</sub>O<sub>4</sub>.</p> <p>In the presence of trace amounts of N<sub>2</sub>O<sub>3</sub> the reaction <math>\frac{1}{2}\text{O}_2(\text{g}) + \text{N}_2\text{O}_3 = \text{N}_2\text{O}_4</math> takes place in the liquid N<sub>2</sub>O<sub>4</sub>. As a result the gas appears to obey Sievert's law, <math>K = x_0/P^{1/2}</math>, at low pressures of oxygen.</p> <p>If oxygen is first bubbled through the N<sub>2</sub>O<sub>4</sub>, then the trace amounts of N<sub>2</sub>O<sub>3</sub> are oxidized to N<sub>2</sub>O<sub>4</sub>, and the expected Henry's law behavior is observed at all pressures.</p> <p style="text-align: right;">continued on following page</p>	
<b>AUXILIARY INFORMATION</b>	
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus was of all glass construction. It consisted of three calibrated bulbs for the measurement of the gas, a container for the solvent, which was stirred by a glass enclosed magnet, and a manometer for measuring the pressure with a microslide cathetometer. The solvent container had a capacity for 100 g of solvent with a 5 cm<sup>3</sup> gas space above the liquid surface. The apparatus sections volumes were calibrated to ±0.0002 - 3 cm<sup>3</sup>.</p> <p>The solvent was degassed under vacuum in the previously weighed apparatus. The apparatus and the degassed liquid were weighed. The gas was introduced into the apparatus at a known P and T, the liquid stirred, and the pressure observed until there was no further change. Equilibrium was established within 10 m, and the pressure was followed for 40 m.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. (2) Nitrogen oxide. Source not given. Research grade, 99.5 per cent min. purity. Doubly distilled, then bubbled with O <sub>2</sub> to remove last traces of N <sub>2</sub> O <sub>3</sub> . Density, $\rho/\text{g cm}^{-3} = 1.4916 - 0.00226 t/^\circ\text{C}$
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.03$ $\delta P/\text{mmHg} = \pm 0.01$ $\delta x_1/x_1 = \pm 0.05$	
<b>REFERENCES:</b> 1. Chang, E. T.; Gokcen, N. A.; Poston, T. M. <i>J. Spacecr. Rockets</i> <u>1969</u> , <i>6</i> , 1177. 2. Gokcen, N. A.; Chang, E. T. <i>J. Chem. Ed.</i> <u>1977</u> , <i>54</i> , 368.	

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Nitrogen oxide or dinitrogen-tetraoxide; N <sub>2</sub> O <sub>4</sub> ; [10544-72-6]	ORIGINAL MEASUREMENTS: Chang, E. T.; Gokcen, N. A. <i>J. Phys. Chem.</i> <u>1966</u> , <i>70</i> , 2394-9.
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## EXPERIMENTAL MEASUREMENTS: continued

T/K	P/atm	Henry's Constant K x 10 <sup>4</sup>	Mol Fraction x <sub>1</sub> x 10 <sup>4</sup>	Bunsen Coefficient α	Ostwald Coefficient L
262.02	0.6041	8.84	5.34		
	1.2017	8.80	10.58		
	1.3091	8.76	11.47		
	1.6119	8.83	14.23		
	1.9876	8.75	17.40		
	1.0		8.80	0.325	0.312
273.15	0.2643	9.19	2.43		
	0.6275	9.21	5.78		
	1.1241	9.16	10.30		
	1.7950	9.12	16.37		
	1.0		9.17	0.333	0.333
298.15	0.3728	10.09	3.76		
	0.4989	10.34	5.16		
	0.5745	10.39	5.97		
	0.9963	10.12	10.08		
	1.0809	9.90	10.70		
	1.0		10.16	0.355	0.388
303.16	0.4441	10.65	4.73		
	0.9189	10.31	9.47		
	1.0	10	10.48	0.364	0.404

The solubility values at 1.0 atm oxygen pressure were calculated by the compiler from the average Henry's constant.

The author's define the Henry's constant,  $K/\text{atm}^{-1} = x_1/P_1$ .

The mole fraction solubility at 1 atm oxygen pressure is numerically equal to the Henry's constant.

Smoothed Data:  $\ln x_1 = -5.7652 - 3.3415/(T/100 \text{ K})$

T/K	Mol Fraction x <sub>1</sub> x 10 <sup>4</sup>
258.15	8.59
263.15	8.80
268.15	9.01
273.15	9.22
278.15	9.43
283.15	9.63
288.15	9.83
293.15	10.03
298.15	10.22
303.15	10.41
308.15	10.60

COMPONENTS:		ORIGINAL MEASUREMENTS:					
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Zenner, G. H.; Dana, L. I.					
(2) Nitrogen; N <sub>2</sub> ; [7727-37-9]		Chem. Eng. Prog. Symp. Ser.					
(3) Carbon dioxide; CO <sub>2</sub> ; [124-38-9]		1963, 59, No. 44, 36-41.					
VARIABLES:		PREPARED BY:					
T/K = 218-273 P/MPa = 7-13 Composition		C. L. Young					
EXPERIMENTAL VALUES:							
T/K	P/10 <sup>5</sup> Pa	Mole fractions in liquid			Mole fractions in gas		
		x <sub>O<sub>2</sub></sub>	x <sub>N<sub>2</sub></sub>	x <sub>CO<sub>2</sub></sub>	y <sub>O<sub>2</sub></sub>	y <sub>N<sub>2</sub></sub>	y <sub>CO<sub>2</sub></sub>
273.15	106.9	0.030	0.159	0.811	0.057	0.344	0.599
		0.0706	0.1224	0.8070	0.139	0.262	0.599
		0.1085	0.0888	0.8027	0.211	0.188	0.601
		0.1525	0.0515	0.7960	0.295	0.109	0.596
		0.286	0.1534	0.8180	0.0542	0.3353	0.6105
		0.557	0.1333	0.8110	0.1095	0.2865	0.6039
		0.1096	0.0801	0.8103	0.2217	0.1793	0.599
		0.1356	0.0669	0.7975	0.264	0.140	0.596
		0.1766	0.0308	0.7926	0.3383	0.0684	0.5933
		0.0643	0.1770	0.7587	0.1806	0.5610	0.2584
232.85	124.4	0.166	0.1100	0.724	0.4196	0.3190	0.2614
		0.2572	0.0523	0.6905	0.6017	0.1416	0.2567
		0.210	0.084	0.706	0.503	0.234	0.263
		0.1475	0.1215	0.731	0.3805	0.3575	0.2620
		0.1327	0.1307	0.7366	0.3396	0.4092	0.2512
		0.058	0.180	0.762	0.159	0.583	0.258
		0.024	0.206	0.770	0.071	0.671	0.258
		0.124	0.143	0.733	0.321	0.420	0.259
		0.0913	0.0321	0.8766	0.5092	0.2414	0.2494
		0.0662	0.0506	0.8832	0.3858	0.3676	0.2466
232.85	68.95	0.0477	0.0665	0.8858	0.277	0.473	0.250
		0.0349	0.0740	0.8911	0.2128	0.5407	0.2465
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Static bomb. Pressure measured with dead weight tester. Temperature measured with resistance thermometer. Samples of liquid and gas analysed by removing carbon dioxide from sample with potassium hydroxide solution. Oxygen was then removed with "ammoniacal copper" solution and remainder assumed to be nitrogen only.				(1) and (2) No details given. (3) Purified - no other details given.			
				ESTIMATED ERROR:			
				$\delta T/K = \pm 0.2$ ; $\delta P/MPa = \pm 0.05$ ; $\delta x_{O_2}$ , $\delta x_{N_2}$ , $\delta x_{CO_2}$ , $\delta y_{O_2}$ , $\delta y_{N_2}$ , $\delta y_{CO_2}$ $= \pm 0.002$ (estimated by compiler).			
				REFERENCES:			

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Zenner, G. H.; Dana, L. I.			
(2) Nitrogen; N <sub>2</sub> ; [7727-37-9]				<i>Chem. Eng. Prog. Symp. Ser.</i> <u>1963</u> ,			
(3) Carbon dioxide; CO <sub>2</sub> ; [124-38-9]				59, No. 44, 36-41.			
EXPERIMENTAL VALUES:							
T/K	P/10 <sup>5</sup> Pa	Mole fractions in liquid			Mole fractions in gas		
		x <sub>O<sub>2</sub></sub>	x <sub>N<sub>2</sub></sub>	x <sub>CO<sub>2</sub></sub>	y <sub>O<sub>2</sub></sub>	y <sub>N<sub>2</sub></sub>	y <sub>CO<sub>2</sub></sub>
232.85	68.95	0.0686	0.0503	0.8811	0.396	0.354	0.250
		0.0516	0.0628	0.8856	0.292	0.454	0.254
		0.0610	0.0564	0.8826	0.3472	0.3936	0.2592
232.85	51.7	0.0658	0.0540	0.8802	0.3746	0.3820	0.2434
		0.0787	0.0470	0.8743	0.4436	0.3093	0.2471
		0.0620	0.0231	0.9149	0.4943	0.2299	0.2758
218.15	131.0	0.0482	0.0336	0.9182	0.382	0.338	0.280
		0.0557	0.0277	0.9166	0.4479	0.2789	0.2732
		0.0376	0.0441	0.9183	0.2934	0.4256	0.2810
		0.0315	0.0435	0.9250	0.2463	0.4717	0.2820
		0.0269	0.0491	0.9240	0.2137	0.5035	0.2828
		0.0564	0.0300	0.9136	0.4363	0.2893	0.2744
		0.0604	0.0242	0.9154	0.4837	0.2373	0.2790
		0.0445	0.0325	0.9230	0.3714	0.3492	0.2794
		0.0565	0.0273	0.9162	0.4504	0.2731	0.2765
		0.0357	0.0427	0.9216	0.2880	0.4297	0.2823
		0.0404	0.0370	0.9226	0.3246	0.3978	0.2776
218.15	103.5	0.0507	0.1885	0.7608	0.1448	0.6560	0.1992
		0.158	0.121	0.721	0.422	0.388	0.190
		0.0874	0.1656	0.7470	0.2522	0.5620	0.1858
		0.1410	0.1365	0.7225	0.3875	0.4240	0.1885
		0.1797	0.1161	0.7042	0.455	0.348	0.197
		0.238	0.081	0.681	0.602	0.217	0.181
		0.314	0.042	0.644	0.681	0.107	0.212
		0.2182	0.0922	0.6896	0.5325	0.2682	0.1993
		0.087	0.109	0.804	0.327	0.514	0.159
		0.125	0.084	0.791	0.455	0.388	0.157
		0.148	0.065	0.787	0.555	0.287	0.158
218.15	68.95	0.0660	0.1217	0.8123	0.2427	0.600	0.1573
		0.100	0.098	0.802	0.473	0.369	0.158
		0.116	0.089	0.795	0.432	0.412	0.156
		0.136	0.076	0.788	0.499	0.3395	0.1615
		0.0936	0.0347	0.8717	0.5681	0.2822	0.1497
		0.078	0.046	0.876	0.481	0.367	0.152
		0.062	0.058	0.880	0.385	0.462	0.153
		0.0610	0.0580	0.8810	0.3742	0.4677	0.1581
		0.0508	0.0646	0.8846	0.3142	0.5293	0.1565
		0.041	0.073	0.886	0.250	0.598	0.152
		0.029	0.079	0.892	0.166	0.673	0.161
0.0219	0.0849	0.8932	0.1387	0.7051	0.1562		
0.0133	0.0912	0.8955	0.0858	0.7596	0.1546		
0.129	0.013	0.858	0.760	0.084	0.156		



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Mineral oil, white	<b>ORIGINAL MEASUREMENTS:</b> Kubie, L. S. <i>J. Biol. Chem.</i> <u>1927</u> , <i>72</i> , 545-8.				
<b>VARIABLES:</b> T/K = 297. 5 P/kPa = 101.325 (1 atm)	<b>PREPARED BY:</b> H. L. Clever				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha/\text{cm}^3</math> (STP) <math>\text{cm}^{-3} \text{atm}^{-1}</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">297. 5</td> <td style="text-align: center;">0.134 ± 0.004</td> </tr> </tbody> </table>		T/K	Bunsen Coefficient $\alpha/\text{cm}^3$ (STP) $\text{cm}^{-3} \text{atm}^{-1}$	297. 5	0.134 ± 0.004
T/K	Bunsen Coefficient $\alpha/\text{cm}^3$ (STP) $\text{cm}^{-3} \text{atm}^{-1}$				
297. 5	0.134 ± 0.004				
<b>AUXILIARY INFORMATION</b>					
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus was the constant volume Van Slyke and Neill type (1). Saturation was attained by bubbling the gas through the oil for several hours. A 1.990 ± 0.007 cm <sup>3</sup> volume of saturated solution was analyzed. The Van Slyke correction factor for unextracted and redissolved gas was 1.02.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Commercial cylinder. (2) Mineral oil."Amalie" brand, L. Sonneborn Sons, Inc., NY. A medicinal white oil which meets US Pharmacopeia standards. Specific gravity 0.890 - 0.895 at 15 °C , viscosity 285 at 100 °F. Prepared by fractional distillation from a naphthene base, unsaturated hydrocarbons removed. <b>ESTIMATED ERROR:</b> $\delta T/K = 1$ <b>REFERENCES:</b> 1. Van Slyke, D. D.; Neill, J. M. <i>J. Biol. Chem.</i> <u>1924</u> , <i>56</i> , 523.				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Oils.	<b>ORIGINAL MEASUREMENTS:</b> Baldwin, R. R.; Daniel, S. G.; <i>J. Appl. Chem.</i> , <u>1952</u> , 2(Apr.), 161-5. <i>J. Inst. Petrol.</i> , London, <u>1953</u> , 39, 105-24.																																																									
<b>VARIABLES:</b> T/K = 273.15 - 373.15 O <sub>2</sub> P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever																																																									
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Bunsen Coefficient <math>\alpha</math></th> <th style="text-align: center;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="3">Oil A1, viscosity 615 centistokes at 100°F, mean mol wt 670.</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">0.124</td> <td style="text-align: center;">0.133</td> </tr> <tr> <td colspan="3">Oil A2, viscosity 268 centistokes at 100°F, mean mol wt 610.</td> </tr> <tr> <td style="text-align: center;">273.15</td> <td style="text-align: center;">0.135</td> <td style="text-align: center;">0.135</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">0.126</td> <td style="text-align: center;">0.135</td> </tr> <tr> <td style="text-align: center;">333.15</td> <td style="text-align: center;">0.119</td> <td style="text-align: center;">0.145</td> </tr> <tr> <td style="text-align: center;">373.15</td> <td style="text-align: center;">0.118</td> <td style="text-align: center;">0.161</td> </tr> <tr> <td colspan="3">Oil A3, viscosity 181 centistokes at 100°F, mean mol wt 570.</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">0.129</td> <td style="text-align: center;">0.139</td> </tr> <tr> <td colspan="3">Oil A4, viscosity 80.3 centistokes at 100°F, mean mol wt 530.</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">0.137<sup>1</sup></td> <td style="text-align: center;">0.147</td> </tr> <tr> <td colspan="3">Oil A5, viscosity 34.9 centistokes at 100°F, mean mol wt 400.</td> </tr> <tr> <td style="text-align: center;">273.15</td> <td style="text-align: center;">0.150</td> <td style="text-align: center;">0.150</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">0.1445</td> <td style="text-align: center;">0.155</td> </tr> <tr> <td style="text-align: center;">333.15</td> <td style="text-align: center;">0.135</td> <td style="text-align: center;">0.164</td> </tr> <tr> <td style="text-align: center;">373.15</td> <td style="text-align: center;">0.130</td> <td style="text-align: center;">0.178</td> </tr> <tr> <td colspan="3">Oil B1, viscosity 260 centistokes at 100°F, mean mol wt 630.</td> </tr> <tr> <td style="text-align: center;">293.15</td> <td style="text-align: center;">0.120</td> <td style="text-align: center;">0.129</td> </tr> </tbody> </table>		T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	Oil A1, viscosity 615 centistokes at 100°F, mean mol wt 670.			293.15	0.124	0.133	Oil A2, viscosity 268 centistokes at 100°F, mean mol wt 610.			273.15	0.135	0.135	293.15	0.126	0.135	333.15	0.119	0.145	373.15	0.118	0.161	Oil A3, viscosity 181 centistokes at 100°F, mean mol wt 570.			293.15	0.129	0.139	Oil A4, viscosity 80.3 centistokes at 100°F, mean mol wt 530.			293.15	0.137 <sup>1</sup>	0.147	Oil A5, viscosity 34.9 centistokes at 100°F, mean mol wt 400.			273.15	0.150	0.150	293.15	0.1445	0.155	333.15	0.135	0.164	373.15	0.130	0.178	Oil B1, viscosity 260 centistokes at 100°F, mean mol wt 630.			293.15	0.120	0.129
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<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The method consists of two operations: Saturation of the liquid with the gas under consideration; and determination of the amount of dissolved gas in the liquid saturated with the gas. All gases were passed through a liquid air trap to remove water and CO<sub>2</sub> vapors before passage through the liquid. All gases were passed through a long coil, thermostated, before the saturation process.</p> <p>Oil or similar liquid is deaerated by passing it through a continuously evacuated vessel. Gas is then passed through the liquid to saturation. Liquid is then degassed, and transferred to a storage burette, disconnected from the degassing apparatus, thermostated, and saturated with the desired gas. Burette is now connected to another degassing apparatus, portions of the oil degassed and gas collected.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. From commercial cylinders, and gas analysis on a Bone and Wheeler apparatus shows it to be at least 99.5% pure; no source given. (2) Oils. The oils conform to DTD-472B specifications. Composition and physical properties of the oils are given in the appendix of the 1953 paper. The molecular weights were determined by freezing point depression in naphthalene to within $\pm 5$ percent.																																																									
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<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Four oils</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Rodnight, R.</p> <p><i>Biochem. J.</i> <u>1954</u>, 57, 661-3.</p>																								
<p>VARIABLES:</p> <p>T/K = 311</p>	<p>PREPARED BY:</p> <p>R. Battino</p>																								
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="282 493 1138 830"> <thead> <tr> <th data-bbox="282 512 651 552">Oil</th> <th data-bbox="655 493 940 552"><math>\alpha^a / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}</math> 38°C (311K)</th> <th data-bbox="944 512 1138 552">L<sup>b</sup></th> </tr> </thead> <tbody> <tr> <td data-bbox="282 572 651 612">liquid paraffin<sup>c</sup></td> <td data-bbox="655 572 940 612">0.098 (5)<sup>d</sup></td> <td data-bbox="944 572 1138 612">0.112</td> </tr> <tr> <td data-bbox="282 612 651 652">olive oil<sup>e</sup></td> <td data-bbox="655 612 940 652">0.102 (6)<sup>d</sup></td> <td data-bbox="944 612 1138 652">0.116</td> </tr> <tr> <td data-bbox="282 652 651 691">silicone fluid<sup>f</sup></td> <td data-bbox="655 652 940 691">0.251</td> <td data-bbox="944 652 1138 691">0.286</td> </tr> <tr> <td data-bbox="282 691 651 731"></td> <td data-bbox="655 691 940 731">0.250</td> <td data-bbox="944 691 1138 731">0.285</td> </tr> <tr> <td data-bbox="282 731 651 771"></td> <td data-bbox="655 731 940 771">0.210</td> <td data-bbox="944 731 1138 771">0.239</td> </tr> <tr> <td data-bbox="282 771 651 811">silicone fluid<sup>e</sup></td> <td data-bbox="655 771 940 811">0.304</td> <td data-bbox="944 771 1138 811">0.346</td> </tr> <tr> <td data-bbox="282 811 651 850"></td> <td data-bbox="655 811 940 850">0.297</td> <td data-bbox="944 811 1138 850">0.338</td> </tr> </tbody> </table> <p>a Bunsen coefficient.</p> <p>b Ostwald coefficient calculated by compiler.</p> <p>c Specific gravity of 0.835.</p> <p>d Number of duplicate determinations in parentheses.</p> <p>e Characterized as B.P. (1948).</p> <p>f Viscosity of 5cS.</p> <p>e Viscosity of 1cS.</p>		Oil	$\alpha^a / \text{cm}^3 (\text{STP}) \text{cm}^{-3} \text{atm}^{-1}$ 38°C (311K)	L <sup>b</sup>	liquid paraffin <sup>c</sup>	0.098 (5) <sup>d</sup>	0.112	olive oil <sup>e</sup>	0.102 (6) <sup>d</sup>	0.116	silicone fluid <sup>f</sup>	0.251	0.286		0.250	0.285		0.210	0.239	silicone fluid <sup>e</sup>	0.304	0.346		0.297	0.338
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<p>AUXILIARY INFORMATION</p>																									
<p>METHOD / APPARATUS / PROCEDURE:</p> <p>Oxygen was introduced into a chamber containing degassed oil. The rate of absorption was monitored on a manometer. Then a fresh charge of degassed oil was added and the pressure monitored again. From knowledge of the oil volumes and the change of pressure in both cases the Bunsen coefficient could be calculated. Details and a drawing are given in the paper.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p> <p>ESTIMATED ERROR:</p> <p><math>\delta\alpha/\alpha = \pm 0.03</math>, compiler's estimate.</p> <p>REFERENCES:</p>																								

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Paraffin Oil and a 50:50 mixture of 1-decanol and 1-dodecanol	<b>ORIGINAL MEASUREMENTS:</b> Luther, H.; Hiemenz, W. <i>Chem. Ingr.-Tech.</i> <u>1957</u> , 29, 530-5.																				
<b>VARIABLES:</b> T/K - 293	<b>PREPARED BY:</b> R. Battino																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse; margin-top: 10px;"> <thead> <tr> <th style="text-align: center;">t/°C</th> <th style="text-align: center;">T<sup>a</sup>/K</th> <th style="text-align: center;">10<sup>4</sup>x<sub>1</sub><sup>b</sup></th> <th style="text-align: center;">H<sup>c</sup></th> </tr> </thead> <tbody> <tr> <td colspan="4" style="text-align: center;">Paraffin Oil</td> </tr> <tr> <td style="text-align: center;">20</td> <td style="text-align: center;">293</td> <td style="text-align: center;">27.8</td> <td style="text-align: center;">364</td> </tr> <tr> <td colspan="4" style="text-align: center;">Alcohol Mixture<sup>d</sup></td> </tr> <tr> <td style="text-align: center;">20</td> <td style="text-align: center;">293</td> <td style="text-align: center;">10.4</td> <td style="text-align: center;">962</td> </tr> </tbody> </table> <p style="margin-top: 10px;"> <sup>a</sup> Calculated by compiler.  <sup>b</sup> Mole fraction solubility at 101.325 kPa partial pressure of gas.  <sup>c</sup> Henry's law constant; P<sub>1</sub>/atm = x<sub>1</sub> (H/atm).  <sup>d</sup> 50 mol % 1-decanol + 50 mol % 1-dodecanol.         </p>		t/°C	T <sup>a</sup> /K	10 <sup>4</sup> x <sub>1</sub> <sup>b</sup>	H <sup>c</sup>	Paraffin Oil				20	293	27.8	364	Alcohol Mixture <sup>d</sup>				20	293	10.4	962
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<b>METHOD/APPARATUS/PROCEDURE:</b> Solubilities determined in an apparatus described in the paper by a combined pressure and volume measurement.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) Paraffin oil - density of 0.8795g cm <sup>-3</sup> and molecular weight of 405g mol <sup>-1</sup> . (2) Alcohol mixture is 50 mol % 1-decanol + 50 mol % 1-dodecanol.																				
	<b>ESTIMATED ERROR:</b> δH/H = ±0.05, compiler's estimate.																				
	<b>REFERENCES:</b>																				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Paraffin Oil.	<b>ORIGINAL MEASUREMENTS:</b> Luther, H.; Rottger, H. <i>Elektrotech. Z.</i> <u>1957</u> , A78, 462-4.																				
<b>VARIABLES:</b> T/K = 318 P/kPa = 27-103	<b>PREPARED BY:</b> R. Battino																				
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse; margin-top: 10px;"> <thead> <tr> <th style="text-align: center;">t/°C</th> <th style="text-align: center;">T/K</th> <th style="text-align: center;">P/mm Hg</th> <th style="text-align: center;">S/cm<sup>3</sup>g<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">45</td> <td style="text-align: center;">318</td> <td style="text-align: center;">200</td> <td style="text-align: center;">0.038</td> </tr> <tr> <td style="text-align: center;">45</td> <td style="text-align: center;">318</td> <td style="text-align: center;">400</td> <td style="text-align: center;">0.079</td> </tr> <tr> <td style="text-align: center;">45</td> <td style="text-align: center;">318</td> <td style="text-align: center;">600</td> <td style="text-align: center;">0.117</td> </tr> <tr> <td style="text-align: center;">45</td> <td style="text-align: center;">318</td> <td style="text-align: center;">770</td> <td style="text-align: center;">0.151</td> </tr> </tbody> </table> <p style="margin-top: 10px;"><sup>a</sup> Calculated by compiler.</p>		t/°C	T/K	P/mm Hg	S/cm <sup>3</sup> g <sup>-1</sup>	45	318	200	0.038	45	318	400	0.079	45	318	600	0.117	45	318	770	0.151
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<b>METHOD/APPARATUS/PROCEDURE:</b> Solubilities determined by an apparatus described in the paper by a combined volume and pressure measurement.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) Molecular weight of 357 g mol <sup>-1</sup> , $d_{20} = 0.8420 \text{ g cm}^{-3}$ , $n_D^{20} = 1.4597$ .  <b>ESTIMATED ERROR:</b> $\delta S/S = \pm 0.05$ , estimate by compiler.  <b>REFERENCES:</b>																				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Polydimethylsiloxane oil	<b>ORIGINAL MEASUREMENTS:</b> Cannon, P.: St. Pierre, L.E.; Miller, A.A. J. Chem. Eng. Data <u>1960</u> , 5, 236.				
<b>VARIABLES:</b> T/K = 303 P/kPa = 446 - 2169	<b>PREPARED BY:</b> R. Battino				
<b>EXPERIMENTAL VALUES:</b>					
	t/°C	T/K <sup>a</sup>	P/atm	P/kPa <sup>a</sup>	10 <sup>4</sup> S <sup>b</sup>
30	303	4.40 7.80 12.02 16.31 21.41	446 790 1218 1653 2169	7.7 12.8 20.5 27.7 38.5	
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Solubility in g gas/g oil.</p>					
<b>AUXILIARY INFORMATION</b>					
<b>METHOD/APPARATUS/PROCEDURE:</b>			<b>SOURCE AND PURITY OF MATERIALS:</b>		
A sample of about 10 g is placed in a sintered alumina bucket in an automatic gravimetric sorption balance. At different gas pressures the weight of dissolved gas is measured.			(1) "Tank grade." (2) 26,000 centistoke.		
			<b>ESTIMATED ERROR:</b>		
			$\delta S/S = \pm 0.02$ , compiler's estimate		
			<b>REFERENCES:</b>		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Hydrocarbon fuels and oil	<b>ORIGINAL MEASUREMENTS:</b> Logvinyuk, V. P.; Makarenkov, V. V.; Malyshev, V. V.; Panchenkov, G. M.  <i>Khim. Tekhnol. Topl. Masel</i> 1970, 15, (No. 5), 27-9. <i>Chem. Technol. Fuels Oils (Eng. trans)</i> 1970, 15, 353-5.
<b>VARIABLES:</b> T/K = 253.15 - 365.15 O <sub>2</sub> P/kPa = 101.325	<b>PREPARED BY:</b> S. A. Johnson H. L. Clever

EXPERIMENTAL VALUES:	T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L
Hydrocarbon fuel, T-1, density $\rho_4^{20} = 0.816$			
	253.15	0.258	0.239
	273.15	0.228	0.228
	293.15	0.205	0.220
	323.15	0.182	0.215
Hydrocarbon fuel, TS-1, density $\rho_4^{20} = 0.775$			
	293.15	0.220	0.236
Hydrocarbon fuel, T-6, density $\rho_4^{20} = 0.84$			
	253.15	0.198	0.184
	273.15	0.190	0.190
	293.15	0.198	0.212
	323.15	0.190	0.225
	365.15	0.152	0.203
Hydrogenated fuel, density $\rho_4^{20} = 0.832$			
	293.15	0.198	0.212
Oil, MK-8, density $\rho_4^{20} = 0.855$			
	293.15	0.152	0.163

The compiler calculated the Ostwald coefficients.

## AUXILIARY INFORMATION

<b>METHOD/APPARATUS/PROCEDURE:</b>  The apparatus and procedure were described in reference (1) which was not available to the compiler.	<b>SOURCE AND PURITY OF MATERIALS:</b>  No information given.
<b>REFERENCES:</b>  1. Gogitidize, L. D.; Logvinyuk, V. P.; Makarenkov, V. V.; Panchenkov, G. M.; Malyshev, V. V.; Yakovlevskii, V. V. <i>Method of Evaluating the Operating Properties of Jet Fuels and Lubricating Materials (Russ.)</i> , Mashinostroenie 1966.	<b>ESTIMATED ERROR:</b>  $\delta\alpha/\alpha = 0.06$ (authors)

*Mashinostroenie*, see *Izv. Vyssh. Uchebn. Zaved., Mashinostr.*

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Wax ester oils	<b>ORIGINAL MEASUREMENTS:</b> Ke, P. J.; Ackman, R. G.  <i>J. Am. Oil Chemists' soc.</i> <u>1973</u> 80, 429-35.																																																							
<b>VARIABLES:</b> T/K = 293.15 - 353.15 P/kPa = partial pressure of oxygen in air at 101.325 kPa	<b>PREPARED BY:</b> P. L. Long H. L. Clever																																																							
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<table border="1"> <thead> <tr> <th>Temperature t/°C</th> <th>Density ρ/g cm<sup>-3</sup></th> <th>Bunsen Coefficient<sup>1</sup> α</th> <th>Parts per Million<sup>2</sup> μg g<sup>-1</sup></th> <th>cm<sup>3</sup> (STP) O<sub>2</sub> of oil<sup>2</sup></th> </tr> </thead> <tbody> <tr> <td colspan="5">Sperm whale oil</td> </tr> <tr> <td>20</td> <td>293.15</td> <td>0.8775</td> <td>37.0</td> <td>2.27</td> </tr> <tr> <td>40</td> <td>313.15</td> <td>0.8639</td> <td>43.1</td> <td>2.60</td> </tr> <tr> <td>60</td> <td>323.15</td> <td>0.8514</td> <td>40.9</td> <td>2.46</td> </tr> <tr> <td>80</td> <td>353.15</td> <td>0.8378</td> <td>24.9</td> <td>1.45</td> </tr> <tr> <td colspan="5">Barracudina oil</td> </tr> <tr> <td>20</td> <td>293.15</td> <td>0.8933</td> <td>30.4</td> <td>1.91</td> </tr> <tr> <td>40</td> <td>313.15</td> <td>0.8812</td> <td>32.1</td> <td>1.98</td> </tr> <tr> <td>60</td> <td>323.15</td> <td>0.8679</td> <td>27.5</td> <td>1.67</td> </tr> <tr> <td>80</td> <td>353.15</td> <td>0.8553</td> <td>20.2</td> <td>1.21</td> </tr> </tbody> </table>		Temperature t/°C	Density ρ/g cm <sup>-3</sup>	Bunsen Coefficient <sup>1</sup> α	Parts per Million <sup>2</sup> μg g <sup>-1</sup>	cm <sup>3</sup> (STP) O <sub>2</sub> of oil <sup>2</sup>	Sperm whale oil					20	293.15	0.8775	37.0	2.27	40	313.15	0.8639	43.1	2.60	60	323.15	0.8514	40.9	2.46	80	353.15	0.8378	24.9	1.45	Barracudina oil					20	293.15	0.8933	30.4	1.91	40	313.15	0.8812	32.1	1.98	60	323.15	0.8679	27.5	1.67	80	353.15	0.8553	20.2	1.21
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<b>METHOD/APPARATUS/PROCEDURE:</b> Polarographic exponential dilution method (1). The oil was degassed by the method of Battino et al. (2). A 155-159 cm <sup>3</sup> sample of degassed oil was transferred to a glass vessel and weighed. The vessel was so constructed that the ratio $V_{\text{top air space}}/V_{\text{oil}}$ was between 0.0704 and 0.0981. A magnetic stirring bar (120 rpm) and a polarographic oxygen sensor were placed in the sample. Air was bubbled through the sample at 15 cm <sup>3</sup> m <sup>-1</sup> for two hours. The air was stopped, and helium gas preheated to the sample temperature was introduced into the oil at a rate of 7-10 cm <sup>3</sup> m <sup>-1</sup> . The oxygen concentration was measured as a function of the volume of helium passed through the solution. A plot of log (O <sub>2</sub> ) vs. V <sub>helium</sub> is linear. The slope is a function of the Ostwald coefficient. The Ostwald coefficient was converted to Bunsen coefficient.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Breathing grade compressed air. (2) Sperm whale oil. Oil from sperm whale ( <i>Physeter catodon</i> ) blubber obtained from local commercial reduction plant in Nova Scotia. Barracudina oil. Oil from whole barracudina ( <i>Paralepis rissoi Krøyeri</i> ) was produced in pilot scale reduction plant at the Vancouver Lab of The Fisheries Research Board of Canada. All oils were kept under nitrogen in cold storage at 3°C except when the experiment was in progress. <b>ESTIMATED ERROR:</b> Solubility values are the average of three determinations with relative standard deviation of 7% or less. <b>REFERENCES:</b> 1. Aho, L.; Wahlroos, O. <i>J. Am. Oil Chem. Soc.</i> <u>1967</u> , 44, 65. 2. Battino, R.; Banzhof, M.; Bogan, M.; Wilhelm, E. <i>Anal. Chem.</i> <u>1971</u> , 45, 806.																																																							



<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Petroleum	<b>ORIGINAL MEASUREMENTS:</b> Gniewosz, S.; Walfisz, A. <i>Z. Phys. Chem.</i> <u>1887</u> , 1, 70-2.									
<b>VARIABLES:</b> T/K = 283.15, 293.15 Pressure = "Atmospheric"	<b>PREPARED BY:</b> M. E. Derrick H. L. Clever									
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="359 473 911 652" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td>283.15</td> <td>0.229</td> <td>0.237</td> </tr> <tr> <td>293.15</td> <td>0.202</td> <td>0.217</td> </tr> </tbody> </table> <p data-bbox="359 691 942 737" style="text-align: center;">The Ostwald coefficients were calculated by the compiler.</p>		T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	283.15	0.229	0.237	293.15	0.202	0.217
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<b>AUXILIARY INFORMATION</b>										
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The apparatus consisted of an absorption flask connected to a gas buret by a flexible lead capillary. The system was thermostated in a large water bath.</p> <p>The volume of oxygen absorbed in a known volume of degassed petroleum was directly measured using the gas buret.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. No information. (2) Petroleum. Russian petroleum. Cleaned by boiling in a large copper flask.									
<b>ESTIMATED ERROR:</b> $\delta\alpha/\alpha = 0.05$ (compiler)										
<b>REFERENCES:</b>										

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [ 7782-44-7 ] (2) Hydrocarbon fuels	<b>ORIGINAL MEASUREMENTS:</b> Baldwin, R. R.; Daniel, S. G. <i>J. Appl. Chem.</i> <u>1952</u> , <i>2</i> , 161-5. <i>J. Inst. Petrol.</i> , London, <u>1953</u> , <i>39</i> , 105-24.																		
<b>VARIABLES:</b> T/K = 273.15 - 293.15 O <sub>2</sub> P/kPa = 101.325	<b>PREPARED BY:</b> P. L. Long H. L. Clever																		
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse; text-align: center;"> <thead> <tr> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">T/K</th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Bunsen Coefficient <math>\alpha</math></th> <th style="border-top: 1px solid black; border-bottom: 1px solid black;">Ostwald Coefficient L</th> </tr> </thead> <tbody> <tr> <td colspan="3" style="text-align: left; padding-left: 20px;">100 octane fuel D</td> </tr> <tr> <td>293.15</td> <td>0.344</td> <td>0.369</td> </tr> <tr> <td colspan="3" style="text-align: left; padding-left: 20px;">Kerosene</td> </tr> <tr> <td>273.15</td> <td>0.220</td> <td>0.220</td> </tr> <tr> <td>293.15</td> <td>0.212</td> <td>0.228</td> </tr> </tbody> </table>		T/K	Bunsen Coefficient $\alpha$	Ostwald Coefficient L	100 octane fuel D			293.15	0.344	0.369	Kerosene			273.15	0.220	0.220	293.15	0.212	0.228
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<b>AUXILIARY INFORMATION</b>																			
<b>METHOD/APPARATUS/PROCEDURE:</b> 1. Degassing. The liquid was deaerated by passage through a continuously evacuated vessel. The liquid was saturated with gas, then degassed again. 2. Saturation of liquid with gas. The gas was passed through a liquid air trap to remove water and carbon dioxide, then through a long coil thermostated at the temperature of the solubility measurement, and then bubbled through the liquid up to five hours. 3. Determination of the amount of gas liberated under vacuum from a known volume of the saturated liquid. The saturated liquid is placed in a vessel attached to a calibrated buret. The whole apparatus was initially evacuated. The gas released from the liquid was transferred to the calibrated buret by a Toplep pump. Five operations and transfers recover all but a trace of the gas. The last trace (2 - 5 %) removed by boiling the liquid.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Commercial cylinder, source not given. 99.5 per cent pure by gas analysis on Bone and Wheeler apparatus. (2) 100 Octane Fuel. Molecular weight estimated to be 100. Kerosene. Mean molecular weight measured, obtained 165. <b>ESTIMATED ERROR:</b> $\delta P/P = 0.01$ $\delta \alpha/\alpha = 0.01$ <b>REFERENCES:</b>																		

COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Liquid paraffin		Ruppel, D. Can. J. Chem. <u>1971</u> , 44, 3762-4.	
VARIABLES:		PREPARED BY:	
T/K = 304 - 363 P/kPa = 39 - 111		R. Battino	
EXPERIMENTAL VALUES:			
P/Torr	P <sup>a</sup> /kPa	$\beta^b/\text{cm}^3(\text{STP})$ $\text{cm}^{-3} \text{ atm}^{-1}$	$10^{-5} K_H^C$
35°C (308.2 K)			
290	38.7	0.052	2.76
397	52.9	0.068	2.90
506	67.5	0.091	2.75
631	84.1	0.112	2.80
760	101.3	0.135	2.80
834	111.2	0.150	2.76
t/°C	T <sup>a</sup> /K	$\beta^b/\text{cm}^3(\text{STP})$ $\text{cm}^{-3} \text{ atm}^{-1}$	$10^{-5} K_H^C$
31	304.2	0.139	2.73
35	308.2	0.137	2.75
44	317.2	0.134	2.80
57	330.2	0.135	2.74
69	342.2	0.133	2.78
79	352.2	0.133	2.76
90	363.2	0.131	2.78
<p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Bunsen coefficient.</p> <p><sup>c</sup> Henry's constant in Torr per mole fraction.</p>			
AUXILIARY INFORMATION			
METHOD / APPARATUS / PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Method based on that in reference (1). The liquid was equilibrated with the gas; then transferred to a gas stripping cell; and then the extracted gas was analyzed by gas chromatography. The oxygen was determined on a 2 m molecular sieve type 5A of 40-60 mesh at 50°C.		(1) No details given. (2) LP, Anachemia AC7014. Average molecular weight of 390, viscosity and density, respectively, at 20°C of 126 cs and 0.871 g cm <sup>-3</sup> . Refractive index of 1.4748 at 21.4°C.	
		ESTIMATED ERROR: $\delta\beta/\beta = \pm 0.03$ , compiler's estimate. $\delta T/K = \pm 0.1$	
		REFERENCES: 1. Gubbins, K.E.; Carden, S.N.; Walker, R.D. <i>J. Gas Chromatogr.</i> <u>1965</u> , 3, 98.	

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Paraffin wax</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Ridenour, W. P.; Weatherford, W. D.; Capell, R. G.</p> <p><i>Ind. Eng. Chem.</i> <u>1954</u>, <i>46</i>, 2376-81.</p>																										
<p>VARIABLES:</p> <p>T/K = 345.35</p> <p>P/kPa = 31.70 - 107.79</p>	<p>PREPARED BY:</p> <p>A. L. Cramer H. L. Clever</p>																										
<p>EXPERIMENTAL VALUES:</p> <table border="1" data-bbox="205 469 1165 707"> <thead> <tr> <th>T/K</th> <th>Pressure/ mmHg</th> <th>Mol Fraction X<sub>1</sub> × 10<sup>3</sup></th> <th>Bunsen Coefficient α</th> <th>Solubility Coefficient cm<sup>3</sup> O<sub>2</sub> (STP) g<sup>-1</sup> wax</th> </tr> </thead> <tbody> <tr> <td rowspan="5">245.35</td> <td>237.8</td> <td>1.00</td> <td>0.156</td> <td>0.064</td> </tr> <tr> <td>402.9</td> <td>1.70</td> <td>0.158</td> <td>0.109</td> </tr> <tr> <td>602.5</td> <td>2.58</td> <td>0.161</td> <td>0.165</td> </tr> <tr> <td>808.5</td> <td>3.47</td> <td>0.161</td> <td>0.222</td> </tr> <tr> <td>760.0</td> <td>(3.28)</td> <td>0.161</td> <td>0.21</td> </tr> </tbody> </table> <p>The mole fraction solubility at 760 mmHg was calculated by the compiler.</p>		T/K	Pressure/ mmHg	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Solubility Coefficient cm <sup>3</sup> O <sub>2</sub> (STP) g <sup>-1</sup> wax	245.35	237.8	1.00	0.156	0.064	402.9	1.70	0.158	0.109	602.5	2.58	0.161	0.165	808.5	3.47	0.161	0.222	760.0	(3.28)	0.161	0.21
T/K	Pressure/ mmHg	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Solubility Coefficient cm <sup>3</sup> O <sub>2</sub> (STP) g <sup>-1</sup> wax																							
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>The apparatus was similar to the equilibrium adsorption apparatus described by Brunauer, Emmett, and Teller (1) for the measurement of the surface area of a solid catalyst.</p> <p>A weighed amount of wax was placed in the apparatus. The gas and solvent were equilibrated for 20 to 60 minutes. The gas volume in the buret system was calculated from the ideal gas law.</p> <p>The results of the absorption measurements were checked by a desorption measurement. The two measurements agreed very well.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Oxygen. Prepared from KMnO<sub>4</sub>. Contained 97.8% O<sub>2</sub>, 1.1% N<sub>2</sub>, and 0.1% CO<sub>2</sub>.</p> <p>(2) Paraffin wax. Described as 122°F English melting point wax. Molecular weight 350, actual melt point 123.2°F (323.8 K), density 0.7716 g cm<sup>-3</sup> at 293.3 K and 0.7662 g cm<sup>-3</sup> at 298.0 K.</p> <p>ESTIMATED ERROR:</p> <p>δT/K = 2.</p> <p>δP/mmHg = 0.2</p> <p>δα/cm<sup>3</sup> = 0.004 (low pressure) -0.001 (high pres.)</p> <p>REFERENCES:</p> <p>1. Brunauer, S.; Emmett, P. H.; Teller, E. <i>J. Am. Chem. Soc.</i> <u>1938</u>, <i>60</i>, 309.</p>																										

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Petrowax A	<b>ORIGINAL MEASUREMENTS:</b> Pidenour, W. P.; Weatherford, W. D.; Capell, R.G. <i>Ind. Eng. Chem.</i> <u>1954</u> , <i>46</i> , 2376-81.
<b>VARIABLES:</b> T/K = 354.75 P/kPa = 38.60 - 104.92	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever

**EXPERIMENTAL VALUES:**

T/K	Pressure/ mmHg	Mol Fraction X <sub>1</sub> × 10 <sup>3</sup>	Bunsen Coefficient α	Solubility Coefficient cm <sup>3</sup> O <sub>2</sub> (STP) g <sup>-1</sup> wax
354.75	289.5	1.27	0.081	0.038
	361.9	1.67	0.084	0.050
	480.0	2.37	0.090	0.071
	583.5	3.18	0.099	0.095
	787.0	4.43	0.103	0.133

**AUXILIARY INFORMATION****METHOD/APPARATUS/PROCEDURE:**

The apparatus was similar to the equilibrium adsorption apparatus described by Brunauer, Emmett, and Teller (1) for the measurement of the surface area of a solid catalyst.

A weighed amount of wax was placed in the apparatus. The gas and solvent were equilibrated for 20 to 60 minutes. The gas volume in the buret system was calculated from the ideal gas law.

The results of the absorption measurements were checked by a desorption measurement. The two measurements agreed very well.

**SOURCE AND PURITY OF MATERIALS:**

(1) Oxygen. Prepared from KMnO<sub>4</sub>. Contained 97.8% O<sub>2</sub>, 1.1% N<sub>2</sub>, and 0.1% CO<sub>2</sub>.

(2) Petrowax A. Molecular weight 750, melting point 159.6°F (352.8 K) density 0.8039 g cm<sup>-3</sup> at 355.6 K and 0.7949 g cm<sup>-3</sup> at 370.2 K.

**ESTIMATED ERROR:**

$$\delta T/K = 2.$$

$$\delta P/\text{mmHg} = 0.2$$

$$\delta \alpha/\text{cm}^3 = 0.004 \text{ (low pressure)}$$

$$- 0.001 \text{ (high pres.)}$$

**REFERENCES:**

- Brunauer, S.; Emmett, P. H.; Teller, E.  
*J. Am. Chem. Soc.* 1938, *60*, 309.

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Amsco 123-5	<b>ORIGINAL MEASUREMENTS:</b> Steinberg, M.; Manowitz, B. <i>Ind. Eng. Chem.</i> <u>1959</u> , <i>51</i> , 47 - 51.				
<b>VARIABLES:</b> T/K = 297.15 P/kPa = 101.325	<b>PREPARED BY:</b> H. L. Clever				
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="435 486 800 635" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">T/K</th> <th style="text-align: center;">Absorption Coefficient <math>\beta</math></th> </tr> </thead> <tbody> <tr> <td style="text-align: center;">297.15</td> <td style="text-align: center;">0.159</td> </tr> </tbody> </table> <p>The authors define the Absorption coefficient as the volume of gas, corrected to 288.15 K and 101.325 kPa, absorbed under a total system pressure of 101.325 kPa per unit volume (at 288.15 K) of solvent.</p>		T/K	Absorption Coefficient $\beta$	297.15	0.159
T/K	Absorption Coefficient $\beta$				
297.15	0.159				
<b>AUXILIARY INFORMATION</b>					
<b>METHOD/APPARATUS/PROCEDURE:</b> Van Slyke Method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Matheson Co. (2) Amsco 123-5. American Mineral Spirits Co. No. 140. Paraffin 59.6 wt %, naphthene 27.3 wt %, and aromatics 13.2 wt %. <b>ESTIMATED ERROR:</b> $\delta\beta/\beta = 0.05 - 0.10$ (authors) <b>REFERENCES:</b>				

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) L-1822, which is a mixture of mostly 10-carbon fluorocarbons, including cyclic, open chain, and branched molecules.	<b>ORIGINAL MEASUREMENTS:</b> Sargent, J. W.; Seffl, R. J. <i>Fed. Proc.</i> <u>1970</u> , <i>29</i> , 1699 - 1703.																
<b>VARIABLES:</b> T/K = 298 - 310 Total P/kPa = 101.325	<b>PREPARED BY:</b> A. L. Cramer H. L. Clever																
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="360 469 1060 648" style="margin: 10px auto;"> <thead> <tr> <th colspan="2">Temperature</th> <th colspan="2">Oxygen Solubility</th> </tr> <tr> <th>t/°C</th> <th>T/K</th> <th>g O<sub>2</sub> 1000 g<sup>-1</sup></th> <th>cm<sup>3</sup> O<sub>2</sub> 100 cm<sup>-3</sup></th> </tr> </thead> <tbody> <tr> <td>25</td> <td>298.15</td> <td>0.285</td> <td>41.5</td> </tr> <tr> <td>37</td> <td>310.15</td> <td>0.271</td> <td>40.7</td> </tr> </tbody> </table> <p data-bbox="360 662 1060 731">The authors solubility, cm<sup>3</sup> O<sub>2</sub> 100 cm<sup>-3</sup>, appears to be the Ostwald coefficient times 100.</p>		Temperature		Oxygen Solubility		t/°C	T/K	g O <sub>2</sub> 1000 g <sup>-1</sup>	cm <sup>3</sup> O <sub>2</sub> 100 cm <sup>-3</sup>	25	298.15	0.285	41.5	37	310.15	0.271	40.7
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<b>METHOD/APPARATUS/PROCEDURE:</b> The equilibrium apparatus is a 50 cm <sup>3</sup> three neck flask equipped with a water condenser, a thermometer, and a gas dispersing tube extending below the fluid surface level. Between 25 and 35 cm <sup>3</sup> of solvent are placed in the flask. Gas is bubbled through the solvent for 2 - 3 h. An 80 micro-liter sample is slowly taken into a gas tight syringe. The sample is injected into a gas chromatograph. The results of three sampling and analyses are averaged.  The chromatograph is an F and M Model 720 equipped with a thermal conductivity detector at 320 °C, and a 6' by ¼" stainless steel column packed with 13X molecular sieve at room temperature. The apparatus is calibrated with pure gas samples.  Details of the procedure were furnished by R. D. Danielson of the 3 M Co.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. Source not given. Commercial cylinder. (2) L-1822. Minnesota Mining and Manufacturing Co. All H in an organic compound are replaced by F by Simons electrochemical process (1).  <b>ESTIMATED ERROR:</b> δT/K = 0.1 δc/c = 0.01 (reproducibility) = 0.05 (absolute)  <b>REFERENCES:</b> 1. Simons, J. H., Editor <i>Fluorine Chemistry</i> Academic Press, New York, <u>1950</u> .																

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Surfactants (see below) (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Kousaka, K.; Kise, H.; Seno, M. <i>Yukagaku</i> <u>1980</u> , 29, 177-80.																																															
<b>VARIABLES:</b> T/K = 298 Concentration	<b>PREPARED BY:</b> R. Battino																																															
<b>EXPERIMENTAL VALUES:</b> 25°C (298K) <table border="1" data-bbox="177 470 1112 754" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th rowspan="2">Surfactant<sup>a</sup></th> <th colspan="5">Relative concentration (S/S<sub>0</sub>)<sup>b</sup> of oxygen in surfactant at indicated concentration</th> </tr> <tr> <th>0.2M<sup>c</sup></th> <th>0.4M</th> <th>0.6M</th> <th>0.8M</th> <th>1.0M</th> </tr> </thead> <tbody> <tr> <td>Sodium acetate</td> <td>0.871</td> <td>0.798</td> <td>0.787</td> <td>0.747</td> <td>0.716</td> </tr> <tr> <td>Sodium propionate</td> <td>0.897</td> <td>0.860</td> <td>0.797</td> <td>0.765</td> <td>0.708</td> </tr> <tr> <td>Sodium butyrate</td> <td>0.881</td> <td>0.846</td> <td>0.834</td> <td>0.780</td> <td>0.730</td> </tr> <tr> <td>Sodium pentanoate</td> <td>0.887</td> <td>0.846</td> <td>0.838</td> <td>0.784</td> <td>0.735</td> </tr> <tr> <td>Sodium hexanoate</td> <td>0.900</td> <td>0.860</td> <td>0.840</td> <td>0.793</td> <td>0.735</td> </tr> <tr> <td>Sodium octanoate</td> <td>0.916</td> <td>0.936</td> <td>0.983</td> <td>0.990</td> <td>-</td> </tr> </tbody> </table> <p data-bbox="177 793 480 940"> <sup>a</sup> Sodium acetate;            Sodium propionate;            Sodium butyrate;            Sodium pentanoate;            Sodium hexanoate;            Sodium octanoate;         </p> <p data-bbox="177 950 1177 1009"> <sup>b</sup> Relative solubilities. S is in the solution and S<sub>0</sub> is in the pure solvent. Solubilities are on a weight basis.         </p> <p data-bbox="177 1019 1033 1058"> <sup>c</sup> Concentrations are in units of mol dm<sup>-3</sup>, i.e., molarity.         </p>		Surfactant <sup>a</sup>	Relative concentration (S/S <sub>0</sub> ) <sup>b</sup> of oxygen in surfactant at indicated concentration					0.2M <sup>c</sup>	0.4M	0.6M	0.8M	1.0M	Sodium acetate	0.871	0.798	0.787	0.747	0.716	Sodium propionate	0.897	0.860	0.797	0.765	0.708	Sodium butyrate	0.881	0.846	0.834	0.780	0.730	Sodium pentanoate	0.887	0.846	0.838	0.784	0.735	Sodium hexanoate	0.900	0.860	0.840	0.793	0.735	Sodium octanoate	0.916	0.936	0.983	0.990	-
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<b>METHOD/APPARATUS/PROCEDURE:</b> Solubilities determined by a gas chromatographic method which yielded ratios of solubilities in the aqueous surfactant solutions to that in pure water.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given. <table border="1" data-bbox="672 1544 1226 1675" style="width: 100%; border-collapse: collapse;"> <tbody> <tr> <td> <b>ESTIMATED ERROR:</b>  <math>\delta(S/S_0)' / (S/S_0)' = \pm 0.03</math>, compiler's estimate               </td> </tr> <tr> <td> <b>REFERENCES:</b> </td> </tr> </tbody> </table>	<b>ESTIMATED ERROR:</b> $\delta(S/S_0)' / (S/S_0)' = \pm 0.03$ , compiler's estimate	<b>REFERENCES:</b>																																													
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<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> : [7782-44-7] (2) Various solvents (see table below.)	<b>ORIGINAL MEASUREMENTS:</b> Sinn, E.; Mattes, K.; Naumann, E. <i>Wiss. Z. Friedrich-Schiller-Univ. Jena, Math.-Naturwiss. Reihe</i> <u>1967</u> , 16, 523-9.																																																	
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<table border="1"> <thead> <tr> <th data-bbox="202 485 306 512">Solvent</th> <th data-bbox="817 485 847 512">L<sup>a</sup></th> <th data-bbox="961 485 992 512">ℓ<sup>b</sup></th> </tr> </thead> <tbody> <tr> <td colspan="3" data-bbox="494 558 668 586" style="text-align: center;">20°C (293 K)</td> </tr> <tr> <td data-bbox="202 608 615 636">n-pentane; C<sub>5</sub>H<sub>12</sub>; [109-66-0]</td> <td data-bbox="790 608 860 632">0.507</td> <td data-bbox="948 608 1018 632">0.212</td> </tr> <tr> <td data-bbox="202 644 586 671">n-hexane; C<sub>6</sub>H<sub>14</sub>; [110-54-3]</td> <td data-bbox="790 644 860 667">0.495</td> <td data-bbox="948 644 1018 667">0.386</td> </tr> <tr> <td data-bbox="202 679 600 707">n-heptane; C<sub>7</sub>H<sub>16</sub>; [142-82-5]</td> <td data-bbox="790 679 860 703">0.390</td> <td data-bbox="948 679 1018 703">0.346</td> </tr> <tr> <td data-bbox="202 715 586 743">n-octane; C<sub>8</sub>H<sub>18</sub>; [111-65-9]</td> <td data-bbox="790 715 860 739">0.348</td> <td data-bbox="948 715 1018 739">0.320</td> </tr> <tr> <td data-bbox="202 751 586 779">n-nonane; C<sub>9</sub>H<sub>20</sub>; [111-84-2]</td> <td data-bbox="790 751 860 775">0.331</td> <td data-bbox="948 751 1018 775">0.307</td> </tr> <tr> <td data-bbox="202 787 725 815">dichloromethane; CH<sub>2</sub>Cl<sub>2</sub>; [3474-12-2]</td> <td data-bbox="790 787 860 811">0.257</td> <td data-bbox="948 787 1018 811">0.130</td> </tr> <tr> <td data-bbox="202 823 692 850">trichloromethane; CHCl<sub>3</sub>; [67-66-3]</td> <td data-bbox="790 823 860 846">0.278</td> <td data-bbox="948 823 1018 846">0.204</td> </tr> <tr> <td data-bbox="202 858 705 886">tetrachloromethane; CCl<sub>4</sub>; [56-23-5]</td> <td data-bbox="790 858 860 882">0.331</td> <td data-bbox="948 858 1018 882">0.271</td> </tr> <tr> <td data-bbox="202 894 777 922">1,2-dichloroethane; C<sub>2</sub>H<sub>4</sub>Cl<sub>2</sub>; [1300-21-6]</td> <td data-bbox="790 894 860 918">0.178</td> <td data-bbox="948 894 1018 918">0.153</td> </tr> <tr> <td data-bbox="202 930 692 958">trichloroethylene; C<sub>2</sub>HCl<sub>3</sub>; [79-01-6]</td> <td data-bbox="790 930 860 954">0.292</td> <td data-bbox="948 930 1018 954">0.252</td> </tr> <tr> <td data-bbox="202 966 744 994">tetrachloroethylene; C<sub>2</sub>Cl<sub>4</sub>; [127-18-4]</td> <td data-bbox="790 966 860 990">0.264</td> <td data-bbox="948 966 1018 990">0.241</td> </tr> <tr> <td data-bbox="202 1001 751 1057">1,1,2-trifluoro-1,2,2-trichloroethane; C<sub>2</sub>Cl<sub>3</sub>F<sub>3</sub>; [76-13-1]</td> <td data-bbox="790 1001 860 1025">0.602</td> <td data-bbox="948 1001 1018 1025">0.359</td> </tr> <tr> <td data-bbox="202 1065 567 1093">methanol; CH<sub>4</sub>O; [67-56-1]</td> <td data-bbox="790 1065 860 1089">0.231</td> <td data-bbox="948 1065 1018 1089">0.188</td> </tr> <tr> <td data-bbox="202 1101 567 1129">ethanol; C<sub>2</sub>H<sub>6</sub>O; [64-17-5]</td> <td data-bbox="790 1101 860 1125">0.195</td> <td data-bbox="948 1101 1018 1125">0.171</td> </tr> </tbody> </table>	Solvent	L <sup>a</sup>	ℓ <sup>b</sup>	20°C (293 K)			n-pentane; C <sub>5</sub> H <sub>12</sub> ; [109-66-0]	0.507	0.212	n-hexane; C <sub>6</sub> H <sub>14</sub> ; [110-54-3]	0.495	0.386	n-heptane; C <sub>7</sub> H <sub>16</sub> ; [142-82-5]	0.390	0.346	n-octane; C <sub>8</sub> H <sub>18</sub> ; [111-65-9]	0.348	0.320	n-nonane; C <sub>9</sub> H <sub>20</sub> ; [111-84-2]	0.331	0.307	dichloromethane; CH <sub>2</sub> Cl <sub>2</sub> ; [3474-12-2]	0.257	0.130	trichloromethane; CHCl <sub>3</sub> ; [67-66-3]	0.278	0.204	tetrachloromethane; CCl <sub>4</sub> ; [56-23-5]	0.331	0.271	1,2-dichloroethane; C <sub>2</sub> H <sub>4</sub> Cl <sub>2</sub> ; [1300-21-6]	0.178	0.153	trichloroethylene; C <sub>2</sub> HCl <sub>3</sub> ; [79-01-6]	0.292	0.252	tetrachloroethylene; C <sub>2</sub> Cl <sub>4</sub> ; [127-18-4]	0.264	0.241	1,1,2-trifluoro-1,2,2-trichloroethane; C <sub>2</sub> Cl <sub>3</sub> F <sub>3</sub> ; [76-13-1]	0.602	0.359	methanol; CH <sub>4</sub> O; [67-56-1]	0.231	0.188	ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	0.195	0.171	<p style="text-align: right;">continued on following page</p>	
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tetrachloromethane; CCl <sub>4</sub> ; [56-23-5]	0.331	0.271																																																
1,2-dichloroethane; C <sub>2</sub> H <sub>4</sub> Cl <sub>2</sub> ; [1300-21-6]	0.178	0.153																																																
trichloroethylene; C <sub>2</sub> HCl <sub>3</sub> ; [79-01-6]	0.292	0.252																																																
tetrachloroethylene; C <sub>2</sub> Cl <sub>4</sub> ; [127-18-4]	0.264	0.241																																																
1,1,2-trifluoro-1,2,2-trichloroethane; C <sub>2</sub> Cl <sub>3</sub> F <sub>3</sub> ; [76-13-1]	0.602	0.359																																																
methanol; CH <sub>4</sub> O; [67-56-1]	0.231	0.188																																																
ethanol; C <sub>2</sub> H <sub>6</sub> O; [64-17-5]	0.195	0.171																																																
<b>AUXILIARY INFORMATION</b>																																																		
<b>METHOD/APPARATUS/PROCEDURE:</b> The various solvents were saturated with oxygen and the amount of dissolved oxygen was determined electrochemically using a Clark electrode. Details and drawings are given in the original paper.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.																																																	
	<b>ESTIMATED ERROR:</b> δL/L = ±0.05, compiler's estimate.																																																	
	<b>REFERENCES:</b>																																																	

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Various solvents (see table below.)	EVALUATOR: Sinn, E.; Matthes, K.; Naumann, E. <i>Wiss. Z. Friedrich-Schiller-Univ. Jena, Math.-Naturwiss. Reihe</i> <u>1967</u> , 16, 523-9.
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 CRITICAL EVALUATION: continued

Solvent	L <sup>a</sup>	ℓ <sup>b</sup>
1-propanol; C <sub>3</sub> H <sub>8</sub> O; [540-67-0]	0.206	0.188
1-butanol; C <sub>4</sub> H <sub>10</sub> O; [71-36-3]	0.199	0.185
1-pentanol; C <sub>5</sub> H <sub>12</sub> O; [71-41-0]	0.203	0.189
1-heptanol; C <sub>7</sub> H <sub>16</sub> O; [111-70-6]	0.185	0.172
1-octanol; C <sub>8</sub> H <sub>18</sub> O; [111-87-5]	0.183	0.170
1-nonanol; C <sub>9</sub> H <sub>20</sub> O; [143-08-8]	0.173	0.161
1-decanol; C <sub>10</sub> H <sub>22</sub> O; [112-30-1]	0.161	0.150
ethylene glycol; C <sub>2</sub> H <sub>6</sub> O <sub>2</sub> ; [107-21-1]	0.031	0.029
2,4,6-trimethoxy-1,3,5-trioxane (paraldehyde); C <sub>12</sub> H <sub>12</sub> O <sub>3</sub> ; [123-63-7]	0.206	0.190
acetone; C <sub>3</sub> H <sub>6</sub> O; [67-64-1]	0.313	0.221
methylethyl ketone; C <sub>4</sub> H <sub>8</sub> O; [78-93-3]	0.314	0.263
diethyl ketone; C <sub>5</sub> H <sub>10</sub> O; [96-22-0]	0.293	0.268
methylpropyl ketone; C <sub>5</sub> H <sub>10</sub> O; [107-87-9]	0.290	0.266
formic acid (85%); CH <sub>2</sub> O <sub>2</sub> ; [64-18-6]	0.062	0.055
acetic acid; C <sub>2</sub> H <sub>4</sub> O <sub>2</sub> ; [64-19-7]	0.195	0.179
propionic acid; C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> ; [79-09-4]	0.277	0.257
n-propylamine; C <sub>3</sub> H <sub>9</sub> N; [107-10-8]	0.242	0.159
n-butylamine; C <sub>4</sub> H <sub>11</sub> N; [109-73-9]	0.272	0.216
methyl formate; C <sub>2</sub> H <sub>4</sub> O <sub>2</sub> ; [107-31-3]	0.303	0.106
ethyl formate; C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> ; [109-94-4]	0.355	0.247
n-octyl formate; C <sub>9</sub> H <sub>18</sub> O <sub>2</sub> ; [112-32-3]	0.240	0.223
methyl acetate; C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> ; [79-20-9]	0.276	0.200
ethyl acetate; C <sub>4</sub> H <sub>8</sub> O <sub>2</sub> ; [141-78-6]	0.314	0.265
n-propyl acetate; C <sub>5</sub> H <sub>10</sub> O <sub>2</sub> ; [109-60-4]	0.318	0.286
n-butyl acetate; C <sub>6</sub> H <sub>12</sub> O <sub>2</sub> ; [123-86-4]	0.302	0.277
diethyl ether; C <sub>4</sub> H <sub>10</sub> O; [60-29-7]	0.485	0.191
ethane, 1,1-oxybis[2-ethoxy]-(diethylene glycol diethyl ether); C <sub>8</sub> H <sub>18</sub> O <sub>3</sub> ; [112-36-7]	0.205	0.191
butane, 1,1'-[oxybis(2,1-ethanedioxy)bis- (diethylene glycol di-n-butyl ether)]; C <sub>12</sub> H <sub>26</sub> O <sub>3</sub> ; [112-73-2]	0.204	0.190
1,4-dioxane; C <sub>4</sub> H <sub>8</sub> O <sub>2</sub> ; [123-91-1]	0.172	0.155
dibenzyl ether; C <sub>14</sub> H <sub>14</sub> O; [103-50-4]	0.086	0.080
benzene; C <sub>6</sub> H <sub>6</sub> ; [71-43-2]	0.249	0.209
toluene; C <sub>7</sub> H <sub>8</sub> ; [108-88-3]	0.221	0.195
p-xylene; C <sub>8</sub> H <sub>10</sub> ; [106-42-3]	0.258	0.235
ethyl benzene; C <sub>8</sub> H <sub>10</sub> ; [100-41-4]	0.219	0.199
chlorobenzene; C <sub>6</sub> H <sub>5</sub> Cl; [108-90-7]	0.214	0.197
bromobenzene; C <sub>6</sub> H <sub>5</sub> Br; [108-86-1]	0.143	0.132
iodobenzene; C <sub>6</sub> H <sub>5</sub> I; [591-50-4]	0.110	0.103

continued on following page

COMPONENTS:  (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) Various solvents (see table below).	EVALUATOR:  Sinn, E.; Matthes, K.; Naumann, E.  <i>Wiss. Z. Friedrich-Schiller-Univ. Jena, Math.-Naturwiss. Reihe</i> <u>1967, 16, 523-9.</u>
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## CRITICAL EVALUATION:

continued

Solvent	L <sup>a</sup>	ℓ <sup>b</sup>
nitrobenzene; C <sub>6</sub> H <sub>5</sub> NO <sub>2</sub> ; [98-95-3]	0.113	0.106
aniline; C <sub>6</sub> H <sub>7</sub> N; [62-53-3]	0.070	0.065

<sup>a</sup> Ostwald coefficient. All measurements at 20°C (293K).

<sup>b</sup> Solubility coefficient defined as  $\ell = L \frac{273}{T/K} \frac{760 - P/\text{mm Hg}}{760}$ .

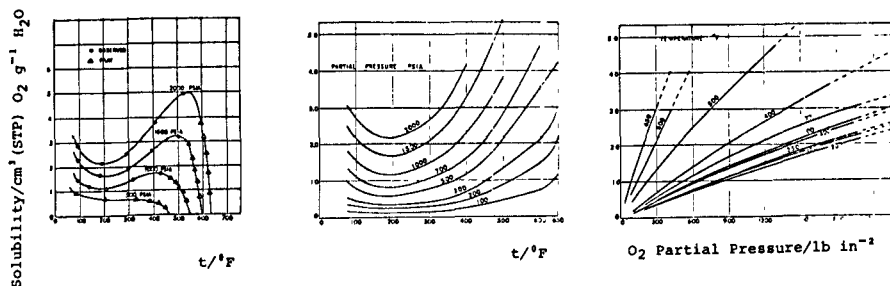
The term P/mm Hg is the saturation vapor pressure of the solvent at 293K. Vapor pressures are given in the original paper as well as temperature dependent data as graphs for tetrachloromethane, methanol, methylpropyl ketone, and water.

OXYGEN SOLUBILITIES ABOVE 200 kPa  
(2 BAR)

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Zoss, L. M. Ph.D. thesis, 1952 Purdue University
<b>VARIABLES:</b> T/K= 273.15 - 604.8 Total P/kPa= 3450 - 13,790	<b>PREPARED BY:</b> H. L. Clever

**EXPERIMENTAL VALUES:**

Later work by O. G. McKee, Jr, Ph. D. thesis, 1953, Purdue University shows that the 273.15 K (32 F) solubility values of Zoss are more than an order of magnitude too high. The solubility values at the higher temperatures appear to be reliable.



The figure above was constructed by Zoss, Suciu, and Sibbitt (1, 2).

The solubility values are from their own work, and from Pray, H. A.; Schweichert, C. E.; Minnich, B. H. Battelle Memorial Institute Report BMI-T-25, May 1950; *Ind. Eng. Chem.* 1952, 44, 1146 - 1151.

continued on following page

**AUXILIARY INFORMATION****METHOD/APPARATUS/PROCEDURE:**

The apparatus (1, 2) consists of a high pressure vessel with integral vapor and liquid sample chambers, heaters, temperature controls, auxiliary pumps, and analytical equipment.

The sequence of operations was: (a) the pressure vessel was evacuated, (b) charged with a known volume of water (about 175 cm<sup>3</sup>), (c) brought to a selected temperature level, (d) charged with gas (under conditions of constant total pressure, constant temperature, and continual agitation) until phase equilibrium was reached, (e) fastened in a vertical position until the vapor and liquid phases separated.

The vapor and liquid phase sample chambers were isolated. The vapor was analysed through a drying train and wet test meter. The liquid phase was analysed at room temperature and pressure in a buret system.

**SOURCE AND PURITY OF MATERIALS:**

- (1) Oxygen. Commercial source. Stated to be 99.9<sup>+</sup> per cent pure.
- (2) Water. Distilled water, boiled three hours and cooled. Tested for pH and for oxygen content (polarography).

**ESTIMATED ERROR:**

$$\begin{aligned} \delta t/^{\circ}\text{F} &= 0.5 \\ \delta P/\text{lb in} &= 3 \\ \delta S/S &= 0.03 \end{aligned}$$

**REFERENCES:**

1. Zoss, L. M.; Suciu, S.; Sibbitt, W. L. *Trans. ASME* 1954, 76, 69 - 71.
2. Zoss, L.M.; Suciu, S.; Sibbitt, W.L. Paper No. 53-S30, American Society of Mechanical Engineers Meeting, Columbus, OH, Apr 1953.

COMPONENTS:		ORIGINAL MEASUREMENTS:				
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Zoss, L. M.				
(2) Water; H <sub>2</sub> O; [7732-18-5]		Ph.D. Thesis, 1952 Purdue University				
EXPERIMENTAL VALUES:		continued				
Temperature		Pressure		Vapor Composition		
t/°F	T/K	p/lb in <sup>-2</sup>	S/cm <sup>3</sup> (STP) g <sup>-1</sup>	C <sub>H<sub>2</sub>O</sub> /mol dm <sup>-3</sup>	mol Fraction x <sub>H<sub>2</sub>O</sub>	
32	273.15	500 (34.0 atm, 3450 kPa)	2.90 1.29 2.55 0.95 <sup>1</sup> 0.72 <sup>1</sup> 0.65 <sup>1</sup> 0.57 <sup>1</sup> 0.50 <sup>1</sup> 0.30 <sup>1</sup>			
80	299.8					
200	366.5					
328	437.6					
382	467.6					
417	487.0					
445	502.6					
32	273.15	1000 (68.0 atm, 6895 kPa)	11.43 6.85 2.92 1.49 1.21 1.13 1.13 1.46 1.70 1.50 <sup>1</sup> 1.30 <sup>1</sup> 1.15 <sup>1</sup> 0.94 <sup>1</sup> 0.54 <sup>1</sup>	0.0145	0.137	
93	307.0					
138	332.0					
181	355.9			0.0139	0.133	
202	367.6					
206	369.8					0.203
313	429.3			0.139	0.594	
316	430.9					
421	489.3			0.687	0.882	
422	489.8					
467	514.8					
486	525.4					
503	534.8					
518	543.15					
532	550.9					
32	273.15	1500 (102.1 atm, 10,340 kPa)	57.7 50.8 2.30 1.68 1.90 2.62 3.20 2.90 <sup>1</sup> 2.30 <sup>1</sup> 1.85 <sup>1</sup> 1.32 <sup>1</sup> 0.73 <sup>1</sup>	0.0556	0.273	
90	305.4					
184	357.6					
189	360.4			0.0440	0.248	
292	417.6			0.117	0.427	
295	419.3					
390	472.0			0.323	0.731	
392	473.15					
503	534.8			1.037	0.917	
545	558.15					
556	564.3					
567	570.4					
577	575.9					
587	581.5					
32	273.15	2000 (136.1 atm, 13,790 kPa)	134. 111. 108. 2.89 2.19 2.54 3.82 4.96 3.75 <sup>1</sup> 3.20 <sup>1</sup> 2.50 <sup>1</sup> 1.70 <sup>1</sup> 0.90 <sup>1</sup>	0.0367	0.155	
88	304.3					
185	358.15			0.0166	0.090	
187	359.3					
285	413.7			0.0980	0.338	
287	414.8					
406	480.9					
413	484.8			0.550	0.719	
523	545.9					
526	547.6			1.830	0.910	
596	586.5					
605	591.5					
613	595.9					
621	600.4					
629	604.8					

COMPONENTS:		ORIGINAL MEASUREMENTS:
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Pray, H. A.; Schweichert, C. E.; Minnich, B. H.
(2) Water; H <sub>2</sub> O; [7732-18-5]		<i>Ind. Eng. Chem.</i> <u>1952</u> , 44, 1147-51.
VARIABLES:		PREPARED BY:
T/K = 436-617 P/bar = 7-28		C. L. Young
EXPERIMENTAL VALUES:		
T/K	P/bar	10 <sup>3</sup> Mole fraction of oxygen in water, $x_{O_2}$
435.9	6.89	0.11
	13.8	0.22
	20.7	0.33
477.6	6.89	0.13
	10.3	0.20
533.1	6.89	0.46
	13.8	0.65
	20.7	0.96
	27.6	1.22
588.7	6.89	0.45
	13.8	1.01
	20.7	1.56
616.5	7.17	0.87
	12.1	1.32
	14.1	1.63
	19.3	2.11
	19.9	1.83
	21.3	2.13
AUXILIARY INFORMATION		
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:
Rocking equilibrium cell of 3 l capacity. Pressure measured with dead weight gauge and temperature measured using chromel-alumel thermocouple. Cell contents equilibrated and liquid sample removed. The amount of dissolved gas estimated volumetrically.		No details given.
		ESTIMATED ERROR:
		$\delta T/K = \pm 1$ ; $\delta P/\text{bar} = \pm 1$ ; $\delta x_{O_2} \approx 1-5\%$ (estimated by compiler).
		REFERENCES:

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]				Pray, H.A.; Stephan, E.F. <i>U. S. Atomic Energy Commission</i> <u>1953</u> , BMI-840.			
VARIABLES:				PREPARED BY:			
T/K = 373 - 436 P/MPa = 1.34 - 9.93				R. Battino			
EXPERIMENTAL VALUES:							
P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> /MPa	S <sup>b</sup>	10 <sup>4</sup> x <sub>1</sub> <sup>a,c</sup>	P <sub>O<sub>2</sub></sub> /psia	P <sub>O<sub>2</sub></sub> <sup>a</sup> /MPa	S <sup>b</sup>	10 <sup>4</sup> x <sub>1</sub> <sup>a,c</sup>
212°F (373K)				275°F (408K)			
332	2.29	0.380	3.06	510	3.52	0.655	5.04
355	2.45	0.435	3.50	525	3.62	0.645	4.97
374	2.58	0.465	3.74	555	3.83	0.685	5.28
453	3.12	0.550	4.42	590	4.07	0.73	5.62
489	3.37	0.570	4.59	1090	7.51	1.42	10.94
500	3.45	0.650	5.23	1145	7.89	1.45	11.17
526	3.63	0.665	5.35	1173	8.09	1.51	11.63
671	4.63	0.870	7.00	1180	8.13	1.60	12.32
808	5.57	0.995	8.00	1195	8.24	1.60	12.32
887	6.11	1.130	9.09	1215	8.38	1.55	11.94
933	6.43	1.180	9.49				
1292	8.91	1.600	12.87	325°F (436K)			
1335	9.20	1.600	12.87	195	1.34	0.303	2.44
1410	9.72	1.820	14.64	195	1.34	0.306	2.46
				195	1.34	0.314	2.53
				530	3.65	0.830	6.68
				560	3.86	0.880	7.08
				600	4.14	0.905	7.28
				950	6.55	1.41	11.34
				950	6.55	1.42	11.42
				960	6.62	1.51	12.15
continued on following page							
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
A sample of saturated solution is withdrawn from a stainless steel pressurized and thermostatted autoclave and analyzed for the dissolved gas content. Details and a drawing are given in the paper.				No details given.			
				ESTIMATED ERROR:			
				δS/S = ±0.03, compiler's estimate.			
				REFERENCES:			



## COMPONENTS:

- (1) Oxygen; O<sub>2</sub>; [7782-44-7]  
 (2) Water; H<sub>2</sub>O; [7732-18-5]

## ORIGINAL MEASUREMENTS:

Pray, H.A.; Stephan, E.F.  
 U. S. Atomic Energy Commission  
 1953, BMI-840.

continued

$P_{O_2}$ /psia	$P_{O_2}^a$ /MPa	$S^b$	$10^4 x_1^{a,c}$
1410	9.72	2.12	17.06
1440	9.93	2.28	18.34

a Calculated by compiler.

b Solubility in units of ml O<sub>2</sub>(STP)/g of water.

c Mole fraction solubility at partial pressure of oxygen indicated. Henry's constants are: 373K, 6897(±240)MPa/mole fraction; 408K, 6995 (±232)MPa/mole fraction; 436K, 5537(±158)MPa/mole fraction (all calculated by compiler).

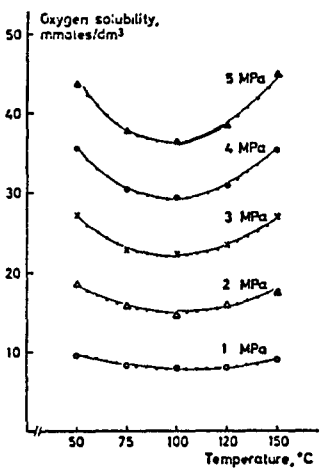
<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> McKee, O. L. Jr. Ph.D. thesis, 1953 Purdue University																							
<b>VARIABLES:</b> T/K= 273.15 Total P/kPa= 3450 - 20,680	<b>PREPARED BY:</b> H. L. Clever																							
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="268 467 907 974"> <thead> <tr> <th>Temperature t/°F</th> <th>T/K</th> <th>Total Pressure P/lb in<sup>-2</sup></th> <th>Oxygen Solubility S/cm<sup>3</sup> (STP) g<sup>-1</sup></th> </tr> </thead> <tbody> <tr> <td rowspan="12">32</td> <td rowspan="12">273.15</td> <td rowspan="4">500</td> <td>1.38</td> </tr> <tr> <td>1.48</td> </tr> <tr> <td>1.56</td> </tr> <tr> <td>1.60</td> </tr> <tr> <td rowspan="2">1000</td> <td>2.74</td> </tr> <tr> <td>2.80</td> </tr> <tr> <td rowspan="2">1500</td> <td>3.93</td> </tr> <tr> <td>3.92</td> </tr> <tr> <td rowspan="2">2000</td> <td>5.01</td> </tr> <tr> <td>4.93</td> </tr> <tr> <td rowspan="2">3000</td> <td>6.34</td> </tr> <tr> <td>6.39</td> </tr> </tbody> </table> <p data-bbox="262 994 907 1063">The author calculated the maximum error to range from 3.5 per cent at a solubility of 1.5 to 1.5 per cent for a solubility of 6.3.</p> <p data-bbox="262 1093 920 1162">The work was carried out in the Department of Mechanical Engineering under the direction of W. L. Sibbitt.</p>		Temperature t/°F	T/K	Total Pressure P/lb in <sup>-2</sup>	Oxygen Solubility S/cm <sup>3</sup> (STP) g <sup>-1</sup>	32	273.15	500	1.38	1.48	1.56	1.60	1000	2.74	2.80	1500	3.93	3.92	2000	5.01	4.93	3000	6.34	6.39
Temperature t/°F	T/K	Total Pressure P/lb in <sup>-2</sup>	Oxygen Solubility S/cm <sup>3</sup> (STP) g <sup>-1</sup>																					
32	273.15	500	1.38																					
			1.48																					
			1.56																					
			1.60																					
		1000	2.74																					
			2.80																					
		1500	3.93																					
			3.92																					
		2000	5.01																					
			4.93																					
		3000	6.34																					
			6.39																					
<b>AUXILIARY INFORMATION</b>																								
<b>METHOD/APPARATUS/PROCEDURE:</b> The apparatus of Zoss (1) with modifications to improve the temperature control at 32 °F, and to improve the sampling of the liquid phase sample.  Total Pressure: <table border="1" data-bbox="100 1640 517 1819"> <thead> <tr> <th>P/lb in<sup>-2</sup></th> <th>P/atm</th> <th>P/kPa</th> </tr> </thead> <tbody> <tr> <td>500</td> <td>34.0</td> <td>3450</td> </tr> <tr> <td>1000</td> <td>68.0</td> <td>6895</td> </tr> <tr> <td>1500</td> <td>102.1</td> <td>10340</td> </tr> <tr> <td>2000</td> <td>136.1</td> <td>13790</td> </tr> <tr> <td>3000</td> <td>204.1</td> <td>20680</td> </tr> </tbody> </table>	P/lb in <sup>-2</sup>	P/atm	P/kPa	500	34.0	3450	1000	68.0	6895	1500	102.1	10340	2000	136.1	13790	3000	204.1	20680	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Oxygen. No information given. (2) Water. Distilled water, boiled for three hours before use.  <b>ESTIMATED ERROR:</b> See comment under table above.  <b>REFERENCES:</b> 1. Zoss, L. M. Ph. D. thesis, 1952 Purdue University					
P/lb in <sup>-2</sup>	P/atm	P/kPa																						
500	34.0	3450																						
1000	68.0	6895																						
1500	102.1	10340																						
2000	136.1	13790																						
3000	204.1	20680																						

COMPONENTS:			ORIGINAL MEASUREMENTS:		
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]			Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H.		
(2) Water; H <sub>2</sub> O; [7732-18-5]			<i>Battelle Memorial Institute Report</i> BMI-1067, <u>1956</u> .		
VARIABLES:			PREPARED BY:		
T/K = 373-561 P/bar = 14-200			C. L. Young		
EXPERIMENTAL VALUES:					
T/K	P <sup>†</sup> /bar	Mole fraction of oxygen in liquid, x <sub>O<sub>2</sub></sub>	T/K	P <sup>†</sup> /bar	Mole fraction of oxygen in liquid, x <sub>O<sub>2</sub></sub>
373.15	19.7	0.000301	408.15	14.1	0.000233
	22.9	0.000306		14.8	0.000265
	24.5	0.000350		35.2	0.000527
	25.8	0.000374		36.2	0.000519
	31.2	0.000442		38.3	0.000551
	33.7	0.000458		40.0	0.000587
	34.5	0.000523		75.2	0.00114
	36.3	0.000535		77.6	0.00125
	36.9	0.000547		78.9	0.00116
	46.3	0.000699		80.9	0.00121
	55.7	0.000800		81.4	0.00129
	61.2	0.000908		100.6	0.00157
	64.3	0.000948		103.0	0.00161
	89.1	0.00129		105.1	0.00161
	92.0	0.00129		120.2	0.00176
	97.6	0.00130		122.3	0.00178
	117.6	0.00167		123.7	0.00178
	121.7	0.00165		133.0	0.00189
	147.2	0.00197		138.2	0.00197
	149.3	0.00199		144.4	0.00201
	156.9	0.00200		145.1	0.00204
	161.0	0.00201		147.1	0.00213
	192.0	0.00221		148.5	0.00205
	201.7	0.00231			
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:		
Gas and liquid equilibrated for 18 hours. Pressure measured with Bourdon gauge and temperature measured with thermocouple. Composition of liquid estimated by volumetric method. Details in source. Partial pressure estimated by subtracting vapor pressure from total pressure.			No details given.		
			ESTIMATED ERROR:		
			δT/K = ±0.6; δP/bar = ±0.3; δx <sub>O<sub>2</sub></sub> = ±0.00002 (estimated by compiler)		
			REFERENCES:		

<b>COMPONENTS:</b> (1) Oxygen; O <sub>2</sub> ; [7782-44-7] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Stephan, E. L.; Hatfield, N. S.; Peoples, R. S.; Pray, H. A. H. <i>Battelle Memorial Institute Report</i> <i>BMI-1067, 1956.</i>
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EXPERIMENTAL VALUES: <span style="float: right;">continued</span>					
T/K	P <sup>†</sup> /bar	Mole fraction of oxygen in liquid, x <sub>O<sub>2</sub></sub>	T/K	P <sup>†</sup> /bar	Mole fraction of oxygen in liquid, x <sub>O<sub>2</sub></sub>
408.15	152.0	0.00213	477.59	58.8	0.00135
	155.4	0.00217		80.9	0.00193
	158.2	0.00218		85.7	0.00216
	162.0	0.00225		128.1	0.00319
	172.6	0.00233		133.3	0.00336
	193.3	0.00246		138.8	0.00341
	196.8	0.00250		158.1	0.00353
	199.6	0.00255		167.7	0.00399
435.93	13.4	0.000244		176.0	0.00413
	13.4	0.000246		187.6	0.00424
	13.4	0.000252	533.15	37.9	0.00159
	36.5	0.000667		39.9	0.00169
	38.6	0.000707		39.9	0.00165
	41.4	0.000727		41.3	0.00165
	65.5	0.00113		42.7	0.00165
	65.5	0.00114		58.5	0.00252
	66.2	0.00121		60.6	0.00263
	97.2	0.00170		70.3	0.00319
	99.3	0.00183		74.4	0.00317
	132.7	0.00233		77.2	0.00329
	138.2	0.00230		77.8	0.00329
	156.1	0.00250		79.9	0.00325
	163.0	0.00263		88.0	0.00369
	171.3	0.00270		92.3	0.00390
	179.5	0.00271		128.2	0.00536
	192.0	0.00294		132.3	0.00578
	198.8	0.00293		136.4	0.00568
477.59	17.4	0.000490		137.8	0.00584
	18.8	0.000498	560.93	31.4	0.00181
	19.5	0.000514		33.4	0.00195
	35.4	0.000892		63.1	0.00385
	36.7	0.000924		66.5	0.00395
	37.4	0.000988		98.9	0.00612
	56.7	0.00133		100.3	0.00619
	58.1	0.00129			

P<sup>†</sup> - partial pressure of oxygen

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Broden, A.; Simonson, R.</p> <p><i>Svensk Papperstidning</i> 1978, 81, 541-4.</p> <p><i>Chem. Abstr.</i> 1979, 90, 1427084.</p>
<p>VARIABLES:</p> <p>T/K = 323-423</p> <p>P/MPa = 1-5</p>	<p>PREPARED BY:</p> <p>R. Battino</p>
<p>EXPERIMENTAL VALUES:</p> <p>Data at the right in Figure 3 from the original paper. The following equation fits the data with a standard deviation of <math>\pm 0.45 \text{ mmol dm}^{-3}</math>. The solubility, <math>[\text{O}_2]</math>, is expressed as <math>\text{mmol dm}^{-3}</math> where the solvent volume is at the pressure and temperature of the measurement.</p> $[\text{O}_2] = 5.351 - 1.252 \times 10^{-2} (T/K) - 79.54 (P/\text{MPa}) + 2.135 \times 10^{-4} (P/\text{MPa}) (T/K)^2 + 2.125 \times 10^4 (P/\text{MPa}) / (T/K)$ <div style="text-align: right;">  </div> <p><i>Fig. 3. Oxygen solubility at different pressure levels versus temperature. The dotted lines included are those corresponding to eq. [1].</i></p>	
<p>AUXILIARY INFORMATION</p>	
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>An autoclave was filled with 2 dm<sup>3</sup> of water. Bubbling oxygen through it served to degas the water and saturate it at the same. At equilibrium, 0.426 cm<sup>3</sup> samples were analyzed for oxygen via a gas chromatograph.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>No details given.</p>
<p>ESTIMATED ERROR:</p> <p><math>\delta P = \pm 0.005 \text{ Ma}</math></p> <p><math>\delta T/K = \pm 0.3</math></p> <p><math>\delta [\text{O}_2]/[\text{O}_2] = \pm 0.01</math>, compiler's estimate</p>	
<p>REFERENCES:</p>	

COMPONENTS:			ORIGINAL MEASUREMENTS:			
(1) Oxygen; $O_2$ ; [7782-44-7]			Krievé, W.F.; Mason, D.M.			
(2) Chlorine; $Cl_2$ ; [7782-50-5]			J. Phys. Chem. <u>1956</u> , 60, 374.			
VARIABLES:			PREPARED BY:			
T/K = 298			R. Battino; C.L. Young			
P/kPa = 529 - 1215						
EXPERIMENTAL VALUES:						
t/°C	T/K	Mol %	$10^2 x_1$	$P_{O_2}/\text{atm}$	$P_{O_2}/\text{kPa}$	
25	298	0.785	0.785	5.22	529	
25	298	0.936	0.936	6.67	676	
25	298	1.31	1.31	9.13	925	
25	298	1.49	1.49	10.53	1067	
25	298	1.65	1.65	11.99	1215	
<p>T/K, <math>x_1</math>, and <math>P_{O_2}/\text{kPa}</math> calculated by compiler. <math>x_1</math> is the mole fraction solubility at the given partial pressure of gas. The data conforms to Raoult's Law with an average deviation of 3.3%.</p>						
AUXILIARY INFORMATION						
METHOD/APPARATUS/PROCEDURE:			SOURCE AND PURITY OF MATERIALS:			
<p>Measurements were carried out using 175 cm<sup>3</sup> stainless steel bombs and calibrated stainless steel bourdon tube gages. A known weight of gas from one bomb is admitted to another containing a known amount of liquid. After equilibrium is established the pressure in the second bomb is determined and the solubility calculated from the pressure and weight measurements.</p>			(1) Matheson Co., Inc.			
			(2) Commercial chlorine purified by fractional distillation to remove air and carbon dioxide.			
			ESTIMATED ERROR:			
			$\delta P/P = \pm 0.005$ (authors).			
			$\delta x_1/x_1 = \pm 0.03$ (compiler).			
			$\delta T = \pm 0.1$ K			
			REFERENCES:			

COMPONENTS: (1) Oxygen; O <sub>2</sub> ; [7782-44-7]  (2) Nitrous oxide; N <sub>2</sub> O; [10024-97-3]				ORIGINAL MEASUREMENTS: Zeininger, H.  <i>Chemie-Ing.-Tech.</i> <u>1972</u> , 44, 607-12.			
VARIABLES:  T/K = 213-293 P/MPa = 0.6-8.2				PREPARED BY:  C. L. Young			
EXPERIMENTAL VALUES:							
T/K	P/10 <sup>5</sup> Pa	Mole fraction of oxygen in liquid, in gas, $x_{O_2}$ $y_{O_2}$		T/K	P/10 <sup>5</sup> Pa	Mole fraction of oxygen in liquid, in gas, $x_{O_2}$ $y_{O_2}$	
213.15	6.1	0.004	0.196	233.15	53.3	0.139	0.756
	8.9	0.009	0.444		58.1	0.110	0.744
	14.7	0.031	0.648		65.5	0.168	0.764
	21.5	0.048	0.779		71.1	0.197	0.805
	31.7	0.086	0.835		72.1	0.205	0.771
	35.6	0.081	0.861		82.9	0.267	0.830
	42.0	0.123	0.871		89.9	0.678	0.787
	47.3	0.143	0.873	253.15	21.7	0.012	0.166
	50.7	0.169	0.879		27.2	0.023	0.306
	59.0	0.194	0.886		31.6	0.039	0.393
	70.4	0.251	0.898		34.2	0.032	0.432
	83.7	0.410	0.883		37.7	0.057	0.478
	87.3	0.526	0.879		45.3	0.086	0.527
	91.3	0.589	0.920		47.9	0.081	0.536
233.15	16.9	0.016	0.371		56.9	0.116	0.588
	22.9	0.036	0.514		60.7	0.126	0.607
	38.2	0.057	0.665		64.8	0.146	0.625
	44.6	0.068	0.689		74.4	0.265	0.663
	49.9	0.125	0.751		82.3	0.418	0.666
	50.8	0.157	0.743				(cont.)
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:  Static equilibrium cell stirred with a steel ball. Samples of gas and liquid phases removed and analysed by mass spectrometry. Care was taken to avoid large changes in pressure during sampling by taking small samples. Details in source.				SOURCE AND PURITY OF MATERIALS:  Nitrous oxide was "pure" as determined by gas chromatography.			
				ESTIMATED ERROR: $\delta T/K = \pm 0.3$ ; $\delta P/10^5 Pa = \pm 0.2$ ; $\delta x_{O_2} = \pm 0.01$ ; $\delta y_{O_2} = \pm 0.012$ (errors in composition greater near critical region).			
				REFERENCES:			

COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Zeininger, H.			
(2) Nitrous oxide; N <sub>2</sub> O; [10024-97-3]				Chem. -Inq.-Tech. <u>1972</u> , 44, 607-12.			
EXPERIMENTAL VALUES:							
T/K	P/10 <sup>5</sup> Pa	Mole fraction of oxygen		T/K	P/10 <sup>5</sup> Pa	Mole fraction of oxygen	
		in liquid, x <sub>O<sub>2</sub></sub>	in gas, y <sub>O<sub>2</sub></sub>			in liquid, x <sub>O<sub>2</sub></sub>	in gas, y <sub>O<sub>2</sub></sub>
273.15	35.5	0.006	0.060	273.15	70.1	-	0.441
	41.0	0.017	-		70.4	0.13	-
	44.6	-	0.225		79.0	-	0.450
	47.1	0.023	0.201		79.6	0.205	0.477
	49.1	0.045	-		81.1	0.203	0.450
	54.7	0.052	0.370	293.15	67.1	0.10	0.155
	59.0	0.091	0.390		71.1	0.059	0.177
	59.3	0.079	0.408		78.0	0.092	0.20
	65.4	0.095	-				



COMPONENTS:				ORIGINAL MEASUREMENTS:			
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]				Zenner, G. H.; Dana, L. I.			
(2) Carbon dioxide; CO <sub>2</sub> ; [124-38-9]				Chem. Eng. Prog. Symp. Ser. <u>1963</u> , 59, No. 44, 36-41.			
VARIABLES:				PREPARED BY:			
T/K = 234-273 P/MPa = 6-15				C. L. Young			
EXPERIMENTAL VALUES:							
T/K	P/MPa	Mole fraction of oxygen in liquid, in vapor,		T/K	P/MPa	Mole fraction of oxygen in liquid, in vapor,	
		x <sub>O<sub>2</sub></sub>	y <sub>O<sub>2</sub></sub>			x <sub>O<sub>2</sub></sub>	y <sub>O<sub>2</sub></sub>
273.15	6.03	0.0801	0.302	232.85	14.87	-	0.544
	6.10	0.063	0.302		14.30	0.497	0.617
	6.02	0.0603	0.298		5.92	0.113	0.774
	5.32	0.0432	0.254		7.28	-	0.770
	6.97	0.0843	0.353		4.92	-	0.749
	8.49	0.1293	0.407		3.79	-	0.716
	9.42	0.160	0.4205		2.66	-	0.553
	10.41	0.1985	0.422		3.85	-	0.671
	11.11	0.237	0.399	218.15	2.19	0.033	0.704
232.85	13.87	0.402	0.763		3.94	0.072	0.812
	12.39	0.331	-		5.91	0.119	0.847
	12.53	0.340	0.720		7.88	0.174	0.853
	11.15	0.276	0.753		9.72	0.234	0.851
	9.46	0.217	0.768		11.82	0.312	0.822
	7.77	0.1645	0.770		13.01	0.382	0.789
	13.49	0.403	0.707		14.02	0.468	0.736
	14.77	0.531	-				
AUXILIARY INFORMATION							
METHOD/APPARATUS/PROCEDURE:				SOURCE AND PURITY OF MATERIALS:			
Static bomb. Pressure measured with dead weight tester. Temperature measured with resistance thermometer. Samples of liquid and gas analysed by removing carbon dioxide from sample with potassium hydroxide solution. Oxygen determined volumetrically.				(1) No details given.			
				(2) Purified - no other details given.			
				ESTIMATED ERROR:			
				$\delta T/K = \pm 0.2$ ; $\delta P/MPa = \pm 0.05$ ; $\delta x_{O_2}, \delta y_{O_2} = \pm 0.002$ (estimated by compiler).			
				REFERENCES:			

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Carbon dioxide; CO<sub>2</sub>; [124-38-9]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Kaminishi, G.; Toriumi, T. Kogyo Kagaku Zasshi <u>1966</u>, 69, 175-8.</p>																																																																																												
<p>VARIABLES:</p> <p>T/K = 233-298</p> <p>P/MPa = 4-13</p>	<p>PREPARED BY:</p> <p>C. L. Young</p>																																																																																												
<p>EXPERIMENTAL VALUES:</p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">T/K</th> <th style="text-align: left;">P/MPa</th> <th style="text-align: center;">Mole fraction of oxygen in liquid, <math>x_{O_2}</math></th> <th style="text-align: center;">in gas, <math>y_{O_2}</math></th> </tr> </thead> <tbody> <tr><td>298.15</td><td>7.42</td><td>0.030</td><td>0.081</td></tr> <tr><td></td><td>7.87</td><td>0.042</td><td>0.088</td></tr> <tr><td></td><td>8.05</td><td>0.049</td><td>0.088</td></tr> <tr><td></td><td>8.22</td><td>0.055</td><td>-</td></tr> <tr><td>288.15</td><td>6.45</td><td>-</td><td>0.132</td></tr> <tr><td></td><td>7.42</td><td>0.062</td><td>0.196</td></tr> <tr><td></td><td>8.05</td><td>0.079</td><td>-</td></tr> <tr><td></td><td>8.84</td><td>0.102</td><td>0.228</td></tr> <tr><td></td><td>9.22</td><td>0.117</td><td>0.236</td></tr> <tr><td>273.15</td><td>5.07</td><td>0.036</td><td>0.220</td></tr> <tr><td></td><td>7.42</td><td>0.096</td><td>0.371</td></tr> <tr><td></td><td>9.63</td><td>0.166</td><td>0.411</td></tr> <tr><td></td><td>10.57</td><td>0.206</td><td>0.408</td></tr> <tr><td></td><td>10.85</td><td>-</td><td>0.405</td></tr> <tr><td></td><td>11.01</td><td>-</td><td>0.404</td></tr> <tr><td></td><td>11.18</td><td>-</td><td>0.397</td></tr> <tr><td>253.15</td><td>3.70</td><td>0.036</td><td>0.383</td></tr> <tr><td></td><td>5.27</td><td>0.072</td><td>0.516</td></tr> <tr><td></td><td>10.18</td><td>0.218</td><td>0.612</td></tr> <tr><td></td><td>12.74</td><td>0.371</td><td>0.564</td></tr> <tr><td>233.15</td><td>5.27</td><td>0.092</td><td>0.722</td></tr> <tr><td></td><td>10.18</td><td>0.242</td><td>0.757</td></tr> </tbody> </table>		T/K	P/MPa	Mole fraction of oxygen in liquid, $x_{O_2}$	in gas, $y_{O_2}$	298.15	7.42	0.030	0.081		7.87	0.042	0.088		8.05	0.049	0.088		8.22	0.055	-	288.15	6.45	-	0.132		7.42	0.062	0.196		8.05	0.079	-		8.84	0.102	0.228		9.22	0.117	0.236	273.15	5.07	0.036	0.220		7.42	0.096	0.371		9.63	0.166	0.411		10.57	0.206	0.408		10.85	-	0.405		11.01	-	0.404		11.18	-	0.397	253.15	3.70	0.036	0.383		5.27	0.072	0.516		10.18	0.218	0.612		12.74	0.371	0.564	233.15	5.27	0.092	0.722		10.18	0.242	0.757
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<p>METHOD/APPARATUS/PROCEDURE:</p> <p>Static equilibrium cell with agitator. Pressure measured with Bourdon gauge. After equilibrium established sample removed and analysed by volumetric and gravimetric technique. Carbon dioxide absorbed in potassium hydroxide solution.</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>Better than 99.5 mole per cent.</p> <p>ESTIMATED ERROR:  <math>\delta T/K = \pm 0.05</math>; <math>\delta P/MPa = \pm 0.01</math>;  <math>\delta x_{O_2}, \delta y_{O_2} = \pm 0.003</math> (estimated by compiler)</p> <p>REFERENCES:</p>																																																																																												

EXPERIMENTAL VALUES:				EXPERIMENTAL VALUES:			
T/K	P/bar	Mole fraction of oxygen in liquid, in vapor,		T/K	P/bar	Mole fraction of oxygen in liquid, in vapor,	
		$x_{O_2}$	$y_{O_2}$			$x_{O_2}$	$y_{O_2}$
223.15	10.1	0.008	0.312	233.15	121.6	0.334	0.780
	20.3	0.025	0.617		131.7	0.393	0.762
	30.4	0.049	0.712	243.15	20.3	0.010	0.275
	40.5	0.071	0.761		30.4	0.031	0.463
	50.7	0.096	0.789		40.5	0.052	0.551
	60.8	0.117	0.809		50.7	0.080	0.609
	70.9	0.150	0.814		60.8	0.104	0.644
	81.1	0.189	0.818		70.9	0.140	0.671
	91.2	0.220	0.820		81.1	0.162	0.693
	101.3	0.267	0.819		91.2	0.191	0.689
	111.5	0.293	0.797		101.3	0.236	0.694
	121.6	0.334	0.780		111.5	0.266	0.682
	131.7	0.394	0.762		121.6	0.306	0.671
233.15	10.1	-	0.118	253.15	20.3	0.006	0.061
	20.3	0.021	0.419		30.4	0.030	0.302
	30.4	0.041	0.589		40.5	0.042	0.400
	40.5	0.064	0.651		50.7	0.062	0.500
	50.7	0.087	0.695		60.8	0.092	0.540
	60.8	0.120	0.723		70.9	0.125	0.560
	70.9	0.141	0.741		81.1	0.141	0.574
	81.1	0.167	0.757		91.2	0.170	0.601
	91.2	0.205	0.766		101.3	0.220	0.599
	101.3	0.248	0.767		111.5	0.255	0.601
	111.5	0.274	0.760		121.6	0.300	0.570

## AUXILIARY INFORMATION

(cont.)

## METHOD/APPARATUS/PROCEDURE:

High pressure recirculating vapor flow apparatus. Temperature measured with quartz thermometer; pressure measured with Bourdon gauge. Samples analysed by gas chromatography.

## SOURCE AND PURITY OF MATERIALS:

No details given.

## ESTIMATED ERROR:

$\delta T/K = \pm 0.02$ ;  $\delta P/\text{bar} = \pm 0.5\%$ ;  $\delta x_{O_2}$ ,  $\delta y_{O_2} = \pm 0.02$  (estimated by compiler).

## REFERENCES:

<p>COMPONENTS:</p> <p>(1) Oxygen; O<sub>2</sub>; [7782-44-7]</p> <p>(2) Carbon dioxide; CO<sub>2</sub>; [124-38-9]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Fredenslund, A.; Sather, G. A. <i>J. Chem. Eng. Data</i> <u>1970</u>, 15, 17-22.</p>
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EXPERIMENTAL VALUES:								
T/K	P/bar	Mole fraction of oxygen		T/K	P/bar	Mole fraction of oxygen		
		in liquid, $x_{O_2}$	in vapor, $y_{O_2}$			in liquid, $x_{O_2}$	in vapor, $y_{O_2}$	
263.15	30.4	0.009	0.096	273.15	60.8	0.062	0.298	
	40.5	0.035	0.263		70.9	0.090	0.336	
	50.7	0.056	0.346		81.1	0.126	0.372	
	60.8	0.079	0.417		91.2	0.147	0.398	
	70.9	0.110	0.463		101.3	0.185	0.401	
	81.1	0.134	0.493		111.5	0.247	0.362	
	91.2	0.162	0.495		283.15	50.7	0.028	0.115
	101.3	0.195	0.500			60.8	0.040	0.161
	111.5	0.243	0.498			70.9	0.071	0.218
	121.6	0.299	0.446			81.1	0.087	0.263
273.15	40.5	0.010	0.099	91.2	0.115	0.294		
	50.7	0.042	0.214	101.3	0.187	0.263		

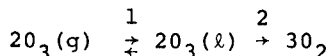
COMPONENTS:		ORIGINAL MEASUREMENTS:	
(1) Oxygen; O <sub>2</sub> ; [7782-44-7]		Fredenslund, A.; Mollerup, J.; Persson, O.	
(2) Carbon dioxide; CO <sub>2</sub> ; [124-38-9]		J. Chem. Eng. Data <u>1972</u> , 17, 440-3.	
VARIABLES:		PREPARED BY:	
T/K = 224 P/bar = 9-142		C. L. Young	
EXPERIMENTAL VALUES:			
T/K	P/bar	Mole fraction of oxygen in liquid, $x_{O_2}$	in gas, $y_{O_2}$
223.75	9.31	0.0040	0.2222
	14.08	0.0122	0.4461
	25.94	0.0306	0.6453
	34.2	0.0426	0.7101
	50.5	0.0756	0.7771
	77.5	0.1433	0.8137
	87.1	0.1808	-
	118.6	0.3056	0.7970
	127.3	0.3413	0.7808
	137.8	0.3929	0.7113
	142.4	0.4462	0.6240
AUXILIARY INFORMATION			
METHOD /APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Equilibrium established by re-circulating vapor by pump outside thermostat. Temperature measured with platinum resistance thermometer. Pressure measured with dead weight gauge. Samples of liquid and vapor analysed by gas chromatography. Details in source.		No details given.	
		ESTIMATED ERROR:	
		$\delta T/K = \pm 0.01$ ; $\delta P/\text{bar} = \pm 0.1$ ; $\delta x_{O_2} = \delta y_{O_2} \approx \pm 2.5\%$ .	
		REFERENCES:	

## OZONE SOLUBILITIES

COMPONENTS: (1) Ozone; O <sub>3</sub> ; [ 10028-15-6 ] (2) Water; H <sub>2</sub> O; [ 7732-18-5 ] (3) Buffer + H <sub>2</sub> SO <sub>4</sub> or NaOH	EVALUATOR: John A. Roth Department of Chemical Engineering Vanderbilt University Nashville, Tennessee 37235  April 1981
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## CRITICAL EVALUATION:

Gases which react upon diffusing into the liquid phase present unique problems in establishing gas-liquid solubilities. Since ozone decomposes irreversibly in water, the overall mechanism in aqueous systems can be presented as



The gas-liquid equilibrium involves step 1. Classical solubility measurements involving the equilibration of a fixed volume of gas with a measured mass of solvent cannot be used when step 2 is significant relative to the ozone transfer from the gas phase. Historically, investigators have generated ozone by passing an air or oxygen stream between electrodes across which an electrical discharge is generated. The exiting gas stream, typically 2 to 4% ozone by weight, is bubbled continuously through water. A steady state concentration is achieved as time increases. This approaches the ozone solubility only when the kinetic rate for step 2 is very slow compared to the gas to liquid mass transfer step. For the ozone water system, this occurs only in the low temperature and low pH regions. At higher relative reaction rates (step 2) however, the observed steady state concentration is not the thermodynamic equilibrium (i.e., solubility) concentration.

An experimental approach has been developed by Sullivan (1) and Roth and Sullivan (2) to determine the solubility of ozone in aqueous systems in which significant decomposition occurs. The experiment consists of sparging a high quality ozone demand-free water with an air-ozone or oxygen-ozone gas stream. The system is sampled during the unsteady state ozone uptake period until a steady state ozone concentration is achieved. The ozone stream is then stopped and the unsteady state batch decomposition is determined by taking concentration time measurements during decomposition. An unsteady state mass balance on ozone in the completely mixed system which describes the ozone uptake portion of the experiment is:

$$\left( \text{rate of ozone transferred into the liquid} \right) = \left( \text{rate of disappearance by chemical reactor} \right) + \left( \text{rate of ozone accumulation in the reactor} \right) \quad (1)$$

$$k_L a (C_i - C) V = (-r_{\text{O}_3}) V + V \frac{dC}{dt} \quad (2)$$

where  $a$  = interfacial area, cm<sup>2</sup>

$C$  = concentration of the ozone in the bulk liquid, g mol<sup>-1</sup>

$C_i$  = concentration of the ozone at the interface, g mol<sup>-1</sup>

$r_{\text{O}_3}$  = rate of ozone decomposition, mol l<sup>-1</sup> min<sup>-1</sup>

$k_L$  = liquid film mass transfer coefficient, cm<sup>2</sup> min<sup>-1</sup>

$t$  = time, min.

$V$  = bulk liquid volume, l

The ozone decomposition can be represented adequately over the range of experimental data (Sullivan and Roth (3)) as first order. The interfacial ozone concentration is assumed to be liquid film controlling valid for high Henry's law constants (see, for example, Sherwood et al. (4)). The interfacial concentration,  $C_i$ , is then equal to  $C^*$ , the equilibrium solubility concentration.

Recognizing also that the accumulation term,  $dC/dt$ , is zero at steady state,

$$C^* = (1 + k/k_L a) C_{\text{SS}} \quad (3)$$

## COMPONENTS:

- (1) Ozone;  $O_3$ ; [10028-15-6]  
 (2) Water;  $H_2O$ ; [7732-18-5]  
 (3) Buffer +  $H_2SO_4$  or NaOH

## EVALUATOR:

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 Vanderbilt University  
 Nashville, Tennessee 37235

April 1981

## CRITICAL EVALUATION:

continued

where  $C_{SS}$  is the steady state ozone concentration. Substituting  $C_i = C^*$  and eq. 3 in eq. 2, integrating and rearranging, the following equation is obtained

$$C = C_{SS} [1 - \exp(-k_L a + k)t] \quad (4)$$

The rate constant,  $k$ , is determined from the ozone decomposition data. The value of  $k_L a$ , specific for each experimental apparatus, is determined from the ozone uptake data using eq. 4 and the decomposition rate data. It is assumed further that the gaseous solution is ideal and Henry's law,

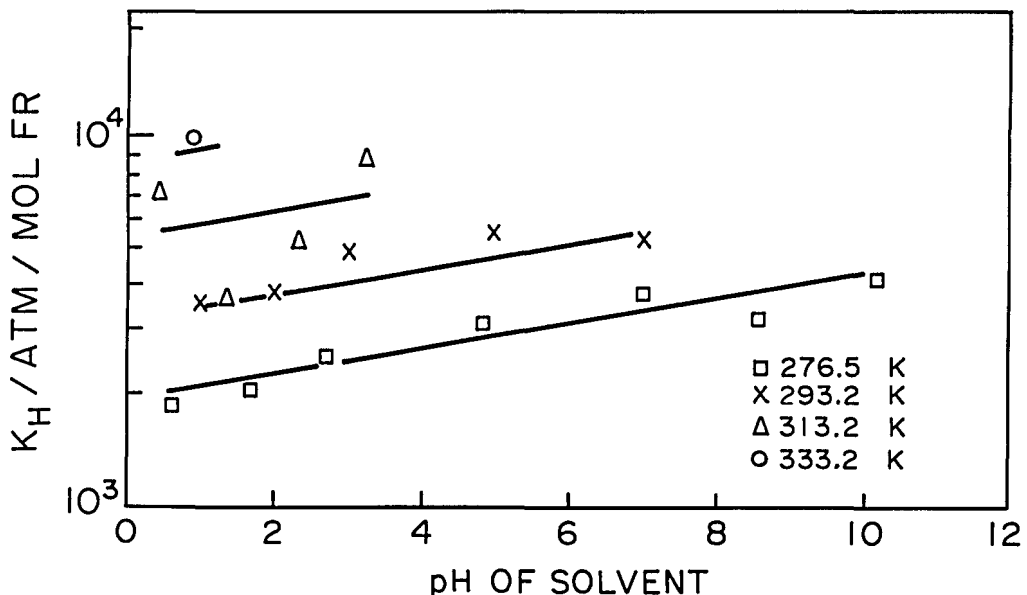
$$P(g) = K_H x \quad (5)$$

is valid for the nondissociating step. The analysis of the gas phase oxone concentration provides the corresponding gas phase partial pressure for eq. 5 and  $K_H$  can be determined.

Roth and Sullivan (2) have determined the solubility of ozone in a buffered water system. Either  $H_2SO_4$  or NaOH was used to adjust the pH to the desired value. The Henry's law constants are shown in Figure 1. These are fit by the equation,

$$K_H = 3.84 \times 10^7 [OH^-][\exp(-2428/(T/K))] \quad (6)$$

where  $[OH^-]$  = hydroxide concentration, mole  $l^{-1}$ , and with an index of determination of 0.84 and standard error of estimate of 0.20. This equation is plotted in Figure 1 for comparison with the experimental data. These data are more consistent at the lower temperatures. At higher temperatures and pH's accurate measurements are much more difficult, and accordingly are less reliable.



continued on following page



COMPONENTS:	EVALUATOR:
(1) Ozone: O <sub>3</sub> ; [10028-15-6]	John A. Roth
(2) Water; H <sub>2</sub> O: [7732-18-5]	Department of Chemical Engineering
(3) Buffer + H <sub>2</sub> SO <sub>4</sub> or NaOH	Vanderbilt University
	Nashville, Tennessee 37235
	April 1981

## CRITICAL EVALUATION:

continued

Li (5) recognized the problem of determining the solubility of ozone in water. He estimated the solubility from his measurements in a buffered aqueous system, but did not fully account for the simultaneous decomposition. Sullivan (1) recalculated Li's data taking into account the decomposition. These values, converted to Henry's law constants, are given in Table 1 and compared with Sullivan's results predicted by equation (6).

TABLE 1. Comparison of the Recalculated Henry's Law Constants of Li and Sullivan, 298 K

pH	Li (5)	Li (5)	Sullivan (1)
	K <sub>H</sub> (range) atm/mole fr.	K <sub>H</sub> (mean) atm/mole fr.	K <sub>H</sub> atm/mole fr.
220	6747-8442	7582	4296
410	7172-7251	7212	5007
615	7440-8274	7857	5906
710	7603-8644	8123	6376

Li's values are 29 to 44% higher than those of Sullivan, disregarding the 2.20 pH data of Li, which appear to be inconsistent. Li's data varied up to 25% at the same experimental conditions. The differences between the Sullivan and the Li data are, however, not fully resolved.

Some of the early reported solubility data for the ozone-water system were obtained by Carius (6). Schone (7) demonstrated that when an ozone-oxygen stream was passed through distilled water, a true equilibrium was not reached. Although the concentration of the dissolved ozone remained constant, the ozone in the gas decomposed to oxygen. Schone accordingly corrected Carius' results. Ingles (8) in 1903 correctly recognized that the measured ozone concentration in water was an "apparent solubility", depending on the gas flow rate. He performed experiments confirming Schone's results and concluded that it is impossible to study the molecular state of dissolved ozone using traditional solubility measurement techniques.

Mailfert (9) in 1894 obtained apparent solubilities for ozone in water from 273 to 333 K and in dilute H<sub>2</sub>SO<sub>4</sub> solutions over a range of 303 to 333 K. He presented his results as Ostwald coefficients. These water and low pH values were found to have small deviations at 293 to 298 K and substantial deviations for 303 to 330 K. The values obtained in distilled water were converted to Henry's law constants, reported in the International Critical Tables (10) and commonly reproduced in standard handbooks, disregarding the work of Ingles (8).

Luther-Leipzig (11) determined the apparent solubility at 273 K and 293 K. Rothmund (12) studied the solubility in H<sub>2</sub>SO<sub>4</sub> solution and 273 K in which the ozone was quite stable. He found the Ostwald coefficient, L, to be constant over a gas concentration of 20 to 100 mg/l, verifying Henry's law under these conditions. He operated under conditions for which the decomposition rate of ozone was negligible compared to the mass transfer rate. Fischer and Tropsch (13) presented a single Ostwald's coefficient at 291 K.

Kawamura (14) studied both a pure water system for which he determined Ostwald coefficients from 323 K to 333 K and in sulfuric acid solutions ranging from 0.11 N to 7.57 N at 293 K. He found decreasing values of L with increasing acid normality.

continued on following page

COMPONENTS:  (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Water; H <sub>2</sub> O; [7732-18-5] (c) Buffer + H <sub>2</sub> SO <sub>4</sub> or NaOH	EVALUATOR:  John A. Roth Department of Chemical Engineering Vanderbilt University Nashville, Tennessee 37235  April 1981
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## CRITICAL EVALUATION:

continued

Briner and Perrottet (14) determined the Bunsen absorption coefficient,  $\alpha$ , in water at 276.6 K and 292 K. They also reported  $\alpha$  in solutions containing 35 mg NaCl/l (3.5% dissolved solids) at 236.6 K and 242.0 K. A significant reduction in the dissolved ozone concentration was observed.

Meddows-Taylor (16) references two Ostwald coefficients at 276 K and 293 K.

Hoather (17) noted that the saturation of water with ozone gas was impossible because of the simultaneous occurrence of self-decomposition. He also concluded that reasonably accurate determinations could be made when the mass transfer rate was much greater than the reaction rate. Using conditions where the half-life was about ten minutes, he reported the solubility at 288 K to 312.2 K.

Stumm (19) reported the apparent solubility of ozone in water. Contrary to other investigators, he found the solubility independent of pH up to 8.5. His work was performed over a temperature range of 278 K to 298 K for solutions with an ionic strength of 0.05.

Kirk and Othmer (20) reported Bunsen absorption coefficients from 273 K to 333 K. The original source of these data is not indicated.

The data of these investigators were converted to Henry's law constants, and are given in Table 2. The apparent Henry's law constants for the pure water determinations are shown in Figure 1. Sullivan converted the steady state concentrations to apparent Henry's law constants for comparison with the literature values. These were found to be a function of pH and temperature. Lines are shown in Figure 2 for pH 2 and 7. Values reported in Table 2 fall almost entirely between these two lines. These values are not recommended for use for the following reasons.

1. Solubilities were obtained by static techniques neglecting the effect of reaction or by bubbling a continuous oxygen stream through water. These latter experiments are dependent on the mass transfer characteristics, which differ for different experimental apparatus and are affected by the reaction.
2. Even when extreme care is taken to prepare high purity-ozone demand free water (see Sullivan (1)), the pH will drop during ozonation. Most previous investigators did not monitor the pH during their experiments. Sullivan (1) chose to buffer his experiments thereby maintaining constant pH, but adding dissolved solids.
3. Analysis of the unstable ozone species in water is difficult and is usually based on the reaction of free ozone with the reagents used in analysis. Sullivan et al. (20) review the state of the art in ozone analysis. Some investigators clearly used analyses which gave total oxidants rather than ozone specific results. Although better precision can be obtained using spectrometric methods of analysis, these methods are still based on calibrations using iodometric methods.
4. Ozone-water chemistry is not well established. A number of mechanisms have been postulated (Peleg (21) and Sullivan (1)) but existing kinetic data are not sufficient to distinguish between the hypothesized kinetic mechanisms.

continued on following page

COMPONENTS:		EVALUATOR:			
(1) Ozone; O <sub>3</sub> ; [ 10028-15-6 ]		John A. Roth			
(2) Water; H <sub>2</sub> O; [ 7732-18-5 ]		Department of Chemical Engineering			
(3) Buffer + H <sub>2</sub> SO <sub>4</sub> or NaOH		Vanderbilt University			
		Nashville, Tennessee 37235			
		April 1981.			
CRITICAL EVALUATION:					
continued					
TABLE 2. Apparent Solubility of Ozone in Aqueous Solution (Not Recommended for Use)					
Investigator	T/K	Bunsen Coefficient, $\alpha$	Ostwald Coefficient, L	$K_H$ / (atm/mole frac)	
SCHÖNE (1873)	291.4	0.366		3400	
MAILFERT (1894)	273.2		0.641	1940	
	279.2		0.562	2260	
	285.0		0.500	2600	
	286.2		0.482	2710	
	288.2		0.456	2880	
	292.2		0.381	3500	
	300.2		0.270	5070	
	305.2		0.195	7130	
	313.2		0.112	12750	
	320.2		0.077	18960	
	328.2		0.031	48260	
	333.2		0.000	$\infty$	
	MAILFERT <sup>2</sup> (1894)	303.2		0.240	5760
	all values in weak H <sub>2</sub> SO <sub>4</sub> soln.	306.2		0.224	6230
	315.9		0.174	8280	
	322.2		0.156	9410	
	330.2		0.096	15680	
LUTHER (1905)	273.2		0.44	2830	
	293.2		0.23	5810	
ROTHMUND (1912)	273.2		0.487	2560	
FISCHER AND TROPSCHE (1917)	291.2		0.460	2890	
KAWAMURA (1932)	278.2		0.44	2880	
	283.2		0.38	3400	
	293.2		0.29	4610	
	303.2		0.20	6910	
	313.2		0.15	9520	
	323.2		0.11	13390	
KAWAMURA <sup>2</sup> (1932)	333.2		0.08	18980	
	7.57N H <sub>2</sub> SO <sub>4</sub>	293.2	0.18	7420	
	2.02N H <sub>2</sub> SO <sub>4</sub>	293.2	0.23	5810	
	1.01N H <sub>2</sub> SO <sub>4</sub>	293.2	0.25	5350	
	0.18N H <sub>2</sub> SO <sub>4</sub>	293.2	0.28	4770	
	0.11N H <sub>2</sub> SO <sub>4</sub>	293.2	0.28	4770	
BRINER AND PERROTTET (1939)	276.7	0.480		2590	
	293.0	0.323		3860	
BRINER AND PERROTTET <sup>2</sup> (1939)	276.7	0.24		5190	
	293.0	0.17		7320	
35 g/l NaCl					
MEDDOWS- TAYLOR (1948)	276.2		0.49	2570	
	293.2		0.34	3930	
HOATHER (1948)	288.2		0.173	7590	

continued on following page

## COMPONENTS:

- (1) Ozone;  $O_3$ ; [10028-15-6]  
 (2) Water;  $H_2O$ ; [7732-18-5]  
 (3) Buffer +  $H_2SO_4$  or  $NaOH$

## EVALUATOR:

John A. Roth  
 Department of Chemical Engineering  
 Vanderbilt University  
 Nashville, Tennessee 37235

April 1981

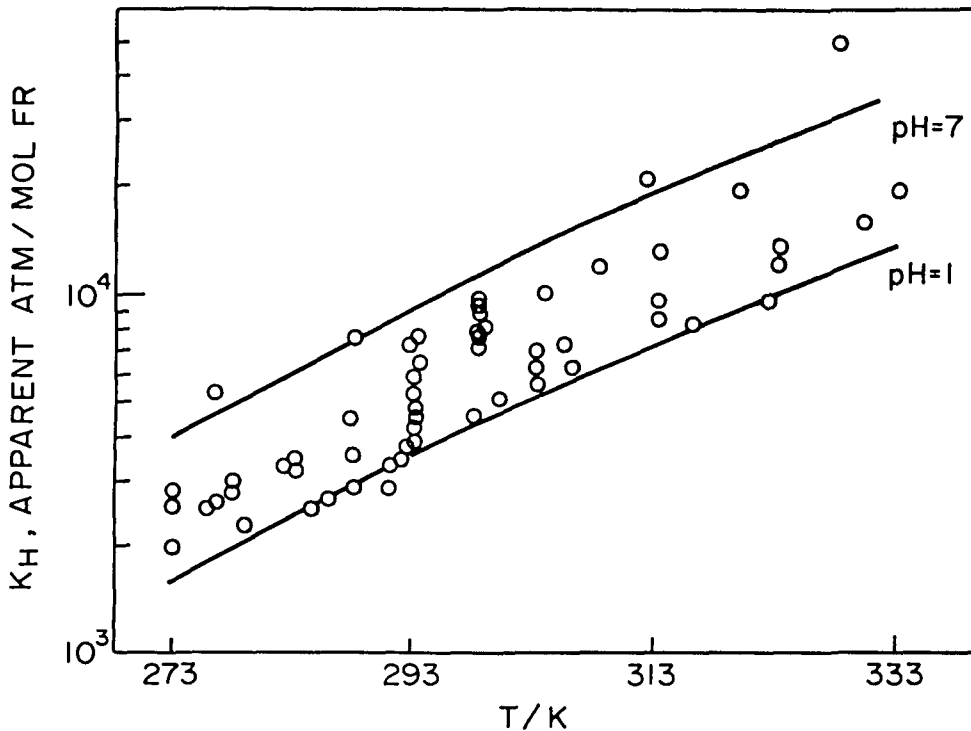
## CRITICAL EVALUATION:

continued

Investigator	T/K	Bunsen Coefficient, $\alpha$	Ostwald Coefficient, L	$K_H$ / (atm/mole frac)
RAWSON (1953)	282.8		0.39	3300
	287.7		0.29	4520
	293.5		0.21	6370
	298.7		0.17	8010
	303.8		0.14	9890
	308.3		0.12	11710
	312.2		0.07	20330
STUMM (1958)	278.2		0.45	2820
	283.2		0.41	3150
	288.2		0.37	3550
	293.2		0.34	3930
	298.2		0.30	4530
KIRK, OTHMER (1967)	273.2	0.49		2530
	278.2	0.44		2820
	283.2	0.375		3330
	293.2	0.285		4370
	303.2	0.2		6210
	313.2	0.145		8550
	323.2	0.105		11770
	333.2	0.080		15600

<sup>1</sup> Henry's Law constants calculated by Sullivan (1).

<sup>2</sup> Not shown on Figure 2.



continued on following page

COMPONENTS: (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Water; H <sub>2</sub> O; [7732-18-5] (3) Buffer + H <sub>2</sub> SO <sub>4</sub> or NaOH	EVALUATOR: John A. Roth Department of Chemical Engineering Vanderbilt University Nashville, Tennessee 37235 April 1981
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## CRITICAL EVALUATION: continued

Because of the above problems, none of these data are recommended for use.

Ozone-water solubility data are of lesser quality than those obtained on stable gas-liquid systems. The reactivity of the ozone, a very strong oxidizer, results in experimental problems as discussed above. The only data available which considers the problems of the simultaneous decomposition reaction are those of Roth and Sullivan (2) and Li (as recalculated by Sullivan (1)). While these values are empirically correlated with the Henry's law constant as a function of pH, careful investigations of ionic strength, dissolved solids, and perhaps the specific ionic species are still needed. The entire question of ozone aqueous chemistry also needs further clarification. Accordingly, the Roth and Sullivan data are recommended recognizing the limitations and assumptions of these data.

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<b>COMPONENTS:</b> (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Matrozov, V.E.; Kashtanov, S.A.; Stepanov, A.M.; Tregubov, B.A.  <i>Zh. Prikl. Khim. (Leningrad)</i> <u>1975</u> , 48 (8), 1838-41.																												
<b>VARIABLES:</b> T/K = 294 - 333	<b>PREPARED BY:</b> R. Battino																												
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="317 489 992 743"> <thead> <tr> <th>T<sup>a</sup>/K</th> <th>10<sup>5</sup>/(T/K)<sup>b</sup></th> <th>log<sub>10</sub>H<sup>b,c</sup></th> <th>10<sup>-4</sup>H<sup>a</sup></th> </tr> </thead> <tbody> <tr> <td>333.3</td> <td>300</td> <td>5.45</td> <td>28.2</td> </tr> <tr> <td>322.6</td> <td>310</td> <td>5.33</td> <td>21.4</td> </tr> <tr> <td>312.5</td> <td>320</td> <td>5.20</td> <td>15.8</td> </tr> <tr> <td>303.0</td> <td>330</td> <td>5.08</td> <td>12.0</td> </tr> <tr> <td>294.1</td> <td>340</td> <td>4.90</td> <td>7.94</td> </tr> <tr> <td>298.5<sup>d</sup></td> <td></td> <td>4.98<sup>a</sup></td> <td>9.46<sup>d</sup></td> </tr> </tbody> </table> <p data-bbox="317 791 1118 994"> <sup>a</sup> Calculated by compiler.  <sup>b</sup> Values read from graph.  <sup>c</sup> H is the Henry's constant in units of atm cm<sup>3</sup> mol<sup>-3</sup>.  <sup>d</sup> Average value of H reported in paper over a small pressure range.         </p>		T <sup>a</sup> /K	10 <sup>5</sup> /(T/K) <sup>b</sup>	log <sub>10</sub> H <sup>b,c</sup>	10 <sup>-4</sup> H <sup>a</sup>	333.3	300	5.45	28.2	322.6	310	5.33	21.4	312.5	320	5.20	15.8	303.0	330	5.08	12.0	294.1	340	4.90	7.94	298.5 <sup>d</sup>		4.98 <sup>a</sup>	9.46 <sup>d</sup>
T <sup>a</sup> /K	10 <sup>5</sup> /(T/K) <sup>b</sup>	log <sub>10</sub> H <sup>b,c</sup>	10 <sup>-4</sup> H <sup>a</sup>																										
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<b>AUXILIARY INFORMATION</b>																													
<b>METHOD/APPARATUS/PROCEDURE:</b> <p>The ozone concentrations in the liquid and gas phases were determined with the aid of neutral 1% KI solution with phosphate buffer (1). Constancy of ozone concentration at the saturation column exit was determined spectrophotometrically at 254 nm. Special precautions were taken to minimize errors due to ozone decomposition in the liquid and gas phases.</p>	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From a LGO-15 ozonizer 3. (2) Distilled.  <b>ESTIMATED ERROR:</b> $\delta H/H = \pm 0.03$ , compiler's estimate. $\delta T/K = \pm 0.1$  <b>REFERENCES:</b> 1. Dietz, R.N.; Pruzansky, J.; Smith, J.D. <i>Anal. Chem.</i> <u>1973</u> , 45, 402.																												

<p>COMPONENTS:</p> <p>(1) Ozone; O<sub>3</sub>; [10028-15-6]</p> <p>(2) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Sullivan, D.E. <i>Ph.D. thesis, Vanderbilt University, 1979.</i></p> <p>Roth, J.A.; Sullivan, D.E. <i>Ind. Eng. Chem. Fundamentals (in press for May 1981).</i></p>																																																																								
<p>VARIABLES:</p> <p>T/K = 277-333</p> <p>pH</p>	<p>PREPARED BY:</p> <p>R. Battino</p>																																																																								
<p>EXPERIMENTAL VALUES:</p> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center;">t/°C</th> <th style="text-align: center;">T<sup>a</sup>/K</th> <th style="text-align: center;">pH</th> <th style="text-align: center;">10<sup>-5</sup>H<sup>b</sup>/ (atm/mol fraction)</th> </tr> </thead> <tbody> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">0.65</td><td style="text-align: center;">1.829</td></tr> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">1.70</td><td style="text-align: center;">2.025</td></tr> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">2.75</td><td style="text-align: center;">2.502</td></tr> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">4.85</td><td style="text-align: center;">3.070</td></tr> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">7.00</td><td style="text-align: center;">3.771</td></tr> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">8.60</td><td style="text-align: center;">3.195</td></tr> <tr><td style="text-align: center;">3.50</td><td style="text-align: center;">276.65</td><td style="text-align: center;">10.20</td><td style="text-align: center;">4.186</td></tr> <tr><td style="text-align: center;">20.00</td><td style="text-align: center;">293.15</td><td style="text-align: center;">1.00</td><td style="text-align: center;">3.524</td></tr> <tr><td style="text-align: center;">20.00</td><td style="text-align: center;">293.15</td><td style="text-align: center;">2.00</td><td style="text-align: center;">3.755</td></tr> <tr><td style="text-align: center;">20.00</td><td style="text-align: center;">293.15</td><td style="text-align: center;">3.00</td><td style="text-align: center;">4.795</td></tr> <tr><td style="text-align: center;">20.00</td><td style="text-align: center;">293.15</td><td style="text-align: center;">5.00</td><td style="text-align: center;">5.497</td></tr> <tr><td style="text-align: center;">20.00</td><td style="text-align: center;">293.15</td><td style="text-align: center;">7.00</td><td style="text-align: center;">5.304</td></tr> <tr><td style="text-align: center;">40.00</td><td style="text-align: center;">313.15</td><td style="text-align: center;">0.45</td><td style="text-align: center;">7.145</td></tr> <tr><td style="text-align: center;">40.00</td><td style="text-align: center;">313.15</td><td style="text-align: center;">1.40</td><td style="text-align: center;">3.590</td></tr> <tr><td style="text-align: center;">40.00</td><td style="text-align: center;">313.15</td><td style="text-align: center;">2.35</td><td style="text-align: center;">5.112</td></tr> <tr><td style="text-align: center;">40.00</td><td style="text-align: center;">313.15</td><td style="text-align: center;">3.30</td><td style="text-align: center;">8.834</td></tr> <tr><td style="text-align: center;">60.00</td><td style="text-align: center;">333.15</td><td style="text-align: center;">0.95</td><td style="text-align: center;">9.671</td></tr> </tbody> </table>		t/°C	T <sup>a</sup> /K	pH	10 <sup>-5</sup> H <sup>b</sup> / (atm/mol fraction)	3.50	276.65	0.65	1.829	3.50	276.65	1.70	2.025	3.50	276.65	2.75	2.502	3.50	276.65	4.85	3.070	3.50	276.65	7.00	3.771	3.50	276.65	8.60	3.195	3.50	276.65	10.20	4.186	20.00	293.15	1.00	3.524	20.00	293.15	2.00	3.755	20.00	293.15	3.00	4.795	20.00	293.15	5.00	5.497	20.00	293.15	7.00	5.304	40.00	313.15	0.45	7.145	40.00	313.15	1.40	3.590	40.00	313.15	2.35	5.112	40.00	313.15	3.30	8.834	60.00	333.15	0.95	9.671
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<p><sup>a</sup> Calculated by compiler</p> <p><sup>b</sup> Henry coefficient in units of atm/mol fraction.</p> <p><sup>c</sup> The authors presented the following smoothing equation: continued on following page</p>																																																																									
<p>AUXILIARY INFORMATION</p>																																																																									
<p>METHOD/APPARATUS/PROCEDURE:</p> <p>A modified iodimetric technique in which arsenious acid, a primary standard, was substituted for sodium thiosulfate. This permitted the analytical procedure to be performed in a neutral medium. The authors also studied the kinetics of the self-decomposition of ozone and corrected their results to true equilibrium solubilities. The pH was maintained with a phosphate buffer using H<sub>2</sub>SO<sub>4</sub> or NaOH to attain the desired pH. Details are given in the thesis (1).</p>	<p>SOURCE AND PURITY OF MATERIALS:</p> <p>(1) Medical grade oxygen was used in a Grace model LG-2-L1 ozone generator.</p> <p>(2) Deionized, then distilled from an alkaline permanganate solution. This was "ozone demand-free" water.</p> <p>ESTIMATED ERROR:</p> <p>δT/K = ±0.1</p> <p>δH/H = ±0.1, compiler's estimate.</p> <p>REFERENCES:</p> <p>1. Sullivan, D.E. Ph.D. thesis, Vanderbilt University, 1979.</p>																																																																								

<p>COMPONENTS:</p> <p>(1) Ozone; O<sub>3</sub>; [10028-15-6]</p> <p>(2) Water; H<sub>2</sub>O; [7732-18-5]</p>	<p>EVALUATOR:</p> <p>Sullivan, D.E. <i>Ph.D. thesis, Vanderbilt University, 1979.</i></p> <p>Roth, J.A.; Sullivan, D.E. <i>Ind. Eng. Chem. Fundamentals (in press for May 1981).</i></p>
<p>CRITICAL EVALUATION:</p> <p style="text-align: center;">continued</p> $H = 3.842 \times 10^7 e^{-2.428 \times 10^3 / (T/K)} [\text{OH}^-] 0.035.$ <p>This fits the data with an average deviation of about ±10 per cent. [OH<sup>-</sup>] denotes a molar concentration.</p>	



<b>COMPONENTS:</b> (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Trichloromethane (Chloroform); CHCl <sub>3</sub> ; [67-66-3]	<b>ORIGINAL MEASUREMENTS:</b> Boer, H.; Sixma, F.L.J. <i>Rec. Trav. Chim.</i> <u>1951</u> , 70, 997-1004.																																																						
<b>VARIABLES:</b> T/K = 234 - 248	<b>PREPARED BY:</b> R. Battino																																																						
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="margin-left: auto; margin-right: auto;"> <thead> <tr> <th style="text-align: center;">t/°C</th> <th style="text-align: center;">T<sup>a</sup>/K</th> <th style="text-align: center;">L<sup>b</sup></th> </tr> </thead> <tbody> <tr><td style="text-align: center;">-25.0</td><td style="text-align: center;">248.2</td><td style="text-align: center;">6.5<sup>c</sup></td></tr> <tr><td style="text-align: center;">-25.0</td><td style="text-align: center;">248.2</td><td style="text-align: center;">7.0<sup>c</sup></td></tr> <tr><td style="text-align: center;">-25.0</td><td style="text-align: center;">248.2</td><td style="text-align: center;">6.5</td></tr> <tr><td style="text-align: center;">-28.0</td><td style="text-align: center;">245.2</td><td style="text-align: center;">6.8<sup>c</sup></td></tr> <tr><td style="text-align: center;">-28.0</td><td style="text-align: center;">245.2</td><td style="text-align: center;">6.8<sup>c</sup></td></tr> <tr><td style="text-align: center;">-28.0</td><td style="text-align: center;">245.2</td><td style="text-align: center;">6.8<sup>c</sup></td></tr> <tr><td style="text-align: center;">-30.5</td><td style="text-align: center;">242.7</td><td style="text-align: center;">7.8</td></tr> <tr><td style="text-align: center;">-30.5</td><td style="text-align: center;">242.7</td><td style="text-align: center;">8.0</td></tr> <tr><td style="text-align: center;">-30.5</td><td style="text-align: center;">242.7</td><td style="text-align: center;">8.1</td></tr> <tr><td style="text-align: center;">-30.5</td><td style="text-align: center;">242.7</td><td style="text-align: center;">8.0</td></tr> <tr><td style="text-align: center;">-31.2</td><td style="text-align: center;">242.0</td><td style="text-align: center;">8.3<sup>c</sup></td></tr> <tr><td style="text-align: center;">-31.2</td><td style="text-align: center;">242.0</td><td style="text-align: center;">8.2<sup>c</sup></td></tr> <tr><td style="text-align: center;">-31.2</td><td style="text-align: center;">242.0</td><td style="text-align: center;">7.8<sup>c</sup></td></tr> <tr><td style="text-align: center;">-35.2</td><td style="text-align: center;">238.0</td><td style="text-align: center;">9.5<sup>c</sup></td></tr> <tr><td style="text-align: center;">-35.2</td><td style="text-align: center;">238.0</td><td style="text-align: center;">9.5<sup>c</sup></td></tr> <tr><td style="text-align: center;">-39.2</td><td style="text-align: center;">234.0</td><td style="text-align: center;">10.9</td></tr> <tr><td style="text-align: center;">-39.2</td><td style="text-align: center;">234.0</td><td style="text-align: center;">11.7</td></tr> </tbody> </table> <p style="margin-left: 40px;"> <sup>a</sup> Calculated by compiler.  <sup>b</sup> Ostwald coefficient.  <sup>c</sup> Solubilities determined by titration. Other solubilities determined from measured concentration of ozone in entrance and exit streams.         </p>		t/°C	T <sup>a</sup> /K	L <sup>b</sup>	-25.0	248.2	6.5 <sup>c</sup>	-25.0	248.2	7.0 <sup>c</sup>	-25.0	248.2	6.5	-28.0	245.2	6.8 <sup>c</sup>	-28.0	245.2	6.8 <sup>c</sup>	-28.0	245.2	6.8 <sup>c</sup>	-30.5	242.7	7.8	-30.5	242.7	8.0	-30.5	242.7	8.1	-30.5	242.7	8.0	-31.2	242.0	8.3 <sup>c</sup>	-31.2	242.0	8.2 <sup>c</sup>	-31.2	242.0	7.8 <sup>c</sup>	-35.2	238.0	9.5 <sup>c</sup>	-35.2	238.0	9.5 <sup>c</sup>	-39.2	234.0	10.9	-39.2	234.0	11.7
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<b>METHOD/APPARATUS/PROCEDURE:</b> The ozone was generated electrolytically to give a mixture of oxygen and ozone that was 12% ozone by weight. In the indirect method the solubility was determined from the composition of the oxygen/ozone mixture entering and leaving the saturated solution. In the direct method an aliquot of the saturated solution is taken, weighed, neutral potassium iodide solution added, acidified with sulfuric acid, and the iodine formed titrated with sodium thiosulphate.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) Generated electrolytically. (2) No details given.																																																						
<b>ESTIMATED ERROR:</b> $\delta T/K = \pm 0.04$ $\delta L/L = \pm 0.04$ , compiler's estimate																																																							
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COMPONENTS:	ORIGINAL MEASUREMENTS:			
(1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Trichlorofluoromethane; CCl <sub>3</sub> F; [75-69-4]	Mahieux, F. <i>Bull. Soc. Chim. France</i> <u>1961</u> , 2275 - 2276.			
VARIABLES:	PREPARED BY:			
T/K: 293.15 p <sub>1</sub> /kPa: 16.2 - 60.8 (0.16 - 0.60 atm)	H. L. Clever			
EXPERIMENTAL VALUES:				
T/K	Ozone Pressure p <sub>1</sub> /atm	Mol Fraction x <sub>1</sub> × 10 <sup>3</sup>	Absorption Coefficient β/cm <sup>3</sup> (STP) cm <sup>-3</sup>	Henry's Constant <sup>1</sup> K'
293.15	0.16 0.22 0.40 0.45 0.55 0.56 0.59 0.60 [1.0	2.5 2.6 6.5 7.1 7.4 7.8 7.8 6.9 14.1	0.60 0.64 1.58 1.72 1.8 1.9 1.91 1.68 3.4	3.7 2.9 3.9 3.8 3.3 3.4 3.2 2.8 3.4 ± 0.5] <sup>2</sup>
<sup>1</sup> Henry's constant, K'/cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup> = (β/cm <sup>3</sup> (STP) cm <sup>-3</sup> ) / (p <sub>1</sub> /atm)				
Note that in this formulation of Henry's constant, that the constant is the Bunsen coefficient.				
<sup>2</sup> Values calculated by the author at one atm ozone pressure.				
AUXILIARY INFORMATION				
METHOD/APPARATUS/PROCEDURE:	SOURCE AND PURITY OF MATERIALS:			
Solubility equilibrium is attained between the ozone and the trichlorofluoromethane in a special cell. The total pressure is measured. The ozone saturated liquid phase is removed, and the ozone is absorbed in a potassium iodide solution. The liberated iodine is titrated by standard methods. The gas phase is also analyzed for ozone by absorption in potassium iodide and titration of the iodine released.	(1) Ozone. No information. (2) Trichlorofluoromethane. No information.			
ESTIMATED ERROR:				
$\delta K'/K' = \pm 0.15$				
REFERENCES:				

<b>COMPONENTS:</b> (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Tetrachloromethane; CCl <sub>4</sub> ; [56-23-5]	<b>ORIGINAL MEASUREMENTS:</b> Briner, E.; Perrottet, E. <i>Helv. Chim. Acta</i> , <u>1939</u> , <i>22</i> , 585-7.																					
<b>VARIABLES:</b> T/K = 261-273	<b>PREPARED BY:</b> V. Katovic																					
<b>EXPERIMENTAL VALUES:</b> <table border="1" data-bbox="172 498 1172 737"> <thead> <tr> <th>Ozone Concn. <sup>a</sup> %</th> <th><math>\alpha</math> <sup>b,c</sup></th> <th><math>\alpha</math> <sup>b,d</sup></th> </tr> </thead> <tbody> <tr> <td>8.2</td> <td>2.8</td> <td></td> </tr> <tr> <td>8.6</td> <td>3.1</td> <td></td> </tr> <tr> <td>9.0</td> <td></td> <td>4.5</td> </tr> <tr> <td>9.4</td> <td></td> <td>4.9</td> </tr> <tr> <td>10.0</td> <td>2.5</td> <td></td> </tr> <tr> <td>10.1</td> <td>2.7</td> <td>4.4</td> </tr> </tbody> </table> <p> <sup>a</sup> Percentage in the gas phase.  <sup>b</sup> Bunsen coefficient in cm<sup>3</sup>(STP) cm<sup>-3</sup> atm<sup>-1</sup>.  <sup>c</sup> At 0°C (273K).  <sup>d</sup> At -12°C (261K).         </p>		Ozone Concn. <sup>a</sup> %	$\alpha$ <sup>b,c</sup>	$\alpha$ <sup>b,d</sup>	8.2	2.8		8.6	3.1		9.0		4.5	9.4		4.9	10.0	2.5		10.1	2.7	4.4
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<b>AUXILIARY INFORMATION</b>																						
<b>METHOD/APPARATUS/PROCEDURE:</b> Solubility of ozone was determined by an apparatus described in reference (1). The amount of ozone in the CCl <sub>4</sub> and the gas phase was determined by an iodometric technique.	<b>SOURCE AND PURITY OF MATERIALS:</b> No details given.																					
<b>ESTIMATED ERROR:</b>																						
<b>REFERENCES:</b> 1. Briner, E.; Perrottet, E. <i>Helv. Chim. Acta</i> <u>1939</u> , <i>22</i> , 397-404.																						

COMPONENTS:		ORIGINAL MEASUREMENTS:			
(1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Tetrachloromethane; CCl <sub>4</sub> ; [56-23-5] (3) Nitric acid, HNO <sub>3</sub> ; [7697-37-2] (4) Water; H <sub>2</sub> O; [7732-18-5]		Stolyarenko, T.E.; Stolyarenko, G.S.  Izv. Vyssh. Uchebn. Zaved. Khim. Khim. Tekhn. 1976, (19) 1613-4.			
VARIABLES:		PREPARED BY:			
T/K = 263-303 Concentration		V. Katovic			
EXPERIMENTAL VALUES:					
CCl <sub>4</sub> solution saturated with	t/°C	10 <sup>2</sup> C <sup>a</sup>	α <sup>b</sup>	10 <sup>5</sup> /(T/K)	Log <sub>10</sub> α <sup>b</sup>
-	-10.0	7.0848	5.760	380.23	0.7604
	0.0	5.1783	4.210	366.30	0.6243
	18.0	3.4071	2.770	343.64	0.4425
	30.0	2.5769	2.095	330.03	0.3212
H <sub>2</sub> O	-10.0	6.7404	5.480	380.23	0.7388
	0.0	6.3591	5.170	366.30	0.7135
	18.0	4.5387	3.690	343.64	0.5670
	30.0	2.5510	2.074	330.03	0.4040
HNO <sub>3</sub> 39.7376%	-8.0	6.7486	4.860	377.36	0.6866
	0.0	6.0960	4.390	366.30	0.6425
	19.5	4.1380	2.980	341.88	0.4742
	30.0	3.1105	2.240	330.03	0.3502
60.2341%	-9.5	7.3140	5.300	379.50	0.6920
	0.0	5.9423	4.306	366.30	0.6343
	19.5	4.0434	2.930	341.88	0.4669
	30.0	2.9946	2.170	330.03	0.3365
68.5889%	-8.0	6.7896	4.920	377.36	0.6920
	0.0	6.2376	4.520	366.30	0.6551
	18.4	4.3194	3.130	343.64	0.4955
	30.0	3.1188	2.260	330.03	0.3541
85.8646%	-12.0	8.8064	5.630	383.14	0.7505
	0.0	7.3048	4.670	366.30	0.6693
	18.0	5.2557	3.360	343.64	0.5262
	30.0	3.8949	2.490	330.03	0.3962
continued on following page					
AUXILIARY INFORMATION					
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:			
Ozone in gas and liquid phases was determined by a spectrophotometric method.		(1) 0.2 - 5% O <sub>3</sub> in oxygen produced by an ozone generator.			
		ESTIMATED ERROR:			
		REFERENCES:			

COMPONENTS: (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Tetrachloromethane; CCl <sub>4</sub> ; [56-23-5] (3) Nitric acid; HNO <sub>3</sub> ; [7697-37-2] (4) Water, H <sub>2</sub> O; [7732-18-5]	EVALUATOR: Stolyarenko, T.E.; Stolyarenko, G.S. <i>Izv. Vyssh. Uchebn. Zaved. Khim. Khim. Tekhn.</i> <u>1976</u> , (19), 1613-4
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 EXPERIMENTAL VALUES: continued

CCL <sub>4</sub> solution saturated with	t/°C	10 <sup>2</sup> C <sup>a</sup>	α <sup>b</sup>	10 <sup>5</sup> /(T/K)	Log <sub>10</sub> α <sup>b</sup>
100.00%	-10.0	10.3863	6.640	380.23	0.8222
	-1.0	9.7340	6.223	367.65	0.7940
	18.0	6.3413	4.054	343.64	0.6079
	30.0	5.1931	3.320	330.03	0.5211

<sup>a</sup> Concentration of ozone in liquid phase in moles per liter.

<sup>b</sup> Solubility coefficient (unidentified).

<b>COMPONENTS:</b> (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Six halocarbons (freons) - see below	<b>ORIGINAL MEASUREMENTS:</b> Chretien, A.; Servigne, M.; Mahieux, F. <i>Bull. Soc. Chim. France</i> <u>1960</u> , 49-54.																																																
<b>VARIABLES:</b> T/K = 163-250	<b>PREPARED BY:</b> V. Katovic																																																
<b>EXPERIMENTAL VALUES:</b> <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: left;">t/°C</th> <th style="text-align: left;">T<sup>a</sup>/K</th> <th style="text-align: left;">CCl<sub>3</sub>F (Freon-11)</th> <th style="text-align: left;">CCl<sub>2</sub>F<sub>2</sub> (Freon-12)</th> <th style="text-align: left;">CClF<sub>3</sub> (Freon-13)</th> <th style="text-align: left;">CHClF<sub>2</sub> (Freon-22)</th> <th style="text-align: left;">CCl<sub>2</sub>FCClF<sub>2</sub> (Freon-113)</th> <th style="text-align: left;">CClF<sub>2</sub>-CClF<sub>2</sub> (Freon-114)</th> </tr> <tr> <th colspan="2"></th> <th colspan="4" style="text-align: center;">α<sup>b</sup>/cm<sup>3</sup> (STP) cm<sup>-3</sup> atm<sup>-1</sup></th> <th colspan="2"></th> </tr> </thead> <tbody> <tr> <td>-110</td> <td>163</td> <td>1610</td> <td>2090</td> <td>2180</td> <td>3490</td> <td></td> <td></td> </tr> <tr> <td>- 90</td> <td>179</td> <td>132</td> <td>136</td> <td></td> <td></td> <td></td> <td></td> </tr> <tr> <td>- 63</td> <td>210</td> <td>25.4</td> <td></td> <td></td> <td></td> <td></td> <td>35</td> </tr> <tr> <td>- 23</td> <td>250</td> <td>6.6</td> <td></td> <td></td> <td></td> <td>9.4</td> <td></td> </tr> </tbody> </table> <p><sup>a</sup> Calculated by compiler.</p> <p><sup>b</sup> Bunsen coefficient calculated by the authors for 100 per cent ozone at 1 atm (101.325 kPa) partial pressure of ozone.</p> <p><sup>c</sup> Methane, trichlorofluoro (Freon-11); CCl<sub>3</sub>F; [75-69-4].            Methane, dichlorodifluoro (Freon-12); CCl<sub>2</sub>F<sub>2</sub>; [1495-28-9].            Methane, chlorotrifluoro (Freon-13); CClF<sub>3</sub>; [75-72-9].            Methane, chlorodifluoro (Freon-22); CHClF<sub>2</sub>; [75-45-6].            1,1,2-Trichloro-1,2,2-trifluoroethane (Freon-113); CCl<sub>2</sub>FCClF<sub>2</sub>; [76-13-1].            1,2-Dichloro-1,1,2,2-tetrafluoroethane (Freon-114); CClF<sub>2</sub>CClF<sub>2</sub>; [76-14-2].</p>		t/°C	T <sup>a</sup> /K	CCl <sub>3</sub> F (Freon-11)	CCl <sub>2</sub> F <sub>2</sub> (Freon-12)	CClF <sub>3</sub> (Freon-13)	CHClF <sub>2</sub> (Freon-22)	CCl <sub>2</sub> FCClF <sub>2</sub> (Freon-113)	CClF <sub>2</sub> -CClF <sub>2</sub> (Freon-114)			α <sup>b</sup> /cm <sup>3</sup> (STP) cm <sup>-3</sup> atm <sup>-1</sup>						-110	163	1610	2090	2180	3490			- 90	179	132	136					- 63	210	25.4					35	- 23	250	6.6				9.4	
t/°C	T <sup>a</sup> /K	CCl <sub>3</sub> F (Freon-11)	CCl <sub>2</sub> F <sub>2</sub> (Freon-12)	CClF <sub>3</sub> (Freon-13)	CHClF <sub>2</sub> (Freon-22)	CCl <sub>2</sub> FCClF <sub>2</sub> (Freon-113)	CClF <sub>2</sub> -CClF <sub>2</sub> (Freon-114)																																										
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<b>AUXILIARY INFORMATION</b>																																																	
<b>METHOD/APPARATUS/PROCEDURE:</b> Solubility of ozone was determined by an apparatus described in the paper. The amount of ozone in the gas phase and in the liquid phase were determined by an iodometric method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) No details given. (2) Freons (99%) were distilled through a column containing silica gel, molecular sieves 5A and P <sub>4</sub> O <sub>10</sub> .																																																
<b>ESTIMATED ERROR:</b> δα/α = ±0.04, authors' estimate δT/K = ±1, authors' estimate																																																	
<b>REFERENCES:</b>																																																	

<b>COMPONENTS:</b> (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Sulfuric acid; H <sub>2</sub> SO <sub>4</sub> ; [7764-93-9] (3) Water; H <sub>2</sub> O; [7732-18-5]	<b>ORIGINAL MEASUREMENTS:</b> Merkulova, V.P.; Lovchikov, V.S.; Ivanovskii, M.D. <i>Zh. Prikl. Khim.</i> 1972, 45, 1608-9.
<b>VARIABLES:</b> T/K = 293-333 O <sub>3</sub> in O <sub>2</sub> /% (vol) = 6.3-9.7	<b>PREPARED BY:</b> V. Katovic
<b>EXPERIMENTAL VALUES:</b> <div style="display: flex; justify-content: space-around; align-items: flex-start;"> <div data-bbox="194 493 526 811"> </div> <div data-bbox="546 532 796 811"> </div> <div data-bbox="868 502 1092 811"> </div> </div> <p>Figure 1. Dependence of solubility of ozone on temperature at introduction of oxygen in the ozone generator at 25 liters per hour and on the concentration of ozone in the O<sub>2</sub>/O<sub>3</sub> mixture. Sulfuric acid concentration of 10g/l. A-axis is the solubility of ozone x 10<sup>6</sup> in mol/cm<sup>3</sup>. B-axis is temperature in °C. The four lines are for volume per cent of O<sub>3</sub> in the O<sub>2</sub>/O<sub>3</sub> mixture: 1-6.3; 2-7.8; 3-8.3; 4-9.7.</p> <p>Figure 2. The solubility of ozone in H<sub>2</sub>SO<sub>4</sub> solution of 10g/l at different temperatures and at different concentrations of ozone in the O<sub>2</sub>/O<sub>3</sub> mixture. A-axis is the solubility of ozone x 10<sup>6</sup> in mol/cm<sup>3</sup>. B-axis is time in minutes. The three lines are for temperature in °C and for volume per cent of O<sub>3</sub> in the O<sub>2</sub>/O<sub>3</sub> mixture.</p> <p style="text-align: right;">continued on following page</p>	
<b>AUXILIARY INFORMATION</b>	
<b>METHOD/APPARATUS/PROCEDURE:</b> An O <sub>3</sub> /O <sub>2</sub> mixture was bubbled through sulfuric acid solution. Ozone in gas and liquid phases was determined by an iodometric method.	<b>SOURCE AND PURITY OF MATERIALS:</b> (1) From O <sub>3</sub> generator. (2,3) No details given.
<b>ESTIMATED ERROR:</b>	
<b>REFERENCES:</b>	

COMPONENTS: (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Sulfuric acid; H <sub>2</sub> SO <sub>4</sub> : [7664-93-9] (3) Water; H <sub>2</sub> O; [7732-18-5]	EVALUATOR: Merkulova, V.P.; Lovchikov, V.S.; Ivanovskii, M.D. <i>Zh. Prikl. Khim.</i> <u>1972</u> , 45, 1608-9.
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EXPERIMENTAL VALUES: continued

mixture: 1-60°C, 7.8%; 2-20°C, 6.3%; 3-20°C, 7.8%.

Figure 3. The dependence of ozone solubility in H<sub>2</sub>SO<sub>4</sub> solution (10g/l) on the concentration of ozone in the O<sub>2</sub>/O<sub>3</sub> mixture. A-axis is the solubility of ozone x 10<sup>6</sup> in mol/cm<sup>3</sup>. B-axis is the volume per cent of O<sub>3</sub> in the O<sub>2</sub>/O<sub>3</sub> mixture.



<b>COMPONENTS:</b>  (1) Ozone; O <sub>3</sub> ; [10028-15-6] (2) Various solvents (see below)	<b>ORIGINAL MEASUREMENTS:</b>  Aleksandrou, Yu.A.; Tarunin, B.I.; Perepletchikov, M.L.  Zh. Obshch. Khim. <u>1976</u> , 46, 3-5.																																
<b>VARIABLES:</b>  T/K = 298	<b>PREPARED BY:</b>  R. Battino																																
<b>EXPERIMENTAL VALUES:</b> <table style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="text-align: center; border-bottom: 1px solid black;">Solvent<sup>a</sup></th> <th style="text-align: center; border-bottom: 1px solid black;">L<sup>b</sup></th> </tr> </thead> <tbody> <tr> <td colspan="2" style="text-align: center;">25°C (298K)</td> </tr> <tr> <td>Tetrachloromethane; CCl<sub>4</sub>; [56-23-5]</td> <td style="text-align: right;">1.96</td> </tr> <tr> <td>Acetic acid; C<sub>2</sub>H<sub>4</sub>O<sub>2</sub>; [64-19-7]</td> <td style="text-align: right;">1.83</td> </tr> <tr> <td>Acetic anhydride; C<sub>4</sub>H<sub>6</sub>O<sub>3</sub>; [108-24-7]</td> <td style="text-align: right;">1.89</td> </tr> <tr> <td>1,1,2,2-Tetrachloroethane; C<sub>2</sub>H<sub>2</sub>Cl<sub>4</sub>; [25322-20-7]</td> <td style="text-align: right;">1.77</td> </tr> <tr> <td>Trifluoroacetic acid; C<sub>2</sub>HO<sub>2</sub>F<sub>3</sub>; [76-05-1]</td> <td style="text-align: right;">2.3</td> </tr> <tr> <td>Trichloromethane; CHCl<sub>3</sub>; [67-66-3]</td> <td style="text-align: right;">2.12</td> </tr> <tr> <td>Methyl acetate; C<sub>3</sub>H<sub>6</sub>O<sub>2</sub>; [79-20-9]</td> <td style="text-align: right;">1.63</td> </tr> <tr> <td>1,2-Dichloroethane; C<sub>2</sub>H<sub>4</sub>Cl<sub>2</sub>; [1300-21-6]</td> <td style="text-align: right;">1.95</td> </tr> <tr> <td>1,1,2-Trifluoro-1,2,2-trichloroethane; C<sub>2</sub>Cl<sub>3</sub>F<sub>3</sub>; [76-13-1]</td> <td style="text-align: right;">2.06</td> </tr> <tr> <td>CCl<sub>4</sub>+CHCl<sub>2</sub>CHCl<sub>2</sub> (14%)</td> <td style="text-align: right;">2.01</td> </tr> <tr> <td>CCl<sub>4</sub>+CHCl<sub>2</sub>CHCl<sub>2</sub> (33%)</td> <td style="text-align: right;">1.99</td> </tr> <tr> <td>CCl<sub>4</sub>+CHCl<sub>2</sub>CHCl<sub>2</sub> (55%)</td> <td style="text-align: right;">2.08</td> </tr> <tr> <td>CH<sub>3</sub>COOH+C<sub>2</sub>H<sub>5</sub>COOH (62%)</td> <td style="text-align: right;">1.93</td> </tr> <tr> <td>Propionic acid; C<sub>3</sub>H<sub>6</sub>O<sub>2</sub>; [79-09-4]</td> <td style="text-align: right;">1.95</td> </tr> </tbody> </table> <p style="text-align: right;">continued on following page</p>		Solvent <sup>a</sup>	L <sup>b</sup>	25°C (298K)		Tetrachloromethane; CCl <sub>4</sub> ; [56-23-5]	1.96	Acetic acid; C <sub>2</sub> H <sub>4</sub> O <sub>2</sub> ; [64-19-7]	1.83	Acetic anhydride; C <sub>4</sub> H <sub>6</sub> O <sub>3</sub> ; [108-24-7]	1.89	1,1,2,2-Tetrachloroethane; C <sub>2</sub> H <sub>2</sub> Cl <sub>4</sub> ; [25322-20-7]	1.77	Trifluoroacetic acid; C <sub>2</sub> HO <sub>2</sub> F <sub>3</sub> ; [76-05-1]	2.3	Trichloromethane; CHCl <sub>3</sub> ; [67-66-3]	2.12	Methyl acetate; C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> ; [79-20-9]	1.63	1,2-Dichloroethane; C <sub>2</sub> H <sub>4</sub> Cl <sub>2</sub> ; [1300-21-6]	1.95	1,1,2-Trifluoro-1,2,2-trichloroethane; C <sub>2</sub> Cl <sub>3</sub> F <sub>3</sub> ; [76-13-1]	2.06	CCl <sub>4</sub> +CHCl <sub>2</sub> CHCl <sub>2</sub> (14%)	2.01	CCl <sub>4</sub> +CHCl <sub>2</sub> CHCl <sub>2</sub> (33%)	1.99	CCl <sub>4</sub> +CHCl <sub>2</sub> CHCl <sub>2</sub> (55%)	2.08	CH <sub>3</sub> COOH+C <sub>2</sub> H <sub>5</sub> COOH (62%)	1.93	Propionic acid; C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> ; [79-09-4]	1.95
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<b>AUXILIARY INFORMATION</b>																																	
<b>METHOD/APPARATUS/PROCEDURE:</b>  The oxygen/ozone mixture was bubbled through the solvent being investigated. The ozone content was determined spectrophotometrically at 254nm in a flow cell. Extinction coefficients are given in the original paper. Henry's law was found to hold in all cases.	<b>SOURCE AND PURITY OF MATERIALS:</b>  (1) Prepared in a laboratory ozonizer from carefully dried oxygen.  (2) Solvents were "chemically pure" grade and purified further by distillation.																																
	<b>ESTIMATED ERROR:</b>  δL/L = ±0.03, compiler's estimate.																																
	<b>REFERENCES:</b>																																

## COMPONENTS:

- (1) Ozone; O<sub>3</sub>; [10028-15-6]  
 (2) Various solvents (see below)

## EVALUATOR:

Aleksandrou, Yu.A.; Tarunin, B.I.;  
 Perepletchikov, M.L.  
 Zh. Obshch. Khim. 1976, 46, 3-5.

## CRITICAL EVALUATION:

continued

Solvent	L <sup>b</sup>
H <sub>2</sub> O+C <sub>2</sub> H <sub>5</sub> COOH (95%)	1.56
H <sub>2</sub> O+C <sub>2</sub> H <sub>5</sub> COOH (90%)	1.28
H <sub>2</sub> O+C <sub>2</sub> H <sub>5</sub> COOH (80%)	0.89
H <sub>2</sub> O+C <sub>2</sub> H <sub>5</sub> COOH (60%)	0.56
H <sub>2</sub> O+C <sub>2</sub> H <sub>5</sub> COOH (50%)	0.32
H <sub>2</sub> O+C <sub>2</sub> H <sub>5</sub> COOH (30%)	0.24
Water; H <sub>2</sub> O; [7732-18-5]	0.20

<sup>a</sup> Composition probably in mol per cent.

<sup>b</sup> Ostwald coefficient. Ratio of concentration of ozone in solution to its concentration in the gas phase.

# SYSTEM INDEX

Underlined page numbers refer to evaluation text and those not underlined to compiled tables. All compounds are listed as in Chemical Abstracts. For example, toluene is listed as benzene, methyl- and dimethylsulfoxide is listed as methane, sulfinylbis-. For the sake of brevity the oxygen is assumed to be the dissolving gas and is not explicitly stated as a component. On the other hand when ozone is the dissolving gas, it is explicitly stated as a component.

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