

<p>COMPONENTS:</p> <p>1. N-Methylmethanamine, (dimethylamine); C₂H₇N; [124-40-3]</p> <p>2. Hexane; C₆H₁₄; [110-54-3]</p>	<p>ORIGINAL MEASUREMENTS:</p> <p>Wolff, H.; Höppel, H.-E. <i>Ber. Bunsenges. Phys. Chem.</i> <u>1966</u>, 70, 874-883.</p>																																																																																																																		
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<p>EXPERIMENTAL VALUES:</p> <p>Variation of the total vapor pressure/Torr with variation of temperature and of mole fraction of C₂H₇N in the liquid phase, $x_{C_2H_7N}$</p> <table border="1" data-bbox="73 584 1198 1128"> <thead> <tr> <th></th> <th colspan="5">T/K</th> </tr> <tr> <th>$x_{C_2H_7N}$</th> <th>223.15</th> <th>233.15</th> <th>253.15</th> <th>273.15</th> <th>293.15</th> </tr> </thead> <tbody> <tr><td>0</td><td>2.2</td><td>3.8</td><td>14.3</td><td>45.4</td><td>121.0</td></tr> <tr><td>0.0126</td><td>3.6</td><td>6.8</td><td>23.7</td><td>66.0</td><td>159.8</td></tr> <tr><td>0.0315</td><td>5.9</td><td>11.2</td><td>36.0</td><td>92.2</td><td>198.7</td></tr> <tr><td>0.0498</td><td>7.7</td><td>14.8</td><td>45.7</td><td>110.0</td><td>239.7</td></tr> <tr><td>0.0714</td><td>9.7</td><td>18.2</td><td>53.8</td><td>131.9</td><td>282.3</td></tr> <tr><td>0.0860</td><td>10.3</td><td>20.3</td><td>59.8</td><td>147.3</td><td>314.0</td></tr> <tr><td>0.1005</td><td>11.7</td><td>22.5</td><td>65.9</td><td>161.3</td><td>341.2</td></tr> <tr><td>0.142</td><td>14.2</td><td>26.4</td><td>80.0</td><td>191.4</td><td>402.3</td></tr> <tr><td>0.196</td><td>16.5</td><td>31.4</td><td>96.2</td><td>234.7</td><td>497.2</td></tr> <tr><td>0.214</td><td>17.3</td><td>32.8</td><td>102.3</td><td>247.5</td><td>525.2</td></tr> <tr><td>0.262</td><td>18.4</td><td>36.1</td><td>114.8</td><td>278.3</td><td>590.4</td></tr> <tr><td>0.325</td><td>20.0</td><td>39.6</td><td>124.8</td><td>315.0</td><td>682.3</td></tr> <tr><td>0.375</td><td>21.1</td><td>41.7</td><td>133.9</td><td>340.8</td><td>739.6</td></tr> <tr><td>0.450</td><td>22.6</td><td>44.6</td><td>144.2</td><td>373.0</td><td>818.2</td></tr> <tr><td>0.512</td><td>23.5</td><td>46.4</td><td>152.3</td><td>397.3</td><td>879.5</td></tr> <tr><td>0.587</td><td>24.5</td><td>48.9</td><td>160.0</td><td>424.4</td><td>948.9</td></tr> <tr><td>0.643</td><td>25.2</td><td>50.3</td><td>166.7</td><td>443.7</td><td>992.0</td></tr> </tbody> </table> <p style="text-align: right;">Cont.</p>			T/K					$x_{C_2H_7N}$	223.15	233.15	253.15	273.15	293.15	0	2.2	3.8	14.3	45.4	121.0	0.0126	3.6	6.8	23.7	66.0	159.8	0.0315	5.9	11.2	36.0	92.2	198.7	0.0498	7.7	14.8	45.7	110.0	239.7	0.0714	9.7	18.2	53.8	131.9	282.3	0.0860	10.3	20.3	59.8	147.3	314.0	0.1005	11.7	22.5	65.9	161.3	341.2	0.142	14.2	26.4	80.0	191.4	402.3	0.196	16.5	31.4	96.2	234.7	497.2	0.214	17.3	32.8	102.3	247.5	525.2	0.262	18.4	36.1	114.8	278.3	590.4	0.325	20.0	39.6	124.8	315.0	682.3	0.375	21.1	41.7	133.9	340.8	739.6	0.450	22.6	44.6	144.2	373.0	818.2	0.512	23.5	46.4	152.3	397.3	879.5	0.587	24.5	48.9	160.0	424.4	948.9	0.643	25.2	50.3	166.7	443.7	992.0
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VARIABLES:		PREPARED BY:			
Composition, temperature		P. G. T. Fogg			
EXPERIMENTAL VALUES: Cont.					
		T/K			
[∞] C ₂ H ₇ N	223.15	233.15	253.15	273.15	293.15
0.692	25.7	51.8	171.0	458.5	1030.9
0.760	26.3	52.7	178.3	478.0	1083.1
0.830	27.0	54.3	184.8	494.7	1120.5
0.867	27.4	55.3	188.5	506.5	1156.1
0.932	28.2	57.5	197.0	528.5	1201.6
0.956	28.6	58.6	201.0	537.8	1222.7
1	29.0	60.6	206.5	562.9	1271.5
760 Torr = 1 atm = 1.013 x 10 ⁵ Pa					
Constants for calculation of activity coefficients from the Redlich-Kister equations given below					
	T/K	A	B	C	
	223.15	1.496	0.149	0.216	
	233.15	1.385	0.065	0.159	
	243.15	1.304	0.061	0.118	
	253.15	1.192	0.069	0.111	
	263.15	1.092	0.122	0.111	
	273.15	0.965	0.082	0.096	
	283.15	0.901	0.116	0.086	
	293.15	0.811	0.133	0.103	
$\ln f_1 = A x_2^2 - B x_2^2(1 - 4 x_1) + C x_2^2(1 - 8 x_1 + 12 x_1^2)$ $\ln f_2 = A x_1^2 + B x_1^2(1 - 4 x_2) + C x_1^2(1 - 8 x_2 + 12 x_2^2)$					
where f_1 = activity coefficient of dimethylamine f_2 = activity coefficient of hexane x_1 = mole fraction of dimethylamine in the liquid phase x_2 = mole fraction of hexane in the liquid phase.					
Note: The authors, in a later paper (4), reported vapor pressure measurements on the same system which they considered to be more precise than measurements reported in this paper.					

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EXPERIMENTAL VALUES:

Constants for calculation of activity coefficients from the Redlich-Kister equations given below

T/K	A	B	C
223.15	1.474	-0.059	0.076
233.15	1.404	+0.002	0.124
243.15	1.294	+0.002	0.089
253.15	1.187	+0.027	0.086
263.15	1.085	+0.035	0.055
273.15	0.989	+0.048	0.057
283.15	0.892	+0.045	0.050
293.15	0.794	+0.042	0.048

$$\ln f_1 = A x_2^2 - B x_2^2(1 - 4 x_1) + C x_2^2(1 - 8 x_1 + 12 x_1^2)$$

$$\ln f_2 = A x_1^2 + B x_1^2(1 - 4 x_2) + C x_1^2(1 - 8 x_2 + 12 x_2^2)$$

where f_1 = activity coefficient of dimethylamine

f_2 = activity coefficient of hexane

x_1 = mole fraction of dimethylamine in the liquid phase

x_2 = mole fraction of hexane in the liquid phase.

COMPONENTS:			ORIGINAL MEASUREMENTS:
1. N-Methylmethanamine, (dimethylamine); C_2H_7N ; [124-40-3] 2. Decane; $C_{10}H_{22}$; [124-18-5]			Gerrard, W. <i>Solubility of Gases and Liquids</i> , <i>Plenum, 1976</i> , Chapter 10.
VARIABLES:			PREPARED BY:
Temperature, pressure			C.L. Young
EXPERIMENTAL VALUES:			
T/K	P/mmHg	P/ 10^5 Pa	Mole fraction of dimethylamine in liquid, $x(CH_3)_2NH$
283.15	100	0.133	0.068
	200	0.267	0.140
	300	0.400	0.235
	400	0.533	0.338
	500	0.667	0.456
	600	0.800	0.598
	700	0.933	0.755
288.15	760	1.013	0.840
	760	1.013	0.665
293.15	100	0.133	0.065
	200	0.267	0.110
	300	0.400	0.168
	400	0.533	0.225
	500	0.667	0.288
	600	0.800	0.352
	700	0.933	0.436
	760	1.013	0.501
298.15	760	1.013	0.390
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Amine was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured by a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was manually controlled to within 0.2K. The apparatus and procedure are described by Gerrard [1,2].		1. British Drug Houses or Cambrian Gases sample. 2. Purified and attested by conventional procedures.	
		ESTIMATED ERROR:	
		$\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler)	
		REFERENCES:	
		1. Gerrard, W. <i>J. Appl. Chem. Biotechnol.</i> <u>1972</u> , 22 623-650. 2. Gerrard, W. <i>Solubility of Gases and Liquids</i> . <i>Plenum Press, New York.</i> <u>1976</u> . Chapter 1.	

EXPERIMENTAL VALUES:			Mole fraction of dimethylamine in liquid, $x(\text{CH}_3)_2\text{NH}$
T/K	P/mmHg	P/10 ⁵ Pa	
Benzene; C ₆ H ₆ ; [71-43-2]			
293.15	760	1.013	0.541
Methylbenzene (toluene); C ₇ H ₈ ; [108-88-3]			
293.15	760	1.013	0.580
1,3-Dimethylbenzene (m-xylene); C ₈ H ₁₀ ; [108-38-3]			
283.15	100	0.133	0.070
	200	0.267	0.157
	300	0.400	0.262
	400	0.533	0.382
	500	0.667	0.517
	600	0.800	0.651
	700	0.933	0.790
293.15	760	1.013	0.862
	400	0.533	0.260
	500	0.667	0.336
	600	0.800	0.415
	700	0.933	0.504
	760	1.013	0.564
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
<p>Amine was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured by a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was manually controlled to within 0.2K. The apparatus and procedure are described by Gerrard [1,2].</p>		<p>1. British Drug Houses or Cambrian Gases sample.</p> <p>2. Purified and attested by conventional procedures.</p>	
		ESTIMATED ERROR:	
		<p>$\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler)</p>	
		REFERENCES:	
		<p>1. Gerrard, W. <i>J. Appl. Chem. Biotechnol.</i> <u>1972</u>, <i>22</i> 623-650.</p> <p>2. Gerrard, W. <i>Solubility of Gases and Liquids.</i> Plenum Press, New York. <u>1976</u>. Chapter 1.</p>	

COMPONENTS:

1. N-Methylmethanamine, (dimethylamine); C₂H₇N; [124-40-3]
2. Aromatic hydrocarbons

ORIGINAL MEASUREMENTS:

Gerrard, W.
Solubility of Gases and Liquids,
Plenum, 1976, Chapter 10.

VARIABLES:

Temperature, pressure

PREPARED BY:

C. L. Young

EXPERIMENTAL VALUES:

COMPONENTS:			ORIGINAL MEASUREMENTS:
1. N-Methylmethanamine (dimethylamine); C ₂ H ₇ N; [124-40-3] 2. 1,3,5-Trimethylbenzene (mesitylene); C ₉ H ₁₂ ; [108-67-8]			Gerrard, W. <i>Solubility of Gases and Liquids</i> , <i>Plenum</i> , 1976, Chapter 10.
VARIABLES:			PREPARED BY:
Pressure			C. L. Young
EXPERIMENTAL VALUES:			
T/K	P/mmHg	P/10 ⁵ Pa	Mole fraction of dimethylamine in liquid, x(CH ₃) ₂ NH
293.15	100	0.133	0.060
	200	0.267	0.124
	300	0.400	0.188
	400	0.533	0.255
	500	0.667	0.327
	600	0.800	0.404
	700	0.933	0.492
	760	1.013	0.549
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
Amine was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured by a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was manually controlled to within 0.2K. The apparatus and procedure are described by Gerrard [1,2].		1. British Drug Houses or Cambrian Gases sample. 2. Purified and attested by conventional procedures.	
		ESTIMATED ERROR:	
		$\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler)	
		REFERENCES:	
		1. Gerrard, W. <i>J. Appl. Chem. Biotechnol.</i> 1972, 22 623-650. 2. Gerrard, W. <i>Solubility of Gases and Liquids</i> . Plenum Press, New York. 1976. Chapter 1.	