

COMPONENTS: 1. Stibine; SbH_3 ; [7803-52-3] 2. Organic liquids	EVALUATOR: P. G. T. Fogg, School of Chemistry, Polytechnic of North London, Holloway, London, N7 8DB, UNITED KINGDOM. August 1983
CRITICAL EVALUATION: <p>Distribution constants for systems consisting of the gas and eight different liquids have been measured by Devyatykh <i>et al.</i> (1) using a chromatographic technique. (See comments under arsine evaluation and on compiled tables.) It is, however, unwise to equate these constants with Ostwald coefficients in order to calculate solubilities for a particular partial pressure of gas. Analogy with measurements on phosphine reported by these authors makes it likely that such estimates could be several hundred per cent too large. The data may perhaps be used to estimate relative solubilities of stibine in different solvents but such estimates are unlikely to be very precise.</p> <p><u>References</u></p> <p>1. Devyatykh, G. G.; Ezheleva, A. E.; Zorin, A. D.; Zueva, M. V. <i>Zh. Neorgan. Khim.</i> <u>1963</u>, <i>8</i>, 1307 (<i>Russ. J. Inorg. Chem.</i> <u>1963</u>, <i>8</i>, 678).</p>	

COMPONENTS: 1. Stibine; SbH_3 ; [7803-52-3] 2. Various liquids	ORIGINAL MEASUREMENTS: Devyatykh, G.G.; Ezhelova, A.E.; Zorin, A.D.; Zueva, M.V. <i>Russ. J. Inorg. Chem.</i> <u>1963</u> , <i>8</i> , 678-682															
VARIABLES: Temperature	PREPARED BY: P.G.T. Fogg															
EXPERIMENTAL VALUES: <table border="1" data-bbox="71 459 1181 822"> <thead> <tr> <th data-bbox="71 459 626 540">Solvent</th> <th data-bbox="626 459 892 540">Distribution constant $\text{vol}_{\text{SbH}_3} / \text{vol}_{\text{solvent}}$</th> <th data-bbox="892 459 1181 540">Heat of solution /kcal mol⁻¹</th> </tr> </thead> <tbody> <tr> <td data-bbox="71 560 626 620">2-Furancarboxaldehyde; $\text{C}_5\text{H}_4\text{O}_2$; [98-01-1]</td> <td data-bbox="626 560 892 620">25.2</td> <td data-bbox="892 560 1181 620">-4.1</td> </tr> <tr> <td data-bbox="71 641 626 701">Triethoxysilane; $\text{C}_6\text{H}_{16}\text{O}_3\text{Si}$; [998-30-1]</td> <td data-bbox="626 641 892 701">39.8</td> <td data-bbox="892 641 1181 701">-6.0</td> </tr> <tr> <td data-bbox="71 721 626 782">Silicic acid, tetraethyl ester; $\text{C}_8\text{H}_{20}\text{O}_4\text{Si}$; [78-10-4]</td> <td data-bbox="626 721 892 782">28.5</td> <td data-bbox="892 721 1181 782">-5.4</td> </tr> <tr> <td data-bbox="71 802 626 822">Silicone VKZh-94B</td> <td data-bbox="626 802 892 822">58.8</td> <td data-bbox="892 802 1181 822">-6.2</td> </tr> </tbody> </table> <p data-bbox="71 852 410 883">Temperature = 293.2 K.</p> <p data-bbox="71 913 1181 1064">Distribution constants were measured between 278.2 K and 323.2 K. The partial pressures of stibine at which these measurements were made were not stated. The total pressure of stibine and carrier gas was about 760 mmHg in each case. Distribution constants were reported at one temperature only but heats of solution, said to have been calculated from the variation of distribution constants with temperature, were given.</p> <p data-bbox="71 1084 1181 1135">If it is assumed that distribution constants vary with temperature according to equations of the form :</p>		Solvent	Distribution constant $\text{vol}_{\text{SbH}_3} / \text{vol}_{\text{solvent}}$	Heat of solution /kcal mol ⁻¹	2-Furancarboxaldehyde; $\text{C}_5\text{H}_4\text{O}_2$; [98-01-1]	25.2	-4.1	Triethoxysilane; $\text{C}_6\text{H}_{16}\text{O}_3\text{Si}$; [998-30-1]	39.8	-6.0	Silicic acid, tetraethyl ester; $\text{C}_8\text{H}_{20}\text{O}_4\text{Si}$; [78-10-4]	28.5	-5.4	Silicone VKZh-94B	58.8	-6.2
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Silicone VKZh-94B	58.8	-6.2														
AUXILIARY INFORMATION																
METHOD/APPARATUS/PROCEDURE: <p data-bbox="71 1302 626 1554">A chromatographic method was used. Temperatures were controlled to $\pm 0.5\text{K}$. The support phase consisted of Nichrome spirals. The carrier gas was either nitrogen or hydrogen. The volume, V_1, of the liquid phase was calculated from the weight of the column before and after filling with liquid and allowing to drain. The free volume, V_g, was equated</p> <p data-bbox="71 1554 626 1655">with the retention volume for hydrogen gas. The distribution constant, K, was calculated from the James and Martin equation:</p> $V_R = V_g + KV_1$ <p data-bbox="71 1735 626 1796">where V_R is the retention volume for stibine.</p>	SOURCE AND PURITY OF MATERIALS: <p data-bbox="646 1302 1181 1423">1. Prepared from SbCl_3 and aqueous sodium tetrahydroborate; purified by vacuum distillation; chromatographic analysis indicated about 5% H_2.</p> <p data-bbox="698 1443 1181 1524">H_2 & N_2: passed through activated carbon and through molecular sieve.</p> ESTIMATED ERROR: REFERENCES:															

COMPONENTS:

1. Stibine; SbH_3 ; [7803-52-3]
2. Various liquids.

ORIGINAL MEASUREMENTS:

Devyatikh, G.G.; Ezheleva, A.E.;
Zorin, A.D.; Zueva, M.V.

Russ. J. Inorg. Chem. 1963, *8*,
678-682.

EXPERIMENTAL VALUES:

$$\ln K = (-\Delta H/RT) + A$$

where K is the distribution constant for a temperature T , ΔH is the heat of solution in the solvent and A is a constant for the solvent, then distribution constants at any temperature in the range 278.2 K to 323.2 K may be estimated from a value at 293.2 K and the corresponding value of the heat of solution. The equation for K may be written in the form :

$$K = \exp [A + (B/T)]$$

The following values of A and B have been calculated by the compiler:

Solvent	A	B/K
2-Furancarboxaldehyde	-3.814	2064
Triethoxysilane	-6.620	3021
Silicic acid, tetraethyl ester	-5.924	2719
Silicone VKZh-94B	-6.573	3122

In the opinion of the compiler these distribution constants cannot be equated with Ostwald coefficients unless the assumption is made that equilibrium was established between gas and liquid phases under the conditions of the experiment.

In addition, possible adsorption of stibine at the stationary phase-carrier gas interface may have lowered the accuracy of the results.

COMPONENTS:		ORIGINAL MEASUREMENTS:	
1. Stibine; SbH_3 ; [7803-52-3] 2. Various liquids		Devyatykh, G. G.; Ezheleva, A. E.; Zorin, A. D.; Zueva, M. V. <i>Russ. J. Inorg. Chem.</i> <u>1963</u> , 8, 678-682.	
VARIABLES:		PREPARED BY:	
Temperature		P. G. T. Fogg	
EXPERIMENTAL VALUES:			
Solvent	P_{SbH_3} /mmHg	Distribution constant $\frac{\text{vol}_{\text{SbH}_3}}{\text{vol}_{\text{solvent}}}$	Heat of solution /kcal mol ⁻¹
2-Ethoxyethanol; $\text{C}_4\text{H}_{10}\text{O}_2$; [110-80-5]	0.3	40.7	-1.2
1,1'-oxybis[2-chloroethane]; $\text{C}_4\text{H}_8\text{Cl}_2\text{O}$; [111-44-4]	0.2	28.9	-3.5
Nitrobenzene; $\text{C}_6\text{H}_5\text{NO}_2$; [98-95-3]	0.2	22.9	-1.82
Liquid paraffin	0.3	39.7	-
Temperature = 293.2 K. 760 mmHg = 1 atm = 1.013×10^5 Pa. Distribution constants were measured between 278.2 K and 323.2 K with a total pressure of stibine and carrier gas of about 760 mmHg. Distribution constants were reported at one temperature only but heats of solution, said to have been calculated from the variation of distribution constants with temperature, were given. If it is assumed that distribution constants vary with temperature according to equations of the form: $\ln K = (-\Delta H/RT) + A$ where K is the distribution constant for a temperature T , ΔH is the heat <p style="text-align: right;">(cont.)</p>			
AUXILIARY INFORMATION			
METHOD/APPARATUS/PROCEDURE:		SOURCE AND PURITY OF MATERIALS:	
A chromatographic method was used. Temperatures were controlled to ± 0.5 K. The support phase consisted of Nichrome spirals. The carrier gas was either nitrogen or hydrogen. The volume, V_L , of the liquid phase was calculated from the weight of the column before and after filling with liquid and allowing to drain. The free volume, V_g , was equated with the retention volume for hydrogen gas. The distribution constant, K , was calculated from the James and Martin equation: $V_R = V_g + KV_L$ where V_R is the retention volume for stibine.		1. Prepared from SbCl_3 and aqueous sodium tetrahydroborate; purified by vacuum distillation; chromatographic analysis indicated about 5% H_2 . H_2 and N_2 : passed through activated carbon and through molecular sieve.	
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EXPERIMENTAL VALUES:

of solution of stibine in the solvent and A is a constant for the solvent, then distribution constants at any temperature in the range 278.2 K to 323.2 K may be estimated from a value at 293.2 K and the corresponding value of the heat of solution. The equation for K may be written in the form:

$$K = \exp [A + (B/T)].$$

The following values of A and B have been calculated by the compiler:

Solvent	A	B/K
2-Ethoxyethanol	1.645	604
1,1'-oxybis[2-chloroethane]	-2.647	1762
Nitrobenzene	0.006	916

In the opinion of the compiler these distribution constants can not be equated with Ostwald coefficients unless the assumption is made that equilibrium was established between gas and liquid phases under the conditions of the experiment.

In addition, possible adsorption of stibine at the stationary phase-carrier gas interface may have lowered the accuracy of the results.