- Propane; C₃H₈; [74-98-6]
- or Butane; C4H10; [106-97-8]
- or 2-Methylpropane; C_4H_{10} ; [75-28-5]

2. Organohalides

EVALUATOR:

Colin L. Young,

Department of Physical Chemistry,

University of Melbourne, Parkville, Victoria 3052,

Australia.

December 1984

CRITICAL EVALUATION:

In general data for these systems can only be evaluated by comparison of techniques and estimation of the reliability of a particular worker's data in general by comparisons on other systems rather than the system being evaluated. Very few systems in the title group have been studied by more than one worker.

Trichloromethane; CHCl₃; [67-66-3]

The solubility of the three gases in trichloromethane has been studied by Lebeau (1,2,3). The data of this worker for the solubility of propane, butane and 2-methylpropane in water are significantly different from the recommended values and hence data for the present systems are classified as doubtful.

Tetrachloromethane; CCl₄; [56-23-5]

The solubility of propane and butane in tetrachloromethane has been investigated by Hayduk and coworkers (4,5) and by Jadot (6). The system 2-methylpropane + tetrachloromethane has also been studied by Blais and Hayduk (5). The values of Jadot (6) were determined at very low partial pressures using gas chromatography. Extrapolation of the data to pressures of 101.3 kPa involves assuming Henry's law is obeyed between zero and 101.3 kPa and such an extrapolation would be expected to give values at 101.3 kPa which are slightly too large. In fact values at 101.3 kPa calculated from Jadot results are somewhat higher than the values of Hayduk and coworkers and therefore both sets of data are classified as tentative but the values of Jadot should be taken as applying to very low partial pressures.

Chlorobenzene; C₆H₅Cl; [108-90-7]

The solubility of the three gases in chlorobenzene have been studied by Hayduk and coworkers (5,7) using a well established volumetric method. The data appear to be of good precision and are classified as tentative.

Fluorocarbons

Fleury and Hayduk (4) and Thomsen and Gjaldbaek (8) studied the solubility of propane in tetradecafluorohexane and hexadecafluoroheptane, respectively. The mole fraction solubilities at 298.15 K differ by only about 5% being greater in hexadecafluoroheptane. This is consistent with trends of the solubility of simple hydrocarbon gases in alkanes. Both sets of values are classified as tentative.

Data of Gerrard

Gerrard (9,10) studied the solubilities of the three gases in several organohalides. These systems have not been studied by other workers. In view of the fact that the temperature dependence of the solubilities do not appear anomalous and that Gerrard's data on other systems are of, at least, moderate accuracy, his data for the current system are classified as tentative.

Data of Berlin et al.

The data of Berlin $et\ al.$ are rejected since they do not appear to correspond to gas solubility, the maximum pressure studied being considerably greater than the vapor pressure of propane, butane or 2-methylpropane at the experimental temperature. It is possible that the data refer to liquid-liquid equilibrium although not indicated as such in the original.

(cont.)

- 1. Propane; C₃H₈; [74-98-6]
- or Butane; C₄H₁₀; [106-97-8]
- or 2-Methylpropane; C4H10; [75-28-5]

2. Organohalides

EVALUATOR:

Colin L. Young,

Department of Physical Chemistry,

University of Melbourne, Parkville, Victoria 3052,

Australia.

December 1984

CRITICAL EVALUATION:

References

- 1. Lebeau, P. Bull. Acad. Roy. Belg. 1908, 300.
- 2. Lebeau, P. Comp. Rend. 1905, 140, 1454 and 1572.
- 3. Lebeau, P. Bull. Soc. Chim. [3] 1905, 33, 1137.
- 4. Fleury, D.; Hayduk, W. Can. J. Chem. Eng. 1975, 53, 195.
- 5. Blais, C.; Hayduk, W. J. Chem. Eng. Data 1983, 28, 181.
- 6. Jadot, R. J. Chim. Phys. 1972, 69, 1036.
- 7. Hayduk, W.; Castaneda, R. Can. J. Chem. Eng. 1973, 51, 353.
- 8. Thomsen, E. S.; Gjaldbaek, J. C. Acta Chem. Scand. 1963, 17, 134.
- Gerrard, W. Solubility of Gases and Liquids, Plenum, New York, 1976, Chapter 12.
- 10. Gerrard, W. J. Appl. Chem. Biotechnol. <u>1973</u>, 23, 1.
- Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Tsybnlevskii,
 A. M. Zh. Fiz. Khim. <u>1977</u>, 51, 767.

COMPONENTS:		ORIGINAL MEASUREMENTS:
(1)	Propane; C ₃ H ₈ ; [74-98-6]	Lebeau, P.
(2)	Water, Benzene, Ethanol, Diethylether, Chloroform, Turpentine	Compt. Rend. 1905, 140, 1454-6 and 1572. Bull. Soc. Chim. [3] 1905, 33, 1137-9.
VARIA	BLES:	PREPARED BY:
	T/K = 290.8 - 294.8 p/kPa = 100.4 - 100.9	H. L. Clever

Temperature		Pressure ^a	Solubility
t/°C	T/K	p/mmHg	Volume propane/100 Volumes Solvent
Water;	H ₂ O;	[7732-18-5]	
17.8	291.0	753	6.5
Benzen	е; С ₆ Н ₆	0; [71-43-2]	
		757	1452
Ethano	1; C ₂ H ₆	0; [64-17-5]	
16.6	290.8	754	790
1,1'-0	xybiset	hane or dieth	ylether; C ₄ H ₁₀ O; [60-29-7]
16.6	290.8	757	926
Chloro	form or	trichloromet	hane; CHC1 ₃ ; [67-66-3]
		757	1299
Oil of	turpen	tine	
17.7	290.9	757	1587

a Not clear whether this is total pressure or propane partial pressure. It is probably total pressure.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE: SOURCE AND PURITY OF MATERIALS: Details not given. (1) Propane. Prepared by author rropane. Prepared by author from carefully purified propyl iodide by reaction with sodium in liquid ammonia. Melting point/°C = -195 Boiling point/°C = -44.5 Critical temperature/°C = 102. The data are reported in both papers. (2) Solvents. No information. ESTIMATED ERROR: REFERENCES:

260 Organo	nandes
COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Propane; C ₃ H ₈ ; [74-98-6]	Jadot, R.
(2) Tetrachloromethane; CCl ₄ ; [56-23-5]	J. Chim. Phys. <u>1972</u> , 69, 1036-40
/ARIABLES: T/K: 298.15 P/kPa: 101.3	PREPARED BY: C.L. Young
XPERIMENTAL VALUES:	
T/K Henry's Law Constant, H/atm	Mole fraction $^+$ # Δ H $^{\infty}$ at partial pressure /cal mol $^{-1}$ of 101.3 kPa, $x_{\rm C_3H_8}$ (/J mol $^{-1}$)
298.15 11.648	0.08585 501 (2096)
AUXILIARY	INFORMATION
METHOD APPARATUS/PROCEDURE:	SOURCE AND PURITY OF MATERIALS:
The conventional gas chromatographic technique was used. The carrier gas was helium. The value of Henry's law constant was calculated from the retention time. The value applies to very low partial pressures of gas and there may be a substantial difference from that measured at l atm. pressure. There is also considerable uncertainty in the value of Henry's constant since no	No details given
allowance was made for surface adsorption.	ESTIMATED ERROR:
	\$m/V - +0 05 - \$11 - +20
	$\delta T/K = \pm 0.05; \delta H = \pm 2\%$
	REFERENCES:

(1) Propane; C₃H₈; [74-98-6]

(2) Tetrachloromethane (carbon tetrachloride); CCl₄; [56-23-5]

ORIGINAL MEASUREMENTS:

Fleury, D.; Hayduk, W.

Can. J. Chem. Eng. 1975, 53,
195-199.

VARIABLES:

COMPONENTS:

T/K: 258.15-323.15 P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

<i>T</i> /K	Ostwald Coefficient ¹ L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction 1
258.15	76.0	80.4	0.254 (0.2536) ³
273.15	42.5	42.5	0.155 (0.1554)
298.15	21.9	20.1	0.0813 (0.0811)
323.15	13.6	11.5	0.0497 (0.0497)

^l Original data.

 3 The mole fraction solubility of the original data was used to determine the following equations for $\Delta {\rm G}^{\circ}$ and $\ln\,x_1^{}$ and table of smoothed values:

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln x_1 = 597.65 T - 77.797 T \ln T - 39807$$

 $\ln x_1 = 4787.9/T + 9.3573 \ln T - 71.885$

Std. deviation for $\Delta G^{\circ} = 4.6 \text{ J mol}^{-1}$

<i>T</i> /K	ΔG°/J mol-1		<i>T/</i> K	ΔG°/J mol ⁻¹	x_1
258.15	2944	0.2536	298.15	6227	0.0811
273.15	4228	0.1554	303.15	6607	0.0727
283.15	5048	0.1171	313.15	7347	0.0595
293.15	5841	0.0910	323.15	8063	0.0497

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmospheric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable The solubility was calculated rate. from the constant slope of volume of gas dissolved and volume of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS:

- Matheson Co. Specified as instrument grade of minimum purity 99.5 per cent.
- Fisher Scientific. Specified minimum purity 99.0 per cent.

ESTIMATED ERROR:

 $\delta T/K = 0.1$ $\delta x_1/x_1 = 0.01$

REFERENCES:

 Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.
 J. Phys. Chem. 1971, 61, 1078.

² Calculated by compiler.

- (1) Propane; C₃H₈; [74-98-6]
- (2) 1,1'-Oxybis, 2-Chloroethane (Chlorex); C₄H₈Cl₂O; [111-44-4]

ORIGINAL MEASUREMENTS:

Ezheleva, A.E.; Zorin, A.D.

Tr. Khim. Khim. Tech. (Gorkii) 1961, 1, 37-40.

VARIABLES:

T/K: 303.15-343.15

P/kPa: 101.325 and above

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

<i>T/</i> K	Ostwald Coefficient ² L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction 1
303.15	8.42	7.54	0.039 (0.0398)3
313.15	7.03	6.09	0.032 (0.0316)
323.15	5.82	4.88	0.026 (0.0254)
333.15	4.78	3.88	0.021 (0.0208)
343.15	3.89	3.07	0.0168(0.0172)

¹Original data given as the inverse of Henry's constant which is equivalent to mole fraction at a gas partial pressure of 101.325 kPa.

$$\ln x_1 = 2186.8/T - 10.437$$

Correlation coefficient = 0.9982

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

The apparatus consisted of a two-chamber, rocking device with separate gas and liquid chambers joined by two tubes and microvalves. The gas chamber was equipped with a pressure gauge. After evacuation, gas and deaerated solvent were separately charged, and then contacted by opening the microvalves and by rocking. The solubility was calculated from a knowledge of the volume of the solvent charged, and the initial and final gas pressures.

The solvent was considered non-volatile and the gas pressure was considered to be the total pressure.

SOURCE AND PURITY OF MATERIALS:

- Source and purity not given. Gas purified by low temperature fractionation and analyzed by gas chromatography.
- Source and purity not given. Refractive index measured:

$$n_D^{20} = 1.4535$$

ESTIMATED ERROR:

 $\delta T/K = 0.05$

 $\delta x_1/x_1 = 0.05$

(estimated by compiler)

REFERENCES:

 $^{^2\}mathrm{Ost}$ wald and Bunsen coefficients calculated by compiler using authors assumption that solvent is non-volatile.

³From equation of smoothed data:

- (1) Propane; C₃H₈; [74-98-6]
- (2) Chlorobenzene; C₆H₅Cl; [108-90-7]

ORIGINAL MEASUREMENTS:

Hayduk, W.; Castañeda, R. Can. J. Chem. Eng. 1973, 51,

353-358.

VARIABLES:

T/K: 273.15-323.15

P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

T/K	Ostwald Coefficient ¹ L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction ¹
273.15	25.4	25.4	0.1034 (0.1029) ³
298.15	14.16	12.97	0.0570 (0.0575)
323.15	9.12	7.71	0.3053 (0.0352)

- Original data.
- ² Calculated by compiler.
- 3 The mole fraction solubility of the original data was used to determine the following equations for $\Delta {\rm G}^{\circ}$ and $\ln~x_1$ and table of smoothed values:

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln x_{1} = 76.625 T - 15766$$

$$\ln x_7 = 1896.3/T - 9.2167$$

Std. deviation for $\Delta G^{\circ} = 18.8 \text{ J mol}^{-1}$; Correlation coefficient = 0.9999

	ΔG°/J mol-1	x	<i>T</i> /K	ΔG°/J mol-1	$\frac{x_1}{}$
273.15	5164	0.1029	303.15	7463	0.0518
283.15	5930	0.0805	313.15	8229	0.0424
293.15	6697	0.0641	323.15	8995	0.0352
298.15	7080	0.0575			

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. A constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmospheric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable rate. The solubility was calculated from the constant slope of volume of gas dissolved and volume of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS;

- Matheson Co. Specified as instrument grade of minimum purity 99.5 per cent.
- Fisher. Fisher Certified Reagent grade of specified purity 99.7 per cent.

ESTIMATED ERROR:

 $\delta T/K = 0.1$

 $\delta x_1/x_1 = 0.01$

REFERENCES:

 Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.
 J. Phys. Chem. 1971, 61, 1078.

EXPERIMENTAL VALUES:

Total pressure = 101.3 kPa.

T/K	Mole ratio	Mole fraction of propane #
268.2	0.214	0.176
273.2	0.186	0.157
278.2	0.162	0.139
283.2	0.141	0.124
293.2	0.116	0.104
298.2	0.106	0.0958

AUXILIARY INFORMATION

METHOD 'APPARATUS/PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS;

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler).

REFERENCES:

 $^{^{\}sharp}$ Calculated by compiler.

- (1) Propane; C₃H₈; [74-98-6]
- (2) Tetradecafluorohexane
 (perfluorohexane); C₆F₁₄;
 [355-42-0]

ORIGINAL MEASUREMENTS:

Fleury, D.; Hayduk, W.

Can. J. Chem. Eng. <u>1975</u>, 53, 195-199.

VARIABLES:

T/K: 258.15-323.15

P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

<i>T</i> /K	Ostwald Coefficient ¹ L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction x_1
258.15	15.5	16.4	0.124 (0.124) ³ 0.0731 (0.0734) 0.0480 (0.0478) 0.0308 (0.0308)
278.15	9.03	8.87	
298.15	5.90	5.41	
323.15	3.99	3.37	

- 1 Original data.
- ² Calculated compiler.
- The mole fraction solubility of the original data was used to determine the following equations for ΔG° and $\ln x_1$ and table of smoothed values:

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln x_1 = 321.95 T - 37.053 T \ln T - 25507$$

 $\ln x_1 = 3067.9/T - 38.724 + 4.4567 \ln T$

Std. deviation for $\Delta G^{\circ} = 10.1 \text{ J mol}^{-1}$

T/K	ΔG°/J mol ⁻¹	<u> </u>	<i>T</i> /K	ΔG°/J mol-1	x_1
258.15	4484	0.1238	298.15	7539	0.04775
273.15	5655	0.0829	303.15	7907	0.0434
278.15	6039	0.0734	313.15	8633	0.0363
293.15	7169	0.0528	323.15	9347	0.03084

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. A constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmospheric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable rate. The solubility was calculated from the constant slope of volume of gas dissolved and volume of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS:

- 1. Matheson Co. Specified as instrument grade of minimum purity 99.5 per cent.
- PCR Inc. Specified minimum purity 99.0 per cent.

ESTIMATED ERROR:

 $\delta T/K = 0.1$

 $\delta x_1/x_1 = 0.01$

REFERENCES:

 Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.
 J. Phys. Chem. 1971, 61, 1078.

COMPONENTS: ORIGINAL MEASUREMENTS: Gerrard, W. (1) Propane; C₃H₈; [74-98-6] (2) 1-Bromo-3-methylbenzene J. Appl. Chem. Biotechnol. (m-bromotoluene); C7H7Br; <u>1973</u>, 23, 1-17. [591-17-3] VARIABLES: PREPARED BY: T/K: 268.2-293.2

P/kPa: 101.3

C. L. Young

EXPERIMENTAL VALUES:

Total pressure = 101.3 kPa

r/k	Mole ratio	Mole fraction of propane
268.2	0.150	0.130
273.2	0.132	0.117
278.2	0.116	0.104
283.2	0.103	0.0937
293.2	0.083	0.0766

AUXILIARY INFORMATION

METHOD /APPARATUS / PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS:

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3$ % (estimated by compiler).

REFERENCES:

[#] Calculated by compiler.

- (1) Propane; C₃H₈; [74-98-6]
- (2) Hexadecafluoroheptane
 (Perfluoroheptane); C₇F₁₆;
 [335-57-9]

ORIGINAL MEASUREMENTS:

Thomsen, E.S.; Gjaldbaek, J.C. Acta Chem. Scand. 1963, 17, 134-138.

VARIABLES:

T/K: 298.15 P/kPa: 101.325

PREPARED BY:

E.S. Thomsen, W. Hayduk

EXPERIMENTAL VALUES:

T/K	Ostwald Coefficient ²	Bunsen Coefficient 1	Mole Fraction ²
	L/cm ³ cm ⁻³	a/cm³ (STP)cm-³atm-1	
298.15	5.67	5.17	0.0505

¹Original data.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

The method utilizes a combined glass manometer and bulb enclosed in an air thermostat which is shaken until equilibrium is established. Mercury is used for calibrating the volumes and as the confining liquid. Details in reference 1.

The absorbed gas volume is calculated from the initial dry gas, and final solvent vapor-saturated gas volume. The amount of solvent is determined by measuring the mass of mercury displaced.

SOURCE AND PURITY OF MATERIALS:

- 1. Phillips Petroleum Co.
 Specified as research grade and
 GC analysis indicated 0.1 per
 cent air and 0.03 per cent
 ethane impurities.
- Source not given. Fractionated to yield boiling point t/°C 82.55-82.56.

ESTIMATED ERROR:

$$\delta T/K = 0.05$$

$$\delta x_1/x_1 = 0.015$$

REFERENCES:

Gjaldbaek, J.C.
 Acta Chem. Scand. <u>1952</u>, 6, 623.

²Calculated by compilers using a real gas molar volume.

COMPONENTS: (1) Propane; C₃H₈; [74-98-6] Gerrard, W. (2) 1-Iodooctane; C₈H₁₇I; J. Appl. Chem. Biotechnol. [629-27-6] 1973, 23, 1-17. VARIABLES: T/K: 268.2-293.2 P/kPa: 101.3

EXPERIMENTAL VALUES:

Total pressure = 101.3 kPa

г/к	Mole ratio	Mole fraction of propane
I/K	Mole latio	More fraction of propane
68.2	0.261	0.207
73.2	0.229	0.186
278.2	0.198	0.165
283.2	0.172	0.147
293.2	0.129	0.114

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS:

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1;$ $\delta x/x = \pm 3\%$ (estimated by compiler).

REFERENCES:

1. Gerrard, W.

J. Appl. Chem. Biotechnol. 1972, 22, 623.

[#] Calculated by compiler.

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Butane; C ₄ H ₁₀ ; [106-97-8]	Lebeau, P.
(2) Water; H ₂ O; [7732-18-5] Ethanol; C ₂ H ₆ O; [64-17-5] Diethylether; C ₄ H ₁₀ O; [60-29-7] Chloroform; CHCl ₃ ; [67-66-3]	Bull. Acad. Roy. Belg. <u>1908</u> , 300-4.
VARIABLES:	PREPARED BY:
T/K = 290, 291 p/kPa = 102.9 - 104.8	H. L. Clever

Temperature		Pressure ^a	Solubility		
t/°C	<i>T</i> /K	p/mmHg	Volume Butane/Volume		Solvent
Water					
17	290	772		0.15	
Ethano:	1				
17	290	775		18.83	
Diethy:	lether	or 1'1'-oxyb	isethane		
18	291	773		29.8	
Chloro	form or	trichlorome	thane		
17	290	786		32.5	

Not clear whether this is total pressure or butane partial pressure. It is probably the total pressure.

	AUXILIARY INFORMATION
THOD/APPARATUS/PROCEDURE:	SOURCE AND PURITY OF MATERIALS:
Details not given.	(1) Butane. Prepared by author by the reaction of sodium in liquid ammonia on butyl iodide. The normal boiling point is 0.5 °C, and the critical temperature is 151-2 °C.
	(2) Solvents. No information.
	ESTIMATED ERROR:
	REFERENCES:

- (1) Butane; C₄H₁₀; [106-97-8]
- (2) Tetrachloromethane (carbon tetrachloride); CCl₄; [56-23-5]

ORIGINAL MEASUREMENTS:

Blais, C.; Hayduk, W.

J. Chem. Eng. Data 1983, 28, 181-184.

VARIABLES:

T/K: 298.15,323.15 P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

T/K	Ostwald Coefficient ¹	Bunsen Coefficient ²	Mole Fraction 1
	L/cm ³ cm ⁻³	α/cm³ (STP)cm-³atm-1	<u> </u>
298.15 323.15	122.7 52.0	112.4 43.95	0.339 (0.3390) ³ 0.167 (0.1670)

¹Original data.

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \quad \text{ln } x_1 = 721.51 \ T \quad \text{ln } T - 4022.1 \ T$$

$$\text{ln } x_1 = 49.0169 - 8.79294 \text{ln } T$$

<i>T/</i> K	10 ⁻⁴ ΔG°/J mol ⁻¹	
298.15	2.646	0.3390
303.15 313.15	3.055 3.889	0.2929 0.2202
323.15	4.746	0.1670

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. A constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmospheric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable rate. The solubility was calculated from the constant slope of volume of gas dissolved and volume of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS:

- Liquid Carbonic. Pure grade of minimum purity 99.0 per cent.
- Canlab (J.T. Baker Company). Spectrophotometric grade of minimum specified purity 99.9 per cent.

ESTIMATED ERROR:

 $\delta T/K = 0.1$

 $\delta x_1/x_1 = 0.01$

REFERENCES:

 Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.
 J. Phys. Chem. <u>1957</u>, 61, 1078.

²Calculated by compiler.

 $^{^3 \, {\}rm The}$ mole fraction solubility of the original data was used to determine the following equations for $\Delta {\rm G}^{\circ}$ and ln x_1 and table of smoothed values:

	271
COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Butane; C ₄ H ₁₀ ; [106-97-8]	Jadot, R.
(2) Tetrachloromethane; CCl ₄ ; [54-23-5]	J. Chim. Phys. <u>1972</u> , 69, 1036-40
VARIABLES:	PREPARED BY: C.L. Young
T/K: 298.15 P/kPa: 101.3	C.H. Foung
P/RPA: 101.3	
EXPERIMENTAL VALUES:	
T/K Henry's Law Constant, H/atm	Mole fraction $^+$ # Δ H $^{\infty}$ at partial pressure /cal mol $^{-1}$ of 101.3 kPa, $x_{\rm C_4H_{10}}$ (/J mol $^{-1}$)
298.15 2.785	0.3591 602 (2519)
# Excess partial molar enthalpy	of solution at infinite dilution.
AUXILIARY	INFORMATION
METHOD/APPARATUS/PROCEDURE:	SOURCE AND PURITY OF MATERIALS:
The conventional gas chromatographic technique was used. The carrier gas was helium. The value of Henry's law constant was calculated from the retention time. The value applies to very low partial pressures of gas and there may be a substantial difference from that measured at l atm. pressure. There is also considerable uncertainty in the value of Henry's constant since no	No details given.
allowance was made for surface	ESTIMATED ERROR:
adsorption.	$\delta T/K = \pm 0.05; \ \delta H = \pm 2\%$
	REFERENCES:

COMPONENTS: ORIGINAL MEASUREMENTS: (1) Butane; C₄H₁₀; [106-97-8] Gerrard, W. (2) 2,2,2-Trichloroethanol; C₂H₃Cl₃O; J. Appl. Chem. Biotechnol. [115-20-8] Dichloroacetic acid; C2H2Cl2O2; 1973, 23, 1-17. [79-43-6]1,2-Dibromoethane; C2H4Br2; 1106-93-41 VARIABLES: PREPARED BY: T/K: 278.2-298.2 C. L. Young P/kPa: 101.3

EXPERIMENTAL VALUES:

Total pressure = 101.3 kPa

T/K	Mole ratio	Mole fraction of butane#	
	2,2,2-Trichloroethanol;	C ₂ H ₃ Cl ₃ O; [115-20-8]	
278.2	0.370	0.270	
283.2	0.250	0.200	
293.2	0.115	0.103	
298.2	0.100	0.0909	
	Dichloroacetic acid; C;	H ₂ Cl ₂ O ₂ ; [79-43-6]	
298.2	0.0667	0.0625	
	1,2-Dibromoethane; C ₂ H ₄	Br ₂ ; [106-93-4]	
278.2	1.81	0.644	

[#] Calculated by compiler.

AUXILIARY INFORMATION

METHOD /APPARATUS / PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS:

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler).

REFERENCES:

- 1. Gerrard, W.
 - J. Appl. Chem. Biotechnol. 1972, 22, 623.

- (1) Butane; C₄H₁₀; [106-97-8]
- (2) Chlorobenzene; C₆H₅Cl; [108-90-7]

ORIGINAL MEASUREMENTS:

Blais, C.; Hayduk, W. J. Chem. Eng. Data 1983,

28, 181-184.

VARIABLES:

T/K: 298.15,323.15

P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

T/K	Ostwald Coefficient ¹ L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction ¹
298.15	85.4	78.24	0.269 (0.2690) ³ 0.131 (0.1310)
323.15	37.3	31.53	

¹⁰riginal data.

 $^3{\rm The}$ mole fraction solubility of the original data was used to determine the following equations for $\Delta {\rm G}^\circ$ and ln x_1 and table of smoothed values:

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln x_1 = 733.24 \ T \ln T - 4070.0 \ T$$

$$\ln x_1 = 49.5998 - 8.93585 \ln T$$

<i>T</i> /K	10-4ΔG°/J mol-1	x 1
298.15	3.212	0.2690
303.15	3.636	0.2319
313.15	4.501	0.1735
323.15	5.390	0.1310

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. A constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmospheric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable rate. The solubility was calculated from the constant slope of volume of gas dissolved and $\bar{\text{volume}}$ of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS:

- Liquid Carbonic. Pure grade of minimum purity 99.0 per cent.
- Canlab (Matheson, Coleman and Bell). Specified minimum purity 98.0 per cent.

ESTIMATED ERROR:

 $\delta T/K = 0.1$

 $\delta x_1/x_1 = 0.01$

REFERENCES:

 Clever, H.L.; Battino, R.; Saylor, J.H.: Gross, P.M.
 J. Phys. Chem. 1957, 61, 1078.

²Calculated by compiler.

COMPONENTS: (1) Butane; C₄H₁₀; [106-97-8] (2) Iodobenzene; C₆H₅I; [591-50-4] VARIABLES: T/K: 278.2-293.2 ORIGINAL MEASUREMENTS: Gerrard, W. J. Appl. Chem. Biotechnol. 1973, 23, 1-17.

EXPERIMENTAL VALUES:

P/kPa: 101.3

Total pressure = 101.3 kPa

T/K	Mole ratio	Mole fraction of propane
278.2	3.55	0.780
283.2	0.612	0.380
293.2	0.280	0.219

AUXILIARY INFORMATION

METHOD /APPARATUS / PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS:

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler).

REFERENCES:

[#] Calculated by compiler.

EXPERIMENTAL VALUES:

P/kPa: 101.3

Total pressure = 101.3 kPa

T/K	Mole ratio	Mole fraction of butane [#]
283.2	0.952	0.488
293.2	0.431	0.301

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS:

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1;$ $\delta x/x = \pm 3\%$ (estimated by compiler).

REFERENCES:

[#] Calculated by compiler.

COMPONENTS: (1) Butane; C₄H₁₀; [106-97-8] (2) 1-Iodooctane; C₈H₁₇I; [629-27-6] VARIABLES: T/K: 278.2-293.2 P/kPa: 101.3 ORIGINAL MEASUREMENTS: Gerrard, W. J. Appl. Chem. Biotechnol. 1973, 23, 1-17. PREPARED BY: C. L. Young

EXPERIMENTAL VALUES:

Total pressure = 101.3 kPa

/K	Mole ratio	Mole fraction of butane
8.2	3.88	0.795
3.2	1.64	0.621
93.2	0.74	0.425

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured using a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was controlled to within 0.2 K. The apparatus and procedure are described by Gerrard, ref. (1).

SOURCE AND PURITY OF MATERIALS:

No details given except that "all compounds were purified by conventional procedures".

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler).

REFERENCES:

[#] Calculated by compiler.

EXPERIMENTAL VALUES:

Temperature		Pressurea	Solubility
t/°C	<i>T</i> /K	p $/ mmHg$	Volume Isobutane/Volume Solvent
Water		·	
17	290	772	0.13
Ethan	ol		
17	290	775	13.2
Diethy	ylether	or 1'1'-oxyb	isethane
18	291	773	27.9
Chlore	oform or	trichlorome	thane
17	290	786	39.5
			2710

Not clear whether this is total pressure or isobutane partial pressure. It is probably the total pressure.

AUXILIARY INFORMATION

AUXILIARY	INFORMATION
METHOD/APPARATUS/PROCEDURE: Details not given.	SOURCE AND PURITY OF MATERIALS: (1) Isobutane. Prepared by the author by the reaction of sodium or calcium in liquid ammonia on isobutyl chloride. The normal boiling point is -10.5 °C and the critical temperature is 134-5 °C. (2) Solvents. No information.
	ESTIMATED ERROR: REFERENCES:

- (1) 2-Methylpropane (isobutane); C_4H_{10} ; [75-28-5]
- (2) Tetrachloromethane (carbon tetrachloride); CCl₄; [56-23-5]

ORIGINAL MEASUREMENTS:

Blais, C.; Hayduk, W. J. Chem. Eng. Data <u>1983</u>, 28, 181-184.

VARIABLES:

T/K: 298.15,323.15

P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

T/K	Ostwald Coefficient ¹ L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction ¹	
298.15	76.5	70.09	0.231 (0.2310) ³	
323.15	39.9	33.73	0.132 (0.1320)	

¹Original data.

 $^3{\rm The}$ mole fraction solubility of the original data was used to determine the following equations for $\Delta{\rm G}^\circ$ and ln x_1 and table of smoothed values:

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -R T \ln x_1 = 600.71 T \ln T - 3304.8 T$$

 $\ln x_1 = 40.2754 - 7.32078 \ln T$

<i>T/</i> K	10-4ΔG°/J mol-1	x
298.15	3.512	0.2380
303.15	3.874	0.2107
313.15	4.612	0.1662
323.15	5.369	0.1320

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. A constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmospheric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable rate. The solubility was calculated from the constant slope of volume of gas dissolved and volume of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS:

- Liquid Carbonic. Pure grade of minimum purity 99.0 per cent.
- Canlab (J.T. Baker Company). Spectrophotometric grade of minimum specified purity 99.9 per cent.

ESTIMATED ERROR:

 $\delta T/K = 0.1$ $\delta x_1/x_1 = 0.01$

REFERENCES:

 Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M.
 J. Phys. Chem. <u>1957</u>, 61, 1078.

²Calculated by compiler.

- (1) 2-Methylpropane (isobutane); $C_4^{H}_{10}$; [75-28-5]
- (2) 1,1 -Oxybis, 2-Chloroethane (Chlorex); C₄H₈Cl₂O; [111-44-4]

ORIGINAL MEASUREMENTS:

Ezheleva, A.E.; Zorin, A.D. Tr. Khim. Khim. Tech. (Gorkii) 1961, 1, 37-40.

VARIABLES:

T/K: 303.15-343.15

P/kPa: 101.325 and above

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

<i>T/</i> K	Ostwald Coefficient ² L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm^3 (STP) cm^{-3} atm ⁻¹	Mole Fraction ¹
303.15	13.3	11.8	0.0610(0.0607)3
313.15	11.6	9.95	0.05224(0.0520)
323.15	10.1	8.38	0.0447(0.0448)
333.15	8.61	6.92	0.0375(0.0387)
343.15	8.08	6.29	0.0345(0.0337)

¹Original data given as the inverse of Henry's constant which is equivalent to mole fraction at a gas partial pressure of 101.325 kPa.

$$\ln x_1 = 24.349 - 4.7515 \ln T$$

Correlation coefficient = 0.9961

"Value corrected to read as shown; original value of $x_1 = 0.0022$ appears to be a misprint.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

The apparatus consisted of a two-chamber, rocking device with separate gas and liquid chambers joined by two tubes and microvalves. The gas chamber was equipped with a pressure gauge. After evacuation, gas and deaerated solvent were separately charged, and then contacted by opening the microvalves and by rocking. The solubility was calculated from a knowledge of the volume of the solvent charged, and the initial and final gas pressures.

The solvent was considered non-volatile and the gas pressure was considered to be the total pressure.

SOURCE AND PURITY OF MATERIALS:

- Source and purity not given. Gas purified by low temperature fractionation and analyzed by gas chromatography.
- Source and purity not given. Refractive index measured:

$$n_D^{20} = 1.4535$$

ESTIMATED ERROR:

 $\delta T/K = 0.05$

 $\delta x_1/x_1 = 0.05$

(estimated by compiler)

REFERENCES:

²Ostwald and Bunsen coefficients calculated by compiler using author's assumption that solvent is non-volatile.

³From equation of smoothed data:

- (1) 2-Methylpropane (isobutane); $C_4H_{10}; [75-28-5]$
- (2) Chlorobenzene; C₆H₅Cl; [108-90-7]

ORIGINAL MEASUREMENTS:

Blais, C.; Hayduk, W. J. Chem. Eng. Data 1983, 28, 181-184.

VARIABLES:

T/K: 298.15,323.15

P/kPa: 101.325

PREPARED BY:

W. Hayduk

EXPERIMENTAL VALUES:

T/K	Ostwald Coefficient ¹ L/cm ³ cm ⁻³	Bunsen Coefficient ² α/cm ³ (STP)cm ⁻³ atm ⁻¹	Mole Fraction ¹	
298.15	45.1	41.32	0.162 (0.1620) ³	
323.15	23.1	19.53	0.0853 (0.0853)	

¹Original data.

$$\Delta G^{\circ}/J \text{ mol}^{-1} = -RT \ln x_1 = 653.658 \ T \ln T - 3574.93 \ T$$

 $\ln x_1 = 43.5669 - 7.9660 \ln T$

<i>T</i> /K	10 ⁻⁴ ΔG°/J mol ⁻¹	
298.15 303.15	4.453	0.1620 0.1419
313.15	4.857 5.682	0.1096
323.15	6.527	0.08530

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A volumetric method using a glass apparatus was employed. Degassed solvent contacted the gas while flowing as a thin film, at a constant rate, through an absorption spiral into a solution buret. A constant solvent flow was obtained by means of a calibrated syringe pump. The solution at the end of the spiral was considered saturated. Dry gas was maintained at atmosphe- ESTIMATED ERROR: ric pressure in a gas buret by mechanically raising the mercury level in the buret at an adjustable rate. The solubility was calculated from the constant slope of volume of gas dissolved and volume of solvent injected.

Degassing was accomplished using a two stage vacuum process described by Clever et al. (1).

SOURCE AND PURITY OF MATERIALS:

- Liquid Carbonic. Pure grade of minimum purity 99.0 per cent.
- Canlab (Matheson, Coleman and Bell). Specified minimum purity 98.0 per cent. 2.

$$\delta T/K = 0.1$$

$$\delta x_1/x_1 = 0.01$$

REFERENCES:

Clever, H.L.; Battino, R.; Saylor, J.H.; Gross, P.M. J. Phys. Chem. 1957 61,

²Calculated by compiler.

 $^{^3}$ The mole fraction solubility of the original data was used to determine the following equations for ΔG° and $\ln x_1$ and table of smoothed values:

- (1) 2-Methylpropane, (isobutane); C_4H_{10} ; [75-28-5]
- (2) Bromobenzene; C₆H₅Br; [108-86-1]

ORIGINAL MEASUREMENTS:

Gerrard, W.

Solubility of Gases and Liquids, Plenum, New York, 1976, Chapter 12.

VARIABLES:

T/K: 273.15

P/kPa: 13.3-101.3

PREPARED BY:

C.L. Young

EXPERIMENTAL VALUES:

T/K	P/mmHg	P/kPa	Mole fraction of 2-methyl propane in liquid, ${}^{x}C_{4}{}^{H}_{10}$
275.13	100	13.3	0.033
	200	26.7	0.068
	300	40.0	0.108
	400	53.3	0.154
	500	66.7	0.208
	600	80.0	0.270
	700	93.3	0.360
	760	101.3	0.435

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured by a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was manually controlled to within 0.2K The apparatus and procedure are described by Gerrard (1, 2).

SOURCE AND PURITY OF MATERIALS:

No details given.

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler)

REFERENCES:

- Gerrard, W.
 J. Appl. Chem. Biotechnol. 1972, 22, 623-650.
- Gerrard, W.
 Solubility of Gases and Liquids,
 Plenum Press, New York, 1976,
 Chapter 1.

COMPONENTS: (1) 2-Methylpropane, (isobutane); C4H10; [75-28-5] (2) 1-Bromooctane; C8H17Br; [111-83-1] VARIABLES: T/K: 273.15 P/kPa: 13.3-101.3 ORIGINAL MEASUREMENTS: Gerrard, W. Solubility of Gases and Liquids Plenum, New York, 1976, Chapter 12.

EXPERIMENTAL	VALUES.
CAFERINGNIAL	VALUES:

212 512-124-1322 1-124-132-132-132-132-132-132-132-132-132-132				
	T/K	P/mmHg	P/kPa	Mole fraction of 2-methylpropane in liquids, $x_{C_4H_{10}}$
	273.15	100	13.3	0.070
		200	26.7	0.138
		300	40.0	0.208
		400	53.3	0.282
		500	66.7	0.355
		600	80.0	0.430
		700	93.3	0.516
		760	101.3	0.580
i				

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

Gas was passed into a known weight of pure liquid in a bubbler tube at a total pressure measured by a manometer assembly. The amount of absorbed gas was estimated by weighing. The temperature was manually controlled to within 0.2K. The apparatus and procedure are described by Gerrard (1,2).

SOURCE AND PURITY OF MATERIALS:

No details given.

ESTIMATED ERROR:

 $\delta T/K = \pm 0.1$; $\delta x/x = \pm 3\%$ (estimated by compiler)

REFERENCES:

- Gerrard, W.
 J. Appl. Chem. Biotechnol. 1972
 22, 623-650.
- 2. Gerrard, W.
 Solubility of Gases and Liquids,
 Plenum Press, New York, 1976,
 Chapter 1.

COMPONENTS: (1) Propane; C₃H₀; [74-98-6] Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. E.; Vasil'eva, N. A.; Tsybnlevskii, A. M. Zh. Prikl. Khim. [108-90-7] VARIABLES: T/K: 293.2 P/MPa: 1.0-6.0 PREPARED BY: C. L. Young

EXPERIMENTAL VALUES:

T/K	P/MPa	"a	Mole fraction of propane $^{\mathrm{b}}$ $^{x}\mathrm{C}_{3}\mathrm{H}_{8}$
293.2	1.0	51.64 567.55	0.1821 0.7099

a Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

b Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Propane; C ₃ H ₈ ; [74-98-6]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. E.; Vasil'eva, N. A.; Tsybnlevskii, A. M.
(2) 1-Chloro-4-methylbenzene;	Zh. Prikl. Khim.
C ₇ H ₇ Cl; [106-43-4]	<u>1980</u> , 53, 1661-3.
VARIABLES:	PREPARED BY:
T/K: 293.2	Q I Voung
P/MPa: 1.0-6.0	C.L. Young

T/K	P/MPa	α ^a	Mole fraction of propane ^b
293.2	1.0	324.50 1115.10	0.6194 0.8483

 $^{^{\}rm a}$ Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:	
(1) Propane; C ₃ H ₈ ; [74-98-6]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M.	
(2) 1-Chlorooctane; C ₈ H ₁₇ Cl; [111-85-3]	2h. Prikl. Khim. 1980, 53, 1661-3.	
VARIABLES: T/K: 293.2 P/MPa: 1.0-6.0	PREPARED BY: C. L. Young	

T/K	P/MPa	α ^a	Mole fraction of propane k C $_{3}$ H $_{8}$
293.2	1.0	293.7	0.6772
	2.0	495.0	0.7811
	3.5	867.1	0.8621
	6.0	1462.1	0.9134

 $^{^{\}mbox{\scriptsize a}}$ Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:	
(1) Propane; C ₃ H ₈ ; [74-98-6] (2) 1-Iodooctane; C ₈ H ₁₇ I;	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M. Zh. Prikl. Khim.	
[629-27-6]	<u>1980</u> , 53, 1661-3.	
VARIABLES:	PREPARED BY:	
T/K: 293.2	C. L. Young	
P/MPa: 1.0-6.0		

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of propane ^b
293.2	1.0	138.2	0.5140
	2.0	269.8	0.6737
	3.5	458.3	0.7781
	6.0	664.2	0.8356

a Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:	
(1) Propane; C ₃ H ₈ ; [74-98-6]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M.	
(2) 2-Iodooctane; C ₈ H ₁₇ I; [557-36-8]	Zh. Prikl. Khim. 1980, 53, 1661-3.	
VARIABLES: T/K: 293.2 P/MPa: 1.0-6.0	PREPARED BY: C. L. Young	

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of propans $^{x}\mathtt{C}_{\mathtt{3}}\mathtt{H}_{\mathtt{6}}$
293.2	1.0	149.9	0.5351
	2.0	292.9	0.6922
	3.5	497.2	0.7924
	6.0	720.5	0.8469

a Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) Propane; C ₃ H ₈ ; [74-98-6]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M.
(2) (1-Chloroethyl)-benzene; C ₈ H ₉ Cl; [672-65-1]	Zh. Prikl. Khim. 1980, 53, 1661-3.
VARIABLES: T/K: 293.2	PREPARED BY:
P/MPa: 1.0-6.0	C. L. Young

T/K	P/MPa	α ^a	Mole fraction of propane ^b
293.2	1.0	104.07 488.50	0.3684 0.7324

 $^{^{\}mbox{\scriptsize a}}$ Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD APPARATUS / PROCEDURE:

A gas chromatographic method. details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

1. Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Tsybnlevskii, A. M. Zh. Fiz. Khim.

1977, 51, 767.

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:	
 (1) Propane; C₃H₈; [74-98-6] (2) 1-Chloronaphthalene; C₁₀H₇Cl; [90-13-1] 	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M. Zh. Prikl. Khim. 1980, 53, 1661-3.	
VARIABLES: T/K: 293.2	PREPARED BY: C. L. Young	
P/MPa: 1.0-6.0		

т/к	P/MPa	α ^a	Mole fraction of propane b x C ₃ H ₈
293.2	1.0	91.03 529.17	0.3454 0.7549

- a Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.
- b Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

COMPONENTS: (1) Propane; C₃H₆; [74-98-6] Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M. [111-83-1] VARIABLES: T/K: 293.2 P/MPa: 1.0-6.0 PRIGINAL MEASUREMENTS: Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M. Zh. Prikl. Khim. [111-83-1] PREPARED BY: C. L. Young

EXPERIMENTAL VALUES:

T/K	P/MPa	$_{lpha}^{ extsf{a}}$	Mole fraction of propane x C $_{3}$ H $_{8}$
293.2	1.0	220.0	0.6181
	2.0	454.5	0.7698
	3.5	724.1	0.8420
	6.0	1092.1	0.8893

 $^{^{\}rm a}$ Volume of propane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

b Calculated by compiler assuming molar volume of propane at 293.2 K and 1 atmosphere is 23.4 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) 2-Methylpropane; C ₄ H ₁₀ ; [75-28-5]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M.
(2) Chlorobenzene; C ₆ H ₅ Cl; [108-90-7]	Zh. Prikl. Khim. 1980, 53, 1661-3.
VARIABLES: T/K: 293.2 P/MPa: 1.0-6.0	PREPARED BY: C. L. Young

T/K	P/MPa	α ^a	Mole fraction of 2-methylpropane b x C4H10
293.2	1.0	121.14 1180.60	0.3460 0.8375

- a Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.
- $^{\rm b}$ Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

- SOURCE AND PURITY OF MATERIALS:
- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) 2-Methylpropane; C ₄ H ₁₀ ; [75-28-5]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M.
(2) 1-Chloro-4-methylbenzene; C ₇ H ₇ Cl; [106-43-4]	Zh. Prikl. Khim. 1980, 53, 1661-3.
VARIABLES: T/K: 293.2 P/ MPa: 1.0-6.0	PREPARED BY: C. L. Young

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2-methylpropane ^b
293.2	1.0	467.70 2894.30	0.6565 0.9220

a Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD APPARATUS / PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:
(1) 2-Methylpropane; C ₄ H ₁₀ ; [75-28-5]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M
(2) 1-Chloroctane; C ₈ H ₁₇ Cl; [111-85-3]	2h. Prikl. Khim. 1980, 53, 1661-3.
VARIABLES:	PREPARED BY:
T/K: 293.2 P/MPa: 1.0-6.0	C. L. Young

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2-methylpropane b	
293.2	1.0 2.0 3.5 6.0	665.5 1207.9 2101.6 3623.2	0.8294 0.8982 0.9388 0.9636	

a Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

b Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:	
(1) 2-Methylpropane; C ₄ H ₁₀ ; [75-28-5]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A.M.	
(2) 1-Bromooctane; C ₈ H ₁₇ Br; [111-83-1]	Zh. Prikl. Khim. 1980, 53, 1661-3.	
VARIABLES: T/K: 293.2 P/MPa: 1.0-6.0	PREPARED BY: C. L. Young	

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2 methylpropane xC4H10
293.2	1.0	559.5	0.8066
	2.0	1131.4	0.8940
	3.5	1791.7	0.9303
	6.0	2592.1	0.9508

a Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

ORIGINAL MEASUREMENTS: COMPONENTS: Berlin, M. A.; Pluzhnikova, M. F.; (1) 2-Methylpropane; C4H10; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M. [75-28-5]Zh. Prikl. Khim. (2) 1-Iodooctane; C,H,,I; 1980, 53, 1661-3. [629-27-6] VARIABLES: PREPARED BY: T/K: 293.2 C. L. Young P/MPa: 1.0-6.0 EXPERIMENTAL VALUES:

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2-methylpropane b
293.2	1.0	323.1	0.7146
	2.0	638.6	0.8319
	3.5	1104.0	0.8954
	6.0	1668.7	0.9282

Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

b Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

COMPONENTS: (1) 2-Methylpropane; C₄H₁₀; [75-28-5]

EXPERIMENTAL VALUES:

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2-methylpropane C4H10
293.2	1.0	348.7	0.7306
	2.0	689.3	0.8428
	3.5	1191.6	0.9026
	6.0	1801.0	0.9334

a Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- 2. Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

b Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

COMPONENTS:	ORIGINAL MEASUREMENTS:	
(1) 2-Methylpropane; C ₄ H ₁₀ ; [75-28-5]	Berlin, M. A.; Pluzhnikova, M. F.; Stepanova, I. N.; Potapov, V. F.; Vasil'eva, N. A.; Tsybnlevskii, A. M.	
(2) (1-Chloroethyl)-benzene; C ₈ H ₉ Cl; [672-65-1]	Zh. Prikl. Khim. 1980, 53, 1661-3.	
VARIABLES:	PREPARED BY:	
T/K: 293.2 P/MPa: 1.0-6.0	C. L. Young	

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2-methylpropane background C4H10
293.2	1.0	243.60 1207.40	0.5803 0.8727

- $^{\rm a}$ Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.
- $^{\rm b}$ Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.

AUXILIARY INFORMATION

A gas chromatographic method. No details given except ref. (1) which

contains little additional information.

METHOD APPARATUS / PROCEDURE:

- SOURCE AND PURITY OF MATERIALS:
- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

M. A.; Pluzhnikova, M. F.; a, I. N.; Potapov, V. F.; a, N. A.; Tsybnlevskii, A. M. l. Khim.
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, 1661-3.
Y: C. L. Young

T/K	P/MPa	$\alpha^{\mathbf{a}}$	Mole fraction of 2-methylpropane ^b *C ₄ H ₁₀
293.2	1.0	198.56 1214.82	0.5372 0.8766

^a Volume of 2-methylpropane measured at 293.2 K and 1 atmosphere pressure dissolved by unit volume of liquid.

AUXILIARY INFORMATION

METHOD/APPARATUS/PROCEDURE:

A gas chromatographic method. No details given except ref. (1) which contains little additional information.

SOURCE AND PURITY OF MATERIALS:

- 1. Purity about 99.6-99.8 mole per cent.
- Purified; final purity checked by refractive index measurements.

ESTIMATED ERROR:

REFERENCES:

 $^{^{\}rm b}$ Calculated by compiler assuming molar volume of 2-methylpropane at 293.2 K and 1 atmosphere is 23.3 L.