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# **SOLUBILITY DATA SERIES**

### Volume 60

# **HALOGENATED METHANES WITH WATER**

### SOLUBILITY DATA SERIES

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# **SOLUBILITY DATA SERIES**

### Volume 60

## **HALOGENATED METHANES WITH WATER**

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### **CONTENTS**





#### INTRODUCTION TO THE SOLUBILITY DATA SERIES

#### SOLUBILITY OF LIQUIDS IN LIQUIDS

#### NATURE OF THE PROJECT

The Solubility Data project (SDP) has as its aim a comprehensive review of published data for solubilities of gases, liquids and solids in liquids or solids. Data of suitable precision are compiled for each publication on data sheets in a uniform format. The data for each system are evaluated and, where data from different sources agree sufficiently, recommended values are proposed. The evaluation sheets, recommended values, and compiled data sheets are published on consecutive pages.

This series is concerned primarily with liquid-liquid systems, but a limited number or related solid-liquid, fluid-fluid and multicomponent (organic-water-salt) systems are included where it is considered logical and appropriate. Solubilities at elevated and low temperatures and at elevated pressures have also been inclUded, as it is considered inappropriate to establish artificial limits on the data presented if they are considered relevant or useful.

For some systems, the two components may be miscible in all proportions at certain temperatures and pressures. Data on reported miscibility gaps and upper and lower critical solution temperatures are included where appropriate and when available.

#### COMPILATIONS AND EVALUATIONS

The formats for the compilations and critical evaluations have been standardized for all volumes. A description of these formats follows.

#### Compilations

The format used for the compilations is, for the most part, self-explanatory. A compilation sheet is divided into boxes, with detailed contents described below.

*Components:* Each component is listed according to IUPAC name, formula, and Chemical Abstracts (CA) Registry Number. The Chemical Abstracts name is also included if this differs from the IUPAC name, as are trivial names if appropriate. IUPAC and common names are cross-referenced to Chemical Abstracts names in the System Index.

The formula is given either in terms of the IUPAC or Hill (1) system and the choice of formula is governed by what is usual for most current users: i.e., IUPAC for inorganic compounds, and Hill system for organic compounds. Components are ordered on a given compilation sheet according to:

- (a) saturating components:
- (b) non-saturating components in alphanumerical order;
- (c) solvents in alphanumerical order.

The saturating components are arranged in order according to the IUPAC 18-column periodic table with two additional rows:



Organic compounds within each Hill formula are ordered in the following succession:

- (a) by degree of unsaturation
- (b) by order of increasing chain length in the parent hydrocarbon
- (c) by order of increasing chain length of hydrocarbon branches
- (d) numerically by position of unsaturation
- (e) numerically by position by substitution
- (f) alphabetically by IUPAC name.



Deuterated (<sup>2</sup>H) compounds follow immediately the corresponding H compounds.

*Original Measurements:* References are abbreviated in the forms given by Chemical Abstracts Service Source Index (CASSI). Names originally in other than Roman alphabets are given as transliterated by Chemical Abstracts. In the case of multiple entries (for example, translations) an asterisk indicates the publication used for compilation of the data.

*Variables:* Ranges of temperature, pressure, etc. are indicated here.

*Prepared* by: The names of all compilers are given here.

*Experimental Values:* Components are described as (I), (2), etc., as defmed in the "Components" box. Data are reported in the units used in the original publication, with the exception that modern names for units and quantities are used; e.g., mass per cent for weight per cent; mol dnf<sup>3</sup> for molar; etc. In most cases, both mass and molar values are given. Usually, only one type of value (e.g., mass per cent) is found in the original paper, and the compiler has added the other type of value (e.g., mole per cent) from computer calculations based on 1989 atomic weights (2). Temperatures are expressed as  $t$ <sup>o</sup>C,  $t$ <sup>o</sup>F or T/K as in the original; if necessary, conversions to T/K are made, sometimes in the compilations, and always in the critical evaluation. However, the author's units are expressed according to IUPAC recommendations (3) as far as possible.

Errors in calculations, fitting equations, etc. are noted, and where possible corrected. Material inserted by the compiler is identified by the word "compiler" or by the compiler's name in parentheses or in a footnote. In addition, compiler-calculated values of mole or mass fractions are included if the original data do not use these units. If densities are reported in the original paper, conversions from concentrations to mole fractions are included, but otherwise this is done in the evaluation, with the values and sources of the densities being quoted and referenced.

Details of smoothing equations (with limits) are included if they are present in the original publication and if the temperature or pressure ranges are wide enough to justify this procedure and if the compiler finds that the equations are consistent with the data.

The precision of the original data is preserved when derived quantities are calculated, if necessary by the inclusion of one additional significant figure. In some cases graphs have been included, either to illustrate presented data more clearly, or if this is the only information in the original. Full grids are not usually inserted as it is not intended that users should read data from the graphs.

*Method:* The apparatus and procedure are mentioned briefly. Abbreviations used in Chemical Abstracts are often used here to save space, reference being made to sources of further detail if these are cited in the original paper.

*Source and Purity of Materials:* For each component, referred to as (1), (2), etc., the

following infonnation (in this order and in abbreviated fonn) is provided if available in the original paper: source and specified method of preparation; properties; degree of purity.

*Estimated Error:* If estimated errors were omitted by the original authors, and if relevant infonnation is available, the compilers have attempted to estimate errors (identified by "compiler" or the compiler's name in parentheses or in a footnote) from the internal consistency of data and type of apparatus used. Methods used by the compilers for estimating and reporting errors are based on Ku and Eisenhart (4).

*Comments and/or Additional Data:* Many compilations include this section which provides short comments relevant to the general nature of the work or additional experimental and thennodynamic data which are judged by the compiler to be of value to the reader.

*References:* The format for these follows the format for the Original Measurements box, except that final page numbers are omitted. References (usually cited in the original paper) are given where relevant to interpretation of the compiled data, or where cross-reference can be made to other compilations.

#### Evaluations

The evaluator's task is to assess the reliability and quality of the data, to estimate errors where necessary, and to recommend "best" values. The evaluation takes the fonn of a summary in which all the data supplied by the compiler have been critically reviewed. There are only three boxes on a typical evaluation sheet, and these are described below.

*Components:* The fonnat is the same as on the Compilation sheets.

*Evaluator:* The name and affiliation of the evaluator(s) and date up to which the literature was checked.

*Critical Evaluation:*

(a) Critical text. The evaluator checks that the compiled data are correct, assesses their reliability and quahty, estimates errors where necessary, and recommends numerical values based on all the published data (including theses, reports and patents) for each given system. Thus, the evaluator reviews the merits or shortcomings of the various data. Only published data are considered. Documented rejection of some published data may occur at this stage, and the corresponding compilations may be removed.

The solubility of comparatively few systems is known with sufficient accuracy to enable a set of recommended values to be presented. Although many systems have been studied by at least two workers, the range of temperatures is often sufficiently different to make meaningful comparison impossible.

Occasionally, it is not clear why two-groups of workers obtained very different but internally consistent sets of results at the same temperature, although both sets of results were obtained by reliable methods. In such cases, a definitive assessment may not be possible. In some cases, two or more sets of data have been classified as tentative even though the sets are mutually inconsistent.

(b) Fitting equations. If the use of a smoothing equation is justifiable the evaluator may provide an equation representing the solubility as a function of the variables reported on all the compilation sheets, stating the limits within which it should be used.

(c) Graphical summary. In addition to (b) above, graphical summaries are often given.

(d) Recommended values. Data are recommended if the results of at least two independent groups are available and they are in good agreement, and if the evaluator has no doubt as to the adequacy and reliability of the applied experimental and computational procedures. Data are reported as tentative if only one set of measurements is available, or if the evaluator considers some aspect of the computational or experimental method as mildly undesirable but estimates that it should cause only minor errors. Data are considered as doubtful if the evaluator considers some aspect of the computational or experimental method as undesirable but still considers the data to have some value where the order of magnitude of the solubility is needed. Data determined by an inadequate method or under iII-defined conditions are rejected. However, references to these data are included in the evaluation together with a comment by the evaluator as to the reason for their rejection.

(e) References. All pertinent references are given here, including all those publications appearing in the accompanying compilation sheets and those which, by virtue of their poor precision, have been rejected and not compiled.

(f) Units. While the original data may be reported in the units used by the investigators, the fmal recommended values are reported in 51 units (3) when the data can be converted accurately.

#### QUANTITIES AND UNITS USED IN COMPILATION AND EVALUATION OF SOLUBILITY **DATA**

#### Mixtures. Solutions and Solubilities

A *mixture* (5, 6) describes a gaseous, liquid or solid phase containing more than one substance, where the substances are all treated in the same way.

A *solution* (5, 6) describes a liquid or solid phase containing more than one substance, when for convenience one of the substances, which is called the *solvent,* and may itself be a mixture, is treated differently than the other substances, which are called *solutes.* If the sum of the mole fractions of the solutes is small compared to unity, the solution is called a *dilute solution.*

The *solubility* of a solute 1 (solid, liquid or gas) is the analytical composition of a saturated solution, expressed in terms of the proportion of the designated solute in a designated solvent (7).

"Saturated" implies equilibrium with respect to the processes of dissolution and demixing; the equilibrium may be stable or metastable. The solubility of a substance in metastable equilibrium is usually greater than that of the same substance in stable equilibrium. (Strictly speaking, it is the activity of the substance in metastable equilibrium that is greater.) Care must be taken to distinguish true metastability from supersaturation, where equilibrium does not exist.

Either point of view, mixture or solution, may be taken in describing solubility. The two points of view find their expression in the reference states used for definition of activities, activity coefficients and osmotic coefficients. Note that the composition of a saturated mixture (or solution) can be described in terms of any suitable set of thermodynamic components.

#### Physicochemical Quantities and Units

Solubilities of solids have been the subject of research for a long time, and have been expressed in a great many ways, as described below. In each case, specification of the temperature and either partial or total pressure of the saturating gaseous component is necessary. The nomenclature and units follow, where possible, ref. (3)

*A note on nomenclature.* The nomenclature of the IUPAC Green Book (3) calls the solute cpmponent B and the solvent component A. In compilations and evaluations, the first-named component (component 1) is the solute, and the second (component 2 for a two-component system) is the solvent. The reader should bear these distinctions in nomenclature in mind when comparing equations given here with those in the Green Book.

1. *Mole fraction* of substance 1,  $x_1$  or  $x(1)$ :

$$
x_1 = n_1 / \sum_{s=1}^{c} n_s
$$
 [1]

where  $n<sub>s</sub>$  is the amount of substance of  $s$ , and  $c$  is the number of distinct substances present (often the number of thermodynamic components in the system). *Mole per cent* of substance 1 is 100  $x_1$ .

2. *Ionic mole fractions* of salt i,  $x_{i+}$ ,  $x_{i}$ .:

For a mixture of s binary salts i, each of which ionizes completely into  $v_{s+}$  cations and  $v_{s-}$  anions, with  $v_s = v_{s+} + v_{s-}$  and a mixture of p non-electrolytes j, of which some may be solvent components, a generalization of the definition in (8) gives:

$$
x_{i+} = \frac{v_{i+}x_i}{1 + \sum_{i=1}^{s} (v_i - 1)x_s}, \quad x_{i-} = \frac{v_{i+}x_{i+}}{v_{i+}} \quad i = 1...s
$$
 [2]

$$
x'_{j} = \frac{x_{j}}{1 + \sum_{i=1}^{s} (v_{i} - 1)x_{i}}, \quad j = (s+1), ..., p
$$
 [3]

The sum of these mole fractions is unity, so that, with  $c = s + p$ ,

$$
\sum_{i=1}^{s} (x_{i+} + x_{i-}) + \sum_{i=s+1}^{c} x_i' = 1
$$
 [4]

General conversions to other units in multicomponent systems are complicated. For a threecomponent system containing non-electrolyte I, electrolyte 2 and solvent 3,

$$
x_1 = \frac{v_{2x}x_1'}{v_{2x}-(v_2-1)x_{2x}} \qquad x_2 = \frac{x_{2x}}{v_{2x}-(v_2-1)x_{2x}} \tag{5}
$$

These relations are used in solubility equations for salts, and for tabulation of salt effects on solubilities of gases (see below).

3. *Mass fraction* of substance 1,  $w_1$  or  $w(1)$ :

$$
w_1 = g_1 / \sum_{s=1}^c g_s \tag{6}
$$

where  $g_s$  is the mass of substance *s. Mass per cent* of substance 1 is 100  $w_1$ . The equivalent terms *weight fraction, weight per cent* and *g* (1)/100 *g solution* are no longer used.

*4. Molality* of solute 1 in a solvent 2, *ml:*

$$
m_1 = n_1/n_2 M_2
$$

 $\overline{r}$ 

SI base units: mol kg<sup>-1</sup>. Here,  $M_2$  is the molar mass of the solvent.

S. *Aquamolality. Solvomolality* of substance 1 in a mixed solvent with components 2, 3 (9), *ml(3):*

$$
m_1^{(3)} = m_1 \overline{M} / M_3
$$
 [8]

SI base units: mol  $kg^{-1}$ . Here, the average molar mass of the solvent is

$$
\overline{M} = x_2' M_2 + (1 - x_2') M_3 \tag{9}
$$

and  $x<sub>2</sub>$ <sup>'</sup> is the solvent mole fraction of component 2. This term is used most frequently in discussing comparative solubilities in water (component 2) and heavy water (component 3) and in their mixtures.

6. *Amount concentration* of solute 1 in a solution of volume  $V$ ,  $c_1$ :

 $c_1$  = [formula of solute] =  $n_1/V$  [10]

SI base units: mol m<sup>-3</sup>. The symbol  $c_1$  is preferred to [formula of solute], but both are used. The old terms *molarity, molar* and *moles per unit volume* are no longer used.

*7. Mass concentration* of solute 1 in a solution of volume *V*,  $\rho_1$ :SI base units: kg m<sup>-3</sup>.

$$
\rho_1 = g_1/V \tag{11}
$$

8. *Mole ratio*,  $r_{n,12}$  (dimensionless)

$$
r_{n,12} = n_1/n_2 \tag{12}
$$

Mass ratio, symbol  $r_{g,12}$ , may be defined analogously.

Mole and mass fractions are appropriate to either the mixture or the solution point of view. The other quantities are appropnate to the solution point of view only. Conversions between pairs of these quantities can be carried out using the equations given in Table 1 at the end of this Introduction. Other useful quantities will be defined in the prefaces to individual volumes or on specific data sheets.

*9. DensIty, p:*

 $p = g/V$ 

[13]

SI base units: kg m<sup>-3</sup>. Here g is the total mass of the system.

10. *Relative density,*  $d = \rho/\rho^0$ : the ratio of the density of a mixture at temperature *t*, pressure *p* to the density of a reference substance at temperature *t',* pressure *p',* For liquid solutions, the reference substance is often water at  $4^{\circ}C$ , 1 bar. (In some cases 1 atm is used instead of 1 bar.) The term *specific gravity* is no longer used.

#### *Thennodynamics of Solubility*

Thermodynamic analysis of solubility phenomena provides a rational basis for the construction of functions to represent solubility data, and thus aids in evaluation, and sometimes enables thermodynamic quantities to be extracted. Both these are often difficult to achieve because of a lack of experimental or theoretical activity coefficients. Where thermodynamic quantities can be found, they are not evaluated critically, since this task would involve examination of a large body of data that is not directly relevant to solubility. Where possible, procedures for evaluation are based on established thermodynamic methods. Specific procedures used in a particular volume will ybe described in the Preface to that volume.

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- 4. Ku, H.H., p. 73; Eisenhart, C., p. 69; in Ku, H.H., ed. Precision Measurement and Calibration. *NBS Special Publication 300.* Vol. 1. Washington. 1969.
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	$x_i$	$w_i$	$m_i$	$\boldsymbol{c_i}$
$x_i =$	$x_i$	$1 + \frac{M_i}{M_c} \left( \frac{1}{w_i} - 1 + \sum_{j \neq i}^{c-1} \left( \frac{M_c}{M_j} - 1 \right) \frac{w_j}{w_i} \right)$	$1+\frac{1}{m_i M_c}+\sum_{j\neq i}^{c-1}\frac{m_j}{m_i}$	$1+\frac{1}{M_c}\left(\frac{\rho}{c_i}-M_i\right)+\sum_{j\neq i}^{c-1}\frac{c_j}{c_i}\left(1-\frac{M_j}{M_c}\right)$
$w_i =$	$1 + \frac{M_c}{M_t} \left( \frac{1}{x_i} - 1 + \sum_{j \neq i}^{c-1} \left( \frac{M_j}{M_c} - 1 \right) \frac{x_j}{x_i} \right)$	$w_i$	$1+\frac{1}{m_iM_i}\left(1+\sum_{j\neq i}^{c-1}m_jM_j\right)$	$c_i M_i$ $\rho$
$m_i =$	$M_0\left(\frac{1}{x_i}-1-\sum_{j\neq i}^{c-1}\frac{x_j}{x_i}\right)$	$-\sum_{j\neq i}^{c-1} \frac{w_j}{w_i}$ $M_i\left(\frac{1}{w_i}-1\right)$	$m_i$	$\frac{1}{c_i}\left(\rho-\sum_{j\neq i}^{c-1}c_jM_j\right)-M_i$
$c_i =$	ρ $M_i + M_c \left( \frac{1}{x_i} - 1 + \sum_{j \neq i}^{c-1} \left( \frac{M_j}{M_c} - 1 \right) \frac{x_j}{x_i} \right)$	$\frac{\rho w_i}{M_i}$	$\frac{1}{m_i}\left(1+\sum_{j\neq i}^{c-1}M_jm_j\right)+M_i$	$\boldsymbol{c}_i$

Table 1. Interconversions between Quantities Used as Measures of Solubility c-component Systems Containing *c* - 1 Solutes *i* and Single Solvent *c*

 $\rho$  - density of solution;  $M_1$  - molar masses of i. For relations for 2-component systems, set summations to 0.

~:

# **PREFACE**

This volume contains a comprehensive coIlection and critical evaluation of solubility data published prior to 1993 for halogenated methanes with water, seawater, heavy water, and aqueous electrolyte solutions. The systems are ordered on the basis of chemical formula according to the Hill system.

A critical evaluation of the solubility data is not satisfactory without a comprehensive literature search foIlowed by compilation of all the available information reported in journals, patents, pamphlets, brochures, books, etc. The difficulties and problems in retrieval of all solubility data are a weIl recognized fact. Some of the difficulties which arose during the retrieval of the original publications for this volume were:

- i. The articles, reports, etc. were not cited in the Chemical Abstracts
- ii. The British Library did not hold the publications
- iii. The Slavonic Section of the British Library was unable to obtain some publications from abroad
- iv. Manufacturers' reports, leaflets, brochures, etc. were not available from industrial source
- v. University reports from experimental stations were not available from university libraries.

In summary, there were several cases where the original sources were not obtainable and the information had to be taken from secondary sources.

The referenced literature sources can be classified into the following groups:

- A. Bibliographies
- B. Secondary sources (books, reviews)
- C. Databases (computer softwares)
- D. Primary sources (journals, reports, etc.)

A list of the various sources of solubility data foIlowing the above classification is summarized in Table 1.

#### Table 1. Sources of Solubility Data

#### A. Bibliographies:

- 1. Wisniak, J.; Tamir, A. *Liquid-Liquid Equilibrium and Ettraction. A Literature Source Book,* Elsevier, Amsterdam, 1980, 1252 pp.
- 2. Wisniak, J.; Herskowitz, M. *Solubility ofGases and Solids. A Literature Source Book,* Parts A and B, Elsevier, Amsterdam, 1984, 2070 pp.

#### B. Secondary Sources:

- 1. Ware, G. W. *Review ofEnvironmental Contamination and Toxicology,* Vol. 116, Springer-Verlag, New York, 1990, 200 pp.
- 2. Freier, R. K. *Aqueous Solutions*, Vol. 1, Walter de Gruyter, Berlin, 1976, 477 pp.
- 3. Landolt-BOmstein zahlenwerte und Funktionen aus Physik, Chemie, Astronomie, Geophysik und Technik, *Gleichgewichte der Absorption von Gasen in FlOSsigkeiten,* Vol. 4a1cl, Springer-Verlag, Berlin, 1976, 479 pp.
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- 15. Dreisbach, R. R. *Physical Propenies ofChemical Compomds,* Am. Chern. Soc. Adv. in Chern. Ser. 15 (1955, 536 pp.), 22 (1959, 491 pp.), and 29(1961, 489 pp.), Washington, D. C.

#### C. Databases:

1. *AQUASOL database of Aqueous Solubility*, 5<sup>th</sup>., S. H. Yalkowsky, Ed., University of Arizona, Tucson, Arizona, 1991.

#### D. Primary Sources:

- 1. Journals
- 2. Reports
- 3. Brochures, leaflets
- 4. Patents
- 5. Private communications

Once a copy of the original document - usually a photocopy - was obtained, the first step was to read it carefully. Often the original article was in a foreign language which required a translation. If the description was not focused on the solubility aspect, then often some relevant details, e.g., source and purity of the solute and solvent, or both, were not included in the text. In many cases, the method, apparatus, and procedure were simply referred to other articles. Furthermore, when the experimental errors were not stated, the compiler sometimes introduced a subjective judgement for the accuracy of the measured solubility and tern-perature. The estimated accuracy of the measured quantities is quite subjective and the readers must take this fact into consideration.

The summaries of the procedures and abstracts were based on the available description of the method, apparatus, and procedures. Often a short statement "Details are not available," had to be used when the main contents of the articles focused not on solubility measurements but some other aspects of chemistry.

The conversion of the published solubility data into conventional units often presented difficulties, particularly when the dimensions were not expressed clearly. For example, the Henry's law constants, separation coefficients, distribution ratio, partition coefficients, etc. were not specified explicitly. Some of the more relevant conversion formulas are given in Table 2.

To convert solubility data from one unit to another, often the density and vapor pressure of the pure components and/or of the mixture were needed. The physical properties of the pure compounds were taken from the DIPPR (ref. 1) and TRCVP (ref. 2) databases. To find or derive the physical properties of mixtures required a more elaborate effort. Experimental data, e.g., density and vapor pressure for aqueous solutions of halogenated hydrocarbons are extremely rare in the literature. Consequently, approximations were obtained using calculations recommended in standard handbooks, e.g., Reid et al. (ref. 2). An illustration of the

Table 2. Conversion Fonnulas for Solubility Units. a. Henry's Law Constant  $(H)$ : *P<sub>vap</sub>* (aliii) *M<sub>so lute</sub>* Mass % =  $H$  (dimensionless)  $\frac{1}{1} \times 100$ 82. 06 *T(* K) *<sup>d</sup>'olvwnl* (g em -3) Mass  $\%$  =  $P_{vap}$  (atm)  $M_{s}$ <sub>olula</sub>  $H$  (m<sup>3</sup> atm mol<sup>-1</sup>  $\frac{d}{d}$ <sub>solvent</sub> (g cm<sup>-3</sup>) × 10<sup>-4</sup>  $H$  ( dimensionless ) =  $\frac{C_{av}}{C_{av}}$  =  $\frac{16.04 \ P_{vap}$  (mmHg)  $M_{solub}$ b. Air/Water Partition Coefficient (K*AW):*  $T(K)$  S<sub>solute</sub> (mg / dm<sup>3</sup>) Mass % =  $\frac{100 \text{ K}_{AW} P_{vap}}{82.054 \text{ T(K)} \cdot d_{solvent}}$ c. Distribution Ratio  $(p/c)$ :  $(p/c) =$ Solute vapor pressure d. Partition Coefficient (K): e. Distribution Coefficient  $(K<sub>i</sub>)$ :  $K = \frac{1}{\sqrt{2\pi}}$ solute concentration Ostwald coefficient (mmHg)  $\pmod{dm^3}$ 1 L Ostwald coefficient =  $L = \frac{y}{x_i}$ difficulty of obtaining accurate conversions is shown by the following typical case. The solubility of carbon tetrachloride (CCl<sub>4</sub>) in water (H<sub>2</sub>O) is 0.10 cm<sup>3</sup>/100 cm<sup>3</sup> water at 25 °C. The solubility in mass per cent (100  $w<sub>i</sub>$ ) is required. The density of pure carbon tetrachloride is 1.5834 g CCl<sub>4</sub>/cm<sup>3</sup> at 25°C (DIPPR database). The solution density is required to convert the pure water density using the mass

of the aqueous solution of carbon tetrachloride at 25°C. However, the density of the aqueous solution of carbon tetrachloride has not been reported in the literature. The reason is quite simple; the difference between the density of pure water and that of the aqueous solution of carbon tetrachloride at 25 °C is marginal. As a consequence, the errors obtained upon the determination of solubility are considerably greater than the possible difference between the solubility in pure water or in its aqueous solutions at the same temperature. It follows, in this case, one must use the approximation

$$
g \, \text{CCl}_4 / 100 \, g \, \text{H}_2\text{O} \approx 100 \, w_1 \, .
$$

On the other hand, for solubility values larger than, say, 2 - 3 mass per cent, the differences become significant, as the following example illustrates. The solubility in water of dichloromethane  $(CH_2Cl_2)$ is 2.363 g/100 g water at 0°C. The mass per cent solubility, 100  $w<sub>I</sub>$ , at the same temperature is required.

If 100 g water dissolves 2.363 g  $CH_2Cl_2$ , then the total mass of the solution becomes 102.363 g. This means that 100 g aqueous solution will dissolve less  $CH_2Cl_2$  than 100 g pure water, that is,

$$
100 w_1 = \frac{2.363 \text{ g CH}_{12}}{102.363 \text{ g soln}} 100 = 2.3084.
$$

The resulting mass per cent is 2.3084 at O"C. Consequently, there is a 2.31 per cent reduction in the solubility relative to 100 g pure water. This is in comparison to the reduction of only 0.10 per cent in the case of the solubility of CCI<sub>4</sub> in 100 g water or 100 g aqueous solution at 25 $\degree$ C.

All critical evaluations of the solubility data are presented on the evaluation sheets. The information available on the relevant compilation sheets served as the fundamental source for the critical evaluations. The following main aspects of the solubility data have been considered:

Purity of the components (solute and solvents) Date of the experiment Accuracy of the method Reproducibility of the experiment Experience of the investigator(s), previous publications Consistency of the data, trends in series

Once these aspects of the works had been examined, efforts were made to weight the reliability of the reported data. As much as possible, the differences in the quality of the data have been taken into account.

The available solubility data for binary systems may be very scarce, medial, or abundant, depending on the commercial application of the systems. Whenever data from different sources exist, they often disagree. For evaluation of the agreement or disagreement among the data, graphical presentations usually provide the clearest picture. The figures normally contain the original data from all references for a given system. A plot representing the solubility data (expressed in mole fraction or mass per cent) can reveal whether or not a trend exists among the data in addition to highlighting any discrepancies of the experimental solubility measurements.

The final data can be classified as:

obscure or dubious - rejected data tentative - not recommended data recommended - good agreement among the published results.

A graphical presentation of the solubility data may be performed on linear, semi-logarithmic, etc. scales. The unit of solubility may be given as specific or molar scales. For practical reasons, the mass per cent unit is often used, whereas the mole fraction is another common unit of solubility. In this volume most figures are plotted using one of two different scales. For the solubilities in water, linear graphs are used and for the solubilities of water in halogenated hydrocarbons, the so called Cox chart is applied. In the Cox charts, the solubility of water is given as  $\log_{10} x_2$  versus 1/T. A straight line on a Cox plot can be very useful for revealing consistent data covering a limited temperature range. However, the straight line does not apply for solubility data over a very wide temperature interval, e.g., from the triple point to the critical point. Therefore, in some cases (e.g., solubility of water in chloroform), the normal polynomial equations were used for smoothing the solubility data.

To fit experimental data into the various equations, the individual data points are often weighted. The smoothed data may be influenced somewhat by such procedures of weighting individual data points. Data analysis is a process of mathematical and/or graphical treatment of experimental data through the use of statitical or parametric procedures. Whenever the raw data are fragmentary, the aim is to generate an extended range of internally consistent values by synthesis. In any case, the temperature dependence of solubility must be examined and any unusual irregularities must be investigated carefully.

The temperature dependence of the solubility of halogenated hydrocarbons in water has been correlated using normal polynomial equations over limited temperature intervals. These equations should be used only in the temperature range indicated. The equations play two major roles; to provide data users with interpolated data with good accuracy and to provide data users with acceptable data for use in computer programs, if desired. The deviation of the various experimental values from the fitted data are given as standard or average deviations.

If the experimental data cover a reasonable temperature interval, then the data and the smoothing equation are often illustrated in a figure. The graphical presentation of the reported and fitted data clearly indicates the risks involved when one attempts to extrapolate the raw experimental data. In some cases, an extrapolation is quite safe for the desired temperature (see for example, the solubility of water in halogenated hydrocarbons over moderate temperature intervals); whereas, in other cases, the risk is very high and it is not recommended. The shape of the solubility curves suggests the extrapolation and interpolation possibilities.

Whether the mutual solubility between two liquids is partial or complete depends on the similarities or differences between the molecules of the two chemical compounds. The halogenated hydrocarbon and water systems are only partially miscible without exception. Furthermore, the miscibility or immiscibility of water with other liquids is also very dependent upon temperature. At ambient temperature and atmospheric pressure, the miscibility is very limited between water and halogenated hydrocarbons. For most systems, the mutual solubility is less than 2 mass per cent at ambient room temperatures.

In a liquid-liquid system the variation of solubility with temperature depends on the sign of the heat of mixing or solution. The minimum dissolution temperature occurs for most halogenated hydrocarbon - water systems between 270 and 310 K. The interactions between the solute and solvent molecules provide the explanation for the phenomena. The temperature dependence of solubility is a result of temperature dependent structural modifications of water. A different energy is required for cavity formation and for the changes in rigidity of the lattice as temperature is changed.

The appearance of these minima resembles the dependence of the critical micelle concentration upon temperature. Here, the iceberg formation of water molecules around the monodisperse solute enhances the critical micelle concentration, the logarithm of which would be decreased linearly with  $1/T$  provided the solution behaves regularly, and the iceberg formation increases with a temperature reduction.

It is well recognised that the rare gases and hydrocarbon gases form iceberg-like structures when dissolved in cold water, followed by an iceberg melting as the temperature is raised. The solubility of most gases in water shows a minimum when plotted against temperature. The shape of the solubility curves for molecules with alkyl groups is explained by considering that the ice-like structure of water is also formed around the nonpolar alkyl group of molecules in water. This structure tends to break down as the temperature of the solution is increased.

The minimum solubility temperature can be calculated from a calorimetric measurement of the enthalpy of solution at infinite dilution ( $\Delta_{solv}H^{\infty}$ ). This value is very large and varies from negative to positive values within a small temperature range. Consequently, very large errors may be caused by an erroneous interpretation. In addition to the enthalpy of solution, the change in the heat capacity at infinite dilute aqueous solution ( $\Delta_{\text{cal}} C_{\text{e}}^{\bullet}$ ) is required for the calculation of the minimum solubility temperature  $(T_{\text{min}})$ ;

$$
T_{\min} = 298.15 \text{ K} - \frac{\Delta_{\text{soln}} H^{\text{eq}} (298.15 \text{ K})}{\Delta_{\text{soln}} C_p^{\infty}}
$$

A more detailed description of the minimum solubility phenomenon is given by Horvath (ref. 4), Shinoda (ref. 5), Nishino and Nakamura (ref. 6), and Privalov and Gill (ref. 7).

The relations between the solubility and some of the physical properties of the solute or solvent have been investigated from early times in solution studies. The various experiments showed that in very diluted solutions the influence of the solute molecules does not extend to all solvent molecules in the solution. Consequently, the large fraction of solvent molecules, which are not affected by solute molecules, must exist more or less in the same state of aggregation as in the pure state. A change of solvent molar volume in dilute solutions is very small. However, in more concentrated solutions the effects of the presence of the solute molecules on the solvent molecules are not negligible. The amount of molar volume change of the solvent depends on the nature of the solutes. The dissolution process is related to the disintegration of the solute in the solvent, as compared to its pure state molecular order, as a result of the mutual action of attraction of the solute and solvent.

In general, solubility depends on many parameters and is of a very complex nature. There is no simple relation established between solubility and the other properties of the pure components (solute and solvent). Despite the lack of a simple relationship, the solubility of halogenated benzenes in water at 25°C has been correlated with a reasonable success using the molar volume of the solutes (ref. 8). Similarly, the solubility of halogenated methanes in water shows a linear relationship (ref. 9). The correlation is based on the assumption that the molar volumes in saturated solutions are not greatly different from those in the pure state. The simple linear relation at 25°C is illustrated graphically in Figure 1. This is a very useful and practical way to show the consistency of the solubility data. Any significant deviation from such a linear relationhip suggests some inconsistency and introduces doubt concerning the reliablility of the data.



Figure 1. Logarithm of Saturated Molarity versus Solute Molar Volume at 25 °C for Halogenated Methanes in Water.

Correlation equation:

 $\log_{10}$  (S/ mole dm<sup>-3</sup>) = 1.8995 - 4.3707 *x* 10<sup>-2</sup> ( $V_m$ / cm<sup>3</sup> mole <sup>-1</sup>)

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#### CRITICAL EVALUATION:

The trichlorofluoromethane (1) and water (2) binary system is discussed in two parts; part 1 is trichlorofluoromethane (1) in water (2) and part 2 is water (2) in trichlorofluoromethane (1).

Part 1. The solubility of trichlorofluoromethane (1) in water (2) has been studied by at least eleven different work groups with only partial agreement of results. The data of Howe *et al.* (ref. 1) are substantially lower than other measurements and are therefore rejected. The solubility data reported by du Pont (refs. 2 and 3), Rauws *et al.* (ref. 4), McConnell *et al.* (ref. 5), Pearson and McConnell (ref. 6), and Sukomick (ref. 7) show some consistency, while the measurements reported by Park *et al.* (ref. 8), Warner and Weiss (ref. 9), Wisegarver and Cline (ref. 10), Warner et al. (ref. 11), Balls (ref. 14), and Zeininger (ref. 15) are relatively high in value.

It may be assumed that the solubility data reported in the du Pont bulletins were produced in the same laboratories with similar methods and accuracy at 298.15 and 304.15 K, respectively. There appears to be no significant difference between the two data points despite the 6 K difference in temperature. Similarly, the two measurements reported by McConnell et al. and Pearson and McConnell in 1975 most likely were made in the same laboratories under much the same conditions.

There is no obvious reason to explain the difference between the lower (refs. 2, 3, 5, 6, and 7) and higher (refs. 8, 9, 10, 11, 14, and 15) sets of data. In the opinion of the evaluator, there is not enough evidence to justify rejection of measurements from either of the two data sets. Although both data sets are classified as tentative, the smoothed solubility values in mass per cent (1) for the 273 through 313 K temperature interval (Table 1) are based upon a regression equation for all data shown in Figure 1:

Solubility  $[100 \text{ w}<sub>1</sub>] = 25.0094 - 0.16263 (T/K) + 2.6547 \times 10^4 (T/K)^2$ 

with a standard error of  $5.0 \times 10^{-2}$  about the regression line.

A minimum solubility occurs for most halogenated hydrocarbons in water systems between 270 and 310 K (refs. 12 and 13). A minimum solubility temperature can be calculated from an enthalpy of solution at infinite dilution and a change in solute heat capacity in going from a pure liquid to an infinitely dilute aqueous solution. However, such thermodynamic data are rarely available in the literature.

Part 2. The solubility of water (2) in trichlorofluoromethane (1) has been measured by three research groups (refs. 2, 3, and 7) with only partially consistent results with the exception of the measurements of Sukomick (ref. 7). Generally, the solubility behavior of water in halogenated hydrocarbons shows a definite increase with increasing temperature. This trend has been demonstrated in a comprehensive compilation of solubility data (ref. 12). The two measurements at 294.15 and 298.15 K from the du Pont laboratories compare favorably with the recommended values, whereas the reported value of Sukomick (ref. 7) at 304.15 K is low and classified as doubtful. More accurate solubility measurements are required for more reliable values.

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EXPERIMENTAL VALUES: (continued)





#### CRITICAL EVALUATION:

The tetrachloromethane (1) and water (2) binary system is discussed in two parts; part 1 is tetrachloromethane (1) in water (2) and part 2 is water (2) in tetrachloromethane (1).

**Part** 1. The solubility of tetrachloromethane (1) in water (2) has been studied by 41 workers. The experimental data of most investigators in the 273 to 303 K temperature interval are sufficiently reliable to use in a smoothing equation. Even though a number of measurements above 308 K were reported, the solubility values in this temperature range are rather uncertain and are classified as doubtful.

The experimental work of several workers was not used for the smoothing equation for a variety of reasons. The measured solubility of Booth and Everson (refs. 1 and 2) and of Karger *et al.* (ref. 3) are markedly higher than the solubility values calculated from the smoothing equation. The measurements by Powell (ref. 4), Tettamanti *et al.* (ref. 5), Svetlanov *et al.* (ref. 6), Antropov *et al.* (ref. 7), Simonov *et al.* (ref. 8), Sato and Nakijima (ref. 9), Coca *et al.* (ref. 10), Balls (ref. 11), Yoshioka *et al.* (ref. 12), Howe *et al.* (ref. 13), and Wright *et al.* (ref. 14) are all several per cents lower than the smoothed solubility values and have also been rejected. The solubilities calculated from the distribution coefficients of Prosyanov *et al.* (ref. 15) are in very poor agreement, giving little confidence in their values which were regarded as dubious.

The remaining data from 26 laboratories were compiled or used for the smoothing equation. The data are also shown in Figure 1. The fitting equation obtained for mass per cent (1) is given by:

Solubility  $[100 \, w_1] = 3.4653 - 0.0230285$  (T/K) + 3.91621 x 10<sup>-5</sup> (T/K)<sup>2</sup>

The equation represents the combined data points which yield a standard deviation of 5.8 x  $10^{-3}$  in the 273 to 308 K temperature range.

The curve obtained from the smoothing equation shows a distinct minimum at 294 K, as seen in Figure 1. The existence of the minimum solubility is discussed in the Preface.

The recommended solubility values at 5 K intervals for tetrachloromethane (1) in water (2) are presented in Table 1.

Table 1. Tentative Solubility of Tetrachloromethane (1) in Water (2)



(continued next page)


**Part** 2. The solubility of water (2) in tetrachloromethane (1) has been reported by 37 laboratories since 1921. The solubility measurements cover the 273 to 373 K temperature range, see Figure 2. However, the data available above 323 K originate from only two investigators (refs. 16 and 17). The recommended solubility values are limited to the 283 to 307 K temperature interval.

Although data from all the workers show a general increase in solubility with temperature, the extent of the increase is variable above 313 K.

The data of Bell (ref. 18), Niini (ref. 19), and Fox and Martin (ref. 20) are substantially lower than all other studies and they have been rejected. The data of Eberius (ref. 21), Zielinski (ref. 22), Grigsby (ref. 23), Goldman (ref. 24), Ohtsuka and Kazama (ref. 25), and Kleeberg *et al.* (ref. 26) are significantly higher than the likely solubility and were also rejected. The remaining data mainly due to Clifford (ref. 27), Rosenbaum and Walton (ref. 28), Staverman (ref. 29), Hutchison and Lyon (ref. 30), McGovern (ref. 31), Donahue and Bartell (ref. 32), Rotariu *et al.* (ref. 33), Greinacher *et al.* (ref. 34), Desnoyer (ref. 35), Tettamanti *et al.* (ref. 5), Johnson *et al.* (refs. 36 and 37), Johnson (ref. 38), Christian *et al.* (ref. 39), Hogfeldt and Fredlund (ref. 41), Simonov *et al.* (refs. 8, 41 and 42), Glasoe and Schultz (ref. 43), Antropov *et al.* (ref. 7), Kirchnerova (ref. 44), Kirchnerova and Cave (ref. 45), Coca *et al.* (ref. 10), Ksiazczak and Buchowski (ref. 46), Wu (ref. 17), and Orlandini *et al.* (ref. 47) are in good agreement, especially the values given in (refs. 31, 43, and 17).

The correlating equation for the combined mass per cent solubilities of water in tetrachloromethane between 283 and 308 K is as follows:

Solubility  $[100 \, w_2] = 0.301104 - 2.348078 \times 10^{-3} (T/K) + 4.607143 \times 10^{-6} (T/K)^2$ 

This equation yielded a standard deviation of  $1.5 \times 10^{-3}$  in the 273 to 308 K temperature range.

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### CRITICAL EVALUATION:

All the available solubility data for bromodichloromethane (1) in water (2) are summarized in Table 1.

The data are in very poor agreement and in the absence of other independent studies it is not possible to determine which values are the more reliable. Further studies will be necessary before even tentative values can be assigned. Even so, it may be observed that the solubility trend for halogenated hydrocarbon - water systems, as presented in the Preface, provided some support for the mass per cent (1) value, 100  $w<sub>t</sub>$ , of 1.618 at 298.15 K (ref. 1).

Table 1. Reported Solubility of Bromodichloromethane (1) in Water (2)



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# CRITICAL EVALUATION:

All the available solubility data for dibromochloromethane (1) in water (2) are summarized in Table 1.

The data are in very poor agreement. Considerable discrepancies exists even between the two solubility values reported by the same workers, compare (ref. 2) and (ref. 3). In the absence of further independent studies, it is not possible to determine which value is the more reliable. Additional investigations will be necessary before even tentative values can be assigned. Even so, it may be noted that the solubility trend for halogenated hydrocarbon - water systems, as presented in the Preface, provided some support for the mass per cent (1) value, 100  $w_1$ , of 0.8124 at 298.15 K (ref. 1).

Table 1. Reported Solubility of Dibromochloromethane (1) in Water (2)



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# CRITICAL EVALUATION:

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The tribromomethane (1) and water (2) binary system is discussed in two parts; part 1 is tribromomethane (1) in water (2) and part 2 is water (2) in tribromomethane (1).

Part 1. All the available data for the solubility of tribromomethane (1) in water (2) were considered acceptable for use in the smoothing equation except the following reported values. The datum of Squire and Caines (ref. 1) is rejected because of the lack of details on the purity of the sample, method of the experimental work, and significant deviation from other measurements. The approximate value of Booth and Everson (ref. 2) is also rejected because it is significantly lower than later studies. The datum of McNally and Grob (ref. 3) is rejected because the reported solubility is rather higher than other determinations. The data of Wright *et al.* (ref. 4) are contrary to the general trend of the temperature dependence of the solubilities in water (formation of maximum) and are rejected.

The remaining data, mainly at 298 K, are in reasonable agreement although further studies are required before any values can be recommended without qualification.

The tentative solubility values in mass per cent for tribromomethane (1) in water (2) over the 283 to 303 K temperature range were used to obtain the following equation:

Solubility  $[100 \t w_i] = 2.371 - 0.01517 (T/K) + 2.7808 \t x 10^{-5} (T/K)^2$ 

This regression equation was established using the combined data from (refs. 5 - 12), which yielded a standard deviation of  $1.6 \times 10^{-2}$ .

The tentative solubility values in mass per cent at 5 K intervals for tribromomethane (1) in water (2) are presented in the Table 1.

The curve obtained from the smoothing equation is shown in Figure 1. It should be noted that the solubility minimum, which is discussed in the Preface, appearing in the 283 to 303 K temperature interval is not pronounced.





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## CRITICAL EVALUATION:

The trichloromethane (1) and water (2) binary system is discussed in two parts; part 1 is trichloromethane (1) in water (2) and part 2 is water (2) in trichloromethane (1).

Part 1. The solubility of trichloromomethane (1) in water (2) has been studied by 54 workers with reasonable agreement of reported values from a majority of the investigators.

The experimental data of most investigators in the 273 to 333 K temperature interval are sufficiently reliable to use in the smoothing equation, see Figure 1. (The solid curve in the figure was obtained from the regression of all values shown in the figure.) The experimental work of several workers was not used for the smoothing equation for a variety of reasons. The solubility data of Herz (ref. 1), Salkowski (ref. 2), Ababi *et al.* (ref. 3), Svetlanov *et al.* (ref. 4), Sato and Nakijima (ref. 5), Veith *et al.* (ref. 6), McNally and Grob (ref. 7), and Howe *et al.* (ref. 8) are markedly lower than other results and are therefore rejected. The data of McCollum (ref. 9), Booth and Everson (ref. 10), Arefeva *et al.* (ref. 11), Coca *et al.* (ref. 12), and Warner *et al.* (ref. 13) are several per cent higher than the smoothed solubility values and are also rejected. Although, the measured solubility data of Okuda (ref. 14) above 310 K are in reasonable agreement, the low temperature data, that is, below 303 K are very uncertain. Consequently, the low temperature data were not tncluded in the regression analysis. Similar inconsistency was found in the data of Hunter-Smith *et al.* (ref. 15) and were excluded from further considerations. Lincoff and Gossett (ref. 16) presented two methods for the determination of the solubility. The data determined by the Batch Air Stripping method shows more compatible results and are in good agreement, whereas it appears the EPICS method gave values too low. Therefore, only the solubility data measured by the Batch Air Stripping method were used for fitting the regression equation.

The combined data of 40 laboratories were correlated to obtain the following mass per cent (1) equation:

Solubility  $[100 \t w_I] = 12.5333 - 7.40557 \times 10^2 (T/K) + 1.16374 \times 10^4 (T/K)^2$ 

which shows a standard deviation of 5.6 x 10<sup>-2</sup>. This equation, which shows a maximum deviation of 18  $\%$ (but much less for most of the data), may be considered as representing the combined solubility values in the 273 to 333 K temperature range.

The solubility minimum (see Figure 1) calculated from the regression equation is, in mass per cent (1), 0.752 at 318.18 K. The presence of a minimum in the solubility versus temperature behavior for the halogenated hydrocarbon-water systems is discussed in the Preface.

The recommended solubility values in mass per cent at 5 K intervals for trichloromomethane (1) in water (2) are presented in Table 1.

Table 1. Recommended Solubility of Trichloromethane (1) in Water (2)



(continued next page)

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Figure 1. Solubility of Trichloromethane (1) in Water (2).

Part 2. The solubility of water (2) in trichloromomethane (1) has been studied by 25 workers as recorded in the Compilation Sheets immediately following this Critical Evaluation. The reported solubilities in the 263 to 323 K temperature interval are quite acceptable for using the smoothing equation as seen in Figure 2.

All the available data for the solubility of water (2) in trichloromomethane (1) have been included for the fitting of the correlating equation with the following exceptions. The measured data of Herz (ref. 1), Evans (ref. 17), De Minjer (ref. 18), Reinders and De Minjer (ref. 19), and Kudryavtseva and Krutikova (ref. 20) are rejected because they are significantly higher than later studies. The data of Donahue and Bartell (ref. 21), Tettamanti *et al.* (ref. 22), Christyakov and Shapurova (ref. 23), and Antropov *et al.* (ref. 24) are markedly lower than other determinations and are therefore rejected.

The remaining data of 16 laboratories are in good agreement and the correlated values above 253 K are recommended although the low temperature data (below 273 K) are probably dubious. Further studies are required to establish reliable values in the lower temperature range below 273 K.

The equation for the mass per cent solubility of water (2) in trichloromomethane (1) between 263 and 323 K is as follows:

Solubility  $[100 \t w_i] = 6.1195 \times 10^{-2} - 2.0623 \times 10^{-3} (T/K) + 7.20879 \times 10^{-6} (T/K)^2$ 

This equation represents the combined data with a standard deviation of 2.2  $\times$  10<sup>-2</sup> and a correlation coefficient of 0.916.

The recommended mass per cent solubility values at 5 K intervals for water (2) in trichloromomethane (1) are presented in the Table 2.

(continued next page)



CRITICAL EVALUATION: (continued)

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The curve obtained from the smoothing equation is shown in Figure 2. It may be noted that all the studies show a general increase in the solubility with temperature, which is consistent with the discussion of water solubility versus temperature in the Preface. Often the temperature dependence of the solubility is plotted on a Cox chart, that is,  $\log_{10} x_2$  versus 1/T, where a straight line represents the solubility behavior. This procedure is very useful for the illustration of data covering a limited temperature range. However, for the water (2) trichloromethane (2) system, this method of correlation was found to be less satisfactory than the regression with the normal polynomial equation.

Table 2. Recommended Solubility of Water (2) in Trichloromethane (1)





(continued next page)



## CRITICAL EVALUATION: (continued)

Figure 3 shows the  $log_{10} x_2$  versus the reciprocal of absolute temperature behavior for comparison with the behavior shown in Figure 2.



Figure 3. Solubility of Water (2) in Trichloromethane (1);  $\log_{10} x_2$  versus 1000/T.

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### CRITICAL EVALUATION:

The bromochloromethane (1) and water (2) binary system is discussed in two parts; part 1 is bromochloromethane (1) in water (2) and part 2 is water (2) in bromochloromethane (1).

The solubility of bromochloromethane (1) in water (2) has been studied by three workers, whereas the solubility of water (2) in bromochloromethane (1) has been reported in one paper only.

Part 1. The solubility of bromochloromethane (1) in water (2) has been studied by three workers. The experimental data of Tewari *et al.* (ref. 1) and Miller *et al.* (ref. 2) are in excellent agreement and the mass per cent (1) value of 1.646 at 298.15 K is recommended. In both cases the modified generator column method was used, but the analytical method was more advanced in the latter case. (For a comparison, see the two compilation sheets.) The single mass per cent (1) data point of 1.5 g(1)/100 g soln. at 293.15 K, reported by O'Connell (ref. 3) is considered as tentative. Whether the solubilities at 293.15 and 298.15 K are consistent with the general trend of temperature dependence remains to be investigated.

Part 2. The solubility of water (2) in bromochloromethane (1) has been reported in only one paper, that of O'Connell (ref. 3) and there are no other measurements for comparison. Therefore, it is not possible to perform a critical evaluation. The readers are referred to the compilation sheet for further details.

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#### CRITICAL EVALUATION:

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The dibromomethane (1) and water (2) binary system is discussed in two parts; part 1 is dibromomethane (1) in water (2) and part 2 is water (2) in dibromomethane (1).

Part 1. The solubility of dibromomethane (1) in water (2) has been studied by 6 workers. The Compilation Sheets immediately follow this Critical Evaluation.

The experimental data of all investigators in the 273 to 323 K temperature range are sufficiently reliable for use in the smoothing equation (see Figure 1) with the exception of the experimental work of Booth and Everson (ref. 1) which is markedly higher than other results and is therefore rejected. The combined data of 5 laboratories were correlated to give the following equation for mass per cent (1) solubility:

Solubility  $[100 \t w_l] = 10.1890 - 0.06336789 (T/K) + 1.10906 \t x 10^4 (T/K)^2$ 

which produced a standard deviation of 4.4 x  $10^{-2}$ . This equation represents the combined solubility data with a maximum deviation of 6.0 % (usually less) and may be considered recommended to represent the data in the 273 to 323 K temperature interval.

The recommended mass per cent solubility values at 5 K intervals for dibromomethane (1) in water (2) are recorded in Table 1.

Table 1. Recommended Solubility of Dibromomethane (1) in Water (2)



Part 2. The solubility of water (2) in dibromomethane (1) has been reported in one work (ref. 2) and, therefore, no Critical Evaluation has not been performed. The readers are referred to the relevant Compilation Sheet.

(continued next page)



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### CRITICAL EVALUATION:

The dichloromethane (1) and water (2) binary system is discussed in two parts; part 1 is dichloromethane (1) in water (2) and part 2 is water (2) in dichloromethane (1).

Part 1. The solubility of dichloromethane (1) in water (2) has been studied by at least 32 groups of workers. Most of the data reported have been considered for inclusion in the smoothing equation with the following exclusions. The experimental data of Salkowski (ref. I) are markedly lower than the other results and are therefore rejected. The solubility data of Booth and Everson (ref. 2), Alexandrova *et al.* (ref. 3), and Sadovnikova *et al.* (refs. 4 and 5) are several per cent higher than the smoothed solubility values and are also rejected. The data of Sabinin *et al.* (ref. 6) between 293.15 and 303.15 K show a temperature dependence of solubility much too large and are therefore rejected. The data of Svetlanov *et al.* (ref. 7) also show a change in solubility far too large between 288.15 and 333.15 K and are rejected; however, the value at 303.15 K is retained. The solubilities calculated from the distribution coefficients of Prosyanov *et al.* (ref. 8) are in very poor agreement, providing no confidence in their values which are regarded as dubious. The solubility data of Howe *et al.* (ref. 9) between 283.15 and 303.15 K show a maximum which is inconsistent with the trend of temperature dependence of solubility and are rejected; however, the value at 293.15 K is retained.

The remaining data of 25 laboratories by Rex (ref. 10), van Arkel and VIes (ref. 11), Bakowski and Treszczanovicz (ref. 12), Niini (ref. 13), McGovern (ref. 14), Donahue and Bartell (ref. 15), Kudryavtseva and Krutikova (ref. 16), Maretic and Sirocic (ref. 17), du Pont (ref. 18), Svetlanov *et al.* (ref. 7), Karger *et al.* (ref. 19), Antropov *et al.* (ref. 20), McConnell *et al.* (ref. 21), Pearson and McConnell (ref. 22), Archor and Stevens (ref. 23), Sato and Nakijima (ref. 24), Coca *et al.* (ref. 25), Hutchinson *et al.* (ref. 26), Leighton and Calo (ref. 27), Lincoff and Gossett (ref. 28), Gossett (ref. 29), Warner *et al.* (ref. 30), Howe *et al.* (ref. 9), Vogel (ref. 31), and Wright *et al.* (ref. 32), were used to obtain the following smoothing equation for solubility in mass per cent (1):

Solubility  $[100 \t w_i] = 58.838 - 0.38224 (T/K) + 6.3928 \times 10^4 (T/K)^2$ 

This equation represents the combined data with a 0.37 standard deviation in the 273 to 310 K temperature range.

The curve obtained from the smoothing equation shows a distinct minimum at 299 K as seen in Figure 1. The appearance of the minimum for the solubility versus temperature behavior is discussed in the Preface.

The recommended mass per cent solubility values at 5 K intervals for dichloromethane (1) in water (2) are presented in the Table 1.

Table 1. Recommended Solubility of Dichloromethane (1) in Water (2)



(continued next page)

# COMPONENTS:

- (1) Dichloromethane;  $CH<sub>2</sub>Cl<sub>2</sub>$ ; [75-09-2]
- (2) Water; H<sub>2</sub>O; [7732-18-5]

EVALUATOR:

A. L. Horvath, Imperial Chemical Industries Limited, Runcorn, U.K.

March 1993.

# CRITICAL EVALUATION: (continued)





Part 2. The solubility of water (2) in dichloromethane (1) has been reported from 19 laboratories. The solubility measurements cover the 253 to 313 K temperature range as represented in Figure 2.

The data reported have been considered for inclusion in the smoothing equation with the following exclusions. The data of Bakowski and Terszczanowicz (ref. 12), Niini (ref. 13), Donahue and Bartell (ref. 15), and Kudryavtseva and Krutikova (ref. 16) are markedly higher than other results and are therefore rejected. The measured solubility of Alexandrova et al. (ref. 3), and Sadovnikova *et al.* (refs. 4 and 5) are several per cent lower than the smoothed solubility and are also rejected. The solubilities calculated from the distribution coefficients of Prosyanov *et al.* (ref. 33), are in very poor agreement, providing no confidence in their values which are regarded as dubious.

The remaining data of 11 laboratories by Staverman (Ref. 34), McGovern (ref. 14), Davies *et al.* (ref. 35), Maretic and Sirocic (ref. 17), Sabinin *et al.* (ref. 6). Lees and Sarram (ref. 36), Antropov *et al.* (ref. 20), Archer and Stevens (ref. 23), Coca *et al.* (ref. 25), WU (ref. 37), and Ohtsuka and Kazama (ref. 38) were compiled or used for the smoothing equation. The fitting equation used was:

$$
\log_{10} x_2 = 1.8214 - 1164.63/(T/K)
$$

The equation represents the combined data with a standard deviation of 5.8 x  $10^{-2}$  in the 253 to 313 K temperature range.

The recommended mass per cent solubility values at 5 K intervals for water (2) in dichloromethane (1) are presented in the Table 2.

The linear relation between the solubility expressed as  $log_{10} x_2$  versus the reciprocal of absolute temperature behavior is illustrated in Figure 2. The straight line behavior of such plots is characteristic of the solubility of water in halogenated hydrocarbons, as discussed in the Preface.

(continued next page)

## COMPONENTS:

(1) Dichloromethane;  $CH<sub>2</sub>Cl<sub>2</sub>$ ; [75-09-2]

EVALUATOR:

A. L. Horvath, Imperial Chemical Industries Limited, Runcorn, U.K.

(2) Water; H<sub>2</sub>O; [7732-18-5]

March 1993.

Table 2. Recommended Solubility of Water (2) in Dichloromethane (1)

### CRITICAL EVALUATION: (continued)





Figure 2. Solubility of Water (2) in Dichloromethane (1).

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#### CRITICAL EVALUATION:

The diiodomethane (1) and water (2) binary system is discussed in two parts; part 1 is diiodomethane (1) in water (2) and part 2 is water (2) in diiodomethane (1).

Part 1. The solubility of diiodomethane (1) in water (2) has been studied by four groups of workers. The experimental data of Gross and Saylor (ref. 1) and Andrews and Keefer (ref. 2) are supported by the descriptions of the methods used for determining the reported data. Details are not available for methods, apparatus, and procedures used by van Arkel and Vies (ref. 3) and O'Connell (ref. 4) for obtaining the solubility data.

The three solubility values, see (refs. 1,3, and 4), between 293.15 and 303.15 K compare favorably with the selected value, whereas the datum of Andrews and Keefer (ref. 2) at 298.15 K is low and classified as doubtful. More accurate solubility determinations are required, meanwhile, the tentative mas per cent solubility of diiodomethane (1) in water (2) is 0.124 at 303.15 K.

Part 2. The only datum available for the solubility of water (2) in diiodomethane (1) is that of Hutchison and Lyon (ref. 5) and so no Critical Evaluation is possible. The interested reader is referred to the relevant Compilation Sheet for the experimental solubility.

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#### CRITICAL EVALUATION:

The solubility of iodomethane (1) in water (2) has been studied by 8 groups of workers; whereas, the solubility of water (2) in iodomethane (1) has not been investigated yet.

The experimental data of Glew (ref. 1) covering the 273 to 323 K temperature range are significantly higher than the likely solubility. Furthermore, the continuous decrease in solubility with temperature between 273 and 323 is not consistent with the formation of a minimum shown by most similar binary systems. Therefore, these data are classed as doubtful and are rejected. The presence of a minimum in the solubility versus temperature behavior for the halogenated hydrocarbon-water systems is discussed in the Preface.

The solubility data of Balls (ref. 2) between 283 and 298 K show a continuous rise with temperature which is contrary to the trends shown by all other investigators and are therefore rejected. The single data point of Liss and Slater (ref. 3) at 293 K is lower than other results and is likewise rejected.

The remaining data of Rex (ref. 4), Fiihner (ref. 5), van Arkel and VIes (ref. 6), Swain and Thornton (ref. 7), and Hunter-Smith *et ai.* (ref. 8) are in reasonable agreement, although further studies are required before any values can be recommended. The tentative mass per cent solubilities of iodomethane (1) in water (2) over the 273 to 313 K temperature range were used to obtain the following equation:

Solubility  $[100 \, w_i]$  = 19.0036 - 0.11723 *(T/K)* + 1.95356 x 10<sup>4</sup> *(T/K)*<sup>2</sup>

This regression equation was established using the combined data from (refs. 4 - 8), which yielded a standard deviation of 4.3  $\times$  10<sup>-2</sup>.

The tentative mass per cent solubility values at 5 K intervals for iodomethane (1) in water (2) are presented in Table 1. The curve obtained from the smoothing equation is shown in Figure 1. It shows a distinct minimum at 300.0 K, as discussed in the Preface.

Table 1. Tentative Solubility of Iodomethane (1) in Water (2)



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# **SYSTEM INDEX**

Page numbers preceded by E refer to evaluation texts whereas those not preceded by E refer to compiled tables. Substances are listed as in the Chemical Abstracts.



## **SYSTEM INDEX**



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Pages preceded by an E refer to evaluation texts while those not preceded by E refer to compiled tables.

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